

INFORMATION TO USERS

This material was produced from a microfilm copy of the original document. While the most advanced technological means to photograph and reproduce this document have been used, the quality is heavily dependent upon the quality of the original submitted.

The following explanation of techniques is provided to help you understand markings or patterns which may appear on this reproduction.

- 1. The sign or "target" for pages apparently lacking from the document photographed is "Missing Page(s)". If it was possible to obtain the missing page(s) or section, they are spliced into the film along with adjacent pages. This may have necessitated cutting thru an image and duplicating adjacent pages to insure you complete continuity.**
- 2. When an image on the film is obliterated with a large round black mark, it is an indication that the photographer suspected that the copy may have moved during exposure and thus cause a blurred image. You will find a good image of the page in the adjacent frame.**
- 3. When a map, drawing or chart, etc., was part of the material being photographed the photographer followed a definite method in "sectioning" the material. It is customary to begin photoing at the upper left hand corner of a large sheet and to continue photoing from left to right in equal sections with a small overlap. If necessary, sectioning is continued again — beginning below the first row and continuing on until complete.**
- 4. The majority of users indicate that the textual content is of greatest value, however, a somewhat higher quality reproduction could be made from "photographs" if essential to the understanding of the dissertation. Silver prints of "photographs" may be ordered at additional charge by writing the Order Department, giving the catalog number, title, author and specific pages you wish reproduced.**
- 5. PLEASE NOTE: Some pages may have indistinct print. Filmed as received.**

University Microfilms International

**300 North Zeeb Road
Ann Arbor, Michigan 48106 USA
St. John's Road, Tyler's Green
High Wycombe, Bucks, England HP10 8HR**

7824594

GOIN, KEVIN MANSUR
DEVELOPMENT OF EQUATIONS OF STATE FOR
FLUIDS-CORRELATION METHODOLOGY FOR
THERMODYNAMIC AND PVT PROPERTIES, INCLUDING A
CASE STUDY FOR WATER.

THE UNIVERSITY OF OKLAHOMA, PH.D., 1978

University
Microfilms
International 300 N. ZEEB ROAD, ANN ARBOR, MI 48106

© 1978

KEVIN MANSUR GOIN

ALL RIGHTS RESERVED

THE UNIVERSITY OF OKLAHOMA
GRADUATE COLLEGE

DEVELOPMENT OF EQUATIONS OF STATE FOR FLUIDS-CORRELATION
METHODOLOGY FOR THERMODYNAMIC AND PVT PROPERTIES,
INCLUDING A CASE STUDY FOR WATER

A DISSERTATION
SUBMITTED TO THE GRADUATE FACULTY
in partial fulfillment of the requirements for the
degree of
DOCTOR OF PHILOSOPHY

By
KEVIN MANSUR GOIN
Norman, Oklahoma

1978

DEVELOPMENT OF EQUATIONS OF STATE FOR FLUIDS-CORRELATION
METHODOLOGY FOR THERMODYNAMIC AND PVT PROPERTIES,
INCLUDING A CASE STUDY FOR WATER

APPROVED BY

Kenneth E. Helling

Lloyd L. Lee

S. E. Babh J.

Shen D. Christen

James Christen

DISSERTATION COMMITTEE

ACKNOWLEDGMENTS

I would like to offer my sincere gratitude and appreciation to the following persons and organizations:

Professor K.E. Starling - for his guidance, inspiration and encouragement throughout this research.

Professors S. Babb, Jr., S.D. Christian, L.L. Lee, K.C. Mo, and J. Christensen - for serving on my advisory committee.

Margaret Williford - for her willingness to type the final manuscript.

American Gas Association, Cities Service Corporation, Phillips Petroleum Corporation, U.S. Energy Research and Development Administration and the U.S. Department of Health, Education and Welfare, the University of Oklahoma School of Chemical Engineering and Materials Science and the School of Petroleum Engineering - for financial support for this research and my research assistanceship.

Thomas J. Mercer, Jr., Myrna Carney, and Professors R. Mathis and T. Carey - for their support, encouragement and inspiration.

My parents and sisters - for their support, love, and sacrifice.

TABLE OF CONTENTS

	Page
LIST OF TABLES	v
LIST OF ILLUSTRATIONS	vi
 Chapter	
I. INTRODUCTION AND METHODOLOGY	1
II. REGRESSION METHODS	5
III. SOLUTION METHODS FOR NORMAL EQUATIONS.	10
IV. DATA SELECTION FOR THE CASE STUDY OF WATER	14
V. MODEL SELECTION FOR THE CASE STUDY OF WATER.	33
VI. INITIAL VALUE SELECTION.	41
VII. MODEL IMPROVEMENT BY REMOVAL OF INSIGNIFICANT PARAMETERS	44
VIII. SUMMARY OF METHODOLOGY AND RESULTS FOR CASE STUDY.	51
IX. CONCLUSIONS.	57
BIBLIOGRAPHY.	58
 APPENDIX	
A. DERIVATION OF REDUCED RESIDUAL THERMODYNAMIC PROPERTIES	60
B. EZFIT USERS GUIDE.	65
C. BANKED USERS GUIDE	195
D. TABULATED RESULTS FOR 43 PARAMETER EQUATION OF STATE	206

LIST OF TABLES

TABLE	Page
1. The First Eight Tchebycheff Polynomials.	35
2. Parameter Indices for EZFIT.	36
3. The Integrals of the Tchebycheff Polynomials on the Interval (0,y).	39
4. The Physical and Critical Properties of Water. .	40
5. Weighting Function for Pressure Departure Regressions.	43
6. Effects of Removing Parameters by Setting to Zero in the 48 Parameter Equation.	47
7. Effects of Removing Parameters by Setting to Zero in the 45 Parameter Equation.	49
8. Values of the Parameters for the 43 Parameter Tchebycheff Polynomial Equation of State for Water.	53
9. Results for the 43 Parameter Equation of State for Water.	55

LIST OF ILLUSTRATIONS

	Page
1. Working Density Data Set.	16
2. Typical Equation of State Behavior.	18
3. Working Enthalpy Data Set	20
4. Vapor Pressure Data Set	21
5. Enthalpy, Angus and Newitt.	23
6. Enthalpy, Callendar and Egerton	24
7. Density, Holser and Kennedy	25
8. Density, Keenan and Keyes	26
9. Density, Kell and Whalley	27
10. Density, Kennedy.	28
11. Density, Keyes and Smith.	29
12. Density, Keyes, Smith and Gerry	30
13. Density, Osborne, Stimson, and Ginnings	31
14. Density Data Set Ranges	32

ABSTRACT

A correlation methodology for the development of equations of state containing large numbers of parameters is presented herein, with the development of a forty-three parameter equation of state for water presented as a case study. The methodology consists of six steps: (1) experimental data collection and selection of a working data set (subset), (2) determination of initial values of model parameters by regression on pressure, (3) parameter value improvement by regression on density, (4) development of base equation by multiproperty analysis of density, vapor pressure and enthalpy departure data, (5) model improvement by systematic removal of unnecessary terms, and (6) model validity check using the complete set of available thermodynamic data.

This method was used to develop an equation of state for water covering the extensive range from the triple point, 491.67°R, 0.089 psia (271.15°K, 0.614 KPa) to 2859.67°R and 20,305 psia (1588.7°K, 140,000 KPa). A model of 48 parameters was developed and then improved to a model of 43 parameters which predicted thermodynamic properties with the following average absolute deviations: 0.58% for 1459 density

points, 0.12% for 53 vapor pressure points and 1.59 BTU/lbm (3.70 J/g) for 263 enthalpy points. Continued application of the method should allow even more improvement, especially in the high pressure region.

This methodology will allow the researcher to systematically evaluate and develop complex models for which intuition becomes inadequate.

DEVELOPMENT OF EQUATIONS OF STATE FOR FLUIDS-CORRELATION
METHODOLOGY FOR THERMODYNAMIC AND PVT PROPERTIES,
INCLUDING A CASE STUDY FOR WATER

CHAPTER I

INTRODUCTION AND METHODOLOGY

Equations of state are now being developed that are extremely accurate and are generalized to many fluids. This has led to equations having 40 or more parameters. Insight and intuition developed even by many years experience with equations of state often are inadequate in developing such massive models. This work presents a systematic method to develop such models.

Equations of state are basically either empirical or theoretical. Until recently the theory was not very well developed so that the most accurate equations were highly empirical. Most empirical equations are developed from isochoric data by choosing an empirical temperature dependence and then making the constants a function of density. This method was used in the Beattie-Bridgman [2], Martin-Hou [19], BWR [3], and Vennix [27] equations. Since its development in 1940 the BWR equation has received several modifications

to improve its high density, low temperature prediction. The most popular modification of the BWR equation is the form developed by Starling and Han [24] which was used in a massive correlation work by Hopke and Lin [18].

The van der Waals equation was one of the earliest to have a theoretic foundation. In it deviations from the ideal gas law were accounted for by two effects, one due to the excluded volume a molecule occupies (repulsive forces) and the other due to attractive forces. Redlick and Kwong modified the attractive term to get the R-K equation [21]. As with the BWR equation, many modifications were made to improve the R-K and are reviewed by Tsonopoulos and Prausnitz [26]. The most popular form now used in industry was developed by Soave [23], in which the equation parameters were made functions of temperature and accentric factor, ω . This equation along with the Starling-Han BWR was reviewed by West and Erbar [30].

With the development of high speed digital computers, idealized systems of particles were studied by Monte Carlo and molecular dynamics simulations. From this developed the theory for the properties of a system of hard spheres. This led to equations [19] based on the van der Waals and R-K equations in which the repulsive term is replaced by that for hard spheres developed by Carnahan and Starling [4]. The well-developed hard sphere theory led to the study of more realistic fluids by using hard spheres as a reference

for a perturbation expansion. Since argon was known to be accurately represented by a Lennard-Jones potential, Lennard-Jones fluids were thoroughly studied. The accuracy of perturbation theories for such fluids was studied by comparing predictions with computer simulations. This led to the well developed perturbation theories of Weeks, Chandler and Anderson (WCA) [29] and Verlet and Weiss [28]. The success of perturbation theories encouraged the use of this technique for other molecular effects such as those due to dispersion, overlap and multipole forces.

The accuracy desired and the number of fluids that are to be represented have led to equations of state that have many parameters. When working with many parameters, as the 50 of the Keenan and Keyes [15] equation of state for water, a systematic approach is needed. This work presents a method developed to logically handle large models. It consists of a regression package EZFIT and a set of guidelines.

The steps of the method are:

1. Collect data sets and selection of a working data set (subset).
2. Get initial parameters by a pressure regression.
3. Improve the density regression.
4. Develop a base equation by multi-property analysis.

5. Improve the model by eliminating terms.
6. Check validity of the equation by predicting more data.

This method was used to develop a 43 parameter equation of state for water as a case study in the present work.

CHAPTER II

REGRESSION METHODS

The heart of developing any model is finding the values of the parameters. This leads to the use of linear and nonlinear regression methods.

Our fitting function for the i th point of the random sample is y_i ,

$$Y_i(x_1, x_2, \dots x_i, a_1, a_2, \dots a_\ell) = Y_i(\{x\}_n; \{a\}_\ell) \quad (1)$$

where the x_i 's are the independent variables (in this case temperature and density) and the a_i 's are the parameters whose values are desired. The functional form of Y is dependent upon whether the sample point is density, enthalpy departure or vapor pressure. The parameters we desire are those which maximize the joint probability distribution for the sample. With the assumption the data points are normally distributed with known variance σ_i^2 and mean $Y_i(\{x\}_n; \{a\}_\ell)$, maximizing the probability corresponds to minimizing the function χ^2

$$\begin{aligned} \chi^2 &= \sum_i 1/\sigma_i^2 [Y_i - Y_i(\{x\}_n; \{a\}_\ell)]^2 \\ &= \sum_i \omega_i [Y_i - Y_i(\{x\}_n; \{a\}_\ell)]^2 \end{aligned} \quad (2)$$

where Y_i is the experimental value for the i th sample point and ω_i is the weight for that point. The condition for a minimum is the ℓ normal equations

$$\frac{\partial \chi^2}{\partial a_j} = \frac{\partial}{\partial a_j} \sum_i \omega_i [Y_i - Y_i(\{x\}_n; \{a\}_\ell)]^2 = 0$$

$$j=1,2,\dots,\ell \quad (3)$$

Since our fitting function is in general nonlinear and implicit in the parameters a linearization technique is used [4]. The fitting function when expanded about estimates of the parameters, $\{a_0\}_\ell$, and truncated to first order in the corrections Δa_j becomes

$$Y_i(\{x\}_n; \{a\}_\ell) = Y_{i0}(\{x_i\}_n; \{a_0\}_\ell) + \sum_{j=1}^{\ell} \frac{\partial Y_{i0}}{\partial a_j} \Delta a_j$$

$$(4)$$

To the first order approximation, χ^2 can be expressed as

$$\chi^2 = \sum_i \omega_i \{Y_i - [Y_{i0} + \sum_j \frac{\partial Y_{i0}}{\partial a_j} \Delta a_j]\}^2 \quad (5)$$

where the variables of Y_{i0} have been dropped for convenience. The normal equations are then

$$\frac{\partial \chi^2}{\partial \Delta a_k} = -2 \sum_i \omega_i \{Y_i - Y_{i0} - \sum_j \frac{\partial Y_{i0}}{\partial a_j} \Delta a_j\} \frac{\partial Y_{i0}}{\partial a_k}$$

$$= 0 \quad k = 1, 2, \dots, \ell \quad (6)$$

In matrix form these equations are then

$$\beta_k = \overline{\Delta a} \underline{\alpha} = \sum_j \Delta a_j \alpha_{jk} \quad (7)$$

where

$$\beta_k = \sum_i \omega_i [Y_i - Y_{i0}] \frac{\partial Y_{i0}}{\partial a_k} \quad (8)$$

and

$$\alpha_{jk} = \sum_i \omega_i \frac{\partial Y_{i0}}{\partial a_j} \frac{\partial Y_{i0}}{\partial a_k} \quad (9)$$

The equations are solved for $\overline{\Delta a}$ and the new estimates of the parameters are

$$\bar{a} = \bar{a}_0 + \overline{\Delta a}. \quad (10)$$

This direct solution of equation 7 is the Gauss-Newton method for nonlinear regression.

To solve these equations, the gradient expansion method of Marquardt [4] is used, in which the diagonal elements of the curvature matrix $\underline{\alpha}$ are increased by a factor λ . The matrix equations are then

$$\beta = \overline{\Delta a} \underline{\alpha}', \quad (11)$$

$$\begin{aligned} [\alpha'_{jk}] &= \alpha_{jk}(1+\lambda), \text{ for } j=k \\ &\alpha_{jk}, \text{ for } j \neq k \end{aligned} \quad (12)$$

The factor λ is optimized to reduce χ^2 .

After the vector $\bar{\Delta a}$ is calculated, the parameters are updated. This process of updating the parameters is continued until the minimum of χ^2 is reached.

When the function is linear in the parameters $\{a_j\}_\ell$

$$Y_i(\{x_i\}_n; \{a_j\}_\ell) = \sum_j a_j X_j(\{x_i\}_n) \quad (13)$$

where $X_j(\{x_i\}_n)$ are functions of the x_i set of x , the normal equations can be obtained directly from 6 as

$$\frac{\partial \chi^2}{\partial a_k} = -2 \sum_i w_i (Y_i - Y_i(\{x_i\}_n; \{a\}_\ell)) X_k(\{x_i\}_n) = 0$$

$$k = 1, 2, \dots, \ell \quad (14)$$

This gives rise to the equivalent matrix equations as 7 through 9 in which $Y_{i0} = 0$ and $\partial Y_{i0} / \partial a_k = X_k$

$$\beta_k = \sum_i w_i [Y_i] \frac{\partial Y_{i0}}{\partial a_k} = \sum_i w_i Y_i X_k \{x_i\}_n \quad (15)$$

and

$$\alpha_{jk} = \sum_i w_i \frac{\partial Y_{i0}}{\partial a_j} \frac{\partial Y_{i0}}{\partial a_k} = \sum_i w_i X_j X_k \quad (16)$$

The derivatives with respect to the parameters were approximated by the finite difference method, i.e.

$$\frac{\partial f(x)}{\partial x} = \frac{f(x+h) - f(x-h)}{2h} \quad (17)$$

Also by assuming the percentage error is constant the weight, ω_i , becomes

$$\omega_i = 1/Y_i^2. \quad (18)$$

CHAPTER III

SOLUTION METHODS FOR NORMAL EQUATIONS

In derivation of the least squares problem a set of simultaneous equations called the normal equations must be solved. These equations have similar forms for the linear least squares method and the various expansion methods such as Gauss-Newton and Marquart for nonlinear functions. As shown previously, these equations are symmetric and semi-positive definite. Because of this symmetry, specialized solution techniques for symmetric systems such as the Crout algorithm and the more general methods such as the Gauss-Jordan elimination can be used. The details of these algorithms can be found in books on matrix methods [25]. For most regression work, a method is desired that will not only return the solution vector but also the inverse matrix, which is then used to obtain the variances and covariances for statistical analysis.

Because of the large number of parameters determined in equation of state regression work, stringent requirements are laid upon the solution method. Round off errors in accumulating the sums for the normal equations can lead to loss of the semi-positive definite attribute of the normal

equations and the Crout algorithm can become unstable. Although requiring more storage, the Gauss-Jordan elimination with maximum pivoting strategy is unconditionally stable. By modifying the traditional algorithms to generate the inverse in place of the coefficient matrix, storage requirements can be reduced. Because of its stability, this method was selected for EZFIT. This allowed working with larger numbers of parameters with less calculation instability as indicated by underflows and overflows in the solution. There is a time penalty for using full pivoting in that the matrix must be transformed and the reverse transformation performed upon the inverse at the end of the solution. For models with fewer parameters, the calculation requirements are not as stringent and the method of straight pivoting can be used. This option is also available in EZFIT. It is recommended that the full pivoting method be used when more than 30 parameters are being regressed. The details of the matrix inversion routine, GJEL, are given in appendix B.

One of the problems of working with a large number of parameters in a model is that many of the parameters may be highly correlated, giving rise to nearly equal rows in the normal equations. This problem is indicated when the variances, i.e., the diagonal elements of the inverse, are negative. There are several methods for reducing this problem. The most fundamental approach is to examine the

model with the purpose of eliminating parameters with high correlation or performing a transformation which will reduce the correlation. In polynomials more independence among parameters can be obtained by selecting an appropriate set of orthogonal polynomials. Typically Tchebycheff polynomials are selected for not only their orthogonality but also their ability to reduce the number of terms needed for a desired accuracy [6, 12]. This method was selected for the development of the equation of state for water. Another means to improve the independence of the normal equations is to select more data to be included, which will have the desired effect.

Numerical difficulties also arise when the effects of the parameters vary widely. The parameters with the stronger effects will tend to cause the values of the weaker ones to lose significance. This problem can be minimized by judicious choices for scaling for the parameters. To help this trouble, the regression routine CURFIT scales the normal equations so that the diagonals are unity.

Even when these various precautions have been taken there is sometimes difficulty in the generation of the normal equations. The data points which the parameters least effect are sometimes swamped by the other data points. Since the normal equations are formed as a summation of terms for each data point, the accumulations are done in double precision so that more information from all points will be used.

These accumulations also can be helped by ordering the data points so that the points with the least contribution to chi-squared are summed first.

CHAPTER IV

DATA SELECTION FOR THE CASE STUDY OF WATER

In equation of state development there exists a multitude of possible thermodynamic data that can be used in multiproperty regression. Fundamentally, all thermodynamic properties are related to the equation of state by classical thermodynamics. Some of the property types are P , T , enthalpy, vapor pressure, speed of sound, Joule Thomson coefficient, and specific heats, C_v and C_p . These vary greatly in accuracy even among measurements of the same type from different investigators. They also vary greatly in the calculation needed to determine the property from the equation of state. To keep track of these various types of data as well as data for other compounds (this regression method is presently being used for studies of many other fluids at the University of Oklahoma), a data base system called BANKED was developed. BANKED is a card based system that identifies each data point as to the reference from which it was taken, fluid, and data type. It handles both mixture and pure fluid data. The details of BANKED are given in appendix C.

It is important that the data selected covers the range that is desired for the equation in a uniform manner so that there are not any regions that are empty. This is especially important for very flexible equations with many parameters. For this reason, an even grid of data was generated from the Keenan and Keyes [13] equation for water which was then supplemented by experimental data. The working density set is given in Figure 1. This consists of 382 points covering a temperature range of 491.67-2859.67°R (273.15-1588.7°K) and a pressure range of .66-20,305 psia (4.6-140,000 KPa). The saturated liquid densities of Osborne, Stimson, and Ginnings [20] were used to better define the saturation curve. If the saturation curve is accurate the vapor pressure and heat of vaporization will be more accurate without using these properties in regression. It is important to have high temperature isotherms that go from low densities to well above the critical density without crossing the two phase region in order to have appropriate trends in the two phase region.

In spite of these precautions in selection of density data, behavior for isotherms crossing the two phase region is not well defined because there is no physical behavior that matches the required behavior of an equation of state in this region. Where physically the pressure is constant at a given temperature for a range of densities in the two phase region, the equation of state typically exhibits the

DENSITY WORKING DATA SET

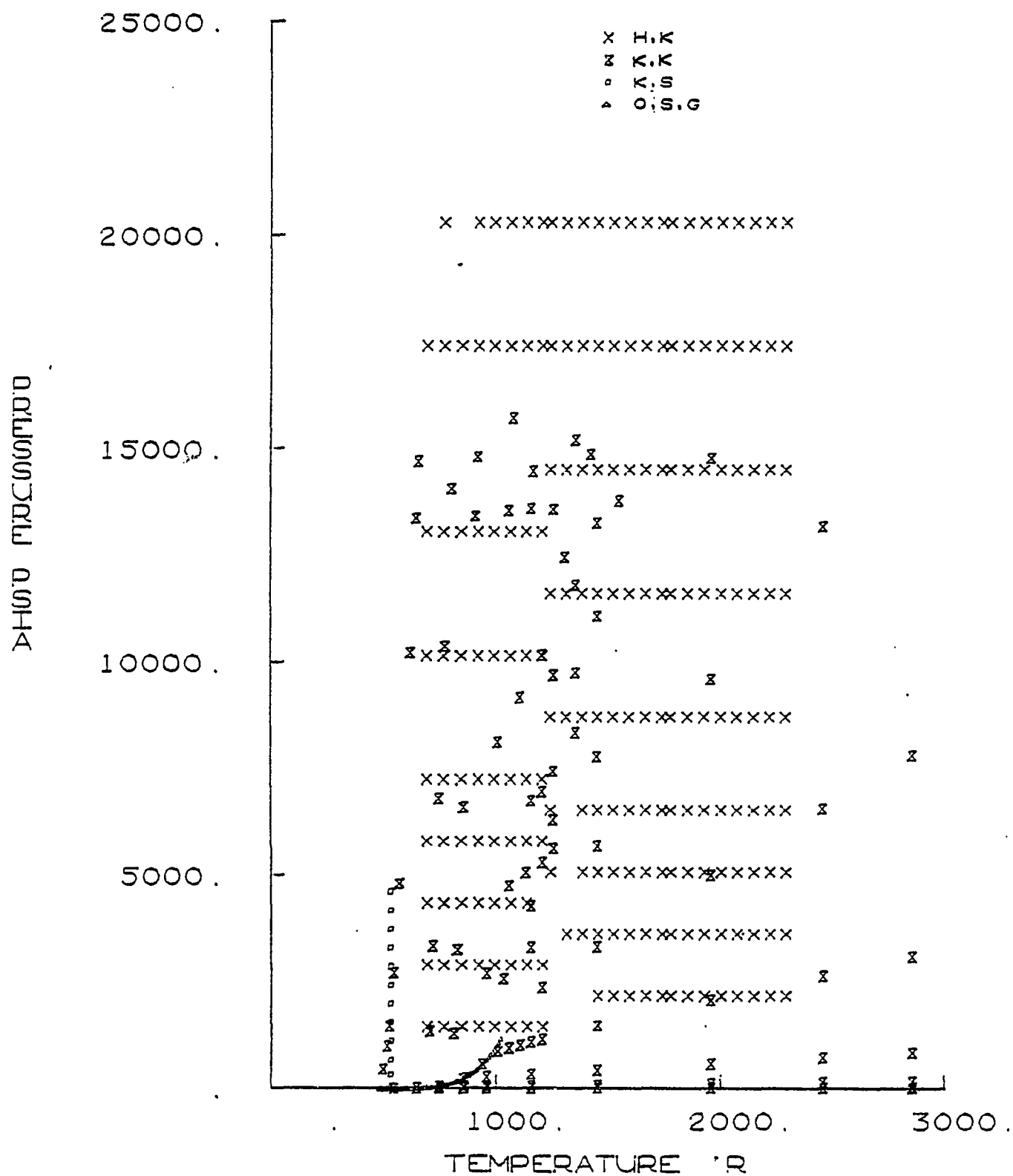


FIGURE 1. Working Density Data Set.

so-called van der Waals loop. Typical behavior of an equation of state is plotted in Figure 2. Information can be augmented for this region by including properties that are calculated as integrals across this region. This includes vapor pressure and enthalpy departure. Therefore, data were included of these types for the water equation. The enthalpy departure data consisted of 113 points generated from the Keenan and Keyes equation in a range of 509.67-2859.67°R (283.15-1588.7°K) and .66-14,694 psia (4.6-101,310 KPa). Since these were derived from an equation of state and not data (although a very accurate equation) they were not given as much importance as experimental data. For vapor pressure, the data of Osborne, Stimson and Ginnings [20] was used. The 53 points covered a range 491.67-1159.7°R (273.15-644.28°K) and 0.089-3090 psia (0.61-21,305 KPa). This covers the saturation curve from the triple point to within 5% of the critical point. The critical point was not covered because calculation algorithms used for vapor pressure and density have trouble in this region due to the flatness of the isotherms and because there is greater numerical uncertainty in the data in the critical region. The enthalpy and vapor pressure data used are plotted in Figures 3 and 4.

While obtaining a working data set, as much data as available were prepared. These data would be used to test the accuracy of both the data and the model. If a specific reference has errors exceeding those for other data sets in

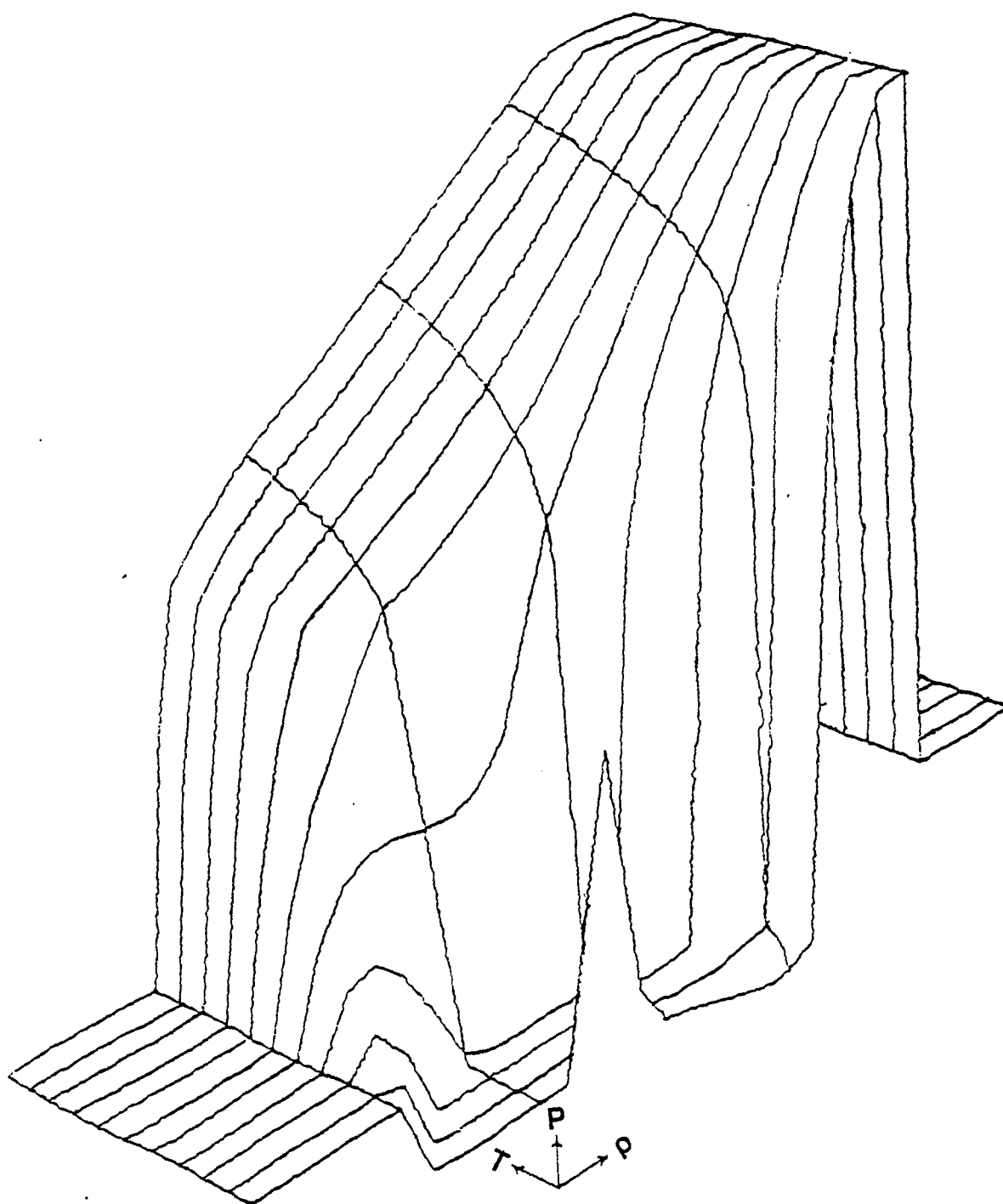


FIGURE 2A. A Three-Dimensional P - T plot of the Typical Behavior of an Equation of State.

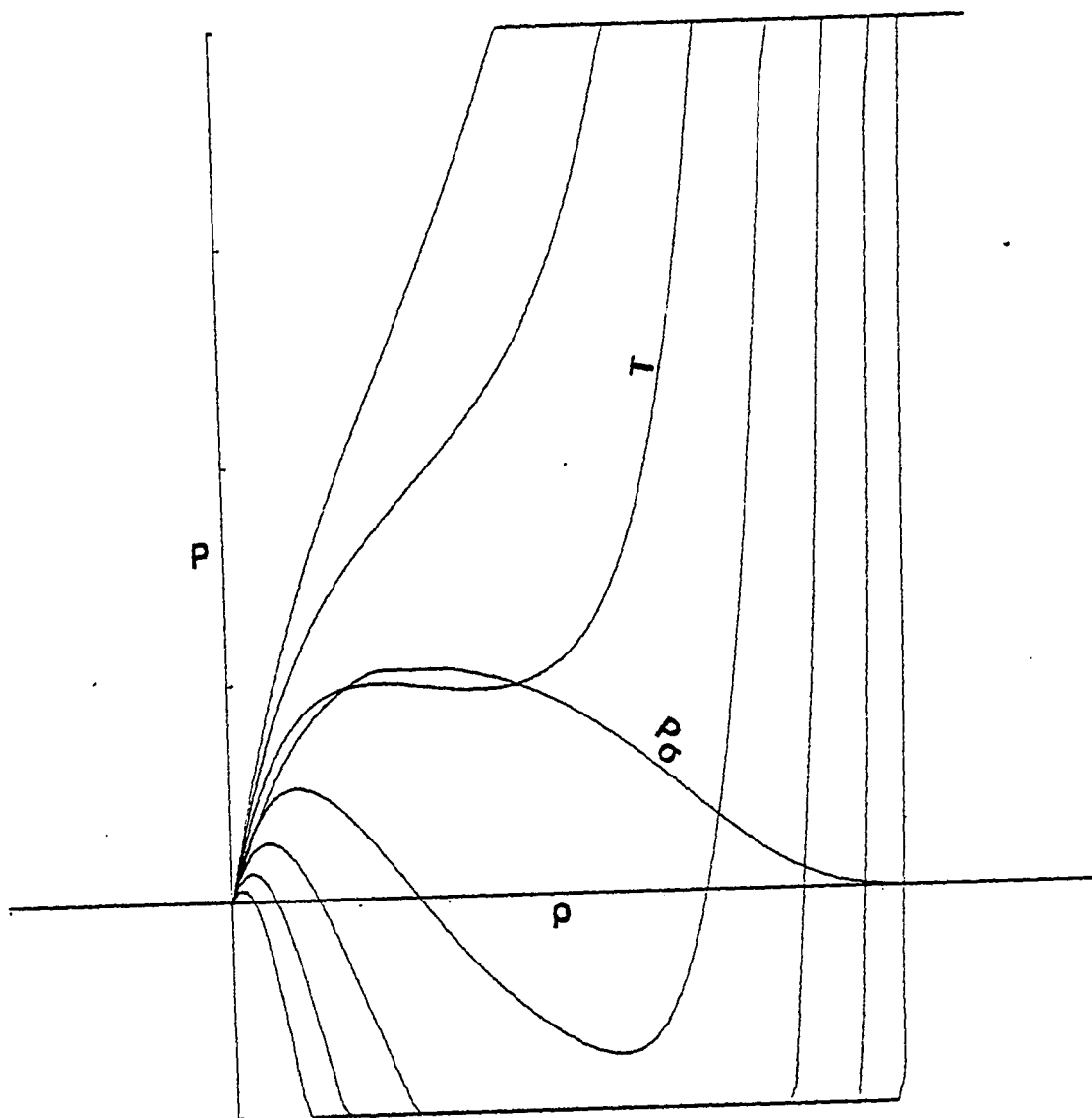


FIGURE 2B. Isotherms of a Typical Equation of State.

ENTHALPY KEENAN, KEYES, ET AL.

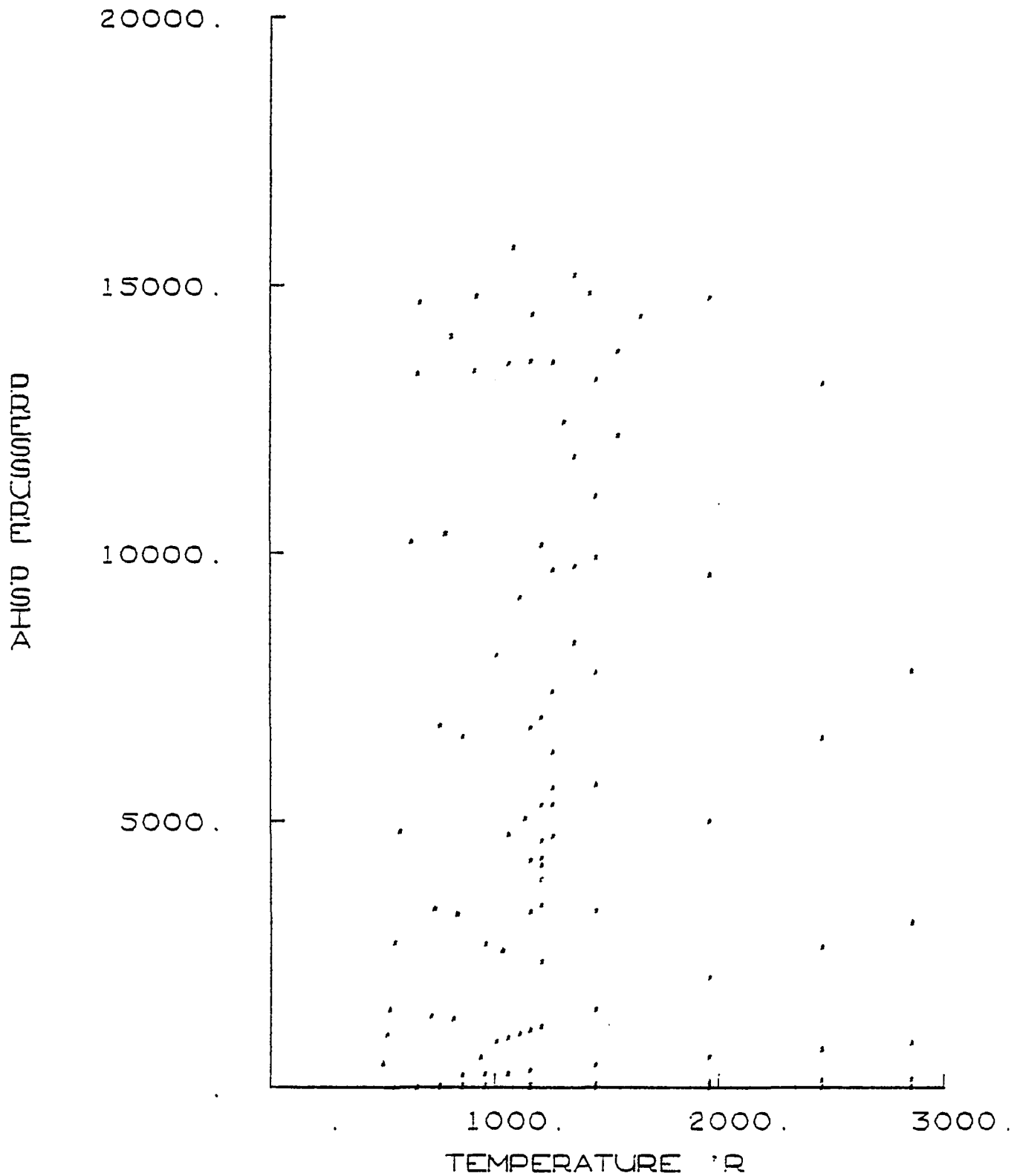


FIGURE 3. Working Enthalpy Data Set.

VAPOR PRESSURE OSBORNE, STIMSON, GINNINGS

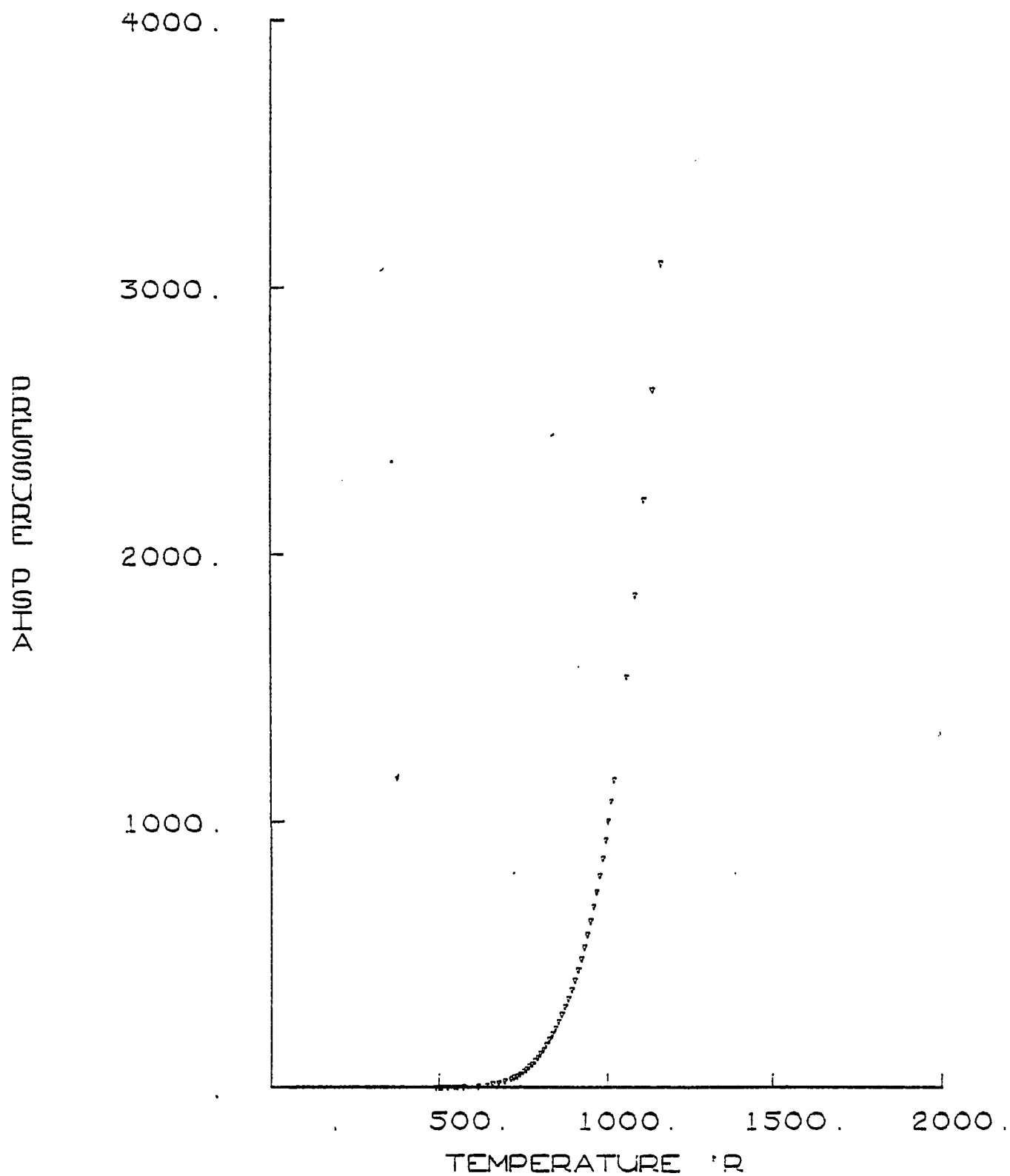


FIGURE 4. Vapor Pressure Data Set.

the region, it would signal the need for an evaluation of the data in that it might be less precise than the rest. For water, besides the working data set, density and enthalpy data were obtained from seven references. For the more massive tabulations only a representative number of points were prepared in BANKED. The data sets used are plotted in Figures 5 to 13. The regions of the pressure-temperature surface that were covered by the various data references for density are shown on Figure 14.

ENTHALPY ANGUS AND NEWITT

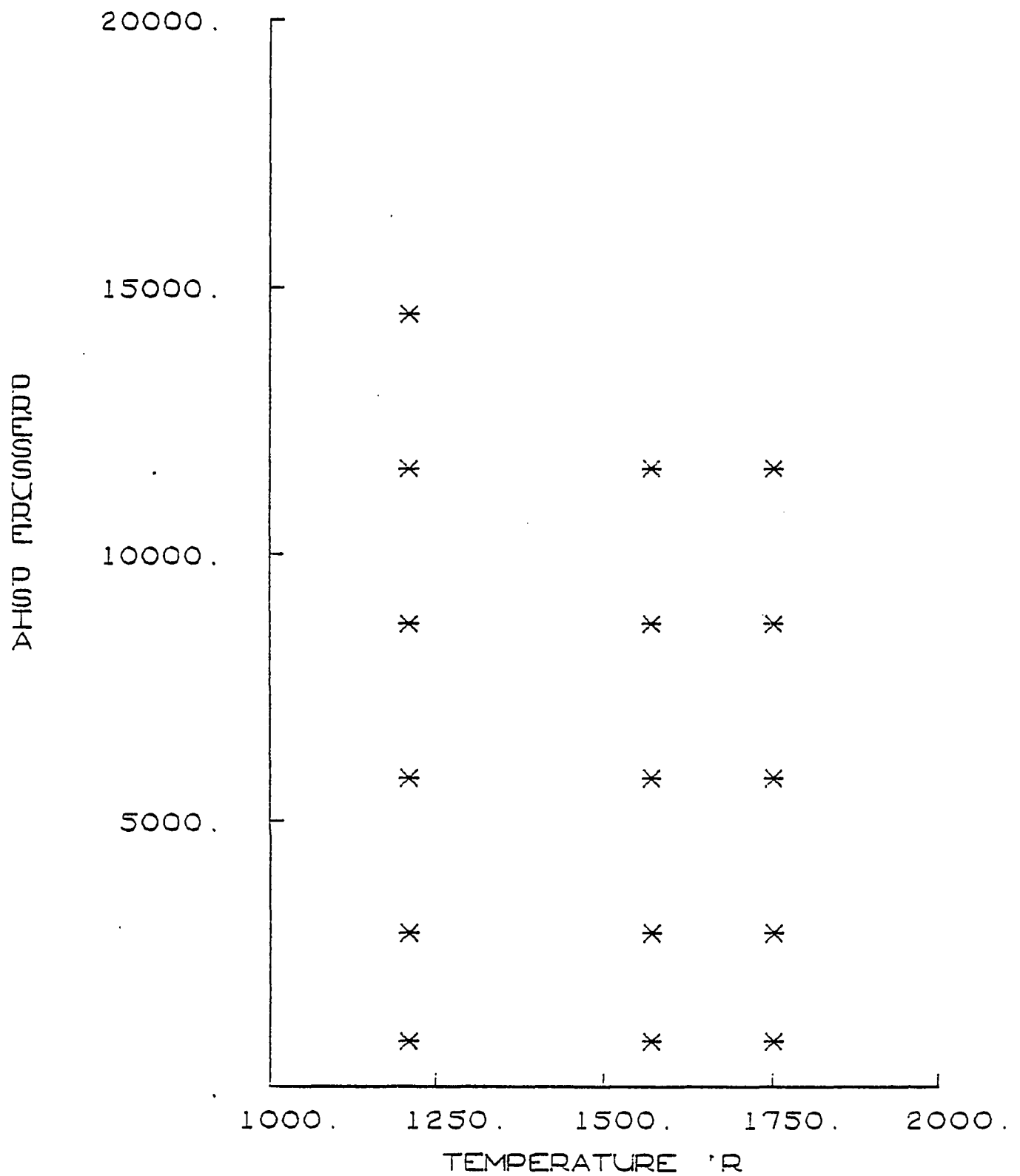


FIGURE 5. Enthalpy, Angus and Newitt

ENTHALPY CALLENDAR AND EGERTON

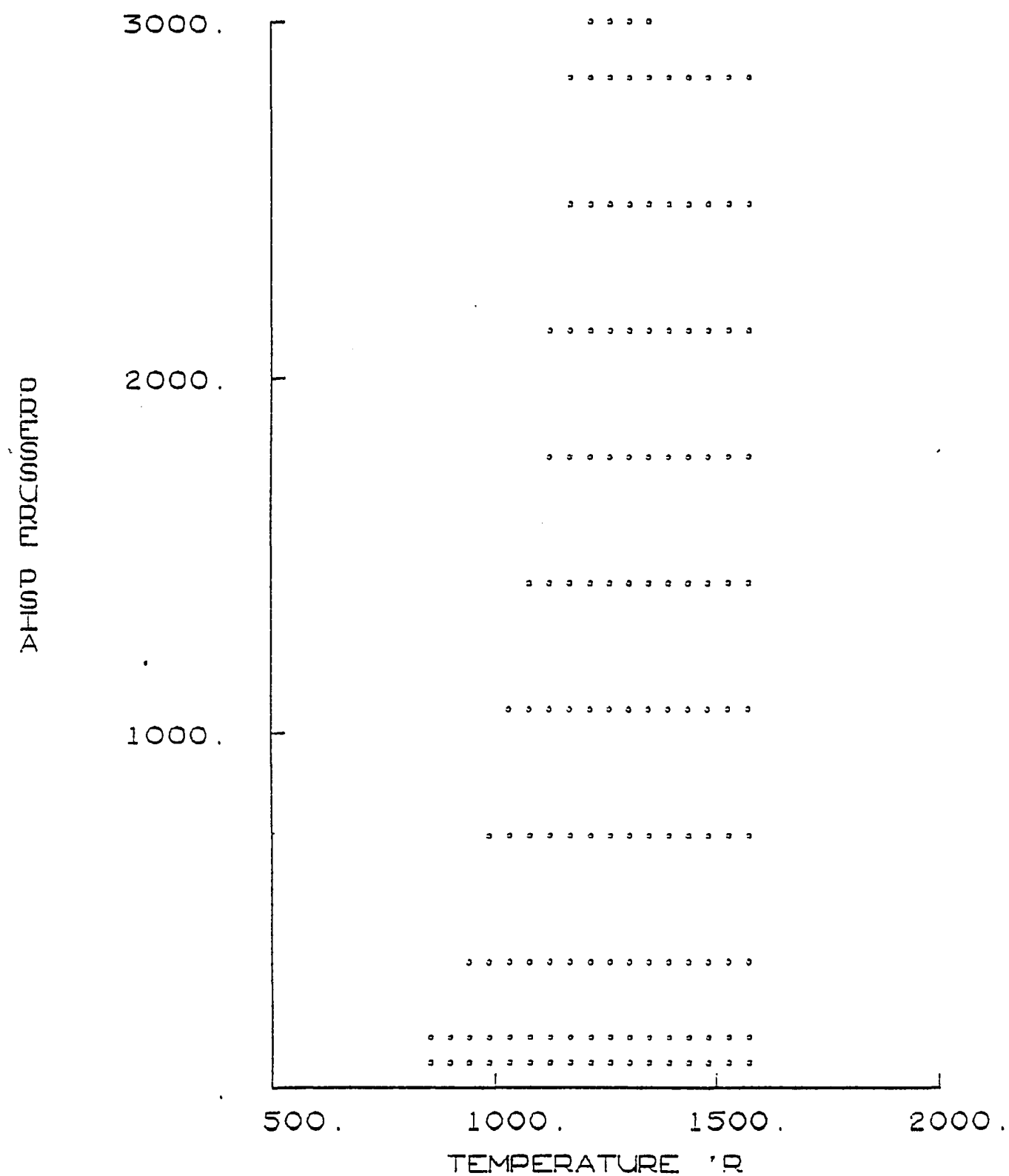


FIGURE 6. Enthalpy, Callendar and Egerton

HOLSER, KENNEDY

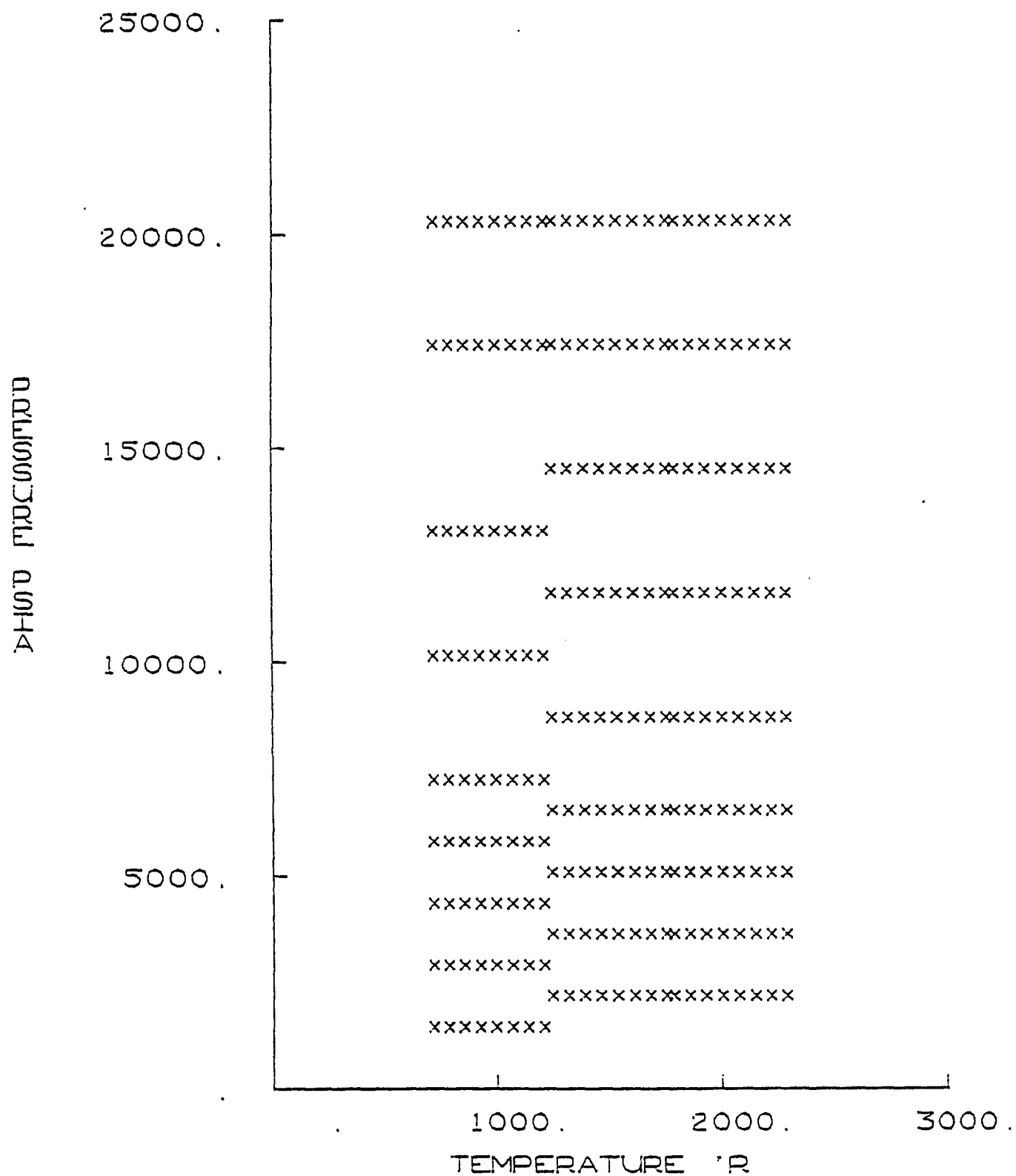


FIGURE 7 Density, Holser and Kennedy

KEENAN, KEYES, ET AL.

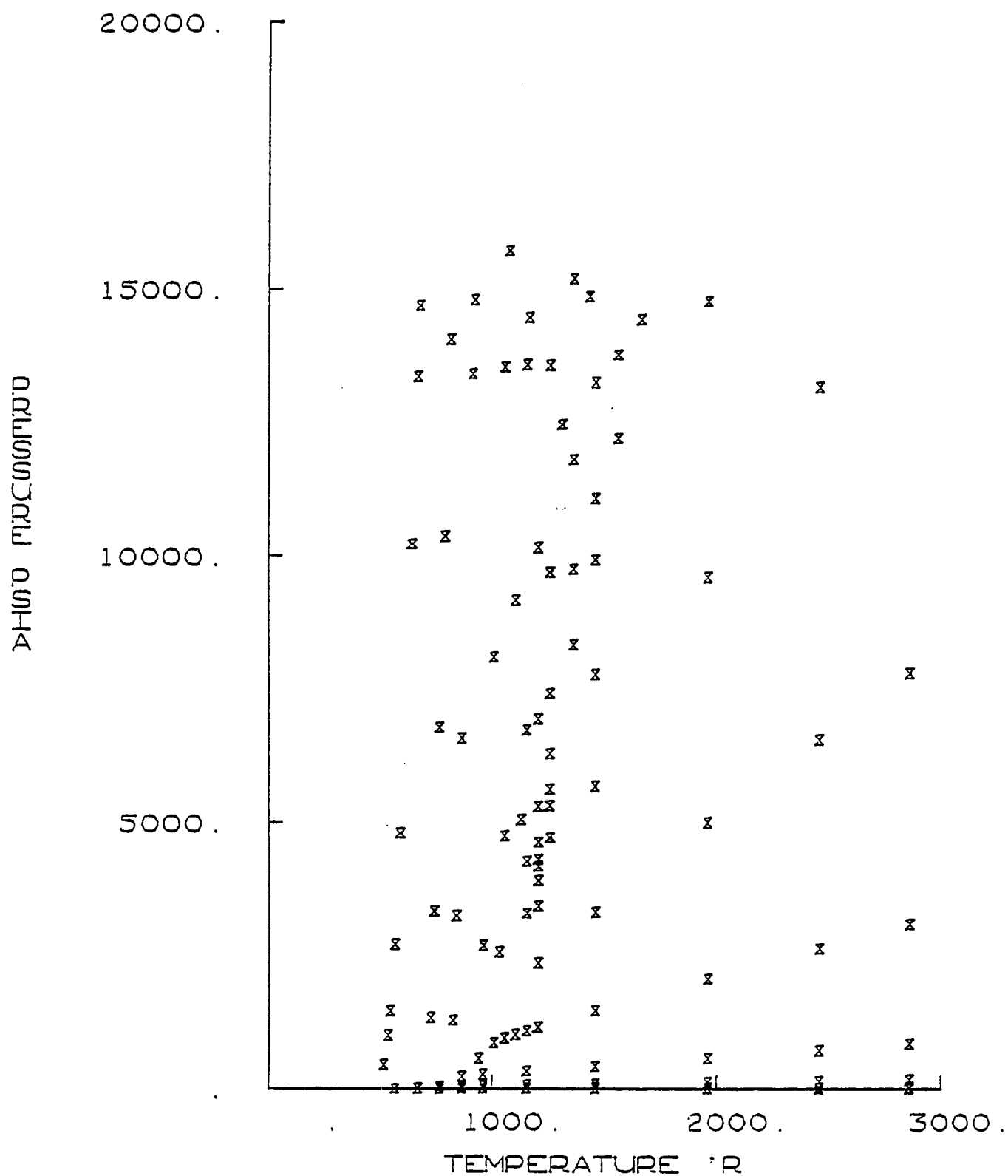


FIGURE 8. Density, Keenan and Keyes

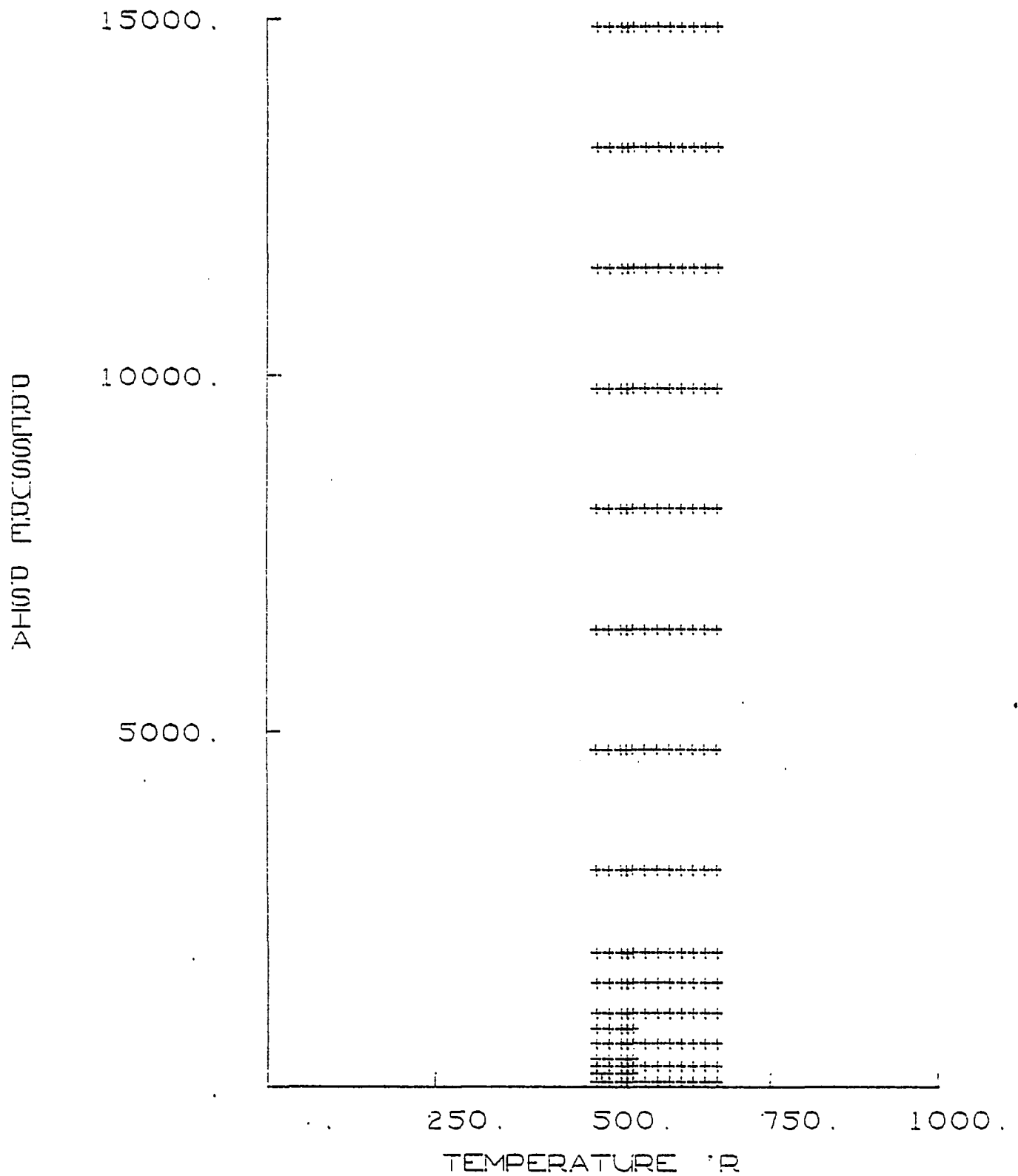


FIGURE 9. Density, Kell and Whalley

KENNEDY

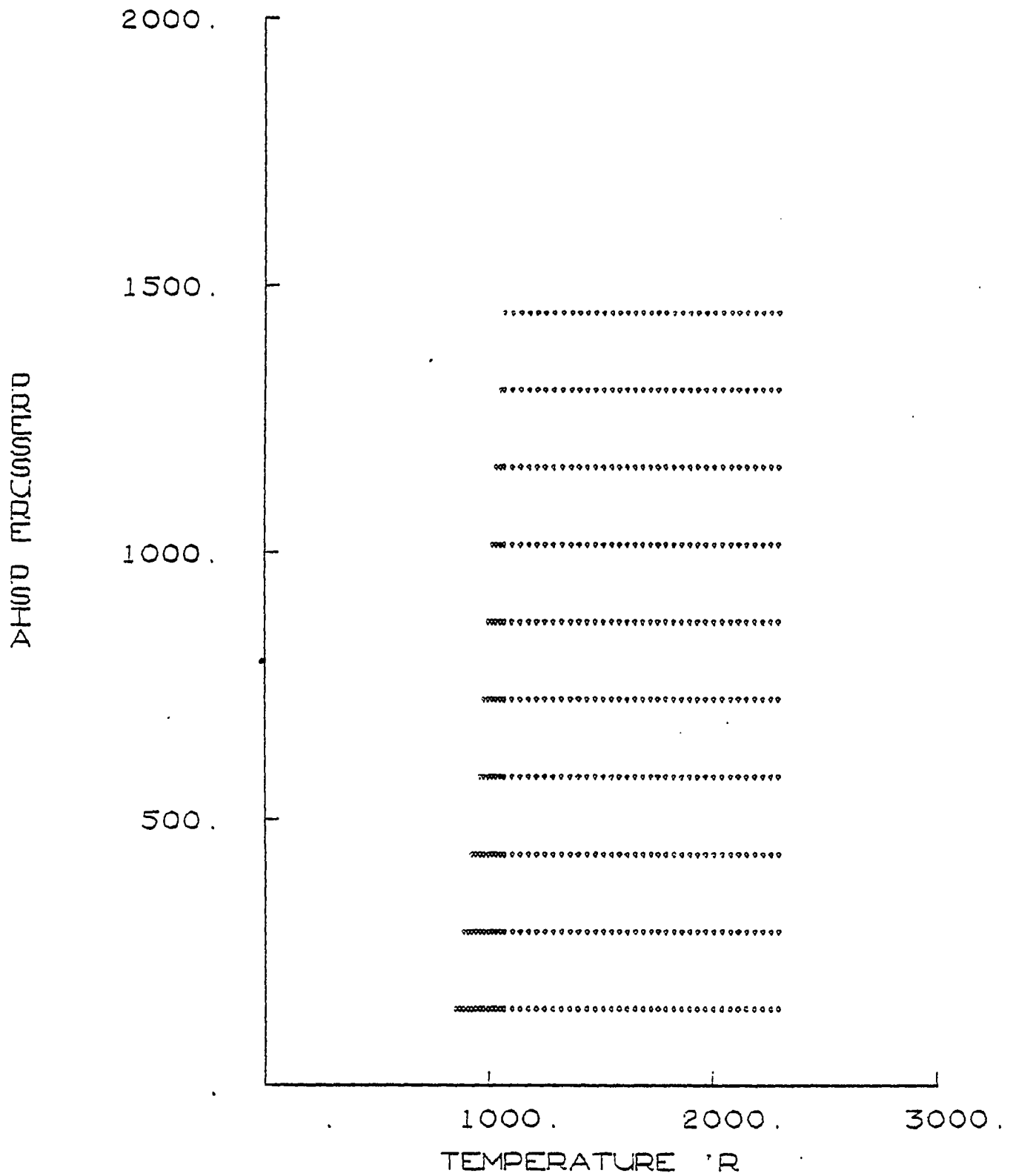


FIGURE 10. Density, Kennedy

KEYES, SMITH

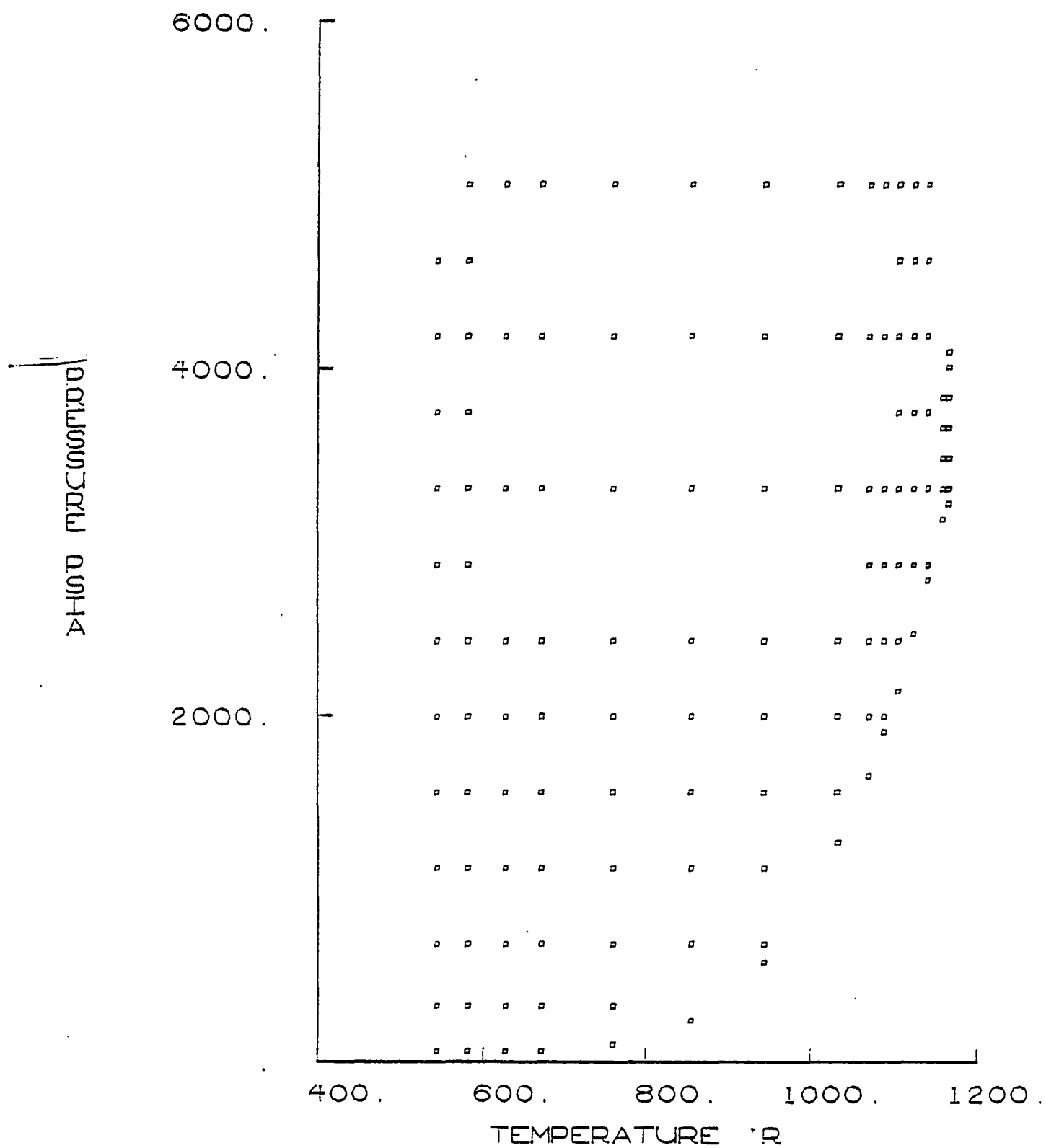


FIGURE 11. Density, Keyes and Smith

KEYES, SMITH, GERRY

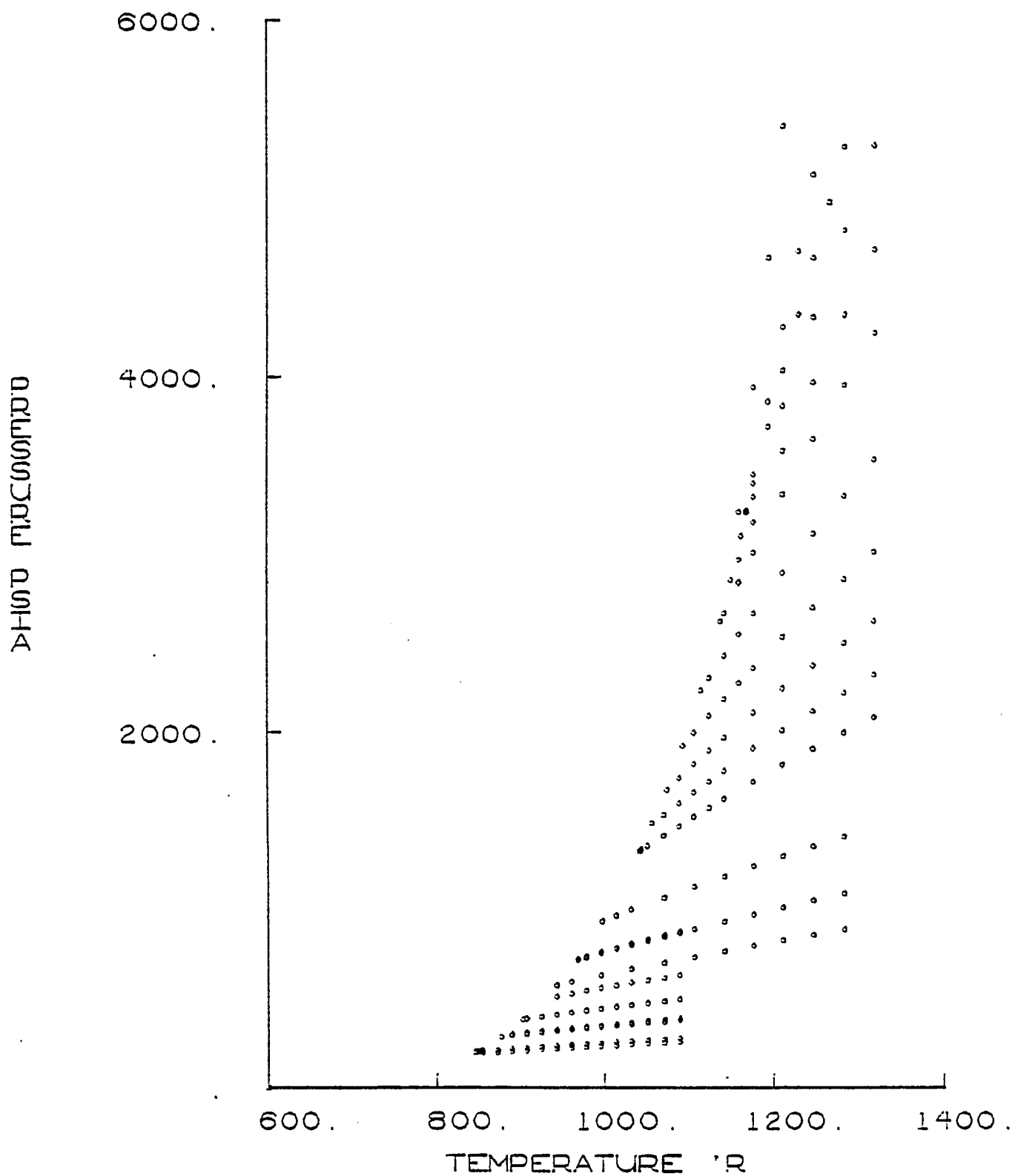


FIGURE 12. Density, Keyes, Smith and Gerry

OSBORNE, STIMSON, GINNINGS

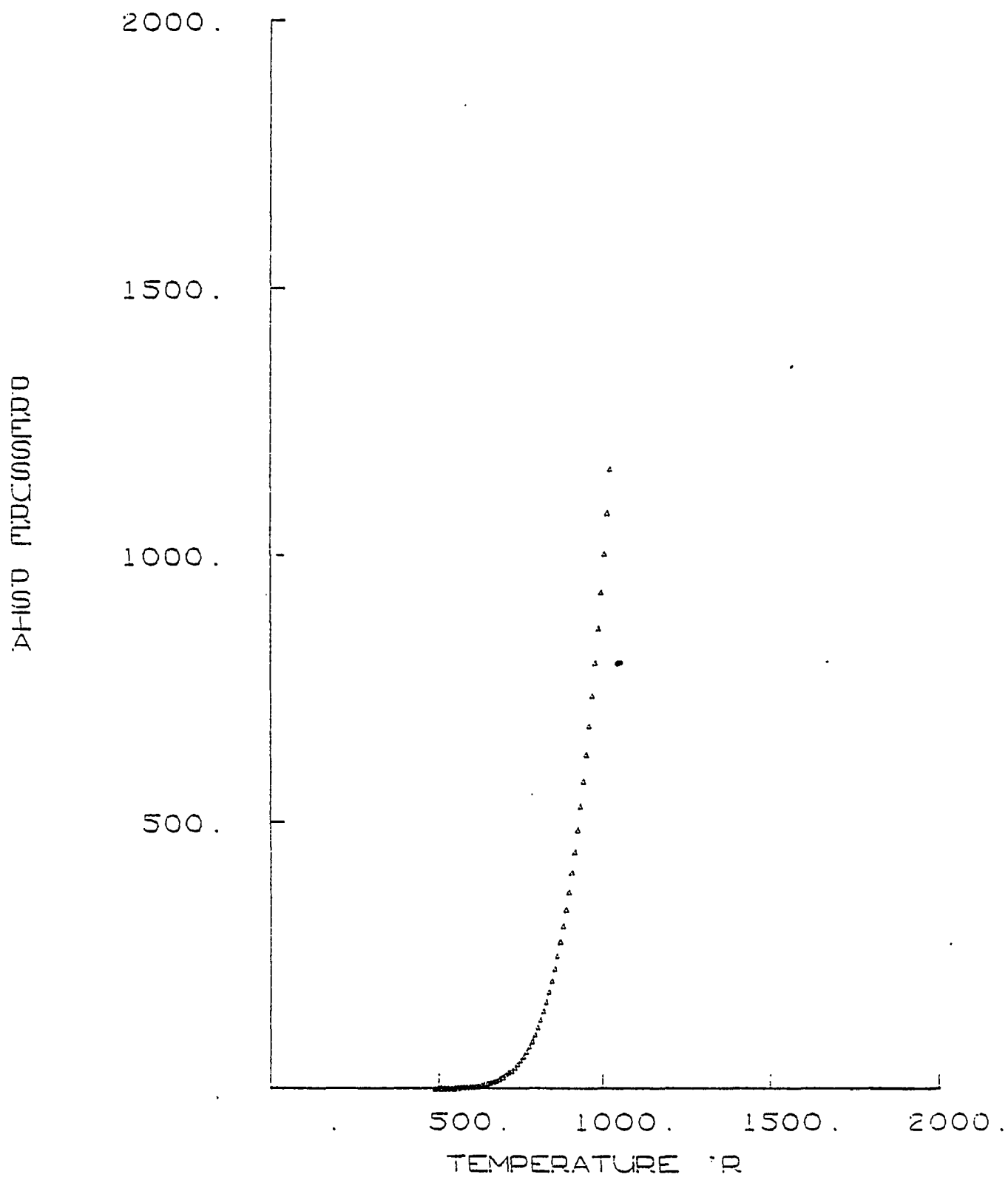


FIGURE 13. Density, Osborne, Stimson and Ginnings

DENSITY

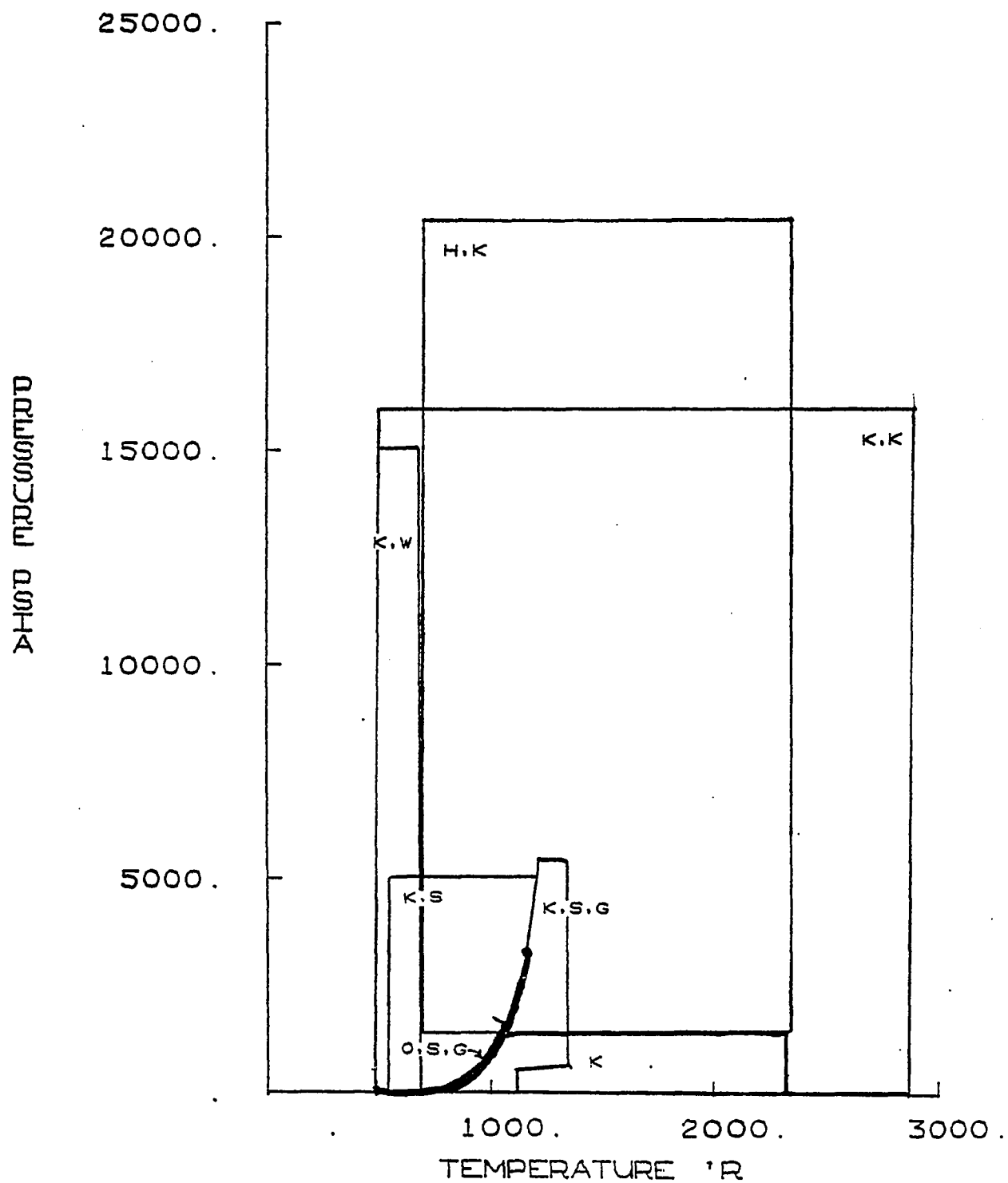


FIGURE 14. Density Data Set Ranges

CHAPTER V

MODEL SELECTION FOR CASE STUDY OF WATER

The compressibility model used for the development of water is linear in the parameters with each term consisting of a monomial of reciprocal temperature and a Tchebycheff polynomial in density. The temperature was reduced by

$$T^* = \alpha T/T_c \quad (19)$$

where α is a scaling parameter used as 1 for water and T_c is the critical temperature. The density was similarly reduced as

$$\rho^* = \beta \rho/\rho_c \quad (20)$$

where $\beta = 1$ and ρ_c is the critical density. The properties for the critical region and other properties used in the equation are given in Table IV.

The Tchebycheff polynomials, T_j , were chosen for their orthogonality, which should improve the calculation stability of the regression program. Another feature of the Tchebycheff polynomials is that they separate into even and odd polynomials. Since they are orthogonal on the

interval $(-1,1)$, the reduced density was divided by 4 to make the largest density be within that range. Since the even polynomials go to 1 at zero but the terms should go to zero when the ideal gas limit one is explicitly given, the terms consist of density times the polynomial.

The terms in the model are then

$$A_{ij}T^{*-1}yT_j(y) \quad (21)$$

where y is the density reduced according to the relation

$$y = \beta\rho/4\rho_c. \quad (22)$$

The full 72 parameter model which was used then is

$$Z = 1 + \sum_{i=0}^7 \sum_{j=0}^8 A_{ij}T^{*-1}yT_j(y). \quad (23)$$

This equation was implemented in the subroutine PRES using a single subscript on the parameters. The listings of PRES and FI1 and FI2, routines used for derived properties are given in appendix C. The Tchebycheff polynomials are given in Table I. A table of the parameter indices corresponding to each term is given in Table II.

Derived Properties. Given an equation of state, the relationships of classical thermodynamics allow the derivation of the other properties. If one starts with a model equation for the Helmholtz free energy, the properties are derived from derivatives. This is the method used by Keenan

TABLE I

The first eight Tchebycheff polynomials

$$T_0(y) = 1$$

$$T_1(y) = y$$

$$T_2(y) = 2y^2 - 1$$

$$T_3(y) = 4y^3 - 3y$$

$$T_4(y) = 8y^4 - 8y^2 + 1$$

$$T_5(y) = 16y^5 - 20y^3 + 5y$$

$$T_6(y) = 32y^6 - 48y^4 + 18y^2 - 1$$

$$T_7(y) = 64y^7 - 112y^5 + 56y^3 - 7y$$

$$T_8(y) = 128y^8 - 256y^6 + 160y^4 - 32y^2 + 1$$

Recursion relation:

$$T_{n+1} - 2yT_n + T_{n-1} = 0$$

TABLE II

Table of the parameter index corresponding to a term of the type $T^{*-i} y^T_j(y)$ in the equation of state. The numbers in parenthesis are the indices of AXTN as implemented in EZFIT.

	y^T_0	y^T_1	y^T_2	y^T_3	y^T_4	y^T_5	y^T_6	y^T_7	y^T_8
T^{*0}	1	7	13	19	25	29	33	37	41(1)
T^{*-1}	2	8	14	20	26	30	34	38	42(2)
T^{*-2}	3	9	15	21	27	31	35	39	43(3)
T^{*-3}	4	10	16	22	28	32	36	40	44(4)
T^{*-4}	5	11	17	23	53(13)	57(17)	61(21)	65(25)	69(29)
T^{*-5}	6	12	18	24	54(14)	58(18)	62(22)	66(26)	70(30)
T^{*-6}	45(5)	47(7)	49(9)	51(11)	55(15)	59(19)	63(23)	67(27)	71(31)
T^{*-7}	46(6)	48(8)	50(10)	52(12)	56(16)	60(20)	64(24)	68(28)	72(32)

and Keyes for their study of water [13]. Alternatively, one can start with the pressure or compressibility formulation and derive the other properties by integration. This method was used by Starling and Han [24] in their work on the modified Benedict, Webb, Rubin equation of state. In each method, one can work with the base model and two derived relations from which all other properties are obtained. When the free energy is used, the derived relations are the temperature and density derivatives. For this work and the EZFIT physical properties package, the three relations are the compressibility and two integrals,

$$Z = P/\rho RT = 1 + \sum_{i=0}^7 \sum_{j=0}^8 A_{ij} T^{*-1} Y T_j(Y) \quad (24)$$

$$FI_1 = \int_0^{\rho^*} (Z-1) d \ln \rho^* \quad (25)$$

$$FI_2 = \int_0^{\rho^*} \partial Z / \partial T^* d \ln \rho^* \quad (26)$$

and the reference condition

$$FI_3 = \ln(\rho RT) \quad (27)$$

Using the definition of the compressibility, FI1 and FI2 are then given as

$$FI_1 = \sum_{i=0}^7 \sum_{j=0}^8 A_{ij} T^{*-1} \int_0^Y T_j(Y) dY \quad (28)$$

$$FI_2 = \sum_{i=1}^7 \sum_{j=0}^8 A_{ij} (-i) T^{*-(i+1)} \int_0^Y T_j(y) dy \quad (29)$$

The integrals of the Tchebycheff polynomials are given in Table III. The physical properties used are given in Table IV.

The reduced departures as derived in appendix A are given as

$$A^* = T^* FI_1 + T^* FI_3 \quad (30)$$

$$U^* = -T^* FI_2 \quad (31)$$

$$H^* = -T^{*2} FI_2 + T^*(Z-1) \quad (32)$$

$$S^* = -FI_1 + T^* FI_2 - FI_3 \quad (33)$$

$$G^* = T^* FI_1 + T^* FI_3 + T^*(Z-1) \quad (34)$$

$$f/f^0 = \exp(FI_3 + FI_1 + Z-1) \quad (35)$$

These relations allow the computation of the derived properties for the water model. The values of the parameters for the model were then determined by regression. For the 48 parameter model which was the base equation, the density terms were used only up to $j=5$.

TABLE III

The integrals of the Tchebycheff polynomials on the interval (0,y).

$$\int T_0 = y$$

$$\int T_1 = y^2/2$$

$$\int T_2 = 2/3 y^3 - y$$

$$\int T_3 = y^4 - 3/2 y^2$$

$$\int T_4 = 8/5 y^5 - 8/3 y^3 + y$$

$$\int T_5 = 8/3 y^6 - 5 y^4 + 5/2 y^2$$

$$\int T_6 = 32/7 y^7 - 48/5 y^5 + 6 y^3 - y$$

$$\int T_7 = 8 y^8 - 56/3 y^6 + 14 y^4 - 7/2 y^2$$

$$\int T_8 = 128/9 y^9 - 256/7 y^7 + 32 y^5 - 32/3 y^3 + y$$

TABLE IV

The physical and critical properties of water

Critical temperature	1165.3°R
Critical pressure	3208.0 psia
Critical density	1.1102 lb moles/ft ³
Molecular weight	18.015
Pitzer Accentric factor	0.348
Universal gas constant	10.7315 psia ft ³ /lb moles °R 0.110308 BTU/lbm °R

CHAPTER VI

INITIAL VALUE SELECTION

In most equation of state models, the equation reduces to the ideal gas equation when the parameters are zero. This is the easiest and most common choice. The problem with the ideal gas as the initial model is that it does so poorly in the high density region that a regression on a full range density set is unable to improve the liquid points. Information is not transmitted appropriately to the parameters. The enthalpy departure will be quite bad and the vapor pressure calculation will not converge. It is therefore usual to make some kind of quick regression for a function of the temperature and density, thereby eliminating any search techniques, to get a preliminary set of parameters. Two applicable functions are the compressibility and the pressure. The compressibility, $Z = P/\rho RT$, is commonly used and gives good results. It was used for the development of the Leonard-Jones perturbation model which was then applied to the prediction of methane [9]. Use of the pressure, on the other hand, has some problems in that in the high density region the large value of the derivative

$\partial P/\partial \rho$ controls the regression. This makes the equation over constrained in this region with a corresponding loss in accuracy in the low density region. This problem can be solved by the selection of appropriate weights for the individual pressure points instead of the usual method of selecting the weight to be $1/P^2$, i.e. the maximum likelihood weight. The weight of the point is proportional to the variance [4] and is theoretically given as

$$w_i = 1/(\sigma_p^2 + \sigma_\rho^2 \frac{\partial P^2}{\partial \rho} + \sigma_T^2 \frac{\partial P^2}{\partial T}) \quad (36)$$

The problem with this method is the evaluation of the derivatives. Since the function has no other parameters yet, the derivatives, if evaluated from the model, would be those of the ideal gas and inaccurate.

In development of the water equation of state, a tabular function was developed for the weight based upon the density. The weighting function is given in Table V. This function was used to perform the regression on just the parameter portion of the model, that is the ideal gas portion was subtracted from the pressure. Good results were obtained. For the 48 parameter equation these pressure terms were able to predict density to 1.08% for 335 points. This set of parameters is quite adequate for starting density and multi-property regression.

TABLE V
WEIGHTING FUNCTION FOR PRESSURE
DEPARTURE REGRESSIONS

<u>Reduced Density</u>	<u>Weight</u>
4.0-3.0	0.009
3.0-2.5	0.001
2.5-1.2	0.10
1.2-0.5	10.0
0.5-0.1	1.00
0.1-0.001	10.0 ($T_r > 1.2$)
0.001-0.0	100.0 ($T_r > 1.2$)
0.1-0.0	100.0 ($T_r < 1.2$)

CHAPTER VII

MODEL IMPROVEMENT BY REMOVAL OF INSIGNIFICANT PARAMETERS

In working on large models, that is models with over 30 parameters, some logical method is needed to determine if a parameter is significant to model the data. If it is not significant the result will not be as accurate as possible because information was used to determine values for this parameter which should not have been included in the regression. Statistical analysis of the variance σ_a^2 , of the parameters can give the needed guides. For a single parameter the standard way to check is to test the hypothesis that the parameter is zero. This leads to the standard T-test,[4] that the parameter should be zero if the relation is satisfied

$$|a| < t_{\alpha} \sigma_a \quad (37)$$

where t_{α} is the Student's t statistic at the α level, σ_a is the standard error, which is the square root of the variance for the parameter.

For linear functions the model can be generated stepwise by only adding terms that have the highest correlation coefficient with the data. This method has been used to develop equations for oxygen and nitrogen [11]. Since this is only applicable to linear regressions, another method was developed. This method investigates the contribution that each parameter gives to the reduction of the sum of squared errors [8]. The contribution for the parameter a is approximated as

$$SSE_a = \left(\frac{a}{\sigma_a} \right)^2 \quad (38)$$

The parameters with the smallest contributions can many times be eliminated with little effect on the results. When the new parameter set is regressed with the low SSE terms set to zero, improvement over the previous regression is obtained. EZFIT outputs the variance, standard error and the SSE for each parameter allowing easy evaluation of the significance of the parameters.

This method was used to develop the equation of state for water. Using the method, it was possible to reduce the number of parameters from 48 to 43 and to improve the prediction. With the continued application of the method even more improvement would be possible. It was decided to stop at this stage because the method was sufficiently expositied. The procedure was initiated using the previously

mentioned method for getting preliminary parameters for density, that is, a density regression was performed to get the best density results for the 48 parameter version. Using these results, a multiproperty regression of density, enthalpy departure, and vapor pressure was performed to get the base equation from which to work for improvement. Average absolute deviations for properties (also referred to as errors) for this base equation were 0.66% for 382 density points, 1.04% for 53 vapor pressure points and 1.09 BTU/lbm (2.53 J/g) for 113 enthalpy departure points. This is the standard data set plotted in Figures 1, 3 and 4 which was used for the equation development.

The six least significant parameters as determined by the SSE criterion were then studied to see the effect their removal from the model would have upon the results. The details of this study are given in Table VI. As shown in Table VI, the parameters have little effect upon density with the most effect caused by parameter 59, which increased the density deviation to 1.12%. On the other hand, enthalpy departure and vapor pressure are more sensitive. The enthalpy deviation was increased to 27.9 BTU/lbm and vapor pressure deviation to 49.1% with the elimination parameter 59. It was decided to remove the three parameters with the least effect, 22, 46, and 60. This set of parameters when removed increased the errors to 0.73% for density, 2.57% for vapor pressure, and 5.12 BTU/lbm (11.9 J/g) for enthalpy departure.

TABLE VI

Effects of removing parameters by setting to zero
in the 48 parameter equation

Parameters Set to Zero	Errors		Enthalpy Departure(BTU/lbm)
	Density(%)	Vapor pressure(1%)	
None	0.66	1.09	1.09
46	0.68	2.65	2.53
60	0.66	3.18	2.94
22	0.76	6.29	6.43
48	0.88	18.8	26.3
5	0.89	27.6	18.6
59	1.12	49.1	27.9
22, 46, 60	0.73	2.56	5.12

When the reduced set of 45 parameters were regressed there was improvement over the 48 parameter base equation in both density and vapor pressure and slightly less accurate results for enthalpy departure. The average absolute deviations were 0.62% for density, 0.98% for vapor pressure and 1.12 BTU/lbm (2.60 J/g) for enthalpy departure. The method was once again applied to this equation to try for further improvement and reduction in the number of parameters. The three parameters with the lowest SSE this time were 20, 26, and 5, of which only 5 had been in the previous set to be considered. When parameter 20 was removed, there was a remarkable improvement in the vapor pressure prediction; the average absolute deviation was reduced to 0.13%. Only the removal of parameter 5 caused an unacceptable error increase in the enthalpy and vapor pressure predictions. This time parameters 20 and 26 were eliminated. The details of the effects of these parameters are given in Table VII.

When the 43 parameters were regressed it was found that the enthalpy controlled the regression and the improvement in vapor pressure was lost. This was remedied by adjusting the group weights for each data type so that each group contributed about the same amount to chi-squared. This led to the final 43 parameter equation. The resultant average absolute deviations were 0.42% for density, 0.12% for vapor pressure and 1.58 BTU/lbm (3.67 J/g) for enthalpy

TABLE VII

Effects of removing parameters by setting to zero
in the 45 parameter equation

<u>Parameters Set to Zero</u>	<u>Errors</u>		
	<u>Density(%)</u>	<u>Vapor Pressure(%)</u>	<u>Enthalpy Departure(BTU/lbm)</u>
None	0.62	0.98	1.12
20	0.67	0.13	1.87
26	0.63	1.01	1.12
5	0.72	8.20	8.31
20, 26	0.68	0.12	1.84

departure. This is a marked improvement over the 48 parameter equation for density and vapor pressure, which are the most accurate experimental data. The enthalpy departure predictions are acceptable, especially since the enthalpy departures were totally derived data and not measured.

CHAPTER VIII

SUMMARY OF METHODOLOGY AND RESULTS FOR CASE STUDY

Using the method outlined in this work, an equation of state was developed for water as a case study. The steps of the method are:

1. Collect data sets and selection of a working data set (subset).
2. Get initial parameters by a pressure regression.
3. Improve the density regression.
4. Develop a base equation by multi-property analysis.
5. Improve the model by eliminating terms.
6. Check validity of the equation by predicting more data.

This method was used to develop a 43 parameter equation of state of the form

$$Z = 1 + \sum_{i=0}^7 \sum_{j=0}^5 A_{ij} T^{*-i} y_j^T(y) \quad (39)$$

where $y = \beta p / 4 p_c$, $T^* = \alpha T / T_c$ and T_j is the Tchebycheff polynomial. The parameters for the equation are given in Table VIII.

Data Sets. Data from 9 references were collected as well as uniform data sets generated from the high precision equation of Keenan and Keyes. This led to a collection of 1459 density points, 263 enthalpy departure points, and 53 vapor pressure points covering the pressure range 0.089-20,305 psia (0.61-140,000 KPa) and the temperature range 491.67-2859.67°R (273.15-1588.7°K). A working data set was selected from these data points, consisting of 382 density points, 113 enthalpy points and 53 vapor pressure points.

Initial parameters and density regression. The initial values of the 48 parameters were determined by performing regression on the density data set. The data were converted to pressure departure by subtracting the ideal gas pressure and were then fit (using pressure as the objective) using the tabulated weighting function given in Table V. This led to an average absolute error in density of 1.08% for the 382 density points. A regression with the density as the objective was then performed. This led to the prediction of density with 0.50% average absolute error.

Multiproperty base equation. The density results were used to predict enthalpy departure and vapor pressure. As usually happens with equation of state parameters determined from density data alone, several of the low temperature

TABLE VIII

Values of the parameters for the 43 parameter Tchebycheff
polynomial equation of state for water

<u>Index</u>	<u>(I,J)</u>	<u>Value</u>	<u>Index</u>	<u>(I,J)</u>	<u>Value</u>
1	00	0.489078	25	04	0.644619
2	10	-1.33375	27	24	2.89299
3	20	0.0447899	28	34	0.0472269
4	30	-0.0433729	29	05	-0.537426
5	40	0.026460	30	15	-0.697395
6	50	-0.189002	31	25	0.366763
7	01	4.90720	32	35	0.713576
8	11	0.294431	45	60	-0.0773029
9	21	0.439805	47	61	-0.071481
10	31	1.14694	48	71	0.00894616
11	41	0.634109	49	62	0.121502
12	51	0.0938234	50	72	0.0768117
13	02	-0.334176	51	63	-0.258435
14	12	1.48579	52	73	-0.0697795
15	22	4.77029	53	44	-0.141785
16	32	1.49032	54	54	-0.124966
17	42	1.00340	55	64	0.369510
18	52	0.217828	56	74	-0.0548949
19	03	-0.714156	57	45	0.513778
21	23	0.117546	58	55	0.538242
23	43	-0.580674	59	65	-0.127041
24	53	-0.208757			

vapor pressure points did not converge. The lowest temperature enthalpy points also had errors in excess of 5 BTU/lbm (12 J/g). For the first few iterations of the multiproperty regression, the nonconverging vapor pressure points were removed and the weight for the enthalpy points with large errors was reduced. As the results improved with increased iterations, the complete working data set was used. This resulted in the 48 parameter base equation. This equation predicted density to 0.56%, enthalpy departure to 1.09 BTU/lbm (2.53 J/g) and vapor pressure to 1.04%.

Model Improvement. The results for the base equation were improved by eliminating the least significance parameters. An estimate of each parameter's significance was determined as the contribution to the sum of squares, $SSE_j = A_j^2 / \sigma_j^2$, which is the ratio of the parameter squared to its variance. This method was used to eliminate 5 parameters in two steps. This final 43 parameter equation predicted the 382 density points to 0.43%, the 113 enthalpy departure points to 1.58 BTU/lbm (3.67 J/g) and the 53 vapor pressure points to 0.12%. The 43 parameters for the equation of state are given in Table VIII.

Data predictions. This 43 parameter equation was then tested for 1775 data points. The results are summarized in Table IX, see Appendix D for complete tabulation. For the 1459 density points the average error was 0.58%. The high pressure and low temperature compressed liquid region

TABLE IX

Results for the 43 parameter equation of state for water

Reference	Number of Data Points	Pressure Range		Temperature Range	Average Absolute Deviation
<u>DENSITY</u>					
Working set*	382	0.66-20,305	psia	491.67-2859.67 °R	0.43%
Subsets	265	0.66-10,000	psia	491.67-2859.67 °R	0.31%
	117	10.000-20,305	psia	634.67-2459.67 °R	0.68%
Holser, Kennedy ¹⁰	216	1450.38-20,305	psia	707.67-2291.67 °R	0.50%
Keenan, Keyes ¹³	108	0.66-14694	psia	509.67-2859.67 °R	0.4 %
Kennedy ¹⁵	401	145.038-1450.48	psia	851.67-2291.67 °R	0.31%
Keyes, Smith ¹⁶	129	61.96-5066.71	psia	545.67-1139.67 °R	0.58%
Keyes, Smith, Gerry ¹⁷	283	194.28-5403.28	psia	842.67-1319.67 °R	0.73%
Kell, Whalley ¹⁴	217	76.87-14,886.5	psia	491.67-671.67 °R	1.03%
Osborne, Stimson, Ginnings ²⁰	60	0.089-1160.667	psia	491.67-1022.67 °R	0.36%
TOTAL	1459	0.089-20,305	psia	491.67-2859.67 °R	0.58%
<u>ENTHALPY</u>					
Working set					
Keenan, Keyes ¹³	113	0.66-14,694	psia	509.67-2859.67 °R	1.58 BTU/lbm
Angus, Newitt ¹	16	870.2-14,503	psia	1211.67-1751.67 °R	2.90 BTU/lbm
Callendar, Egerton ⁵	134	71.5-2842.	psia	851.67-1571.67 °R	1.45 BTU/lbm
TOTAL	263	0.66-14503	psia	509-67-2859.67 °R	1.59 BTU/lbm
<u>VAPOR PRESSURE</u>					
Osborne, Stimson, Ginnings ²⁰	53	0.089-3090	psia	491.67-1159.67 °R	0.12%

* Included in individual density data sets also.

have the largest errors. As shown in Table IX, the largest density error, 1.03% occurs for the liquid data of Kell and Whalley [14]. Gas densities are predicted quite accurately as shown by the data of Kennedy [15], for which the error is 0.31%. The trouble with the high pressure region is more apparent when the test data set is separated into pressures below and above 10,000 psia (69,000 KPa). For the low pressure set, the error is only 0.32%, while for the high pressure set, the error more than doubles, to 0.68%.

Predictions for the enthalpy departure set of 263 points have an average absolute error of 1.59 BTU/lbm (3.70 J/g). The prediction errors for the gas phase data of Callendar and Egerton [5] were comparable to the errors of the working set, i.e., 1.45 BTU/lbm (3.37 J/g) as compared to 1.58 BTU/lbm (3.67 J/g). The only experimental liquid and high pressure points available were the 16 points of Angus and Newitt [1]. Because of the increased errors in this region for density, it is not surprising that the prediction errors for this set has higher errors, 2.90 BTU/lbm (6.74 J/g).

The vapor pressure data were included totally in the regression. Predicted vapor pressures have an average absolute error of 0.12% from the triple point to within 0.4% of the critical pressure.

CHAPTER IX

CONCLUSIONS

The six step method outlined in this work will allow systematic development of a high precision equation of state. The method gives a logical way of handling the large number of parameters required by complex models. The success of this method was shown by its use to develop the 43 parameter equation for water. This equation was not pushed to its ultimate because of the restriction of time and expense. By using the embodiment of this method in the regression package EZFIT and the guidelines outlined herein, it is now possible for the researcher to quickly and systematically develop as complex a model as needed to represent the data to an accuracy approaching the experimental uncertainty.

BIBLIOGRAPHY

1. Angus, S., Newitt, D.M., Phil. Trans. Roy. Soc. (London), 259, 107 (1966).
2. Beattie, Bridgeman, Proc. Am. Acad. Arts. Sci., 63, 299 (1928).
3. Benedict, M., Webb, G.D., Rubin, L.C., J. of Chem. Phys., 8, 334 (1940).
4. Bevington, P.R., "Data Reduction and Error Analysis for the Physical Sciences", McGraw-Hill, New York, 1969.
5. Callendar, G.S., Egerton, A., Phil. Trans. Roy. Soc. (London), 252, 133 (1960).
6. Carnahan, B., Luther, H.A., and Wilkes, J.O., "Applied Numerical Methods", John Wiley and Sons, New York, 1969.
7. Carnahan, N.F., Starling, K.E., J. of Chem. Phys., 51, 635 (1969).
8. Deming, W.E., "Statistical Adjustment of Data", J. Wiley and Sons, New York, 1944.
9. Goin, K., Mo, K.C., and Starling, K.E., Proc. Ok. Acad. Sci., 57, 119 (1977).
10. Holser, Kennedy, Am. J. Sci., 256, 744 (1958).
11. Jacobsen, R.T., Stewart, R.B., Crain, Jr., R.W., Rose, G.L., and Myers, A.F., Adv. Cryo. Engr., 21, 532 (1975).
12. Johnson, D.E., and Johnson, J.R., "Mathematical Methods in Engineering and Physics", The Ronald Press Co., New York, 1965.
13. Keenan, J.H., Keyes, F.G., Hill, P.G., and Moore, J.G., "Steam Tables", John Wiley and Sons, New York, 1969.

14. Kell, and Whalley, Phil. Trans. Roy. Soc. (London), 258A, 565 (1965).
15. Kennedy, Am. J. Sci., 255, 724 (1957).
16. Keyes, and Smith, Proc. Am. Acad. Arts Sci., 285 (1934).
17. Keyes, Smith, and Gerry, Proc. Am. Acad. Arts Sci., 70, 319 (1936).
18. Lin, C., Hopke, S.W., AIChE Symp. Series No. 140, 70, 37.
19. Martin, J.J., Hou, Y., AIChE J., 1, 142 (1955).
20. Osborne, Stimson, and Ginnings, RP 1229, National Bureau of Standards, 1939.
21. Redlich, and Kwong, Chem. Rev., 44, 233 (1949).
22. Rodosence, J.B., and Miller, R.C., "Calculations of LNG Excess Values by a Modified Hard-Sphere Model", paper No. K-5, University of Wyoming, Wyoming.
23. Soave, Chem. Engr. Sci., 27, 1197 (1972).
24. Starling, K.E., and Han, M.S., Hydrocarbon Proc., 51(6), 107 (1972).
25. Stewart, G.A., "Introduction to Matrix Computations", Academic Press, New York, 1973.
26. Tsonopoulos, and Prausnitz, Cryogenics, 9, 315 (1969).
27. Venniz, A.J. and Kobayashi, R., AIChE J., 15(6), 926 (1969).
28. Verlet, L., and Weiss, J., Phys. Rev., 5(2), 939 (1972).
29. Weeks, J.D., Chandler, D., and Anderson, H.C., J. Chem. Phys., 54, 5237 (1971).
30. West, E.W., and Erbar, J.H., "An Evaluation of Four Methods of Predicting the Thermodynamic Properties of Light Hydrocarbon Systems", Presented at NGPA 52nd Annual Meeting, Dallas, Texas (1973).

APPENDIX A

Derivation of Reduced Residual

Thermodynamic Properties

From classical thermodynamics relationships are obtained for the various thermodynamic properties of a fluid. These are required to obtain the thermodynamic properties used in design from an equation of state. The basic relations for bulk properties are¹

$$A = U - T \cdot S \quad (1-a)$$

$$H = U + P \cdot V \quad (1-b)$$

$$G = U + P \cdot V - T \cdot S \quad (1-c)$$

$$\mu_i = (\partial A / \partial n_i)_{T, V, n_j} \quad (1-d)$$

where A is the Helmholtz free energy, U the internal energy, T the absolute temperature, S the entropy, H the enthalpy, P the pressure, V the volume, and μ_i the chemical potential of a system of n moles of which there are n_i moles of the i th component.

The molar quantities are obtained by dividing by n to get the following relations in which the tilde (\sim) represents a molar quantity

$$\tilde{A} = \tilde{U} - T \cdot \tilde{S} \quad (2-a)$$

$$\tilde{H} = \tilde{U} + P/\rho \quad (2-b)$$

$$\tilde{G} = \tilde{U} + P/\rho - T \cdot \tilde{S} \quad (2-c)$$

$$\mu_i = (\partial \tilde{A} / \partial n_i)_{T, V, n_j} \quad (2-d)$$

where $[n_i$ is the number of moles of the i th component and] ρ is the molar density, $\rho = n/V$.

A modified excess property is defined as the difference between the quantity at the temperature and density of the system and the sum of the product of the mole fraction and the value of the property as an ideal gas at the temperature and unit pressure. For internal energy the modified excess property is

$$\Delta \tilde{U} = \tilde{U} - \sum X_i U_i^O \quad (3)$$

in which the superscript O represents the ideal gas condition of the same temperature and unit pressure. Similarly, equations 2 become

$$\Delta \tilde{A} = \tilde{U} - T \cdot \tilde{S} - (\sum X_i U_i^O - T \sum X_i S_i^O) = \Delta \tilde{U} - T \Delta \tilde{S} \quad (4-a)$$

$$\Delta \tilde{H} = \tilde{U} + P/\rho - (\sum X_i U_i^O + \sum X_i RT) = \Delta \tilde{U} + R \cdot T(Z-1) \quad (4-b)$$

$$\begin{aligned} \Delta \tilde{G} &= \tilde{U} + P/\rho - T \tilde{S} - (\sum X_i U_i^O + RT - T \sum X_i S_i^O) \\ &= \Delta \tilde{U} - T \Delta \tilde{S} + RT(Z-1) \end{aligned} \quad (4-c)$$

$$\Delta \mu = (\partial \tilde{A} / \partial n_i)_{T, V, n_j} - (U_i^O - T \cdot S_i^O) = (\partial \Delta \tilde{A} / \partial n_i)_{T, V, n_j} \quad (4-d)$$

where R is the universal gas constant and Z is the compressibility $Z = P/\rho RT$.

By defining a dimensionless temperature, $T^* = \alpha T/T_c$, where α is a scaling parameter and T_c is the critical temperature and using the universal gas constant, dimensionless properties are given as

$$A^* = \alpha \Delta \tilde{A}/RT_c \quad (5-a)$$

$$U^* = \alpha \Delta \tilde{U}/RT_c \quad (5-b)$$

$$H^* = \alpha \Delta \tilde{H}/RT_c = U^* + T^*(Z-1) \quad (5-c)$$

$$S^* = \Delta \tilde{S}/R = (U^* - A^*)/T^* \quad (5-d)$$

$$G^* = \alpha \Delta \tilde{G}/RT_c = U^* - T^* S^* + T^*(Z-1) \quad (5-e)$$

$$\mu_i^* = \alpha \Delta \mu_i/RT_c = (\partial A^*/\partial n_i)_{T,V,n_j} \quad (5-f)$$

The fugacity f , which is defined as

$$RT \ln f_i = \mu_i \quad (6)$$

then is

$$T^* \ln f_i/f_i^O = \mu_i^* \quad (7)$$

where f_i^O is the fugacity of the i th component in an ideal gas mixture at the same temperature and unit pressure.

The Helmholtz free energy is derived from a pressure explicit equation of state as¹

$$A = \int_V^\infty (P - nRT/V) dV - RT \sum n_i \ln(V/n_i RT) + \sum n_i (U_i^O - TS_i^O) \quad (8)$$

As in equation 2-a, A is given in molar form as

$$\tilde{A} = \int_v^\infty (P - RT/v) dv - RT \sum X_i \ln(v/X_i RT) + \sum X_i (U_i^O - TS_i^O) \quad (9)$$

The modified excess form (4-a) then is

$$A^* = \alpha/RT_c \int_v^\infty (P-RT/v) dv - T^* \sum X_i \ln(v/X_i RT) \quad (10)$$

By using the relationships $P = Z\rho RT$, $dv = -d\rho/\rho^2$, and $\rho^* = \beta\rho/\rho_c$, where β is a scaling factor and ρ_c is the critical density, 10 is further reduced to

$$\begin{aligned} A^* &= \alpha/RT_c \int_\rho^0 (Z\rho RT - \rho RT) (-d\rho/\rho^2) + T^* \sum X_i \ln(X_i \rho RT) \\ &= T^* \left\{ \int_0^{\rho^*} (Z-1) d \ln \rho^* + \sum X_i \ln X_i \rho^* T^* + \ln(R\rho_c T_c / \beta \alpha) \right\} \end{aligned} \quad (11)$$

In a similar fashion, the internal energy is given as

$$U = \int_v^\infty (P - T(\partial P / \partial T)_{v,n}) dv + \sum n_i U_i^0 \quad (12-a)$$

$$U^* = \alpha/RT_c \int_v^\infty (P - T(\partial P / \partial T)_{v,n}) dv \quad (12-b)$$

$$\begin{aligned} U^* &= \alpha/RT_c \int_\rho^0 (Z\rho RT - \rho RT(Z + T\partial Z / \partial T)) (-d\rho/\rho^2) \\ &= -T^{*2} \int_0^{\rho^*} \partial Z / \partial T^* d \ln \rho^* \end{aligned} \quad (12-c)$$

By defining the following terms

$$FI_1 = \int_0^{\rho^*} (z-1) d \ln \rho^* \quad (13-a)$$

$$FI_2 = \int_0^{\rho^*} \partial Z / \partial T^* d \ln \rho^* \quad (13-b)$$

$$FI_3 = \sum X_i \ln(X_i \rho^* T^*) + \ln(R\rho_c T_c / \beta \alpha) \quad (13-c)$$

and using the previous results the thermodynamic properties are given from an equation of state as

$$A^* = T^* FI_1 + T^* FI_3 \quad (14-a)$$

$$U^* = -T^{*2} FI_2 \quad (14-b)$$

$$H^* = -T^{*2} FI_2 + T^*(Z-1) \quad (14-c)$$

$$S^* = -FI_1 + T^* FI_2 - FI_3 \quad (14-d)$$

$$G^* = T^* FI_1 + T^* FI_3 + T^*(Z-1) \quad (14-e)$$

$$\ln f_i/f_i^O = 1/T^* (\partial A^* / \partial X_i)_{T,V,X_j} \quad (14-f)$$

For a pure fluid the fugacity reduces to

$$\ln f_i/f_i^O = FI_3 + FI_1 + Z-1 \quad (15)$$

¹Prausnitz, J.M., "Molecular Thermodynamics of Fluid-phase Equilibria", Prentice-Hall, Englewood Cliffs, New Jersey, 1969.

APPENDIX B

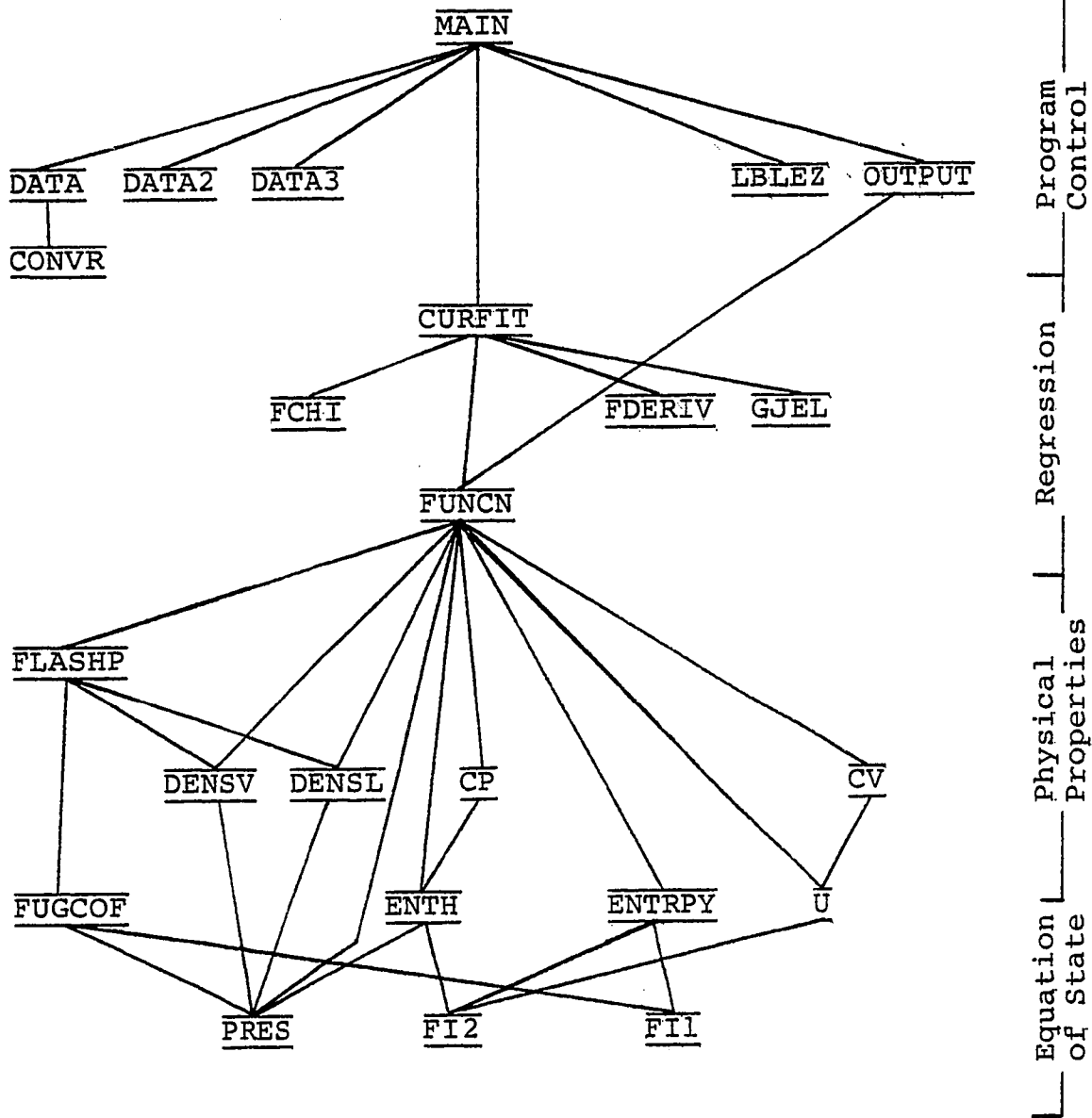
EZFIT USERS GUIDE

EZFIT is a flexible nonlinear regression program designed specifically for equation of state development. By its nature, though, it is easily adapted for any nonlinear regression. Two methods for regression are available by appropriate selection of control variables, the simpler Gauss-Newton and the Marquart¹. EZFIT features the selection of three data input routines that can be tailored to various formats, as standard, the ability to pass 40 parameters and fit 30 and to use any combination of independent variables and data points so long as their product is less than 3000 (such as 10 independent variables and 300 data points). Specific parameters from the maximum of 40 can be selected for regression in any order while the rest are fixed. The program can also do successive regressions with adding a term to the result of the previous regression.

The following sections explain in detail the method of EZFIT. Figure 1 shows the overall organization of the program subroutines. The first section explains the details

¹Bevington, Phillip R., "Data Reduction and Error Analysis for the Physical Sciences", McGraw-Hill, New York, 1969.

Program Organization



of the main program. The second section describes the common blocks used to pass property and control information among the routines. The third section gives detailed descriptions of the subroutines. The fourth sections tells how to adapt EZFIT to fit any function. The last section gives a listing of the FORTRAN source. In these descriptions, card input is detailed as which columns the numbers are in, y i.e., cc 1-5_y, etc. If the variable inputed is an integer as noted by its first letter being I-N, the value is right justified with no periods. Other variables are real numbers and must include periods. In describing the algorithms the level of logic is shown by indentations with the major sections being at the first level.

EZFIT MAIN PROGRAM

The EZFIT main program controls the calculations to be performed. Through the input of 22 control cards the various calculation options of Gauss-Newton, Marquart and linear regression can be selected. The control selects the input method for data points, selection of parameters to be used in the regression, and initial values of the parameters. The main program controls convergence and of the algorithms and checks time limits. Details of the various options of the control cards are given in the following section. The algorithm used is in the succeeding section.

Control Cards for EZFIT

Card Control Functions and Format

- 1 cc. 1-5; IOUT; Program code control selects various calculations performed as given below:
 - 1 Full regression, echo print of input data as received from data input routines, for each iteration a table of Y, Y_{calc}, and % error, regression summary statistics, output tables of calculated properties and correlation coefficients.
 - 3 The echo print is omitted from the features of type 1.
 - 4 Correlation coefficients is omitted.
 - 5 Full regression, regression summary statistics, output tables of calculations.
 - 8 Same as 9 but with table of correlation coefficients added.
 - 9 Calculation of statistics with no parameter update for regression summary statistics, output tables of calculations.
 - 10 No regression, output tables of results.
- 2 cc. 1-5; idata; Selection of data input routines as:
 - 1 DATA; Compound cards, then preBANKED data.
 - 2 DATA2; Blocked, BWR original data format.
 - 3 DATA3; Blocked form of data in BANKED format.
- 3 cc. 1-10; DFLMDA: Selection of regression method as:
 - .001 Marquart
 - 0.00 Gauss-Newton
 - <0 Linear regression
- 4 cc. 1-10; TMAS; Maximum time allowed for regression without the time for calculation of the output tables. It is used to end the regression nearly when convergence is not possible in the time allotted for the job.
- 5 cc. 1-5; ISTATE(3); Parameter constraint mode for allowance of sign change as:
 - 0 Unconstrained
 - 1 Constrained against sign changes
- cc. 6-10; ISTATE(5); Selection of derivative calculation mode:
 - 0 Numeric derivative with precision test
 - 1 Numeric derivative with delta of .01 of parameter.

- 6 cc. 1-5; ISTATE(4); Selection of error message mode:
 0 Full messages
 5 Minimum of error messages
- 7 cc. 1-5; NUMB; Dummy passed to calculation routines for
 their use.
- 8 cc. 1-5; NFPARM; Number of parameters not entering to
 regression but passed to the calculation routines.
 cc. 6-10; FPARM; Initial number of parameters to be fitted
 in a series of regressions.
- 9 cc. 1-5; NNTERM; dummy
- 10 cc. 1-5; NULFR; Initial number of parameters to be fitted
 in a series of regressions.
 cc. 6-10; NULTO; Final number of parameters to be fitted.
- 11- 16I5; ITERM(40); Parameter numbers in order to be fitted.
 13 As standard 40 may be supplied but no more than
 30 can be fitted.
- 14- 8F10.0; A1(40); Initial values of parameters in ascending
 18 order form parameter 1.
- 19 cc. 1-5; NCODE; Weighting mode selected as
 1 Weights supplied by data input routine.
 0 Equal weights
 -1 Weight as $1/y_{exp}$
- 20 cc. 1-10; RGAS; Universal gas constant used to select
 equation units.
- 21 cc. 1-5; N; Maximum number of independent variables per
 data point. (not used in module GOINE as
 restricted to 3 variables).
- 22 cc. 1-5; NPTS; Number of data points.
- 23 Control cards as specified by the selected data
 input routine

COMPOUND CODE CARD

Short Form

- 1 cc. 1-8; Eight character acronym for compound.
 cc. 9-10; Two digit compound code.
 cc. 11-20; TCRIT; critical temperature in Rankine.
 cc. 21-20; PCRTIT; critical pressure in psia.
 cc. 31-40; RHOC; critical density in lbmole/ft³.
 cc. 41-50; XMW; molecular weight.
 cc. 51-60; W; Pitzer acentric factor.
 cc. 61-70; ALPHA; reduced temperature scaling factor.
 cc. 71-80; BETA; reduced density scaling factor.

Common Block Definitions

Common Block PRM

Common/PRM/RGAS, RENRGY, TCRIT, PCRIT, RHOC, W, ALPHA, BETA, XMW,
1 A(40), B(7), NTERMS, NPARM, NUMB, RTOP, RMIDL, RMIDV

Common block, PRM, properties management, contains the control variables, scaling parameters, and other things needed by the physical properties package. It contains the parameters for the equation of state. The variables and their usage are:

RGAS	The universal gas constant used to determine the pressure units used by the system.
RENRGY	The universal gas constant used to determine the energy units used by the system.
TCRIT	The critical temperature in consistent absolute units.
PCRIT	The critical pressure in consistent units.
RHOC	The critical density in consistent units.
W	Pitzer acentric factor.
ALPHA	Reduced temperature scaling parameter, $T^* = \text{ALPHA} * T / \text{TCRIT}$
BETA	Reduced density scaling parameter, $\text{RHO}^* = \text{BETA} * \text{RHO} / \text{RHOC}$
XMW	The molecular weight.
A(40)	Parameters for the equation of state.
B(7)	Parameters for the ideal gas function.
NTERMS	Used by some equations; defined as parameters fitted minus NNTERM, see control variable definitions.
NPARM	The number of parameters in the equation of state.

NUMB	Used in do-loop control in some equations.
RTOP	The maximum liquid density allowed in DENSL.
RMIDL	The minimum liquid density allowed in DENSL.
RMIDV	The maximum vapor density allowed in DENSX.

Algorithm for MAIN Program

1. Initialization
 1. Set CPU clock
 2. Zero ICOMP, ISTATE
2. Data Input
 1. Input control variables: IOUT, IDATA, DFLAMDA, EPS, TMAX, ISTATE(3,4&5), NUMB, NFPARM, FPARM, NTERM, NUIFR, NUITO, ITERM, A1, NCODE, RGAS, N, NPTS
 2. Print summary of program status
 3. Input data points
 1. If IDATA=1, Call DATA
 2. If IDATA=2, Call DATA2
 3. If IDATA=3, Call DATA3
 4. Echo data points if desired.
If IOUT<3, Print DATAID and X
3. Initialize regression: IPRES=0, NPART=1, CHI=1
4. Do series of regressions

For NUL=NUIFR to NUITO

 1. Initialize;

NTERMS=NUL-NNTERM
 NPARM=NUL+NFPARM
 DF=NPTS-NUL
 CHI=10⁶⁰
 2. Store parameters; STORE(LL)=A1(LL)
 3. Check for output only
 1. If IOUT<10 Go to 4,4
 2. Move parameters to COMMON; A=A1₁₌₄₀, AXTN=A1₄₁₋₁₀₀
 3. Go to 1110
 4. Initialize for regression
 1. FLAMDA=DFLAMDA
 2. STORE(1)=CHI
 3. STORE(1+L)=A1(L)

5. Perform regression iterations
 - For I=1 to 20
 1. Do one iteration; Call CURFIT
 2. Calculate and output relative change in parameters;
 $STORED(L) = (STORED(L+1) - A1(L)) / A1(L)$
 3. Calculate and output length of change as
 $SSQ = \sum (STORED(L+1) - A1(L))^2$
 4. If first iterations store variances; $STORE(1+NPARM+L) = SIGMAA(L)$
 5. Evaluate results of iteration
 1. If chi-squared increased, $CHI < CHISQR$, Print message and go to 4.6.
 2. If change less than EPS, Print convergence message and go to 7.6.
 3. If no improvement on initial values of parameters, i.e. $FLAMDA > 100$ and $CHI > 10^{50}$, Print message and go to 8.
 4. Output results at valid improvement
 1. Print new parameters A1, new chi-squared CHI, and variances SIGMAA(1),
 2. Store new parameters and variances;
 $STORE(1) = CHI$, $STORE(1+L) = A1(L)$,
 $STORE(1+NPARM+L) = SIGMAA(L)$
 5. Check for exceeding time limit,
 1. Call CPUTIM(TIME,ST2) and print elapsed time, ST2.
 2. If no regression to be made, $ISTATE(2) > 5$, print message and go to 4.6.
 3. If time limits exceeded print message and go to 4.6.
6. Output results
 1. Retrieve parameters and variances from STORE.
 2. Output tabled parameter index, ITERM(J), parameter, A1, standard error, $SE = \sqrt{SIGMAA * CHISQR}$, variance, SIGMAA, and contributions to chi-squared, $ASE = (A1/SE)^2$.

3. Print statistics: CHISQR,chi-squared;
DF,degrees of freedom; FR, F-statistic
for correlation, FCH1, F-statistic for adding
term to regression.
4. Store unreduced chi-squared for next
FCH1, CH11=CHIN
5. Output results for points; call OUTPUT
5. Stop program with regression series complete.

Common Block DAT

```
COMMON/DAT/IPRES,ISTATE(20)
```

Common block DAT, control data, contains status and control variables for both the curvefitting and physical properties package. The variables and their usage are:

IPRES	The number of times the pressure routine, PRES, has been called.
ISTATE(1)	Number of the data point being evaluated.
ISTATE(2)	Calculation mode control.
ISTATE(3)	Parameter constraint control.
ISTATE(4)	Error message control.
ISTATE(5)	Derivative precision control.
ISTATE(6)	Program control bits.
ISTATE(7)	Program status bits.
ISTATE(8)	Subroutine status bits.
ISTATE(9)	Derivative status indicator.
ISTATE(10-20)	are not presently used.

Common Block PRP

```
COMMON/PRP/ICOMP(20),CPC(20),CRC(20),CMW(20),CW(20),CTC(20),  
1  CA(20),CB(20),CNAME(20,2)
```

Common block PRP, properties package, contains identification codes, names, and physical properties for twenty substances used by the calculation routines. The variables and their usage are:

ICOMP(20)	The BANKED compound identification code.
CPC(20)	The critical pressure for the compound in consistent units.
CRC(20)	The critical density in consistent units.
CMW(20)	The molecular weight.
CW(20)	The Pitzer acentric factor.
CTC(20)	The critical temperature in consistent units.
CA(20)	The reduced temperature scaling parameter.
CB(20)	The reduced density scaling parameter.
CNAME(20,2)	An eight character compound acronym.

Documentation of Subroutines

Subroutine CONVR

1. Hierarchy: Called by: DATA
Calls: -

2. Functional Description:

This subroutine converts a positive integer INUM, less than 9999 into its EBCDIC representation and returns it in a real, CHAR, and an integer, ICHAR, variable.

3. Variables:

- a. Input:

1. Argument: INUM,

- b. Output:

1. Arguments: ICHAR, CHAR.

- c. Intermediate:

1. IFACT power of 256 place keeper.
2. I10 working variable.
3. I, working variable.
4. J, do-loop parameter.
5. IDUM, DUM equivalenced variable for changing type specification.

4. Algorithm:

1. Initialize: ICHAR = 0, IFACT = 1,
2. Transfer number to working area, I = INUM
3. For J = 1 to 4
 1. Isolate character, multiply by place value and add to character variable:
I10 = I/10
ICHAR = (I-I10*10+240)*IFACT+ICHAR
 2. Prepare for next digit:
I = I10

3. Prepare next place value: $IFACT = IFACT * 256.$
4. Move bit pattern to real variable:
 1. $IDUM = ICHAR$
 2. $CHAR = DUM$

Subroutine CP

1. Hierarchy: Called By: FUNCN
Calls: ENTH

2. Functional Description:

This subroutine calculates the specific heat at constant pressure C_p by numerical derivative of the enthalpy as

$$C_p = (\partial H / \partial T)_p$$

The method of finite differences is used with the interval adjusted to obtain the precision desired by an internal testing algorithm.

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

- b. Output:

1. CP, the calculated specific heat.

- c. Intermediate:

1. The same as FDERIV.

4. Algorithm:

The algorithm is the same as that used in FDERIV with the appearances of FUNCN replaced by ENTH.

Subroutine CV

1. Hierarchy: Called By: FUNCN
Calls: U

2. Functional Description:

This subroutine calculates the specific heat at constant volume, C_v , by numerical derivative of the internal energy as

$$C_v = (\partial U / \partial T)_v$$

The method of finite differences is used with the interval adjusted to obtain the precision desired by an internal testing algorithm.

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

- b. Output:

1. CV, the calculated specific heat.

- c. Intermediate:

1. The same as FDERIV.

4. Algorithm:

The algorithm is the same as that used in FDERIV with the appearances of FUNCN replaced by U.

Subroutine DATA

1. Hierarchy: Called By: MAIN
Calls: -

2. Functional Description:

This subroutine inputs data in pre-BANKED format, generates weights, mean and variance. It may be custom programmed to fit the users needs.

3. Variables:

a. Input:

1. Arguments:

N, number of independent variables.
NPTS, number of data points to be read.
NCODE, code for weighting method

2. Card Input:

Card 1; NCOMP, number of components.
Card 2-NCOMP+1; NCOMP physical properties cards
BANKED short form: CNAME, IWHOLE, CTC,
CPC, CRC, CMW, CW, CA, CB
Cards NCOMP+2-; NPTS cards in pre-BANKED format.
CONTROL, T,P,Y,DATAID(2X,4F10.0,26X,3A4)

b. Output:

1. Arguments:

X, array of independent variables for data points
Y, dependent variables for data points
WEIGHT, weights for data points
YBAR, mean of Y's
YVAR, variance of Y's
NPTRHO, number of density data points
NPTRH, number of enthalpy departure data points
NPTRVP, number of vapor pressure points
DATAID, array of data identifications for points

2. COMMON/PRP/ICOMP(20), . . . CNAME(20,2)

c. Intermediate

1. I,J,L, do-loop parameters

2. SUM, accumulator for weighted mean

3. SUMW, sum of the weights

- 4. SUMY, accumulator for the variances
- 5. IFRACT, fraction portion of control variable

4. Algorithm:

1. Initialize counters to 0; NPTRHO, NPTH, NPTVP=0
2. Input and echo print NCOMP
3. Input physical property cards;
For L=1 to NCOMP;
 1. Read the Lth CNAME, ICOMP, CTC, CPC, CRC, CMW, CW,
 CA, CB
4. Input data cards;
For I=1 to NPTS
5.
 1. Read the Ith X's, Y, and DATAID
 2. Prepare weight; WEIGHT(I)=Y(I)
 3. Separate control variables;
IWHOLE= $|X(I,1)| + .005$
IFRACT= $|X(I,1) - IWHOLE + .005| * 100$
 4. Calculate subtotal for data types;
If IFRACT=0, NPTRHO=NPTRHO+1
If IFRACT=10, NPTH=NPTH+1
If IFRACT=20, NPTVP=NPTVP+1
6. Initialize accumulators for mean and variance;
SUM=0, SUMW=0
7. For I=1 to NPTS
 1. Evaluate weights;
 1. If NCODE<0, and Y≠0, WEIGHT(I)=1/|Y(I)|
 2. If NCODE<0, and Y(I)=0, WEIGHT(I)=1
 3. If NCODE=0, WEIGHT(I)=1
 4. If NCODE>0, WEIGHT(I)=1/WEIGHT(I)**2
 2. Accumulate sum of weights and weighted Y's;
SUM=SUM+WEIGHT(I)*Y(I)
SUMW=SUMW+WEIGHT(I)

8. Calculate weighted mean;
SUM=SUM/SUMW; YBAR=SUM
9. Calculate weighted variance;
 1. Initialize accumulator; SUMY=0
 2. For I=1 to NPTS,
SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2
 3. YVAR=SUMY*NPTS/(SUMW*(NPTS-1))

Subroutine DATA2

1. Hierarchy: Called By: MAIN
Calls: CONVR

2. Functional Description:

This subroutine inputs data in the pre-BANKED and original Han format, generates weights, data point identification, and means and variance. It may be custom programmed to fit the users needs.

3. Variables:

a. Input:

1. Arguments:

N, number of independent variables.
NPTS, number of data points to be read
NCODE, code for weighting method

2. Card input

Card 1; NCOMP number of data blocks
Card 2; Physical properties in BANKED short form
CNAME, IWHOLE, CTC, CPC, CRC, CMW, CW, CA, CB
Card 3; Data block control: NPTRHL- number of
density points, NPTRL- number of enthalpy
points, NPTVPL- number of vapor pressure
points, NPTA- total number of points pre-
BANKED format. SCALE- weight for group.
Card 4- a: NPTA cards in pre-BANKED format.
Control, T,P,Y,DATAID (2X,4F10.0,26X,3A4)
b: NPTRHL cards in Han density format
(T,P, ρ ,CODE-3F10.0,20X,I5)
c: NPTRL cards in Han enthalpy format
(T,P, ΔH ,CODE-3F10.0,20X,I5)
d: NPTVPL cards in Han vapor pressure
format (T,P-F5.0,F10.0)
Repeat from Card 2 NCOMP times.

b. Output:

1. Arguments:

X, array of independent variables for data points
Y, dependent variables for data points
WEIGHT, weights for data points
YBAR, mean of Y's.
YVAR, variance of Y's
NPTRHO, number of density data points
NPTRH, number of enthalpy departure data points
NPTRVP, number of vapor pressure points
DATAID, array of data identifications for points

2. COMMON/PRP/ICOMP(20) . . . CNAME(20,2)

c. Intermediate

1. COMMON/PRM/RHOC
2. I, do-loop and index parameter
3. J, L, JA, do-loop parameters
4. P, inputed pressure
5. T, inputed temperature
6. D1, D2, Characters for identification code
7. SUM, accumulator for weighted mean
8. CODE, inputed phase code
9. NPTL, number of points read in previous groups.
10. SUMW, sum of the weights
11. SUMY, accumulator for the variances
12. IFRACT, fraction portion of control variable
13. IWHOLE, whole portion of control variable

4. Algorithm

1. Initialize counters to 0; NPTL, NPTRHO, NPTH, NPTVP=0
2. Input and echo print NCOMP
3. Input blocks of data;
 - For L=1 to NCOMP
 1. Read Lth physical property card into
COMMON/PRP/
 2. Read number of each type of data; NPTRHL,
NPTH, NPTVPL, NPTA, SCALE
 3. Calculate group weight;
If SCALE=0, SCALE=1.
SCALE=SQRT(SCALE)
 4. Read in any data in pre-BANKED form;
 1. If NPTA=0 go to 3.5
 2. For JA=1 to NPTA
 1. Read Ith data point; I=JA+NPTL
 2. Calculate WEIGHT=Y/SCALE

3. Calculate subtotal for data types;
 $IWHOLE = |X(I,1)| + .005$
 $IFRACT = |X(I,1) - IWHOLE + .005| * 100$
 If $IFRACT = 0$ $NPTRHO = NPTRHO + 1$
 If $IFRACT = 10$, $NPTH = NPTVP + 1$
 If $IFRACT = 20$, $NPTVP = NPTVP + 1$
3. Update index offset; $NPTL = NPTL + NPTA$
5. Read in any density data;
 1. If $NPTRHL = 0$, go to 3.6
 2. For $J = 1$ to $NPTRHL$
 1. Read the Ith data point; $I = J + NPTL$
 $DATAID(I,1) = D1$, $DATAID(I,2) = D2$
 2. Convert to pre-BANKED form;
 $T = T + 460$, $CODE = -1$
 If $RHO < RHOC$, $CODE = 1$
 If $CODE < 0$ $X(I,1) = -IWHOLE$
 If $CODE < 0$, $X(I,1) = IWHOLE$
 $X(I,3) = P$, $X(I,2) = T$, $Y(I) = RHO$
 3. Prepare weight; $WEIGHT = Y(I) / SCALE$
 3. Update counters;
 $NPTRHO = NPTL + NPTRHL$
6. Read in any enthalpy departure data;
 1. If $NPTHL = 0$, go to 3.7
 2. For $J = 1$ to $NPTHL$
 1. Read the Ith data point; $I = J + NPTL$
 $DATAID(I,1) = D1$, $DATAID(I,2) = D2$
 2. Convert to pre-BANKED form;
 $T = T + 460$,
 If $CODE < 0$, $X(I,1) = -(IWHOLE + .10)$
 If $CODE > 0$, $X(I,1) = IWHOLE + .10$
 $X(I,2) = T$, $X(I,3) = P$, $Y(I) = DELH$
 3. Prepare weight; $WEIGHT = Y(I) / SCALE$
 3. Update counters;
 $NPTH = NPTH + NPTHL$
 $NPTL = NPTL + NPTHL$
7. Read in any vapor pressure data;
 1. If $NPTVPL = 0$, go to 3.8
 2. For $J = 1$ to $NPTVPL$
 1. Read the Ith data point; $I = J + NPTL$
 $DATAID(I,1) = D1$, $DATAID(I,2) = D2$
 2. Convert to pre-BANKED form;
 $T = T + 460$; $X(I,1) = IWHOLE + .2$; $X(I,2) = T$;
 $X(I,3) = P$; $Y(I) = P$

3. Prepare weight; $WEIGHT=Y(I)/SCALE$
3. Update counters;
 $NPTVP=NPTVP+NPTVPL$
 $NPTV=NPTL+NPTVPL$
8. Continue read loop
4. Initialize accumulators for mean and variance;
 $SUM=Q$, $SUMW=Q$
5. For $I=1$ to $NPTS$
 1. Make character id number for data in Han's format;
 If $DATAID(I,1)=D1$ and $DATA(I,2)=D2$, Call
 $CONVR(I,ICAR,DATAID(I,3))$
 2. Evaluate weights;
 1. If $NCODE<0$, and $Y(I)\neq 0$, $WEIGHT(I)=1/|Y(I)|$
 2. If $NCODE<0$, and $Y(I)=0$, $WEIGHT(I)=1$.
 3. If $NCODE=0$, $WEIGHT(I)=1$
 4. If $NCODE>0$, $WEIGHT(I)=1/WEIGHT(I)**2$
 3. Accumulate sum of weights and weighted Y's;
 $SUM=SUM+WEIGHT(I)*Y(I)$
 $SUMW=SUMW+WEIGHT(I)$
6. Calculate weighted mean;
 $SUM=SUM/SUMW$; $YBAR=SUM$
7. Calculate weighted variance;
 1. Initialize accumulator; $SUMY=0$
 2. For $I=1$ to $NPTS$,
 $SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2$
 3. $YVAR=SUMY*NPTS/(SUMW*(NPTS-1))$

Subroutine DATA3

1. Hierarchy: Called By: MAIN

2. Functional Description:

This subroutine inputs data in the BANKED format in blocks with individual group weights from the specified input unit. It generates individual point weights, and the mean and variance for the data set.

3. Variables:

a. Input:

1. Arguments:

N, number of independent variables.
 NPTS, number of data points to be read
 NCODE, code for weighting method
 ND, dimension for DATAID, ND=3

2. Card input:

Card 1; NBLKS, number of data blocks
 Card 2; Physical properties in BANKED short form,
 CNAME,IWHOLE,CTC,CPC,CRC,CMW,CW,CA,CB
 Card 3; Data block control:
 IFILE, unit number from which data is read
 NPTA, number of points in data block
 SCALE, weight for group
 Card 4-; Data cards in BANKED format, X, Y, ICONT,
 DATAID
 Repeat from Card 2 to Card 4 NBLKS times.

b. Output:

1. Arguments

X, array of independent variables for data points
 Y, dependent variables for data points
 WEIGHT, weights for data points
 YBAR, mean of Y's
 YVAR, variance of Y's
 DATAID, array of data identifications for points

2. COMMON/PRP/ICOMP(20), . . . CNAME(20,2)

c. Intermediate:

1. I,JBLK,J,K,JJ,JL,JS,JJJ, do-loop parameters

2. NPTL, number of points read in previous groups.

3. SUM, accumulator for weighted mean
4. SUMW, accumulator for the weights
5. SUMY, accumulator for the variances

4. Algorithm:

1. Initialize counters and control;
NPTL=0, ICOMP(1)=0, L=1
2. Input NBLKS
3. Input blocks of data:
 - For JBLK=1 to NBLKS
 1. Read the Lth CNAME,IWHOLE,CTC,CPC,CRC,CMW,CW,CA,CB
 2. Check if properties for compound have already been read:
 1. L1=L-1
 3. For JL=1 to L1
 1. Check if IWHOLE is already present
If ICOMP(JL)=IWHOLE go to 4.4
 4. IWHOLE is not present so include in PRP
 1. ICOMP(L)=IWHOLE
L=L+1
 5. Check to see if there is free space in PRP
If L>20, print no more room.
ICOMP(L)=0
4. Read data control card; IFILE, NPTA, SCALE
5. Prepare group weights; IWT=0
 1. If SCALE>0, go to 3.4.1.2
 1. Else, Set code for equal weights for points in group;
IWT=1,
SCALE= |SCALE|
 2. If SCALE=0, SCALE=1
 3. SCALE=1/SCALE
6. Input cards in BANKED format
For L=1 to NPTA
 1. Set storage index; I=NPTL+L
 2. Read lead card from unit IFILE, if end of file go to 5; X(I,1),X(I,2),X(I,3),Y(I),ICONT,DATAID

3. Prepare to read following card for point;
 $JL=3$,
 If $ICONT=0$, go to 3.5.5, no more cards.
4. Read rest of cards for point:
 For $JJ=1$ to $ICONT$
 1. Set indices for X's;
 $JS=JL+1$
 $JL=JS+5$
 If $JL>N$, $JL=N$
 2. Read $X(I,JS)$ to $X(I,JL)$ from unit IFILE.
5. Check for all X's filled as read:
 1. If $JL=N$, go to 3.5.6
 2. Fill $X(I,JL+1)$ to $X(I,N)$ with 0.
6. Prepare weight for point:
 1. $WEIGHT(I)=1$
 2. If $Y(I) \neq 0$, $WEIGHT(I)$
 3. $WEIGHT(I)=WEIGHT(I)/SCALE$
 4. If $IWT=1$, $WEIGHT(I)=1/SCALE$
7. Update offset for indices;
 $NPTL=NPTL+NPTA$
5. Update Number of points, $NPTS=NPTL$, and go to 6.
6. Print end of file error message and stop.
7. Initialize accumulators for mean and variance:
 $SUM=0$, $SUMW=0$
8. For $I=1$ to $NPTS$
 1. Evaluate weights;
 1. If $NCODE<0$, and $Y \neq 0$, $WEIGHT(I)=1/|Y(I)|$
 2. If $NCODE<0$, and $Y(I)=0$, $WEIGHT(I)=1$
 3. If $NCODE=0$, $WEIGHT(I)=1$
 4. If $NCODE>0$, $WEIGHT(I)=1/WEIGHT(I)**2$
 2. Accumulate sum of weights and weighted Y's;
 $SUM=SUM+WEIGHT(I)*Y(I)$
 $SUMW=SUMW+WEIGHT(I)$
9. Calculate weighted mean;
 $SUM=SUM/SUMW$; $YBAR=SUM$
10. Calculate weighted variance:
 1. Initialize accumulator; $SUMY=0$
 2. For $I=1$ to $NPTS$;
 $SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2$
 3. $YVAR=SUMY*NPTS/(SUMW*(NPTS-1))$

Subroutine DENSL

1. Hierarchy: Called By: FUNCN, FLASHP
Calls: PRES

2. Functional Description:

This subroutine finds the density root of equations of state in the region between the critical density and four times it, i.e. the liquid density. It does this by a combined method of false position and successive bisections. It uses the ideal gas value as the initial approximation and has several safe guards to secure the selection of the correct root.

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature
P, pressure

2. COMMON/PRM/RGAS, TCRIT, RMIDL, RTOP

3. COMMON/DAT/ISTATE(4), ISTATE(9)

- b. Output:

1. Argument:

DENSL, liquid density root

- c. Intermediate:

1. IT, ITMAX, iteration parameters

2. PQ, local storage for P

3. P1, P2, P3, intermediate pressures used in the search

4. DEL, search interval

5. CODE, status variable

6. EPSP, tolerance in pressure, 10^{-5}

7. EPSR, tolerance in density, 10^{-5}

8. PMIN, minimum pressure in secondary search.

9. RHOMIN, density corresponding to PMIN
10. RHO1, RHO2, RHO3, intermediate densities used in search.
11. SRHO, SP, results of previous calculation used for start when called from FDERIV

4. Algorithm:

a. Basis;

The density is found by a false position search. If this fails by not meeting convergence criteria or the root having a negative derivative, a search from RTOP is made down to RMIDL by step DEL until the root is bounded. When it is bounded successive bisection is performed until the convergence criteria are satisfied. If the root was unable to be bounded the density corresponding to the minimum pressure is used. If the routine is called from FDERIV the results from the previous calculation are used for the initial locations saving some time in that they were for the same T and P conditions.

b. Procedure:

1. Initialize:
ITMAX=20, set maximum iterations for false position
PO=P, move P to local storage
PMIN=10⁶⁰, initialize minimum search pressure.
CODE=0, initialize minimum search pointer.
DEL=RTOP/20, delta as twentieth of top bound
IT=1, start counter
2. Check if T is so small that false position will be skipped
If T/TCRIT<.4 go to 7
3. Check if in derivative routine and if so use last result to start;
If ISTATE(9)≠0, RHO1=RHO2
4. Set up initial values for false position;
RHO2=1.01*RHO1
P1=PRES(T,RHO1)-PO
P2=PRES(T,RHO2)-PO

5. Start false position iteration:
 1. Check for convergence;
 If $|P1-P2| < EPSP \cdot PO$ or $|RHO1-RHO2| < |RHO2| \cdot EPSR$
 go to 6
 2. Check if exceeded
 2. Check if exceeded 20 iterations;
 If $IT > ITMAX$, go to 7
 3. Project by false position;
 $RHO3 = (RHO1 \cdot P2 - RHO2 \cdot P1) / (P2 - P1)$
 4. If $RHO3$ is out of bounds randomize start
 1. If $RHO3 > RTOP$ or $RHO3 < RMIDL$, $RHO3 = RTOP \cdot (50 + IT) / 50$
 2. Select pair with positive slope to continue
 1. If $RHO1 < RHO2$ and $P1 > P2$ go to 5.5
 2. Make start:
 $RHO2 = RHO1$
 $RHO1 = RHO3$
 $P2 = P1$
 $IT = IT + 1$
 $P1 = PRES(T, RHO1) - PO$
 go to 5.1
 5. Update for next iteration
 $RHO1 = RHO2$
 $RHO2 = RHO3$
 $P1 = P2$
 $P2 = PRES(T, RHO2) - PO$
 6. Go to 5.1
6. Check for positive slope for correct root;
 $RHO1 = .99 \cdot RHO2$
 $P1 = PRES(T, RHO1) - PO$
 If $RHO2 < RMIDL$ it is out of range, go to 7
 If $P1 < P2$, go to 11.
7. Initialize for search to bound root;
 $ITMAX = 40$
 $RHO1 = RTOP$
 $P1 = PRES(T, RHO1)$
8. Check for root outside top bound;
 1. If $P1 > PO$, go to 9
 2. Check if error messages desired;
 If $ISTATE(4) = 5$, print Root too large.
 3. Select root as bound;
 $RHO2 = RHO1$

4. If not in FDERIV return;
If ISTATE(9)=0, go to 11
5. Modify bound root so that derivative will have correct sign;
 1. $P1 = PRES(T, RHO2)$
 2. If $P1 < PS$, go to 8.5.3
 1. Else, $RHO2 = RHO2 - DEL$, go to 11.
 3. $RHO2 = RHO2 + DEL$, go to 11.
9. Begin search for bound;
 1. $P1 = PRES(T, RHO1)$
 2. Check for bounded root;
If $P1 < P0$, go to 10
 3. Check for first minimum;
If $P2 < PMIN$ and $CODE = 0$, go to 9.8
 4. First minimum found; $CODE = 1$
 5. Update iteration values;
 $RHO2 = RHO1$
 $P2 = P1$
 6. Check for reaching left bound;
If $RHO1 < RMIDL$ go to 9.9
 7. Continue search;
 $RHO1 = RHO1 - DEL$
Go to 9.1
 8. Update minimum with lower values;
 $PMIN = P1$
 $RHOMIN = RHO1$
Go to 9.5
 9. Since out of bounds use minimum;
 1. Check if error messages desired;
If $ISTATE(4) < 5$, print minimum used
 2. $RHO2 = RHOMIN$
 3. Go to 11.
10. Begin successive bisections
 1. Calculate values at interval center;
 $RHO3 = (RHO1 + RHO2) / 2$
 $P3 = PRES(T, RHO3)$

2. Check for convergence;
If $|P1-P2| < EPSP*P0$ or $|RHO1-RHO2| < |RHO2|*EPSR$,
go to 11.
3. Check number of iterations;
IT=IT+1
If IT>ITMAX, go to 10.5
4. Find interval containing root;
 1. If $P3 > P0$, go to 10.4.3
 2. Between top and middle;
RHO1=RHO3
P1=P3
Go to 10.1
 3. Between bottom and middle;
RHO2=RHO3
P2=P3
Go to 10.1
5. Search failed;
 1. Check if error messages desired;
If ISTATE(4)<5, Print, L density
did not converge.
11. Prepare to leave;
 1. Transfer result; DENSL=RHO2
 2. If ISTATE(9)=1, return
 3. Not in derivative so store result;
SRHO=DENSL
SP=PRES(T,SRHO)
Return

Subroutine DENS_V

1. Hierarchy: Called By: FUNCN, FLASHP
Calls: PRES

2. Functional Description:

This subroutine finds the density root of equations of state in the region between zero and the critical density, i.e. the vapor density. It does this by a combined method of false position and successive bisections. It uses the ideal gas value as the initial approximation and has several safeguards to secure the selection of the correct root.

3. Variables:

a. Input:

1. Arguments:

T, absolute temperature
P, pressure

2. COMMON/PRM/RGAS, RMIDV, TCRIT

3. COMMON/DAT/ISTATE(9), ISTATE(4)

b. Output:

1. Argument:

DENS_V, gas density root

c. Intermediate:

1. IT, ITMAX iteration parameters

2. PO, local storage for P

3. P1, P2, P3, intermediate pressures used in the search.

4. DEL, search interval

5. CODE, status variable

6. EPSP, tolerance in pressure, 10^{-5}

7. EPSR, tolerance in density, 10^{-5}

8. PMAX, maximum pressure in secondary search.

9. RHOMAX, DENSITY corresponding to PMAX.

10. RHO1, RHO2, RHO3, intermediate densities used in search.

4. Algorithm;

a. Basis;

The density is found by a false position search. If this fails by not meeting convergence criteria or the root having a negative derivative, a search from $P/2RT$ is made up to $RMIDV$ by step DEL until the root is bounded. When it is bounded successive bisection is performed until the convergence criteria are satisfied. If the root was unable to be bounded the density corresponding to the maximum pressure is used.

b. Procedure;

1. Initialize
 $ITMAX=20$, set maximum iterations for false position
 $PO=P$, move X to local storage
 $DEL=PO/RGAS/T/10$, delta as a tenth ideal gas density
 $RHO1=.5*PO/RGAS/10$, first density as half ideal gas
 $IT=1$, start counter
2. Check if T is so small that false position will likely fail
 If $T/TCRIT < .4$, go to 7
3. Check if in derivative routine and if so use last result to start:
 If $ISTATE(9) \neq 0$, $RHO1=RHO2$
4. Set up initial values for false position;
 $RHO2+.8*RHO1-L$
 $P1=PRES(T, RHO1)-PO$
 $P2=PRES(T, RHO2)-PO$
5. Start false position iteration;
 1. Check for convergence;
 If $|P1-P2|KEPS*PO$ or $|RHO1-RHO2| < |RHO2|*EPSR$
 go to 6
 2. Check if exceeded 20 iterations;
 If $IT > ITMAX$ go to 7
 3. Project by false position;
 $RHO3=(RHO1*P2-RHO2*P1)/(P2-P1)$
 4. If $RHO3$ is out of bounds randomize start
 If $RHO3 > RMIDV$ or $RHO3 < 0$, $RHO3=(1-IT/50)*PO/(RGAS*T)$
 5. Update for next iteration;
 $RHO1=RHO2$
 $RHO2=RHO3$
 $P1=P2$
 $P2=PRES(T, RHO2)-PO$
 $IT=IT+1$

6. Go to 5.1
6. Check for positive slope for correct root;
 $RHO1 = .99 * RHO2$
 $P1 = PRES(T, RHO1) - P0$
 If $RHO2 < RMIDV$, it is out of range, go to 7
 If $P1 < P2$ go to 11,
7. Initialize for search to bound root;
 $ITMAX = RMIDV / DEL + 5$, set limit as 5 steps past $RMIDV$
 $IT = 0$
 Convert differences from $P0$ into pressures;
 $P1 = P1 + P0$
 $P2 = P2 + P0$
 $RHO1 = DEL$
8. Begin search to bound root;
 1. $P1 = PRES(T, RHO1)$
 2. Check to be sure $P1$ is below $P0$, i.e. on the left;
 1. If $P1 < P0$, go to 8.3
 2. Else, not bound on left;
 1. Check if error messages desired;
 If $ISTATE(4) < 5$ Print error root too small
 2. $RHO2 = RHO1$
 3. Go to 11,
 3. Start search;
 $RHO2 = RHO1 + DEL$
 $PMAX = P1$
 $RHOMAX = RHO1$
 $CODE = 0.$, shows start of search
 4. $P2 = PRES(T, RHO2)$
 5. Check for bound;
 If $P2 > P0$, go to 9.
 6. Check for first maximum;
 If $P2 > PMAX$ and $CODE = 0$, go to 8.12
 7. First maximum found; $CODE = 1$
 8. Update iteration values;
 $IT = IT + 1$
 $RHO1 = RHO2$
 $P1 = P2$
 $RHO2 = RHO2 + DEL$

9. Test for end of iterations;
If $IT > ITMAX$, go to 8.11
 10. Continue search if not at bound;
If $RHO1 < RMIDV$, go to 8.4
 11. Since out of bounds use maximum;
 1. Check if error messages desired;
If $ISTATE(4) < 5$ print maximum used
 2. $RHO2 = RHOMAX$
 3. Go to 11.
 12. Iteration exceeded without finding bound;
 1. Check if error messages desired;
If $(ISTATE(4) < 5)$ print V root not found
 2. Go to 11.
 13. Update maximum with higher values;
 $PMAX = P2$
 $RHOMAX = RHO2$
 Go to 8.8
9. Root bounded so initialize for bisections;
 $IT = 0$
10. Begin successive bisections
1. Calculate values at interval center;
 $RHO3 = (RHO1 + RHO2) / 2$
 $P3 = PRES(T, RHO3)$
 2. Check for convergence;
 If $|P1 - P2| < EPSP * PO$ or $|RHO1 - RHO2| < |RHO2| * EPSR$
 Go to 10.5
 3. Check number of iterations;
 $IT = IT + 1$
 If $IT > ITMAX$, go to 10.6
 4. Find interval containing root;
 1. If $P3 > PO$, go to 10.4.3
 2. Between top and middle;
 $RHO1 = RHO3$
 $P1 = P3$
 Go to 10.1
 3. Between bottom and middle;
 $RHO2 = RHO3$
 $P2 = P3$
 Go to 10.1

5. Transfer middle solution root for result;
RHO2=RHO3
Go to 11.
6. Search failed;
 1. Check if error messages desired;
If ISTATE(4)<5, Print V density did not converge.
11. Return result;
DENSX=RHO2
Return

Subroutine CURFIT

1. Hierarchy: Called by MAIN
Calls: GJEL, FUNCN, MESSG, FDERIV, LBLEZ, FCHISQ

2. Functional Description:

This subroutine calculates one iteration in a regression by the method of Marquart or Gauss-Newton for non-linear functions. It generates the normal equations, obtains their solution and evaluates the solution. It also reduces to a standard linear regression in which repeated solution of the normal equations is used to reduce round-off error.

3. Variables:

a. Input:

1. Arguments:

X, Y, WEIGHT, N, NPTS, NTERMS, A, FLAMDA, ITERM

b. Output:

1. Arguments:

SIGMAA, YFIT, CHISQ1

2. COMMON/DAT/ISTATE(1), ISTATE(2), ISTATE(3)

c. Intermediate:

4. 1. I,J,K,L, Do-loop parameters.

2. DET, determinant from GJEL

3. IER, error code for the results of GEJEL

4. IBD, control code for calling LBLEZ

5. NPN, dimension of transfer vector to FUNCN

6. BETA, constant vector for normal equations

7. DELM, largest delta for parameters

8. JM, index corresponding to DELM

9. FACT, reducing factor for constrained parameters

10. PERC, percent error in calculating Y
11. SUM1, accumulator for percent errors
12. ALPHA, triangular matrix to accumulate the normal equations
13. ARRAY, scaled coefficient matrix for normal equations
14. DERIV, array of derivatives of Y with respect to the A's
15. NFREE, degrees of freedom
16. CHISQR, trial value of chi-squared

b. Algorithm:

1. Initialize:
 IC/5/Output counter
 IBD/0/, label control saying LBLEZ not called
2. Have LBLEZ called once;
 If IBD \neq 1, CALL LBLEZ, IBD=1
3. Initialize Percent accumulator, SUM1=0, and FACT=.99
4. Check to see if program dimensions are exceeded;
 If NTERMS>100, NTERMS=100, print only 100 fitted
5. Calculate transfer vector dimension; NPN=NPTS+NPARM
6. Check degrees of freedom;
 1. NFREE=NPTS-NTERMS
 2. If NFREE>0, go to 7.
 3. Else, stop calculations
 Print error degrees of freedom less than 1
 FLAMDA=1000
 CHISQR=10⁵⁵
 Go to 24
7. Evaluate alpha and beta matrices;
 1. Zero matrices;
 For J=1 to NTERMS
 1. BETA(J)=0
 2. For K=1 to J
 1. ALPHA(J,K)=0
 2. Put parameters into transfer vector;
 For L=1 to NPARM
 1. Z(L+N)=A(L)

- 3, Zero ARRAY
4. Accumulate terms by data point;
 - For I=1 to NPTS
 1. Put X's for point in Z's;
 - For L=1 to N, Z(L)=X(I,L)
 2. Identify and evaluate YFIT for point
 - ISTATE(1)=I
 - YFIT(I)=FUNCN(Z,NPN)
 3. Calculate and accumulate error;
 1. If Y(I)=0, go to 7.4.3.3
 2. PERC=100*(Y(I)-YFIT(I))/Y(I)
 3. SUM1=SUM1+|PERC|
 4. Check if result is to be printed;
 - If ISTATE(2)>4 go to 7.4.4
 5. If Gauss-Newton skip until 5th time;
 - If IC<5 and FLAMDA=0, go to 7.4.4
 6. Print Y,YFIT,PERC
4. Evaluate parameter derivatives;
 - For L=1 to NTERMS
 1. JJ=ITERM(L)+N, get index.
 2. DERIV(L)=FDERIV(Z,JJ,NPN), calculate derivative
 3. Accumulate derivatives for average
 - ARRAY(L)=ARRAY(L)+|DERIV(L)|
 4. Check for 0 derivative;
 - If |DERIV(L)|<10⁻³⁰, DERIV(L)=0
 5. Accumulate matrices;
 - For J=1 to NTERMS
 1. Check if Linear or Nonlinear
 1. Nonlinear; If FLAMDA≥0,
 - BETA(J)=BETA(J)+WEIGHT*(Y-YFIT)*DERIV(J)
 2. Linear; If FLAMDA<0,
 - BETA(J)=BETA(J)+WEIGHT*Y*DERIV(J)
 2. For K=1 to J
 1. ALPHA(J,K)=ALPHA(J,K)+WEIGHT*DERIV(J)*DERIV(K)

5. Print average percent error;
SUM1=SUM1/NPTS,PRINT,SUM1
8. Update print control;
IC=IC+1
If IC>5 IC=1
9. Evaluate and print CHISQ1 as FCHISQ
10. Calculate and print average absolute derivatives as
ARRAY(J)/NPTS
11. Form scaled augmented matrix;
 1. DIAG=1
 2. Check for Marquart; If FLAMDA<0, DIAG=DIAG+FLAMDA
 3. For J=1 to NTERMS
 1. Check for invalid diagonals
1. If $\text{ALPHA}(J,J) \leq 0$, print error, $\text{ALPHA}(J,J)=10^{-40}$
 2. Calculate constant term;
 $\text{ARRAY}(\text{NTERMS}+1,J)=\text{BETA}(J) / \sqrt{\text{ALPHA}(J,J)}$
 3. Calculate coefficients;
For K=1 to J
 1. $\text{ARRAY}(K,J)=\text{ALPHA}(K,J) / \sqrt{\text{ALPHA}(J,J) * \text{ALPHA}(K,K)}$
 2. $\text{ARRAY}(J,K)=\text{ARRAY}(K,J)$
 4. $\text{ARRAY}(J,J)=\text{DIAG}$
12. Initialize search value for largest delta, DELM=0
13. Solve normal equations;
 1. Check for special case of one parameter;
If NTERMS>1, go to 13.3
 2. One term;
 1. $\text{ARRAY}(1)=1/\text{ARRAY}(1)$
 2. $\text{ARRAY}(2)=\text{ARRAY}(2)*\text{ARRAY}(1)$
 3. Go to 14.
 3. More than one term so call inversion routine, GJEL
14. Check if parameters are to be updated;
If ISTATE(2)=9, go to 20
If ISTATE(2)=8, go to 19

15. Calculate new parameters;
For J=1 to NTERMS
 1. Get index, JJ=ITERM(J)
 2. Check for largest parameter change;
 1. If $|\text{ARRAY}(\text{NTERMS}+1, J)| < \text{DELM}$, go to 15.3
 2. Else, save larger delta;
 $\text{DELM} = |\text{ARRAY}(\text{NTERMS}+1, J)|$
 3. Calculate new parameter as B_J
 1. $B(J) = A(JJ) + \text{ARRAY}(\text{NTERMS}+1, J) / \sqrt{\text{ALPHA}(J, J)}$
 2. Check is parameter is to be constrained;
If $\text{ISTATE}(3) = 0$ or $B(J) * A(JJ) > 0$, go to 15.3.4
 3. Else, constrain parameter against change in sign;
 1. Print message that parameter changed sign
 2. $B(J) = A(JJ) * (1 - \text{FACT})$
 4. Continue loop
16. Print largest delta and index, DELM, JM
17. Evaluate chi-squared at new parameters;
 1. Insert new parameters in transfer vector;
For L=1 to NTERMS
 1. JJ=ITERM(L)
 2. $Z(JJ+N) = B(L)$
 2. Evaluate YFIT;
For I=1 to NPTS
 1. Move X's to Z;
For L=1 to N; $Z(L) = X(I, L)$
 2. Evaluate point;
 1. $\text{ISTATE}(10) = I$
 2. $\text{YFIT}(I) = \text{FUNCN}(Z, \text{NPN})$
 3. $\text{CHISQR} = \text{FCHISQ}(\dots)$
 4. Output results;
Print IPRES, CHISQR

18. Optimize acceleration parameter FLAMDA for reduction in chi-square;
 1. If Gauss-Newton or linear selected skip optimization;
If $FLAMDA \leq 0$, go to 21
 2. If Chi-square decreased don't optimize;
If $(CHISQ1 - CHISQR) > 0$, go to 21
 3. Change FLAMDA
 $FLAMDA = 10 * FLAMDA$
 $FACT = FACT / 2$
 4. CHECK for top bound on FLAMDA
If $FLAMDA > 1000$, go to 23
 5. If FLAMDA is small save variances;
 1. If $FLAMDA > .01$, go to 11.
 2. Calculate variances in SIGMAA
For I=1 to NTERMS
 1. $SIGMAA(I) = ARRAY(I, I) / \sqrt{ALPHA(I, I)}$
 3. go to 11
19. Output correlation coefficients;
For I=1 to NTERMS;
 1. For J=1 to I
 1. Calculate row of correlation coefficients;
 $B(J) = ARRAY(I, J) / \sqrt{ARRAY(I) * ARRAY(J)}$
 2. Output row of coefficients; Print B, 1 to I
20. Calculate variances
 1. For J=1 to NTERMS
 1. $SIGMAA(J) = ARRAY(J, J) / \sqrt{ALPHA(J, J)}$
 2. $CHISQR = CHISQ1$
Return
21. Move parameters and variances for leaving;
 1. For J=1 to NTERMS
 1. Insert new parameters;
 $JJ = ITERM(J)$
 $A(JJ) = B(J)$

```

2. Check for invalid variances;
   If  $\text{ARRAY}(J,J) \leq 0$ ,  $\text{ARRAY}(J,J) = 10^{-30}$ ,
   Print variance is negative,

3. Calculate variance;
    $\text{SIGMAA}(J) = \text{ARRAY}(J,J) / \sqrt{\text{ALPHA}(J,J)}$ 

2. FLAMDA=FLAMDA/10

22. Output correlation coefficients;

1. Check is coefficient desired;
   If ISTATE(2) 4, go to 24

2. For I=1 to NTERMS;
   1. For J=1 to I
      1. Calculate row of correlation coefficients;
          $B(J) = \text{ARRAY}(I,J) / \sqrt{\text{ARRAY}(I) * \text{ARRAY}(J)}$ 
      2. Output row of coefficients; Print B, 1 to I
   3. go to 24

23. Evaluate at original parameters;

1. Insert parameters in transfer vector;
   For L=1 to NPARM;
   1.  $Z(L+N) = A(L)$ 

2. Evaluate YFIT;
   For I=1 to NPTS;
   1. Move X's to Z;
      For L=1 to N;  $Z(L) = X(I,L)$ 
   2. Evaluate point;
      1. ISTATE(1)=I
      2.  $\text{YFIT}(I) = \text{FUNCN}(Z, \text{NPN})$ 
      3.  $\text{CHISQR} = \text{CHISQ1}$ 

24. Return

```

Subroutine ENTH

1. Hierarchy: Called By: FUNCN, CP
Calls: PRES, FI2

2. Functional Description:

This subroutine calculates the enthalpy departure at the state condition specified by the arguments temperature and density. This value is calculated for an equation of state in EZFIT form as:

$$\Delta H = R_e T_c (-T^{*2} FI2 + T^* (Z-1))/\alpha$$

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

2. COMMON/PRM/RENRGY, TCRIT, RGAS, ALPHA

- b. Output:

1. ENTH, the calculated enthalpy departure

- c. Intermediate:

1. TSTAR, reduced temperature.

2. HDEV, reduced enthalpy departure

4. Algorithm:

1. Reduce temperature, TSTAR=ALPHA*T/TCRIT

2. Calculate reduced enthalpy departure;
HDEV=(TSTAR**2)*FI2(T,RHO)+TSTAR*(PRES(T,RHO)/(RGAS*T*RHO)-1)

3. Unreduce the departure;
ENTH=HDEV*RENRGY*TCRIT/ALPHA

Subroutine CHISQ

1. Hierarchy: Called By: CURFIT
Calls: -

2. Functional Description:

This subroutine calculates the reduced chi-squared used as the objective function in the nonlinear regression. The is the weighted sum of squares,

3. Variables:

a. Input:

1. Arguments:

Y, the experimental values for the data points
WEIGHT, the weights for each data point,
NPTS, number of data points
NFREE, the degrees of freedom
YFIT, the calculated values for the data points.

b. Output:

1. FCHISQ, the calculated reduced weighted sum of the squared errors, chi-squared.

c. Intermediate:

1. I, do-loop parameter.
2. CHISQ, accumulator for chi-squared,
3. FREE, real variable for degrees of freedom.

4. Algorithm:

a. Procedure:

1. Initialize accumulator to zero; CHISQ=0.
2. Check to be sure that the degrees of freedom are positive;
If NFREE \leq 0 FCHISQ=0 and return,
3. Calculate chi-squared;
For I=1 to NPTS
1. CHISQ=CHISQ + WEIGHT_i * (Y_i*YFIT_i)**2

Subroutine ENTRPY

1. Hierarchy: Called By: FUNCN
Calls: FI1, FI2

2. Functional Description:

This subroutine calculates the entropy departure at the state condition specified by the arguments temperature and density. This value is calculated for an equation of state in EZFIT form as

$$S = R_e (-\ln(\rho RT) - FI1 - T^* FI2)$$

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density,

2. COMMON/PRM/RENRGY, TCRIT, ALPHA

- b. Output:

1. ENTRPY, the calculated entropy departure.

- c. Intermediate:

1. TSTAR, reduced temperature.

4. Algorithm:

1. Reduce temperature;
TSTAR=ALPHA*T/TCRIT

2. Calculate the unreduced entropy departure;
ENTRPY=RENRGY*(-ln(RHO*RGAS*T)-FI1-TSTAR*FI2)

- 4, Reduce chi-squared;
 1. $FREE = NFREE$
 2. $FCHISQ = CHISQ / FREE$

Subroutine FDERIV

1. Hierarchy: Called By: CURFIT
Calls: FUNCN

2. Functional Description:

This subroutine calculates the numerical derivative for the i th variable in the function FUNCN by finite differences. The interval can optionally be adjusted to obtain the precision desired by an internal testing algorithm.

3. Variables:

a. Input:

1. Arguments:

X, array of independent variables
I, number of parameter in array of which the
derivative is taken
NDIM, number of independent variables

2. COMMON/DAT/ISTATE(5)

b. Output:

1. FDERIV, the calculated derivative
2. ISTATE(9), the state of FDERIV being active, •

c. Intermediate:

1. EPS, Minimum size for variable for which delta is
calculated as fraction of variable.
2. IT, do-loop parameter
3. N, Number of significant digits desired,
4. F1, FUNCN evaluated at X-delta
5. F2, FUNCN evaluated at X+delta
6. DEL, the delta used for the finite difference.
7. DFDX, trial finite difference derivative
8. SAVE, original value of the variable of which the
derivative is calculated.

4. Algorithm:

a. Basis:

A first order numerical derivative can be calculated by finite differences as

$$f' = \frac{f_1 - f_2}{\Delta x} = \frac{f_2(x + \Delta x/2) - f_1(x - \Delta x/2)}{\Delta x} \quad (1)$$

Let the two functions differ by Δb in the t^{th} least significant digit, then

$$f' = \frac{f_1 - f_2(1 \pm \Delta b \cdot 10^{-t})}{\Delta x} = f_1 \cdot (\pm \Delta b \cdot 10^{-t}) / \Delta x \quad (2)$$

where

$$0 < |\Delta b| \leq 1 \quad (3)$$

If t' is the number of significant digits the machine has and N is the number of significant digits desired in the derivative, then,

$$t = t' - N, \quad (4)$$

Therefore,

$$f' = f_1 / \Delta x (\pm \Delta b \cdot 10^{-(t' - N)}) \quad (5)$$

which gives the following inequality

$$|f'| \leq |f_1 / \Delta x| \cdot 10^{-t' + N} \quad (6)$$

For the condition that f' will have at least N digits, it then follows

$$|f'| > |f_1 / \Delta x| \cdot 10^{-t' + N} \quad (7)$$

In single precision $t'=6$ and for this work $N=3$. When the 7 inequality is not satisfied the delta is increased up to five times.

b. Procedure;

1. Initialize values; EPS=.01, N=3
2. Save x; SAVE=X(I) and indicate FDERIV is active;
ISTATE(9)=1.
3. Determine first delta;
If SAVE<EPS, DEL=EPS
Else DEL=|EPS*SAVE|.
4. For IT=1 to 3
 1. Calculate upper and lower functions and derivative;
 $f_2 = \text{FUNCN}(X_i + \text{DEL})$
 $f_1 = \text{FUNCN}(X_i - \text{DEL})$
 $\text{DFDX} = (f_2 - f_1) / 2\text{DEL}$
 2. If derivative precision is not required,
ISTATE(5)=1, indicate leaving FDERIV, and go to 6.
 3. Check for equal values;
If $|f_1 - f_2| < |f_1| 10^{-5}$, $f_2 = f_1$
 4. Check number of significant digits;
If $|f_1 - f_2| 10^{*(6-N)} > |f_1|$, go to 6.
 5. Determine new delta;
 $\text{ESP} = \text{ESP} * 10$
 IF $|\text{SAVE}| < 10^{-6}$, DEL=EPS
 Else DEL=|EPS*SAVE|
5. Check for 0 derivative;
If $|f_1 - f_2| < |f_1| 10^{-5}$, DFDX=0
6. Indicate leaving FDERIV;
 ISTATE(9)=0
 FDERIV=DFDX
 X_i=SAVE

Subroutine F11

1. Hierarchy: Called By: FUGCOF, ENTRPY
Calls: ~

2. Functional Description;

This subroutine calculates the integral of $\partial Z/\partial T \, d \ln \rho$ from 0 to ρ for the equation of state, for a given temperature and density. This is used to calculate entropy properties.

3. Variables:

a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

2. COMMON/PRM/RGAS,, . . . NUMB

b. Output:

1. F11; the value of the integral.

4. Algorithm:

The method is any that will calculate the integral

$$F11 = \int_0^{\rho} \partial Z / \partial T \, d \ln \rho$$

for a given equation of state. The scaling values for temperature and density and the physical properties of the substance are given in the common block. The parameters that will be fitted in the equation of state are in A of the common block,

Subroutine FI2

1. Hierarchy: Called By: ENTH, ENTRPY, U
Calls: -

2. Functional Description:

This subroutine calculates the integral of $(Z-1)/d \ln \rho$ from 0 to ρ for the equation of state. This is used to calculate energy properties. For a given temperature and density.

3. Variables:

a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

2. COMMON/PRM/RGAS, . . . NUMB

b. Output:

1. FI2, the value of the integral.

4. Algorithm:

The method is any that will calculate the integral

$$FI2 = \int_0^{\rho^*} (Z-1) d \ln \rho^*$$

for a given equation of state. The scaling values for temperature and density and the physical properties of the substance are given in the common block. The parameters that will be fitted in the equation of state are in A of the common block.

Subroutine FLASHP

1. Hierarchy: Called By: FUNCN
Calls: DENSV,DENSL,FUGCOF

2. Functional Description:

This subroutine performs an adiabatic flash for a pure fluid to find the saturation pressure.

3. Variables:

- a. Input:

1. Arguments:

T, the absolute saturation temperature.
PO, initial estimate of saturation pressure

2. COMMON/DAT/ISTATE(4),ISTATE(9)

- b. Output:

1. FLASHP, the calculated saturation pressure.

- c. Intermediate:

1. P, intermediate calculated pressure,
 2. IT, do-loop parameter.
 3. EPS, precision for convergence criteria
 4. RHOL, liquid density
 5. RHOV, vapor density
 6. ITMAX, maximum number of iterations.
 7. PCRIT, critical pressure
 8. KVALUE, equilibrium ratio.

4. Algorithm:

1. Initialize precision and maximum iterations;
EPS=.001
ITMAX=20

2. If called by derivative routine FDERIV, use previous pressure for initial value;
If $ISTATE(9) \neq 1$, $P = P_0$
3. Calculate densities
 $RHOV = DENS(V, T, P)$
 $RHOL = DENS(L, T, P)$
4. Start loop, $IT = 1$
5. $KVALUE = FUGCOF(T, RHOL) / FUGCOF(T, RHOV)$
6. Update pressure;
 $P = P * KVALUE$
7. Make sure pressure does not go too high;
If $P > 1.3 * P_C$, $P = 1.3 * P_C$, If $ISTATE(4) < 4$ print error, $FLASHP = P$ return.
Else;
8. Check for convergence;
If $|1 - KVALUE| < EPS$, $FLASHP = P$, return.
Else;
9. Check for exceeding iteration maximum;
 $IT = IT + 1$
If $IT > ITMAX$, and if $ISTATE(4) < 4$, print error, $FLASHP = P$, return.
Else;
10. Calculate new densities:
 $RHOV = DENS(V, T, P)$
 $RHOL = DENS(L, T, P)$
11. Go to 5

Subroutine FUGCOF

1. Hierarchy; Called By: FLASHP
Calls: FIL and PRES

2. Functional Description:

This subroutine calculates the pure fluid fugacity coefficient from an equation of state in EZFIT form as

$$f/f^0 = \exp(\ln(\rho RT) + \text{FIL} + (Z-1))$$

3. Variables,

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

2. COMMON/PRM/RGAS

- b. Output:

1. FUGCOF, the calculated pure fluid fugacity.

- c. Intermediate

1. FP, reduced chemical potential.

4. Algorithm:

1. $FP = \ln(RHO * RGAS * T) + FIL + (PRES / (RHO * RGAS * T) - 1)$
 2. Check for overflow;
If $FP > 100$, $FP = 0$
 3. $FUGCOF = EXP(FP)$

Subroutine FUNCN

1. Hierarchy: Called By: CURFIT, OUTPUT
 Calls: FLASHP, DENSV, DENSL, ENTH, CP, ENTRPY,
 U, CV, PRES

2. Functional Description:

This subroutine controls the calling of the calculation subroutines for the evaluation of the data point.

3. Variables:

a. Input:

1. COMMON/PRM/RGAS, . . , RMIDV
2. COMMON/PRP/ICOMP(20), . . , .CNAME(20,2)
3. Argument X, transfer vector, NDIM, the dimension of the transfer vector.

b. Output:

1. COMMON/PRM/TCRIT, PCRIT, RHOC, RENRGY, W, ALPHA, BETA, RTOP, RMIDL, RMIDV, A

c. Intermediate:

1. SL, save location for the compound code presently active.
2. X1, the absolute value of the control variable
3. IWHOLE, the whole portion of the control variable.
4. IFRACT, the fraction portion of the control variable.
5. LIQVAP, the sign of the control variable.
6. L, do-loop parameter.
7. RHOL, calculated liquid density.
8. RHOV, calculated vapor density.

4. Algorithm:

1. Transfer parameters to A;
 N=NDIM-NPARM
 For I=1 to NPARM

1. $A_i = X_{N+i}$
2. Separate control variables;
 $X_1 = |X_1|$
 $IWHOLE = X_1 + .005$
 $IFRACT = |X_1 - IWHOLE + .005| * 100$
 $LIQVAP = \text{SIGN}(1, X_1)$
3. Find index of compound;
For L=1 to 20
1. If $ICOMP_1 = IWHOLE$, go to 5
4. Print error message.
5. Check if properties are for right compound;
If $SL=L$ go to 6
Else;
1. Set properties for compound;
 $TCRIT = CTC(L)$
 $PCRIT = CPC(L)$
 $RHOC = CRC(L)$
 $RENRGY = 1.9872 / CMW(L)$
 $W = CW(L)$
 $ALPHA = CA(L)$
 $BETA = CB(L)$
 $RTOP = 4 * RHOC$
 $RMIDL = RHOC$
 $RMIDV = RHOC$
 $SL = L$
6. Calculate properties;
If $IFRACT = 30$ and $LIQVAP = -1$, calculate $DENSL$
If $IFRACT = 30$ and $LIQVAP = 1$, calculate $DENSV$
If $IFRACT = 40$ and $LIQVAP = -1$, calculate $DENSL, ENTH$
If $IFRACT = 40$ and $LIQVAP = 1$, calculate $DENSV, ENTH$
If $IFRACT = 75$, calculate $FLASHP$
If $IFRACT = 60$, calculate $PRES$
If $IFRACT = 25$, and $LIQVAP = -1$, calculate $DENSL, CV$
If $IFRACT = 25$, and $LIQVAP = 1$, calculate $DENSV, CV$
If $IFRACT = 20$, and $LIQVAP = -1$, calculate $DENSL, CP$
If $IFRACT = 20$, and $LIQVAP = 1$, calculate $DENSV, CP$
If $IFRACT = 12$, and $LIQVAP = 1$, calculate $DENSL, U$
If $IFRACT = 12$, and $LIQVAP = -1$, calculate $DENSV, U$
If $IFRACT = 14$, and $LIQVAP = -1$, calculate $DENSL, ENTRPY$
If $IFRACT = 14$, and $LIQVAP = 1$, calculate $DENSV, ENTRPY$

Subroutine GJEL

1. Hierarchy: Called By: CURFIT
Calls: -

2. Functional Description:

This subroutine finds the solution to system of simultaneous linear equations by the Gauss-Jordan elimination with optional maximum pivot selection. The inverse matrix is generated over the coefficient matrix. More than one solution vector may be obtained at one time.

3. Variables:

a. Input:

1. Arguments:

A, augmented matrix of coefficients and constants.
ND, number of rows in matrix,
MD, number of columns in matrix.

b. Output:

1. Arguments:

DETD, the determinant.
IER, the error code;
IER=0, successful inversion
IER=ND+1, pivot element was zero.
IER=I, pivot was smaller than 10^{-20}

c. Intermediate:

1. I,J,K,II,JJ,IR, do-loop parameters.
2. L,LL, indices.
3. EPS, precision for pivot element.
4. FACT, storage for normalizing, etc.
5. PIVOTS, row transformation vector
6. CPIVOT, column transformation vector.
7. IPIVOT, LPIVOT transformation indices.
8. N,M, local storage for arguments ND,MD respectively.
9. DET, accumulator for determinant

4. Algorithm:

1. Initialize:
IER=0, N=ND, M=MD, DET=1
 2. Begin Elimination;
For I=1 to N
 1. Optional maximum pivot strategy:
 1. Find largest pivot;
If I=N go to 2.1.6
 2. Initialize search;
LPIVOT=I, IPIVOT=I, FACT=|A(I,I)|
 3. Search;
For II=1 to N
 1. For JJ=1 to N
 1. If A(JJ,II) FACT go to 2.1.3.1.3
 2. Else, save larger pivot;
FACT = A(JJ,II)
LPIVOT=JJ
IPIVOT=II
 3. Continue loop
 4. Trade columns:
 1. record trade; CPIVOT(I)=IPIVOT
 2. For K=1 to N
 1. Trade elements
FACT=A(K,I)
A(K,I)=A(K,IPIVOT)
A(K,IPIVOT)=FACT
 5. Trade rows;
 1. Record trade; PIVOTS(I)=LPIVOT
 2. For K=1 to M
 1. Trade elements;
FACT=A(I,K)
A(I,K)=A(LPIVOT,K)
A(LPIVOT,K)=FACT
 6. CPIVOT(N)=N
LPIVOT(N)=N
2. Test for invalid pivot;
 1. If A(I,I)=0, DET=0, IER=N+1, return
 2. If |A(I,I)| < EPS, DET=0, and IER=I
3. Generate determinant; DET=DET*A(I,I)

4. Test for ill conditioned matrix;
If $|\text{DET}| < 10^{-60}$, Print error message, $\text{DET}=0$
5. Normalize pivot row;
 1. $\text{FACT}=\text{A}(\text{I},\text{I})$, $\text{A}(\text{I},\text{I})=1$
 2. For $\text{J}=1$ to M
 1. $\text{A}(\text{I},\text{J})=\text{A}(\text{I},\text{J})/\text{FACT}$
6. Reduce other rows;
For $\text{J}=2$ to N ;
 1. Select row; $\text{L}=\text{MOD}(\text{I}+\text{J}-2,\text{N})+1$
 2. If $\text{A}(\text{L},\text{I})=0$, go to 2.6.6
 3. Save term for reduction, $\text{FACT}=\text{A}(\text{L},\text{I})$
 4. Insert term for inverse; $\text{A}(\text{L},\text{I})=0$
 5. Reduce row;
For $\text{K}=1$ to M
 1. Select index; $\text{LL}=\text{MOD}(\text{I}+\text{K}-2,\text{M})+1$
 2. If $\text{A}(\text{I},\text{LL}) \neq 0$, $\text{A}(\text{L},\text{LL})=\text{A}(\text{L},\text{LL})-\text{A}(\text{I},\text{LL}) * \text{FACT}$
 6. Continue loop.
3. Optional maximum pivot strategy;
 1. transfer columns of inverse;
For $\text{IR}=1$ to N
 1. Calculate index so that transformation is in reverse; $\text{I}=\text{N}-\text{IR}+1$
 2. See if transfer was made;
If $\text{PIVOTS}(\text{I})=\text{I}$, go to 3.1.5
 3. $\text{LPIVOT}=\text{PIVOTS}(\text{I})$
 4. For $\text{J}=1$ to N
 1. Trade terms;
 $\text{FACT}=\text{A}(\text{J},\text{I})$
 $\text{A}(\text{J},\text{I})=\text{A}(\text{J},\text{LPIVOT})$
 $\text{A}(\text{J},\text{LPIVOT})=\text{FACT}$
 5. Continue loop.
 2. Transfer rows of solution and inverse;
For $\text{IR}=1$ to N
 1. Calculate index so that transformation is in reverse; $\text{I}=\text{N}-\text{IR}+1$

2. See if transfer was made;
If CPIVOT(I)=I go to 3.2,5
 3. JPIVOT=CPIVOT(I)
 4. For J=1 to M
 1. Trade terms;
FACT=A(I,J)
A(I,J)=A(JPIVOT,J)
A(JPIVOT,J)=FACT
 5. Continue loop.
4. Output determinant; DETD=DET

Subroutine LBLEZ

1. Hierarchy: Called By: MAIN, CURFIT
Calls: -

2. Functional Description;

This subroutine prints a title page identifying the use of the package EZFIT.

3. Variables; None

4. Algorithm:

Upon its first call it outputs a title page.

Subroutine MESSG

1. Hierarchy: Called By: MAIN CURFIT, tec.
Calls: -

2. Functional Description:

This subroutine prints the character string TEXT of length NCHR at the left margin.

3. Variables:

a. Input:

1. Arguments: TEXT, NCHR.

b. Output:

1. TEXT printed on stream printer.

4. Algorithm:

1. Print TEXT after advancing one line on stream printer.

Subroutine OUTPUT

1. Hierarchy: Called By: MAIN
Calls: FUNCN

2. Functional Description:

This subroutine forms tables of output for a set of parameters for the experimental data. It can be custom tailored to the users needs. This version makes tables of each data type with point identification, weight, errors and independent variables. At the end of each table is a summary of error statistics for that block.

3. Variables:

a. Input:

1. Argument X,N,Y,NPTS,NPARM,A1,WEIGHT,DATAID,ND
2. COMMON/PRP/ICOMP(20),, ,CNAME(20,2)
3. HEADER, Heading, and IN for use on tables.
4. IXPRINT, variable read in for optional output control.

b. Output:

1. All inputs except N,NPTS,NPARM,A1, and ND.
2. Calculated Y's, percent errors, absolute errors, headings, summary errors, optional intermediate values.

c. Intermediate:

1. I,J, and K used for do-loop evaluation.
2. LF the save location for the fraction portion of the control variable
3. LW the save location for the whole portion of the control variable.
4. SUM1, the accumulator for average absolute percent error.
5. SUM2, the accumulator for average absolute error.
6. JO, counter for data block.

7. SUM, the accumulator for the average absolute percent error for the entire data set.
8. Z, the transfer vector for the parameters and variables to FUNCN,
9. YC, calculated value for data point.
10. PERC, percent error for data point
11. DIFF, difference in calculated and experimental.
12. X1, the absolute value of the control variable.
13. IWHOLE, the whole portion of the control variable for the point.
14. IFRACT, the fraction portion of the control variable for the point.
15. IRHO, fraction code for density point.
16. IDH, fraction code for enthalpy departure point.
17. IVP, code for vapor pressure point.
18. RHO, calculated density.
19. RHOL, saturated liquid density at vapor pressure point.
20. RHOV, saturated vapor density at vapor pressure point.
21. PRESC, calculated pressure for density point.
22. PERC2, percent error in calculated pressure.

4. Algorithm:

What ever is desired by the user for tables of results.

Subroutine PRES

1. Hierarchy: Called By: FUNCN, DENSL, DENS, ENTH,
FUGCOF, ENTRPY.

Calls: -

2. Functional Description:

This subroutine calculates the pressure for a given equation of state using parameters in the common blocks for the arguments of temperature and density.

3. Variables:

a. Input:

1. Arguments:

T, absolute temperature,
RHO, density,

2. COMMON/PRM/RGAS, . . . NUMB

b. Output:

1. PRES, the calculated pressure,

4. Algorithm:

The method is any that will calculate the pressure for a given equation of state. The scaling values for temperatures and density and the physical properties of the substance are given in the common block. The parameters that will be fitted in the equation of state are in A of the common block.

Subroutine U

1. Hierarchy: Called By; FUNCN,CV
Calls; FI2

2. Functional Description:

This subroutine calculates the internal energy departure at the state condition specified by the arguments temperature and density. This value is calculated for an equation of state in EZFIT form as

$$\Delta U = R_e T_c (-T^*{}^2 FI_2) / \alpha$$

3. Variables:

- a. Input:

1. Arguments:

T, absolute temperature.
RHO, density.

2. COMMON/PRM/RENRGY,TCRIT,ALPHA

- b. Output:

1. U, the calculated internal energy departure.

- c. Intermediate:

1. TSTAR, reduced temperature.

4. Algorithm:

1. Reduce temperature;
TSTAR=ALPHA*T/TCRIT

2. Calculate the unreduced internal energy departure;
U=RENRGY*TCRIT*(-TSTAR*TSTAR*FI2)/ALPHA

Adapting EZFIT to Any General Function

EZFIT can be adapted for fitting any general function of parameters $[A]_m$ and variables $[X]_n$, $y=f([X]_n; [A]_m)$, by changing the input and output routines and the calculation routine FUNCN. The specific requirements of the routines are given below along with an example for fitting a polynomial.

Subroutine Input DATA, DATA2, DATA3. The use of three data input routines allows each to be specialized to a specific data format. The requirements of the routines are basically the same. The form of the definition and arguments are

```
SUBROUTINE DATA3(X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,DATAID,ND)
DIMENSION X(NPTS,N),Y(NPTS),WEIGHT(NPTS),DATAID(NPTS,ND)
```

The arguments are:

- X The matrix of experimental data of NPTS points with N independent variables in each row.
- N The number of independent variables per data point.
- Y The vector of length NPTS of the dependent variables for each data point.
- NPTS The number of data points inputed.
- WEIGHT A vector of length NPTS containing the weights for each data point.
- YBAR The weighted average of the dependent variables.
- YVAR The variance of the independent variable,
- NCODE The control variable selecting the method of calculation of the weights given as:
 - 1 the weighting is $1/Y_{\text{exp}}$

0 the weight is 1, or equal weights.

1 the weight is $1/(\text{WEIGHT})^2$ where WEIGHT is supplied in the input section. This is usually used for percent weighting.

DATAID A matrix of NPTS rows of ND=3 columns that contain a 12 character identification for each data point.

ND The second dimension for DATAID, which is 3, to allow object time dimensioning.

Note that object time dimensioning is used allocating work space defined in the main program. The work space is allowed for X to have 3000 variables and therefore $\text{NPTS} \times \text{N} \leq 3000$.

The weighted mean is calculated as:

$$Y = \sum w_i y_i / \sum w_i.$$

The variance is then given as:

$$\text{Var}(Y) = \sum w_i (Y_i - \bar{Y})^2.$$

A sample routine is given in Table I. It reads from a card unidentified data on which the first N are variables and the last is the experimental value of Y. The data are in F10.0 format and the program generates an identification number for each point.

Subroutine Calculation FUNCN, The subroutine FUNCN is used to calculate the function to be fitted, $y=f([x]_n; [A]_m)$. The form of the definition and the arguments are

```
FUNCTION FUNCN(X,NDIM)
  DIMENSION X(NDIM)
```

The arguments are:

- X A transfer vector containing N independent variables first and then NPARM parameters,
- NDIM The total length of the transfer vector, i.e., N+NPARM. The maximum length of the transfer vector is set to 44 in CURFIT and OUTPUT,

FUNCN requires the common block PRM to obtain the number of parameters that are passed. It can be used to pass the parameters in the transfer vector to other calculation routines through the array A. A maximum of 40 parameters can be passed this way. The calculated independent variable, Y, is returned by assigning it to FUNCN. In the example in Table 1 FUNCN is set up to calculate the (N-1)th degree polynomial,

$$Y = A_1 + A_2X + A_3X^2 + \dots + A_NX^{N-1}.$$

Subroutine OUTPUT. The subroutine OUTPUT is used to generate tabulated results of calculations from a set of parameters. It usually calls FUNCN for the calculation of the independent variable but can also be used to calculate auxiliary information for use in analysis. The form of the definition and the arguments are:

```
SUBROUTINE OUTPUT(X,N,Y,NPTS,NPARM,A1,WEIGHT,DATAID,ND)
  DIMENSION X(NPTS,N),Y(NPTS),A1(NPARM),WEIGHT(NPTS),
  1 DATAID(NPTS,ND)
```

- X The matrix of experimental data of NPTS points with N independent variables in each row,
- N The number of independent variables per data point.
- Y The vector of length NPTS of the dependent variables for each data point.
- NPTS The number of data points inputted.
- NPARM The number of parameters used in the calculations.
- A1 The vector of length NPARM containing the parameters to be used in the calculation.
- WEIGHT A vector of length NPTS containing the weights for each data point.
- DATAID A matrix of NPTS rows of ND=3 columns that contain a 12 character identification for each data point.
- ND The second dimension for DATAID, which is 3, to allow object time dimensioning.

The user can custom program OUTPUT to his needs. A rather general version is given in the example in Table I. It reads a header used to label the table which also has column headings. The routine prints each point's identification code, experimental value, calculated value, the percent difference, the difference, the weight, and the independent variables. It also calculates the average absolute percent deviation, A.A.P.D., and the average absolute deviation, A.A.D., as

$$\text{A.A.P.D.} = \Sigma |(Y_c - Y_{\text{exp}}) / Y_{\text{exp}}| * 100 / \text{NPTS}$$

$$\text{A.A.D.} = \Sigma |Y_c - Y_{\text{exp}}| / \text{NPTS}$$

where the summation is over all data points, The transfer vector Z of 44 variables is used to communicate with FUNCN.

TABLE 1

An Example of Modifying EZFIT for Polynomial Regression

Source Listing

```
//NEW LEXEC FORTGCLG,LIB='S4.KGGIN.MOD',PARM.LKED='LIST,LET'      EZPL0010

C  FUNCTION FUNCN(X,NDIM)      EZPL0020
C                               EZPL0030
C  PURPOSE      EZPL0040
C    EVALUATES THE FITTED FUNCTION AT THE POINT X      EZPL0050
C                               EZPL0060
C  USAGE      EZPL0070
C    RESULT = FUNCN(X,NDIM)      EZPL0080
C                               EZPL0090
C  DESCRIPTION OF PARAMETERS      EZPL0100
C    X - ARRAY OF VALUES OF INDEPENDENT VARIABLES      EZPL0110
C    NDIM - NUMBER OF INDEPENDENT VARIABLES      EZPL0120
C                               EZPL0130
C    FUNCTION FUNCN(X,NDIM)      EZPL0140
C    DIMENSION X(NDIM)      EZPL0150
C    COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW      EZPL0160
C    1 ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV      EZPL0170
C    DOUBLE PRECISION SUM      EZPL0180
C    N=NDIM-NPARM      EZPL0190
C    DO 20 I=1,NPARM      EZPL0200
C  20 A(I)=X(N+I)      EZPL0210
C    SUM=0      EZPL0220
C  POLYNOMIAL IN X,Y=A(1)+A(2)*X+A(3)*X2 .....      EZPL0230
C    X1=X(1)      EZPL0240
C    DO 30 I=1,NPARM      EZPL0250
C    SUM=SUM*X1+A(NPARM-I+1)      EZPL0260
C  30 CONTINUE      EZPL0270
C    FUNCN=SUM      EZPL0280
C  40 RETURN      EZPL0290
C    END      EZPL0300
```


2	WEIGHT(I)=1	EZPL0810
	GO TO 10	EZPL0820
3	WEIGHT(I)=1/WEIGHT(I)**2	EZPL0830
10	CONTINUE	EZPL0840
	SUM=SUM+WEIGHT(I)*Y(I)	EZPL0850
	SUMW=SUMW+WEIGHT(I)	EZPL0860
60	CONTINUE	EZPL0870
	SUM=SUM/SUMW	EZPL0880
C	CALCULATE THE WEIGHTED MEAN AND VARIANCE	EZPL0890
	YBAR=SUM	EZPL0900
	SUMY=0	EZPL0910
	DO 50 I=1,NPTS	EZPL0920
	SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2	EZPL0930
50	CONTINUE	EZPL0940
	YVAR=SUMY	EZPL0950
	RETURN	EZPL0960
	END	EZPL0970
	SUBROUTINE OUTPUT(X,N,Y,NPTS,NPARM,A1,WEIGHT,DATAID,ND)	EZPL0980
	COMMON /PRM/RGAS,RENTRY,ICRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW	EZPL0990
1	,A(40),B(7),NTERMS,NPAR1,NUMB,RTOP,RMIDL,RMIDV	EZPL1000
	DIMENSION X(NPTS,N),Y(NPTS),A1(NPARM),WEIGHT(NPTS),DATAID(NPTS,ND)	EZPL1010
	DIMENSION HEADER(20)	EZPL1020
	DIMENSION Z(44)	EZPL1030
100	FORMAT(1X,8G14.6)	EZPL1040
200	FORMAT(20A4)	EZPL1050
300	FORMAT(/////1X,'AVERAGE ABSOLUTE DEVIATION',G14.6)	EZPL1060
400	FORMAT(20X,20A4//)	EZPL1070
500	FORMAT(1H1)	EZPL1080
1100	FORMAT(16I5)	EZPL1090
	DATA IRHO, IDH, IVP/30,40,75/	EZPL1100
	READ 200,HEADER	EZPL1110
	PRINT 500	EZPL1120
	PRINT 400,HEADER	EZPL1130
	PRINT 100	EZPL1140
	PRINT 1600	EZPL1150
1600	FORMAT(5X,'DATAID',8X,'YEXP',8X,'YCALC',7X,'PERCENT',7X,'DELTA'	EZPL1160
1	,8X,'WEIGHT',6X,'CONTROL',9X,'X2',11X,'X3',11X,'X4'/57X,'X','S...	EZPL1170
2	,//)	EZPL1180
	SUM1=0	EZPL1190
	J0=0	EZPL1200
	SUM2=0	EZPL1210
	SUM=0	EZPL1220

```

NDIM=N+NPARM
DO 10 J=1,NPARM
  Z(N+J)=A1(J)
10 CONTINUE
DO 20 I=1,NPTS
  DO 50 J=1,N
    Z(J)=X(I,J)
50 CONTINUE
  YC=FUNCN(Z,NDIM)
  PERC=100*(YC-Y(I))/Y(I)
  DIFF=Y(I)-YC
  PRINT 2000,(DATAID(I,K),K=1,ND),Y(I),YC,PERC,DIFF,WEIGHT(I),
    1 (X(I,K),K=1,N)
  JO=JO+1
  SUM=SUM+ABS(PERC)
  SUM1=SUM1+ABS(PERC)
  SUM2=SUM2+ABS(DIFF)
2000 FORMAT(1X,3A4,1X,9G13.5,(/53X,6G13.5))
20 CONTINUE
  SUM1=SUM1/JO
  SUM2=SUM2/JO
  PRINT 100
  CALL MESSG('AVE. ABS. PERCENT,NUMBER PTS.,AVE.ABS.DEVIATION ',48)
  PRINT 100,SUM1,JO,SUM2
  PRINT 100
  SUM=SUM/NPTS
  PRINT 300,SUM
  PRINT 100
  PRINT 100
  PRINT 500
  RETURN
END
EZPL1230
EZPL1240
EZPL1250
EZPL1260
EZPL1270
EZPL1280
EZPL1290
EZPL1300
EZPL1310
EZPL1320
EZPL1330
EZPL1340
EZPL1350
EZPL1360
EZPL1370
EZPL1380
EZPL1390
EZPL1400
EZPL1410
EZPL1420
EZPL1430
EZPL1440
EZPL1450
EZPL1460
EZPL1470
EZPL1480
EZPL1490
EZPL1500
EZPL1510
EZPL1520
EZPL1530
EZPL1540

```

```

//LKED.S4LIB DD DSN=S4.KGUIN.MOD,DISP=SHR
//LKED.SYSIN DD *
INCLUDE S4LIB(EZFIT)
  ENTRY MAIN
//GD.SYSIN DD *
EZPL1550
EZPL1560
EZPL1570
EZPL1580
EZPL1590

```

5											MINIMUM CURFIT OUTPUT		
3											SUBROUTINE DATA3 2		
0.001											MARQUART		3
25.	0	0									UNCONSTRAINED ,PRECISION 5		
	5										NO ERROR MESSAGES		
	0	3									DUMMY		
	3	4									DUMMY 9		
	1	2	3	4	5	6	7	8	9	10			
	0	0	0	0	0	0	0	0	0	0	0	0	

+1		
10.7315		
1		
10		
1.	1.01	
2.	7.99	
3.	27.01	
4.	63.99	
5.	75.01	
6.	215.99	
7.	343.01	
8.	511.99	
9.	729.01	
10.	999.99	
	POLYNOMIAL REGRESSION	DEGREE 2
	POLYNOMIAL REGRESSION	DEGREE 3

Example Output of EZFIT for a Polynomial Regression

PROGRAM STATUS SUMMARY

EZFIT IS OPERATING IN MODE TYPE 5

DATA READ BY ROUTINE DATA3
 INITIAL VALUE OF ACCELERATION PARAMETER LAMBDA= 0.100000E-02
 METHOD OF DERIVATIVE CALCULATION IS = 0
 CONSTRAINT MODE IS = 0
 ERROR MESSAGE CONTROL IS = 5
 CONVERGENCE CRITERIA EPS= 0.100000E-02
 WEIGHT METHOD IS = 1
 UNIVERSAL GAS CONSTANT IS = 10.7315

TIME	NUMD	NOT FITTED PARMS	FITTED PARMS	NNTERM	FITTING RANGE	
25.0000	0	0	3	0	3	4
PARM FITTING ORDER						
1	2	3	4	5	6	7
9	10	0	0	0	0	0
0	0	0	0	0	0	0
0	0	0	0	0	0	0
0	0	0	0	0	0	0
INITIAL VALUES						
0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0
NUMBER OF POINTS, NO OF INDEPENDENT VAR						
10	1					
NPTRHO	NPTH	NPTVP	NPTS			
0	0	0	10			

NUMBER OF PARAMETERS, NTERMS
3 3

ITERATION 1

AVERAGE ABSOLUTE DEVIATION

99.9998

INITIAL VALUE OF OBJECTIVE FCN

1.42857

AVERAGE ABSOLUTE DERIVATIVE OF FCN

1.00000

5.50000

38.5000

MAX SCALED PARM DELTA, PARM NO.

0.21847

3

TRIAL OBJECTIVE FCN

0

0.125804

RELATIVE CHANGE IN PARAMETERS

1: -1.00

2: -1.00

3: -1.00

LENGTH OF PARAMETER CHANGE

14.7929

NEW PARMS

6.23195

-11.7398

6.49380

OBJECTIVE FCN

0.125804

PARM VARIANCE

1: 11.4

2: 14.5

3: 3.62

ELAPSED TIME

0.217315

ITERATION 2

AVERAGE ABSOLUTE DEVIATION

24.2912

INITIAL VALUE OF OBJECTIVE FCN
0.125804

AVERAGE ABSOLUTE DERIVATIVE OF FCN
1.00002 5.50006 38.5002

MAX SCALED PARM DELTA, PARM NO.
1.79770 3

TRIAL OBJECTIVE FCN
0 0.107375

RELATIVE CHANGE IN PARAMETERS

1:-0.436 2:-0.346 3:-0.179

LENGTH OF PARAMETER CHANGE
7.98680

NEW PARMS

11.0531 -17.9469 7.91424

OBJECTIVE FCN
0.107375

PARM VARIANCE
1: 13.9 2: 17.8 3: 4.30

ELAPSED TIME
0.301577

ITERATION 3

AVERAGE ABSOLUTE DEVIATION
21.3401

INITIAL VALUE OF OBJECTIVE FCN
0.107375

AVERAGE ABSOLUTE DERIVATIVE OF FCN
0.999995 5.49997 38.4998

MAX SCALED PARM DELTA, PARM NO.
0.101995 3

TRIAL OBJECTIVE FCN
0 0.107319

RELATIVE CHANGE IN PARAMETERS

1:-0.246E-01 2:-0.195E-01 3:-0.101E-01

LENGTH OF PARAMETER CHANGE

0.459960

RATIO OF CHANGE IN OBJECTIVE FUNCTION IS LESS THAN EPS 0.100000E-02

PART = 1 ITERATION = 3
WEIGHT CODE= 1

NUMBER	PARAMETER	STANDARD ERROR	VARIANCE	(A/SE)**2
1	11.0531	1.22257	13.9203	81.7361
2	-17.9469	1.38066	17.7529	168.969
3	7.91424	0.679306	4.29763	135.734

CHISQUARED 0.107375 DEGREES OF FREEDOM 7
F-STATISTIC FOR CORRELATION COEFFICIENT FR= 20.8128
F-STATISTIC ON CHANGE IN CHISQUARED FROM PREVIOUS PART= 1.98272
DEGREES OF FREEDOM ARE NU1= 3 NU2= 6

POLYNOMIAL REGRESSION DEGREE 2

	DATAID	YEXP	YCALC	PERCENT	DELTA X'S...	WEIGHT	CONTROL
GEN	0001	1.0100	1.0204	1.0308	-0.10411E-01	0.98030	1.0000
GEN	0002	7.9900	6.8163	-14.690	1.1737	0.15664E-01	2.0000
GEN	0003	27.010	28.441	5.2965	-1.4306	0.13707E-02	3.0000
GEN	0004	63.990	65.893	2.9745	-1.9034	0.24422E-03	4.0000
GEN	0005	75.010	119.17	58.878	-44.165	0.17773E-03	5.0000
GLN	0006	215.99	188.29	-12.827	27.705	0.21435E-04	6.0000
GLN	0007	343.01	273.22	-20.346	69.787	0.84994E-05	7.0000
GEN	0008	511.99	373.99	-26.954	138.00	0.38148E-05	8.0000
GLN	0009	729.01	490.58	-32.705	238.43	0.18816E-05	9.0000
GEN	0010	999.99	623.01	-37.699	376.98	0.10000E-05	10.000
AVE. ABS. PERCENT, NUMBER PTS., AVE. ABS. DEVIATION							
	21.3401		10	89.9582			

AVERAGE ABSOLUTE DEVIATION 21.3401

NUMBER OF PARAMETERS, NTERMS
4 4

ITERATION 1

AVERAGE ABSOLUTE DEVIATION
21.3401

INITIAL VALUE OF OBJECTIVE FCN
0.125271

AVERAGE ABSOLUTE DERIVATIVE OF FCN
0.999995 5.49997 38.4994 302.500

MAX SCALED PARM DELTA, PARM NO.
6.27766 4

TRIAL OBJECTIVE FCN
0 0.873773E-01

RELATIVE CHANGE IN PARAMETERS

1: 0.417 2: 0.513 3: 0.696 4: -1.00

LENGTH OF PARAMETER CHANGE
7.63627

NEW PARMS

7.79956 -11.8647 4.66699 0.434999

OBJECTIVE FCN
0.873773E-01

PARM VARIANCE
1: 14.5 2: 21.5 3: 9.05 4: 1.09

ELAPSED TIME
0.548258

ITERATION 2

AVERAGE ABSOLUTE DEVIATION
16.4018

INITIAL VALUE OF OBJECTIVE FCN
0.873773E-01

AVERAGE ABSOLUTE DERIVATIVE OF FCN
0.999974 5.49986 38.4994 302.500

MAX SCALED PARM DELTA, PARM NO.
18.8577 4

TRIAL OBJECTIVE FCN
0 0.448081E-01

RELATIVE CHANGE IN PARAMETERS

1: -2.94 2: -2.85 3: -2.86 4: -0.618

LENGTH OF PARAMETER CHANGE
22.9226

NEW PARMS

-4.01558 6.40577 -2.51263 1.13866

OBJECTIVE FCN
0.448081E-01

PARM VARIANCE
1: 26.8 2: 41.1 3: 16.4 4: 1.73

ELAPSED TIME
0.647248

ITERATION 3

AVERAGE ABSOLUTE DEVIATION

11.6921
INITIAL VALUE OF OBJECTIVE FCN
0.448081E-01

AVERAGE ABSOLUTE DERIVATIVE OF FCN
1.00004 5.49985 38.5002 302.494

MAX SCALED PARM DELTA, PARM NO.
7.51088 4

TRIAL OBJECTIVE FCN
0 0.408196E-01

RELATIVE CHANGE IN PARAMETERS

1: -0.540 2: -0.532 3: -0.531 4: -0.196

LENGTH OF PARAMETER CHANGE
9.13138

NEW PARMS

-8.73173 13.6827 -5.36026 1.41659

OBJECTIVE FCN
0.408196E-01

PARM VARIANCE
1: 31.3 2: 48.0 3: 19.1 4: 1.97

ELAPSED TIME
0.743612

ITERATION 4

AVERAGE ABSOLUTE DEVIATION
11.3756

INITIAL VALUE OF OBJECTIVE FCN
0.408196E-01

AVERAGE ABSOLUTE DERIVATIVE OF FCN
1.00000 5.49999 38.5002 302.499

MAX SCALED PARM DFLIA, PARM NO.
0.302499 4

TRIAL OBJECTIVE FCN
0 0.408136E-01

RELATIVE CHANGE IN PARAMETERS

1:-0.213E-01 2:-0.210E-01 3:-0.209E-01 4:-0.783E-02

LENGTH OF PARAMETER CHANGE
0.367744

RATIO OF CHANGE IN OBJECTIVE FUNCTION IS LESS THAN EPS 0.100000E-02

PART = 2 ITERATION = 4
WEIGHT CODE = 1

NUMBER	PARAMETER	STANDARD ERROR	VARIANCE	(A/SE)**2
1	-8.73173	1.12947	31.2520	59.7660
2	13.6827	1.39915	47.9582	95.6341
3	-5.36026	0.862329	19.0719	36.9071
4	1.41659	0.283790	1.97300	24.9170

CHISQUARED 0.408196E-01 DEGREES OF FREEDOM 6
F-STATISTIC FOR CORRELATION COEFFICIENT FR= 42.5062
F-STATISTIC ON CHANGE IN CHISQUARED FROM PREVIOUS PART= 10.3444
DEGREES OF FREEDOM ARE NU1= 4 NU2= 5

POLYNOMIAL REGRESSION DEGREE 3

	DATAID	YEXP	YCALC	PERCENT	DELTA X'S...	WEIGHT	CONTROL
GEN	0001	1.0100	1.0073	-0.26590	0.26855E-02	0.98030	1.0000
GEN	0002	7.9900	8.5254	6.7008	-0.53540	0.15664E-01	2.0000
GEN	0003	27.010	22.322	-17.356	4.6879	0.13707E-02	3.0000
GEN	0004	63.990	50.897	-20.461	13.093	0.24422E-03	4.0000
GEN	0005	75.010	102.75	36.981	-27.740	0.17773E-03	5.0000
GEN	0006	215.99	186.38	-13.709	29.611	0.21435E-04	6.0000
GEN	0007	343.01	310.29	-9.5402	32.724	0.84994E-05	7.0000
GLN	0008	511.99	482.97	-5.6683	29.021	0.38148E-05	8.0000
GEN	0009	729.01	712.93	-2.2059	16.082	0.18816E-05	9.0000
GEN	0010	999.99	1008.7	0.86729	-8.6729	0.10000E-05	10.000

AVE. ABS. PERCENT. NUMBER PTS. AVE. ABS. DEVIATION
11.3756 10 16.2163

AVERAGE ABSOLUTE DEVIATION 11.3756

Source Listing for EZFIT

```

100 FORMAT (1X,8G14.6)
200 FORMAT(1X,'F-STATISTIC FOR CORRELATION COEFFICIENT FR=',G14.6/
1' F-STATISTIC ON CHANGE IN CHISQUARED FROM PREVIOUS PART= ',G14.6/
2' DEGREES OF FREEDOM ARE NU1=',15,' NU2= ',15)
300 FORMAT (1H1,'PART = ',14,' ITERATION = ',14)
400 FORMAT (6X,'YEXP',10X,'YFIT',10X,'PERCENT',8X,'X','S')
500 FORMAT (1H1)
600 FORMAT (1X,5A4,' WEIGHT CODE= ',14)
700 FORMAT(1X,' INPUT DATA X','S Y')
800 FORMAT(1H0,' ITERATION',15)
900 FORMAT(1X,' ***** TIME EXCEEDED *****')
1200 FORMAT(16I5)
1100 FORMAT(8F10.0)
1300 FORMAT(1H1,5X,'YEXP',10X,'YFIT',10X,'PERCENT',8X,'X','S'//)
1400 FORMAT(20A4)
1600 FORMAT(1X,3A4,8G14.6,(/13X,8G14.6))
2100 FORMAT(1X,8X,'NUMBER',4X,'PARAMETER',1X,'STANDARD ERROR',6X,
1' VARIANCE',5X,'(A/SE)*2')
2200 FORMAT(1X,'CHISQUARED',G14.6,' DEGREES OF FREEDOM',15)
2300 FORMAT(1X,'DENS%',G14.6,' H%',G14.6,' VP%',G14.6,
1' TOTALX',G14.6)
2400 FORMAT(1X,2A4,' TC=',G14.6,'PC=',G14.6,'RC=',G14.6,'MW=',G14.6,
1' ALPHA=',G14.6,'BETA=',G14.6,' OMEGA=',G14.6//)
2500 FORMAT(1X,8G14.6,3A4)
2600 FORMAT(1X,6G14.6,28X,3A4)
2700 FORMAT(/52X,'PROGRAM STATUS SUMMARY'//
1' 45X,'EZFIT IS OPERATING IN MODE TYPE',15//)
2800 FORMAT(6X,'TIME',16X,'NUMB',4X,'NOT FITTED PARMS',2X,'FITTED PARMS',
1' 2X,'NNTERM',13X,'FITTING RANGE')
2900 FORMAT(1X,'DATA READ BY ROUTINE DATA',11,' INITIAL VALUE OF ACCE',
1' LERATION PARAMETER LAMDDA=',G14.6,' METHOD OF DERIVATIVE CALCULATIE',
20N IS = ',15,' CONSTRAINT MODE IS = ',15,' ERROR MESSAGE CE',
30N CONTROL IS = ',15)
3100 FORMAT(1X,'RATIO OF CHANGE IN OBJECTIVE FUNCTION IS LESS THAN EPS',
1,G14.6)
3200 FORMAT(11X,'NPTRHU',8X,'NPTH',10X,'NPTVP',9X,'NPTS')
3300 FORMAT(1X,8(13,'G10.3')/(1X,8(13,'G10.3'))
3400 FORMAT(1X,'CONVERGENCE CRITERIA EPS= ',G14.6,
1,' WLIGHT METHOD IS = ',15,' UNIVERSAL GAS CONSTANT IS = ',G14.6/)
3500 FORMAT(53X,'REGRESSION SERIES BEGINNING'//)

C
C
C
COMMON /PRP/ICUMP(20),CPC(20),CRC(20),CMW(20),CW(20),CTC(20)
1 ,CA(20),CB(20),CNAME(20,2)
COMMON /PRM/RGAS,RENRGY,ICRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
1 ,A(40),B(7),NTERM5,NPARM,NUMB,RTOP,RMIDL,RMIDV
COMMON /XTN/AXTN(60)
COMMON /DAT/IPRES,ISTATE(20)
C *****F7I1I*****
EZFIT COMMON BLOCKS

```

	DIMENSION X(1000,3),Y(1000),SIGMAY(1000),YFIT(1000),	EZMN0510
	1 WEIGHT(1000),XX(3000),DATAID(1000,3),DD(3000)	EZMN0520
	MODIFIED FOR EZ EXTENSION	EZMN0530
C	DIMENSION ITERM(100),A1(100),STORE(205),SIGMAA(100),STORED(100)	EZMN0540
	INTEGER DF ,FPARM	EZMN0550
	REAL NAME(5)	EZMN0560
	EQUIVALENCE (XX(1),X(1,1)),(WEIGHT(1),SIGMAY(1))	EZMN0570
	EQUIVALENCE (DD(1),DATAID(1,1))	EZMN0580
	CALL LBLEZ	EZMN0590
	PRINT 500	EZMN0600
	CALL CPUTIM	EZMN0610
	DO 80 I=1,20	EZMN0620
	ICOMP(I)=0	EZMN0630
	ISTATE(I)=0	EZMN0640
80	CONTINUE	EZMN0650
C	INPUT CONTROL DATA	EZMN0660
	READ 1200,IOUT	EZMN0670
	READ 1200,IDATA	EZMN0680
	READ 1100,DFLMDA,EPS	EZMN0690
	IF(EPS.EQ.0)EPS=.001	EZMN0700
	READ 1100 ,TMAX	EZMN0710
	READ 1200,ISTATE(3),ISTATE(5)	EZMN0720
	READ 1200,ISTATE(4)	EZMN0730
	READ 1200,NUMB	EZMN0740
	READ 1200 ,NFPARM,FPARM	EZMN0750
	READ 1200,NNTERM	EZMN0760
	READ 1200,NUIFR,NUITO	EZMN0770
	READ 1200,ITERM	EZMN0780
	READ 1100,A1	EZMN0790
	READ 1200 ,NCODE	EZMN0800
	READ 1100,RGAS	EZMN0810
	READ 1200,N	EZMN0820
	READ 1200,NPTS	EZMN0830
	PRINT 2700,IOUT	EZMN0840
	PRINT 2900,IDATA,DFLMDA,ISTATE(5),ISTATE(3),ISTATE(4)	EZMN0850
	PRINT 3400,EPS,NCODE,RGAS	EZMN0860
	PRINT 2800	EZMN0870
	PRINT 100,TMAX,NUMB,NFPARM,FPARM,NNTERM,NUIFR,NUITO	EZMN0880
	PRINT 100	EZMN0890
	CALL MESSG('PARM FITTING ORDER',18)	EZMN0900
	PRINT 100	EZMN0910
	PRINT 100,ITERM	EZMN0920
	PRINT 100	EZMN0930
	CALL MESSG('INITIAL VALUES',14)	EZMN0940
	PRINT 100	EZMN0950
	PRINT 100,A1	EZMN0960
	PRINT 100	EZMN0970
	CALL MESSG('NUMBER OF POINTS,NO OF INDEPENDENT VAR',40)	EZMN0980
	PRINT 100,NPTS,N	EZMN0990
	PRINT 100	EZMN1000


```

C
ND=3
      INPUT DATA
      IF (IDATA.EQ.1) CALL DATA (X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,
1    NPTRHQ,NPTH,NPTVP,DATAID)
      IF (IDATA.EQ.2) CALL DATA2(X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,
1    NPTRHQ,NPTH,NPTVP,DATAID)
      IF (IDATA.EQ.3) CALL DATA3(X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,
1    DATAID,ND)
      PRINT 100
      PRINT 3200
      PRINT 100,NPTRHQ,NPTH,NPTVP,NPTS
      ISTATE(2)=IOUT
      IF (IOUT.GE.3) GO TO 1130
      DISPLAY DATA
C
      PRINT 700
      DO 70 I=1,NPTS
      PRINT 1600,(DD(I+(K-1)*NPTS),K=1,3),(XX(I+(K-1)*NPTS),K=1,N),Y(I)
70 CONTINUE
1130 CONTINUE
      PRINT 500
      PRINT 3500
      IPRES=0
      NPART=1
      CH1=1
C
      START REGRESSION
      DO 40 NUI=NUIFR,NUITO
      NTERMS=NU1-NNTERM
      NPARM=NU1+NFPARM
      CALL MSGG('NUMBER OF PARAMETERS, NTERMS',28)
      PRINT 100,NPARM,NTERMS
      DF=NPTS-NU1
      CHI=1.E+60
      DO 1160 LL=1,NPARM
      STORE(I+LL)=A1(LL)
1160 CONTINUE
      IF (IOUT.LT.10) GO TO 1120
      MODIFIED FOR EZ EXTENSION
C
      DO 3110 LL=1,40
      A(LL)=A1(LL)
3110
      DO 3120 LL=1,60
      AXN(LL)=A1(LL+40)
3120 CONTINUE
      PERFORM OUTPUT ONLY
C
      CHISQR=-10
      GO TO 1110
1120 CONTINUE
      FLAMDA=DFLMDA
      STORE(1)=CHI
      DO 260 L=1,NPARM
      STORE(I+L)=A1(L)

```

```

EZMN1010
EZMN1020
EZMN1030
EZMN1040
EZMN1050
EZMN1060
EZMN1070
EZMN1080
EZMN1090
EZMN1100
EZMN1110
EZMN1120
EZMN1130
EZMN1140
EZMN1150
EZMN1160
EZMN1170
EZMN1180
EZMN1190
EZMN1200
EZMN1210
EZMN1220
EZMN1230
EZMN1240
EZMN1250
EZMN1260
EZMN1270
EZMN1280
EZMN1290
EZMN1300
EZMN1310
EZMN1320
EZMN1330
EZMN1340
EZMN1350
EZMN1360
EZMN1370
EZMN1380
EZMN1390
EZMN1400
EZMN1410
EZMN1420
EZMN1430
EZMN1440
EZMN1450
EZMN1460
EZMN1470
EZMN1480
EZMN1490
EZMN1500

```

```

260 CONTINUE
DO 5 I=1,20
PRINT 800,I
C
CALL CURFIT (X,N,Y,WEIGHT,NPTS,NUI,A1,SIGMAA,FLAMDA,
1 YFIT,CHISQR,NPARM,ITERM)
RMS=SQR(CHISQR*DF/NPTS)
RMS=RMS*100
SSQ=0
DO 1170 L=1,NPARM
DEL=STORE(L+1)-A1(L)
STORED(L)=0
IF(A1(L).NE.0)STORED(L)=DEL/A1(L)
SSQ=SSQ+DEL*DEL
1170 CONTINUE
PRINT 100
CALL MSGG('RELATIVE CHANGE IN PARAMETERS',29)
PRINT 100
PRINT 3300,(JJ,STORED(JJ),JJ=1,NPARM)
PRINT 100
SSQ=SQR(SSQ)
CALL MSGG('LENGTH OF PARAMETER CHANGE',26)
PRINT 100,SSQ
IF(I.NE.1) GO TO 1140
DO 1150 L=1,NUI
1150 STORE(1+NPARM+L)=SIGMAA(L)
1140 CONTINUE
C
CHECK RESULTS OF REGRESSION
IF(CHI,LT,CHISQR) GO TO 220
IF(ABS(CHI-CHISQR).LE.EPS*CHISQR) GO TO 230
IF(FLAMDA.GT.100.AND.CHI.GT.1.E+50) GO TO 240
CHI=CHISQR
PRINT 100
CALL MSGG('NEW PARMS',9)
PRINT 100
PRINT 100,(A1(L),L=1,NPARM)
PRINT 100
CALL MSGG('OBJECTIVE FCN',13)
PRINT 100,CHI
PRINT 100
CALL MSGG('PARM VARIANCE',13)
PRINT 3300,(ITERM(L),SIGMAA(L),L=1,NUI)
PRINT 100
STORE(1)=CHI
DO 20 L=1,NPARM
STORE(1+L)=A1(L)
20 CONTINUE
DO 90 L=1,NUI
STORE(1+NPARM+L)=SIGMAA(L)
90 CONTINUE
EZMN1510
EZMN1520
EZMN1530
EZMN1540
EZMN1550
EZMN1560
EZMN1570
EZMN1580
EZMN1590
EZMN1600
EZMN1610
EZMN1620
EZMN1630
EZMN1640
EZMN1650
EZMN1660
EZMN1670
EZMN1680
EZMN1690
EZMN1700
EZMN1710
EZMN1720
EZMN1730
EZMN1740
EZMN1750
EZMN1760
EZMN1770
EZMN1780
EZMN1790
EZMN1800
EZMN1810
EZMN1820
EZMN1830
EZMN1840
EZMN1850
EZMN1860
EZMN1870
EZMN1880
EZMN1890
EZMN1900
EZMN1910
EZMN1920
EZMN1930
EZMN1940
EZMN1950
EZMN1960
EZMN1970
EZMN1980
EZMN1990
EZMN2000

```

```

EZMN2010
EZMN2020
EZMN2030
EZMN2040
EZMN2050
EZMN2060
EZMN2070
EZMN2080
EZMN2090
EZMN2100
EZMN2110
EZMN2120
EZMN2130
EZMN2140
EZMN2150
EZMN2160
EZMN2170
EZMN2180
EZMN2190
EZMN2200
EZMN2210
EZMN2220
EZMN2230
EZMN2240
EZMN2250
EZMN2260
EZMN2270
EZMN2280
EZMN2290
EZMN2300
EZMN2310
EZMN2320
EZMN2330
EZMN2340
EZMN2350
EZMN2360
EZMN2370
EZMN2380
EZMN2390
EZMN2400
EZMN2410
EZMN2420
EZMN2430
EZMN2440
EZMN2450
EZMN2460
EZMN2470
EZMN2480
EZMN2490
EZMN2500

IF(I.EQ.1)CALL CPUTIM(STIME)
CALL CPUTIM(TIME,ST2)
CALL MSGG('ELAPSED TIME',12)
PRINT 100,ST2
PRINT 100
PRINT 100

C
      CHECK TIME
      IF(ISTATE(2).EQ.9.OR.ISTATE(2).EQ.8) GO TO 250
      IF(I.EQ.1.AND.(2*STIME).GT.TMAX) GO TO 210
      IF((TIME+STIME).LT.TMAX.AND.(TIME+ST2).LT.TMAX) GO TO 5
210  CONTINUE
      PRINT 900
      GO TO 8
5    CONTINUE
      CALL MSGG('NO CONVERGENCE IN 20 ITERATIONS',31)
      GO TO 8
220  CONTINUE
      CALL MSGG('OBJECTIVE FCN INCREASED',23)
      GO TO 8
230  CONTINUE
      PRINT 3100,EPS
      GO TO 8
240  CONTINUE
      CALL MSGG('NO IMPROVEMENT CVER INITIAL',27)
      GO TO 8
250  CONTINUE
      CALL MSGG('NO REGRESSION MADE',18)
      GO TO 8

C      CONVERGED OUTPUT
8    CONTINUE
      CHISQR=STORE(1)
      DO 170 L=1,NPARM
      A1(L)=STORE(1+L)
170  CONTINUE
1110 CONTINUE
      PRINT 300,NPART,I
      DO 120 L=1,NU1
      SIGMAA(L)=STORE(1+NPARM+L)
120  CONTINUE
      NDIM=NPARM+N
      NPART=NPART+1
      PRINT 600,NAME,NCODE
      PRINT 100
      PRINT 2100
      DO 60 J=1,NU1
      JJ=ITERM(J)
      SE=SQRT(SIGMAA(J)*CHISQR)
      ASE=0
      IF(SE.NE.0)ASE=(A1(JJ)/SE)**2
      PRINT 100,JJ,A1(JJ),SE,SIGMAA(J),ASE

```

```

60 CONTINUE
PRINT 100
C          CALCULATE STATISTICS
PRINT 2200,CHISQR,DF
NU2=NPTS-NU1-1
CHIN=CHISQR*(NU2+1)
FR=(1-CHIN/YVAR)*NU2*YVAR/CHIN/NU1
FCHI=(CHI1-CHIN)*NU2/CHIN
CHI1=CHIN
PRINT 200,FR,FCHI,NU1,NU2
PRINT 100
PRINT 100
SAVE=ISTATE(4)
ISTATE(4)=0.
C          OUTPUT RESULTS FOR DATA POINTS
CALL OUTPUT(X,N,Y,NPTS,NPARM,A1,WEIGHT,DATAID,ND)
ISTATE(4)=SAVE
40 CONTINUE
STOP
END

```

```

EZMN2510
EZMN2520
EZMN2530
EZMN2540
EZMN2550
EZMN2560
EZMN2570
EZMN2580
EZMN2590
EZMN2600
EZMN2610
EZMN2620
EZMN2630
EZMN2640
EZMN2650
EZMN2660
EZMN2670
EZMN2680
EZMN2690
EZMN2700

```

C	SUBROUTINE CONVR	EZCN0010
C		EZCN0020
C	PURPOSE	EZCN0030
C	CONVERTS A 4 DIGIT INTEGER INTO EBCDIC CODE	EZCN0040
C		EZCN0050
C	USAGE	EZCN0060
C	CALL CONVR(INUM,ICHAR,CHAR)	EZCN0070
C		EZCN0080
C	DESCRIPTION OF PARAMETERS	EZCN0090
C	INUM - INTEGER TO BE CONVERTED	EZCN0100
C	FCHAR - EBCDIC CODE IN AN INTEGER VARIABLE	EZCN0110
C	CHAR - EBCDIC CODE IN A REAL VARIABLE	EZCN0120
C		EZCN0130
	SUBROUTINE CONVR(INUM,ICHAR,CHAR)	EZCN0140
	EQUIVALENCE(IDUM,DUM)	EZCN0150
	ICHAR=0	EZCN0160
	IFACT=1	EZCN0170
	I=INUM	EZCN0180
	DO 40 J=1,4	EZCN0190
	I10=I/10	EZCN0200
	ICHAR=(I-I10*10+240)*IFACT+ICHAR	EZCN0210
	I=I10	EZCN0220
	IFACT=IFACT*256	EZCN0230
40	CONTINUE	EZCN0240
	IDUM=ICHAR	EZCN0250
	CHAR=DUM	EZCN0260
	RETURN	EZCN0270
	END	EZCN0280

C	FUNCTION CP	EZCP0010
C		EZCP0020
C	PURPOSE	EZCP0030
C	CALCULATES HEAT CAPACITY OF PRESSURE BY NUMERICAL DERIV.	EZCP0040
C		EZCP0050
C	USAGE	EZCP0060
C	RESULT = CP(T,RHO)	EZCP0070
C		EZCP0080
C	DESCRIPTION OF PARAMETERS	EZCP0090
C	T-ABSOLUTE TEMPERATURE	EZCP0100
C	RHO-DENSITY	EZCP0110
C		EZCP0120
C	SUBROUTINES NEEDED	EZCP0130
C	ENTH(T,RHO)	EZCP0140

EZCP0150
EZCP0160
EZCP0170
EZCP0180
EZCP0190
EZCP0200
EZCP0210
EZCP0220
EZCP0230
EZCP0240
EZCP0250
EZCP0260
EZCP0270
EZCP0280
EZCP0290
EZCP0300
EZCP0310
EZCP0320
EZCP0330
EZCP0340
EZCP0350
EZCP0360
EZCP0370
EZCP0380
EZCP0390
EZCP0400
EZCP0410
EZCP0420
EZCP0430
EZCP0440
EZCP0450
EZCP0460
EZCP0470
EZCP0480
EZCP0490

```

C      CALCULATES ENTHALPY
C
      FUNCTION CP(T,RHO)
      COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
      1  ,A(40),B(7),NTERM,S,NPAKM,NUMB,RTOP,RMIDL,RMIDV
      EPSMAX=.1
      EPS=.0001
      SAVE=T
      IF (ABS(SAVE).LT.EPS) GO TO 10
      DEL=ABS(EPS*SAVE)
      14 CONTINUE
      DO 12 IT=1,5
      T=SAVE+DEL
      F2=ENTH(T,RHO)
      T=SAVE-DEL
      F1=ENTH(T,RHO)
      DFDX=(F2-F1)/2./DEL

      TESTS PRECISION OF DERIVATIVE
      IF (ABS(DEL*2*DFDX).GE.((10**(-6+N))*ABS(F1))) GO TO 40
      IF (ABS(DFDX).LT.1.1E-65*ABS(F1)) DFDX=1.E-65*F1
      DEL=((10**(-6+N))*ABS(F1)/DFDX)
      IF (ABS(SAVE).LT.1.E-06) GO TO 20
      IF (DEL.GT.ABS(SAVE*EPMAX)) DEL=ABS(SAVE*EPMAX)
      GO TO 12
      20 IF (DEL.GT.EPMAX) DEL=EPMAX
      12 CONTINUE
      GO TO 40
      10 DEL=EPS
      GO TO 14
      40 CP=DFDX
      T=SAVE
      RETURN
      END

```

EZCR0010
EZCR0020
EZCR0030
EZCR0040
EZCR0050
EZCR0060
EZCR0070

```

C      SUBROUTINE CURFIT
C
C      PURPOSE
C      MAKE A LEAST-SQUARES FIT TO A NON-LINEAR FUNCTION
C      WITH A LINEARIZATION OF THE FITTING FUNCTION
C
C      USAGE

```

C	CALL CURFIT (X,N,Y,WEIGHT,NPTS,NTERMS,A,	EZCR0080
C	SIGMAA,FLAMDA,YFIT,CHISQR,NPARM,ITERM)	EZCR0090
C		EZCR0100
C	DESCRIPTION OF PARPMETERS	EZCR0110
C	X - ARRAY OF DATA POINTS FOR INDEPENDENT VARIABLE	EZCR0120
C	Y - ARRAY OF DATA POINTS FOR DEPENDENT VARIABLE	EZCR0130
C	WEIGHT - ARRAY OF WEIGHTS FOR DATA POINTS	EZCR0140
C	N - NUMBER OF INDEPENDENT VARIABLES	EZCR0150
C	NPTS - NUMBER OF PAIRS OF DATA POINTS	EZCR0160
C	NTERMS - NUMBER OF PARAMETERS	EZCR0170
C	A - ARRAY OF PARAMETERS	EZCR0180
C	SIGMAA - ARRAY OF STANDARD DEVIATIONS FOR PARAMETERS A	EZCR0190
C	FLAMDA - PROPORTION OF GRADIENT SEARCH INCLUDED	EZCR0200
C	YFIT - ARRAY OF CALCULATED VALUES OF Y	EZCR0210
C	CHISQ1 - REDUCED CHI SQUARE FOR FIT	EZCR0220
C	ITERMS - ARRAY OF INDICES TO BE REGRESSED	EZCR0230
C		EZCR0240
C	SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED	EZCR0250
C	FUNCN (X,NDIM)	EZCR0260
C	EVALUATES THE FITTING FUNCTION	EZCR0270
C	FCHISQ (Y,WEIGHT,NPTS,NFREE,YFIT)	EZCR0280
C	EVALUATES REDUCED CH SQUARE FOR FIT TO DATA	EZCR0290
C	FDERIV (X,I,NDIM)	EZCR0300
C	EVALUATES THE DERIVATIVES OF THE FITTING FUNCTION	EZCR0310
C	WITH RESPECT TO THE ITH VARIABLE	EZCR0320
C	GJEL(ARRAY,NTERMS,NTERMS+1,DET,IER)	EZCR0330
C	SOLVES A SYSTEM BY THE GAUSS JORDAN METHOD RETURNING THE	EZCR0340
C	DETERMINANT AND THE INVERSE IN PLACE	EZCR0350
C		EZCR0360
C		EZCR0370
C	COMMENTS	EZCR0380
C	DIMENSION STATEMENT VALID FOR NTERMS UP TO 10	EZCR0390
C	SET FLAMDA =0.001 AT BEGINNING OF SEARCH	EZCR0400
C		EZCR0410
C	SUBROUTINE CURFIT (X,N,Y,WEIGHT,NPTS,NTERMS,A,	EZCR0420
C	1 SIGMAA,FLAMDA,YFIT,CHISQR,NPARM,ITERM)	EZCR0430
C	COMMON /DAT/IPRES,ISTATE(20)	EZCR0440
C	DOUBLE PRECISION ALPHA,DSQRT,ARRAY	EZCR0450
C	DOUBLE PRECISION DABS	EZCR0460
C	DIMENSION X(NPTS,N),Y(NPTS),WEIGHT(NPTS),YFIT(NPTS)	EZCR0470
C	DIMENSION SIGMAA(NPARM),A(NPARM),ITERM(NPARM)	EZCR0480
C	DIMENSION ALPHA(1830),BETA(60),DERIV(60),ARRAY(3660),B(60),Z(110)	EZCR0490
C	DATA IC/S/	EZCR0500
C	DATA IBD/O/	EZCR0510
C	100 FORMAT (1X,8G14.6)	EZCR0520
C	700 FORMAT(1X,I3,' ',8(I3,' ',G10.3),/(5X,8(I3,' ',G10.3)))	EZCR0530
C	IF(IBD.EQ.1) GO TO 5000	EZCR0540
C	IBD=1	EZCR0550
C	CALL LBLEZ	EZCR0560
C	5000 CONTINUE	EZCR0570

```

FACT=.99
SUM1=0.
IF(NTERMS.LE.60) GO TO 6000
PRINT 600
FORMAT(1X,10('*.').* MORE THAN 35 PARAMETERS FITTED. ONLY 60*.
4 6(4X, '*/')////)
NTERMS=60
6000 CONTINUE
NPN=N+NPARM
11 NFREE =NPTS-NTERMS
13 IF (NFREE) 13,13,20
13 CONTINUE
2700 PRINT 2700,NFREE
FORMAT(//,*,DEGRES OF FREEDOM *,14,*, IS LESS THAN 1. */)
FLAMDA =1000.
CHISQR=1.E+55
GO TO 110

C
C
C
EVALUATE ALPHA AND BETA MATRICES
C
20 CONTINUE
31 DO 34 J=1,NTERMS
BETA(J)=0
DO 34 K=1,J
34 ALPHA(K+J*(J-1)/2)=0
NOTE - 1ST N OF Z ARE VARIABLES. (N+1-NTERMS) ARE PARAMETERS
44 Z(L+N)=A(L)
DO 230 J=1,NTERMS
ARRAY(J)=0
230 CONTINUE
IF(ISTATE(2).LE.3)PRINT 3900
3900 FURMAT(4X,'Y',13X,'YFIT',10X,'PERCENT')
41 DO 45 L=1,N
DO 45 L=1,N
45 Z(L)=X(L,L)
ISTATE(1)=1
62 YFIT(1)=FUNCN(2,NPN)
IF(Y(1).EQ.0) GO TO 290
PERC=100*(Y(1)-YFIT(1))/Y(1)
SUM1=SUM1+ABS(PERC)
290 CONTINUE
IF(ISTATE(2).GT.3) GO TO 220
IF(IC.LT.5.AND.FLAMDA.EQ.0) GO TO 220
210 PRINT 100, Y(1),YFIT(1),PERC
220 CONTINUE
DO 43 L=1,NTERMS
JJ=ITERM(L)+N
DERIV(L)=FDERIV(Z,JJ,NPN)
ARRAY(L)=ARRAY(L)+ABS(DERIV(L))
EZCR0580
EZCR0590
EZCR0600
EZCR0610
EZCR0620
EZCR0630
EZCR0640
EZCR0650
EZCR0660
EZCR0670
EZCR0680
EZCR0690
EZCR0700
EZCR0710
EZCR0720
EZCR0730
EZCR0740
EZCR0750
EZCR0760
EZCR0770
EZCR0780
EZCR0790
EZCR0800
EZCR0810
EZCR0820
EZCR0830
EZCR0840
EZCR0850
EZCR0860
EZCR0870
EZCR0880
EZCR0890
EZCR0900
EZCR0910
EZCR0920
EZCR0930
EZCR0940
EZCR0950
EZCR0960
EZCR0970
EZCR0980
EZCR0990
EZCR1000
EZCR1010
EZCR1020
EZCR1030
EZCR1040
EZCR1050
EZCR1060
EZCR1070

```



```

      IF (ABS(DERIV(L)).LT.1.E-30) DERIV(L)=0.
43  CONTINUE
      DO 46 J=1,NTERMS
      IF (FLAMDA.GE.0)
18  BETA(J)=BETA(J)+WEIGHT(I)*(Y(I)-YFIT(I))*DERIV(J)
      IF (FLAMDA.LT.0) BETA(J)=BETA(J)+WEIGHT(I)*Y(I)*DERIV(J)
      DO 46 K=1,J
      ALPHA(K+J*(J-1)/2)=ALPHA(K+J*(J-1)/2)+WEIGHT(I)*DERIV(J)*DERIV(K)
46  CONTINUE
50  CONTINUE
      SUM1=SUM1/NPTS
      PRINT 100
      CALL MSGG('AVERAGE ABSOLUTE DEVIATION',.26)
      PRINT 100,SUM1
      IC=IC+1
      IF (IC.GT.5) IC=1
      EVALUTAE CHI SQUARE AT STARTING POINT
C
C
C
63  CHISQ1 = FCHISQ(Y,WEIGHT,NPTS,NFREE,YFIT)
      CALL MSGG('INITIAL VALUE OF OBJECTIVE FCN',.30)
      PRINT 100,CHISQ1
      DO 240 J=1,NTERMS
      ARRAY(J)=ARRAY(J)/NPTS
240  CONTINUE
      PRINT 100
      CALL MSGG('AVERAGE ABSOLUTE DERIVATIVE OF FCN',.34)
      PRINT 3300,(ITERM(J),ARRAY(J),J=1,NTERMS)
      FORMAT(1X,8(I3,.,.,G10.3),/ (1X,8(I3,.,.,G10.3)))
3300
C
C
C
      INVERT MODIFIED CURVATURE MATRIX TO FIND NEW PARAMETERS
71  CONTINUE
      DIAG=1
      IF (FLAMDA.GT.0) DIAG=DIAG+FLAMDA
      DO 74 J=1,NTERMS
      IF (ALPHA(J*(J+1)/2).GT.0) GO TO 280
      JJ=ITERM(J)
      PRINT 300,J,JJ
      FORMAT(1X,15,.,. DERIVATIVE IS NOT POS. FOR PARAM ',I5.20(.,.,.))
      ALPHA(J*(J+1)/2)=1.E-40
280  CONTINUE
      ARRAY(NTERMS**2+J)=BETA(J)/DSQRT(ALPHA(J*(J+1)/2))
      DO 73 K=1,J
      ARRAY(J+(K-1)*NTERMS)=ALPHA(K+J*(J-1)/2)/DSQRT(ALPHA(J*(J+1)/2))
1  *ALPHA(K*(K+1)/2))
      ARRAY(K+(J-1)*NTERMS)=ARRAY(J+(K-1)*NTERMS)
73  CONTINUE
74  ARRAY(J+(J-1)*NTERMS)=DIAG
      DELM=0.
EZCR1080
EZCR1090
EZCR1100
EZCR1110
EZCR1120
EZCR1130
EZCR1140
EZCR1150
EZCR1160
EZCR1170
EZCR1180
EZCR1190
EZCR1200
EZCR1210
EZCR1220
EZCR1230
EZCR1240
EZCR1250
EZCR1260
EZCR1270
EZCR1280
EZCR1290
EZCR1300
EZCR1310
EZCR1320
EZCR1330
EZCR1340
EZCR1350
EZCR1360
EZCR1370
EZCR1380
EZCR1390
EZCR1400
EZCR1410
EZCR1420
EZCR1430
EZCR1440
EZCR1450
EZCR1460
EZCR1470
EZCR1480
EZCR1490
EZCR1500
EZCR1510
EZCR1520
EZCR1530
EZCR1540
EZCR1550
EZCR1560
EZCR1570

```

```

      IF (NTERMS.GT.1) GO TO 80
      ARRAY(1)=1/ARRAY(1)
      ARRAY(2)=ARRAY(2)*ARRAY(1)
      GO TO 81
80  CALL GJEL(ARRAY,NTERMS,NTERMS+1,DET,IER)
      PRINT 100
      IF(ISTATE(2).EQ.8) GO TO 340
      IF(ISTATE(2).EQ.9) GO TO 260
81  DO 84 J=1,NTERMS
      JJ=ITERM(J)
      IF(DABS(ARRAY(NTERMS*2+J)).LT.DELM) GO TO 250
      DELM=DAES(ARRAY(NTERMS*2+J))
      JM=JJ
250  CONTINUE
      B(J)=A(JJ)+ARRAY(NTERMS*2+J)/DSQRT(ALPHA(J*(J+1)/2))
      IF(ISTATE(3).EQ.0.OR.B(J)*A(JJ).GT.0) GO TO 84
      CALL MSGG('OLD,NEW,PARM SIGN CHANGE',24)
      PRINT 100,B(J),A(JJ),JJ
      B(J)=A(JJ)*(1-FACT)
84  CONTINUE
      CALL MSGG('MAX SCALED PARM DELTA,PARM NO.',30)
      PRINT 100,DELM,JM

C
C
C   IF CHI SQAKE INCREASED, INCREASE FLAMDA AND TRY AGAIN
      DO 94 L=1,NTERMS
      JJ=ITERM(L)
94  Z(JJ+N)=B(L)
91  DO 92 I=1,NPTS
96  Z(L)=X(I,L)
92  ISTATE(1)=I
93  YFIT(I)=FUNCN(Z,NPN)
      CHISQR = FCHISO(Y,WEIGHT,NPTS,NFREE,YFIT)
      CALL MSGG('TRIAL OBJECTIVE FCN',19)
      PRINT 100,IPRES,CHISQR
      IF(FLAMDA.LE.0) GO TO 101
      IF (CHISQ1-CHISQR) 95,101,101
95  FLAMDA =10*FLAMDA
      FACT=FACT/2.
      IF(FLAMDA.GT.1000) GO TO 135
      IF(FLAMDA.GT.0.01) GO TO 71
115  DO 125 I=1,NTERMS
125  SIGMAA(I)=ARRAY(I+(I-1)*NTERMS)/DSQRT(ALPHA(I*(I+1)/2))
      GO TO 71
340  CONTINUE
C   OUTPUT REGRESSION COEFFICIENTS
      PRINT 100
      CALL MSGG('CORRELATION COEFFICIENTS',24)
      PRINT 100
EZCR1580
EZCR1590
EZCR1600
EZCR1610
EZCR1620
EZCR1630
EZCR1640
EZCR1650
EZCR1660
EZCR1670
EZCR1680
EZCR1690
EZCR1700
EZCR1710
EZCR1720
EZCR1730
EZCR1740
EZCR1750
EZCR1760
EZCR1770
EZCR1780
EZCR1790
EZCR1800
EZCR1810
EZCR1820
EZCR1830
EZCR1840
EZCR1850
EZCR1860
EZCR1870
EZCR1880
EZCR1890
EZCR1900
EZCR1910
EZCR1920
EZCR1930
EZCR1940
EZCR1950
EZCR1960
EZCR1970
EZCR1980
EZCR1990
EZCR2000
EZCR2010
EZCR2020
EZCR2030
EZCR2040
EZCR2050
EZCR2060
EZCR2070

```

```

DO 320 I=1,NTERMS
DO 330 J=1,I
II=I+(I-1)*NTERMS
330 B(J)=ARRAY(I+(J-1)*NTERMS)/DSQRT(ARRAY(II)*ARRAY(J+(J-1)*NTERMS))
320 PRINT 700,ITERM(I),(ITERM(JJ),B(JJ),JJ=1,I)
CONTINUE
260 PRINT 100
CONTINUE
DO 270 J=1,NTERMS
SIGMAA(J)=ARRAY(J+(J-1)*NTERMS)/DSQRT(ALPHA(J*(J+1)/2))
270 CONTINUE
CHISQR=CHISQ1
RETURN

C
C
C      EVALUATE PARAMETERS AND UNCERTAINTIES

101 DO 103 J=1,NTERMS
JJ=ITERM(J)
A(JJ)=B(JJ)
IF(ARRAY(J+(J-1)*NTERMS).GT.0) GO TO 103
PRINT 400,J,JJ
400 FORMAT(1X,10(*),' VARIANCE ',13,' FOR PARAMETER ',13,
1 ' IS NEGATIVE. CORRECTION TAKEN..2X,10(*))
ARRAY(J+(J-1)*NTERMS)=1.E-30
103 SIGMAA(J)=ARRAY(J+(J-1)*NTERMS)/DSQRT(ALPHA(J*(J+1)/2))
FLAMDA =FLAMDA/10.
IF(ISTATE(2).GT.4) GO TO 110
C      OUTPUT REGRESSION COEFFICIENTS
PRINT 100
CALL MESSG('CORRELATION COEFFICIENTS',24)
PRINT 100
DO 350 I=1,NTERMS
II=I+(I-1)*NTERMS
DO 360 J=1,I
360 B(J)=ARRAY(I+(J-1)*NTERMS)/DSQRT(ARRAY(II)*ARRAY(J+(J-1)*NTERMS))
PRINT 700,ITERM(I),(ITERM(JJ),B(JJ),JJ=1,I)
350 CONTINUE
PRINT 100
GO TO 110
135 DO 140 L=1,NPARM
140 Z(L+N)=A(L)
DO 150 I=1,NPTS
DO 160 L=1,N
160 Z(L)=X(I,L)
ISTATE(I)=I
150 YFIT(I)=FUNCN(Z,NPN)
CHISQR=CHISQ1
110 RETURN
END

```

```

EZCR2080
EZCR2090
EZCR2100
EZCR2110
EZCR2120
EZCR2130
EZCR2140
EZCR2150
EZCR2160
EZCR2170
EZCR2180
EZCR2190
EZCR2200
EZCR2210
EZCR2220
EZCR2230
EZCR2240
EZCR2250
EZCR2260
EZCR2270
EZCR2280
EZCR2290
EZCR2300
EZCR2310
EZCR2320
EZCR2330
EZCR2340
EZCR2350
EZCR2360
EZCR2370
EZCR2380
EZCR2390
EZCR2400
EZCR2410
EZCR2420
EZCR2430
EZCR2440
EZCR2450
EZCR2460
EZCR2470
EZCR2480
EZCR2490
EZCR2500
EZCR2510
EZCR2520
EZCR2530
EZCR2540
EZCR2550
EZCR2560

```

```

C          FUNCTION CV
C
C          PURPOSE
C          CALCULATES HEAT CAPACITY OF SPECIFIC VOLUME BY NUMERICAL DERIV.
C
C          USAGE
C          RESULT = CV(T,RHO)
C
C          DESCRIPTION OF PARAMETERS
C          T-ABSOLUTE TEMPERATURE
C          RHO-DENSITY
C
C          SUBROUTINES NEEDED
C          U(T,RHO)
C          CALCULATES INTERNAL ENERGY
C
C          FUNCTION CV(T,RHO)
C          COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
C          1      ,A(4,0),B(7),NTERMS,NPARAM,NUMB,RTOP,RMIDL,RMIDV
C          EPS=.0001
C          SAVE=T
C          IF(ABS(SAVE).LT.EPS) GO TO 10
C          DEL=ABS(EPS*SAVE)
C
C          14 CONTINUE
C          DO 12 IT=1,5
C          T=SAVE+DEL
C          F2=U(T,RHO)
C          T=SAVE-DEL
C          F1=U(T,RHO)
C          DFDX=(F2-F1)/2./DEL
C
C          TESTS PRECISION OF DERIVATIVE
C
C          IF(ABS(DEL*2*DFDX).GE.((10**(-6+N))*ABS(F1)))GO TO 40
C          IF(ABS(DFDX).LT.1.1E-65*ABS(F1)) DFDX=1.1E-65*F1
C          DEL=((10**(-6+N))*ABS(F1/DFDX))
C          IF(ABS(SAVE).LT.1.1E-06) GO TO 20
C          IF(DEL.GT.ABS(SAVE*EPMAX)) DEL=ABS(SAVE*EPMAX)
C          GO TO 12
C
C          20 IF (DEL.GT.EPMAX) DEL=EPMAX
C          12 CONTINUE
C          GO TO 40
C          10 DEL=EPS
C          GO TO 14
C          40 CV=DFDX
C          T=SAVE

```

```

EZCV0010
EZCV0020
EZCV0030
EZCV0040
EZCV0050
EZCV0060
EZCV0070
EZCV0080
EZCV0090
EZCV0100
EZCV0110
EZCV0120
EZCV0130
EZCV0140
EZCV0150
EZCV0160
EZCV0170
EZCV0180
EZCV0190
EZCV0200
EZCV0210
EZCV0220
EZCV0230
EZCV0240
EZCV0250
EZCV0260
EZCV0270
EZCV0280
EZCV0290
EZCV0300
EZCV0310
EZCV0320
EZCV0330
EZCV0340
EZCV0350
EZCV0360
EZCV0370
EZCV0380
EZCV0390
EZCV0400
EZCV0410
EZCV0420
EZCV0430
EZCV0440
EZCV0450
EZCV0460
EZCV0470
EZCV0480
EZCV0490
EZCV0500

```

EZCV0510
EZCV0520

RETURN
END

```

C      SUBROUTINE DATA
C
C      PURPOSE
C      INPUTS DATA TO EZFIT IN PREBANKED FORMAT
C
C      MODE - DETERMINES METHOD OF WEIGHTING LEAST-SQUARES FIT
C              +1 (INSTRUMENTAL) WEIGHT(I)=U/SIGMAY(I)**2
C              PERCENT ERROR CONSTANT
C              0 (NO WEIGHTING) WEIGHT(I)=1
C              -1 (STATISTICAL) WEIGHT =1/Y(I)
C
C      SUBROUTINE DATA (X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,NPTRHO,
C      1 NPTH,NPTVP,DATAID)
C      1100 FORMAT(8F10.0)
C      1200 FORMAT(16I5)
C      1300 FORMAT(3F10.0,110)
C      1500 FORMAT(2A4,I2,7F10.0)
C      DIMENSION X(NPTS,N),Y(NPTS),WEIGHT(NPTS)
C      1 ,DATAID(NPTS,N)
C      COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
C      1 ,A(40),B(7),NTERMS,NPARM,NUMB,RTDP,RMIDL,RMIDV
C      COMMON /PRP/ICOMP(20),CPC(20),CMW(20),CW(20),CTC(20)
C      1 ,CA(20),CB(20),CNAME(20,2)
C      INTEGER CODE
C      REAL NAME(40,2)
C      NPTRHO=0
C      NPTH=0
C      NPTVP=0
C      READ 1200,NCOMP
C      DO 30 L=1,NCOMP
C      READ 1500,(CNAME(L,J),J=1,2),IWHOLE,CTC(L),CPC(L),CMW(L),
C      1 CW(L),CA(L),CB(L)
C      ICCOMP(L)=IWHOLE
C      30 CONTINUE
C      DO 40 I=1,NPTS
C      READ 1400,X(1,2),X(1,3),X(1,1),Y(I),(DATAID(I,J),J=1,3)
C      1400 FORMAT(2X,4F10.4,26X,3A4)
C      WEIGHT(I)=Y(I)
C      IWHOLE=ABS(X(1,1))+.005
C      IF(IWHOLE.GT.99) GO TO MIXTURE
C      IFRACT=(ABS(X(1,1))-IWHOLE+.005)*100

```

EZD10010
EZD10020
EZD10030
EZD10040
EZD10050
EZD10060
EZD10070
EZD10080
EZD10090
EZD10100
EZD10110
EZD10120
EZD10130
EZD10140
EZD10150
EZD10160
EZD10170
EZD10180
EZD10190
EZD10200
EZD10210
EZD10220
EZD10230
EZD10240
EZD10250
EZD10260
EZD10270
EZD10280
EZD10290
EZD10300
EZD10310
EZD10320
EZD10330
EZD10340
EZD10350
EZD10360
EZD10370
EZD10380
EZD10390
EZD10400

```

C      IF (IFRACT.EQ.0)NPTRHQ=NPTRHC+1
C      IF (IFRACT.EQ.10)NPTH=NPTH+1
C      IF (IFRACT.EQ.20)NPTVP=NPTVP+1
40  CONTINUE
C      CALCULATE AVERAGE AND VARIANCE
C      SUM=0
C      SUMW=0
C      DO 60 I=1,NPTS
C          EVALUATE WEIGHTS
C          IF (NCODE) 1,2,3
1      IF (Y(I).EQ.0) GO TO 2
C      WEIGHT(I)=1/ABS(Y(I))
C      GO TO 10
2      WEIGHT(I)=1
C      GO TO 10
3      WEIGHT(I)=1/WEIGHT(I)**2
10  CONTINUE
C      SUM=SUM+WEIGHT(I)*Y(I)
C      SUMW=SUMW+WEIGHT(I)
60  CONTINUE
C      SUM=SUM/SUMW
C      YBAR=SUM
C      SUMY=0
C      DO 50 I=1,NPTS
C      SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2
50  CONTINUE
C      YVAR=SUMY*NPTS/SUMW/(NPTS-1)
C      RETURN
C      END

```

EZD10410
EZD10420
EZD10430
EZD10440
EZD10450
EZD10460
EZD10470
EZD10480
EZD10490
EZD10500
EZD10510
EZD10520
EZD10530
EZD10540
EZD10550
EZD10560
EZD10570
EZD10580
EZD10590
EZD10600
EZD10610
EZD10620
EZD10630
EZD10640
EZD10650
EZD10660
EZD10670
EZD10680
EZD10690
EZD10700
EZD10710

```

C      SUBROUTINE DATA2
C      PURPOSE
C      INPUTS DATA TO EZFIT FROM THE ORIGINAL STARLING-HAN FORMAT
C      SUBROUTINE DATA2(X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,NPTRHQ,
1      NPTH,NPTVP,DATAID)
100  FORMAT(1X,8G14.6)
1100 FORMAT(8F10.0)
1200 FORMAT(16I5)
1300 FORMAT(3F10.0,110)

```

EZD20010
EZD20020
EZD20030
EZD20040
EZD20050
EZD20060
EZD20070
EZD20080
EZD20090
EZD20100
EZD20110

```

1600 FORMAT(4I5,F10.0 )
1800 DIMENSION X(NPTS,N),Y(NPTS),WEIGHT(NPTS)
      1 DATAID(NPTS,N)
      COMMON /PRM/RGAS,RENGRY,ICRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
      1 ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
      COMMON /PRP/ICOMP(20),CPC(20),CRC(20),CMW(20),CW(20) ,CTC(20)
      1 ,CA(20),CB(20),CNAME(20,2)
      DATA D1,D2/, 006*,*,5 */
      INTEGER CODE
      REAL NAME(40,2)
      NPTL=0
      NPTRHD=0
      NPTH=0
      NPV=0
      CALL MSGG('DATA INPUT SUMMARY',18)
      READ 1200,NCUMP
      CALL MSGG('NUMBER OF COMPONENTS',20)
      PRINT 100,NCUMP
      CALL MSGG('DENSITY,ENTHALPY, V.P. , PRESET,GRUP WEIGHT',47)
      DO 30 L=1,NCUMP
      READ 1500,(CNAME(L,J),J=1,2),IWHOLE,CTC(L),CPC(L),CRC(L),CMW(L),
      1 CW(L),CA(L),CB(L)
      1500 FORMAT(2A4,I2,7F10.0)
      ICOMP(L)=IWHOLE
      ICRIT=CTC(L)
      RHOC=CRC(L)
      READ 1600,NPTRHL,NPTHL,NPTVPL,NPTA,SCALE
      PRINT 1800,NPTRHL,NPTHL,NPTVPL,NPTA,SCALE,CNAME(L,1)
      IF(SCALE.EQ.0.) SCALE=1.
      SCALE=SQRT(SCALE)
      IF(NPTA.EQ.0) GO TO 160
      DO 140 JA=1,NPTA
      I=NPTL+JA
      READ 1400,X(1,2),X(1,3),X(1,1),Y(1),(DATAID(1,J),J=1,3)
      1400 FORMAT(2X,4F10.4,26X,3A4)
      WEIGHT(1)=Y(1)/SCALE
      IWHOLE=ABS(X(1,1))+.005
      IF(IWHOLE.GT.99) GO TO MIXTURE
      IFRACT=(ABS(X(1,1))-IWHOLE+.005)*100
      IF(IFRACT.EQ.0)NPTRHD=NPTRHC+1
      IF(IFRACT.EQ.10)NPTH=NPTH+1
      IF(IFRACT.EQ.20)NPV=NPV+1
      140 CONTINUE
      NPTL=NPTL+NPTA
      160 CONTINUE
      IF(NPTRHL.EQ.0) GO TO 130
      DO 70 J=1,NPTRHL
      I=NPTL+J
      DATAID(1,1)=D1

```

```

EZD20120
EZD20130
EZD20140
EZD20150
EZD20160
EZD20170
EZD20180
EZD20190
EZD20200
EZD20210
EZD20220
EZD20230
EZD20240
EZD20250
EZD20260
EZD20270
EZD20280
EZD20290
EZD20300
EZD20310
EZD20320
EZD20330
EZD20340
EZD20350
EZD20360
EZD20370
EZD20380
EZD20390
EZD20400
EZD20410
EZD20420
EZD20430
EZD20440
EZD20450
EZD20460
EZD20470
EZD20480
EZD20490
EZD20500
EZD20510
EZD20520
EZD20530
EZD20540
EZD20550
EZD20560
EZD20570
EZD20580
EZD20590
EZD20600
EZD20610

```

```

DATAID(I,2)=D2
READ 2100,T,P,RHO,CODE
T=T+460
CODE=-1
IF(RHO.LT.RHOC)CODE=1
IF (CODE)5,6,6
5 X(I,1)=- (IWHOLE+.3)
GO TO 7
6 X(I,1)=IWHOLE+.3
7 X(I,3)=P
X(I,2)=T
Y(I)=RHO
WEIGHT(I)=Y(I)/SCALE
70 CONTINUE
NPTRHO=NPTRHO+NPTRHL
NPTRL=NPTRL+NPTRHL
130 IF(NPTRL.EQ.0) GO TO 110
DO80 J=1,NPTRL
I=NPTRL+J
DATAID(I,1)=D1
DATAID(I,2)=D2
READ 2100,T,P,DELH,CODE
2100 FORMAT(3F10.0,20X,I5)
T=T+460
IF(CODE)8,9,9
8 X(I,1)=- (IWHOLE+.4)
GO TO 11
9 X(I,1)=+IWHOLE+.4
11 X(I,2)=T
X(I,3)=P
Y(I)=DELH
WEIGHT(I)=Y(I)/SCALE
80 CONTINUE
NPTRL=NPTRL+NPTRL
NPTRL=NPTRL+NPTRL
110 IF(NPTVPL.EQ.0) GO TO 120
DO 90 J=1,NPTVPL
I=NPTRL+J
DATAID(I,1)=D1
DATAID(I,2)=D2
READ 2200,T,P
2200 FORMAT(F5.0,F10.0)
T=T+460
X(I,1)=IWHOLE+.75
X(I,2)=T
X(I,3)=P
Y(I)=P
WEIGHT(I)=Y(I)/SCALE
90 CONTINUE
NPTVP=NPTVP+NPTVPL

```

```

EZD20620
EZD20630
EZD20640
EZD20650
EZD20660
EZD20670
EZD20680
EZD20690
EZD20700
EZD20710
EZD20720
EZD20730
EZD20740
EZD20750
EZD20760
EZD20770
EZD20780
EZD20790
EZD20800
EZD20810
EZD20820
EZD20830
EZD20840
EZD20850
EZD20860
EZD20870
EZD20880
EZD20890
EZD20900
EZD20910
EZD20920
EZD20930
EZD20940
EZD20950
EZD20960
EZD20970
EZD20980
EZD20990
EZD21000
EZD21010
EZD21020
EZD21030
EZD21040
EZD21050
EZD21060
EZD21070
EZD21080
EZD21090
EZD21100
EZD21110

```


	NPTL=NPTL+NPTVPL	EZD21120
120	CONTINUE	EZD21130
30	CONTINUE	EZD21140
	NPTS=NPTL	EZD21150
C	CACULATE AVERAGE AND VARIANCE	EZD21160
	SUM=0	EZD21170
	SUMW=0	EZD21180
	DO 60 I=1,NPTS	EZD21190
	IF((DATAID(1,1).NE.D1).OR.(DATAID(1,2).NE.D2)) GO TO 170	EZD21200
	CALL CONVR(I,ICAR,DATAID(1,3))	EZD21210
170	CONTINUE	EZD21220
C		EZD21230
C	EVALUATE WEIGHTS	EZD21240
C		EZD21250
	IF (NCODE) 1,2,3	EZD21260
	1 IF (Y(I).EQ.0) GO TO 2	EZD21270
	WEIGHT(I)=1/ABS(Y(I))	EZD21280
	GO TO 10	EZD21290
	2 WEIGHT(I)=1	EZD21300
	GO TO 10	EZD21310
	3 WEIGHT(I)=1/WEIGHT(I)**2	EZD21320
10	CONTINUE	EZD21330
	SUM=SUM+WEIGHT(I)*Y(I)	EZD21340
	SUMW=SUMW+WEIGHT(I)	EZD21350
60	CONTINUE	EZD21360
	SUM=SUM/SUMW	EZD21370
	YBAR=SUM	EZD21380
	SUMY=0	EZD21390
	DO 50 I=1,NPTS	EZD21400
	SUMY=SUMY+WEIGHT(I)*(Y(I)-SUM)**2	EZD21410
50	CONTINUE	EZD21420
	YVAR=SUMY*NPTS/SUMW/(NPTS-1)	EZD21430
	RETURN	EZD21440
	END	EZD21450
C	SUBROUTINE DATA3	EZD30010
C	PURPOSE	EZD30020
C	INPUTS DATA IN BANKED FORMAT AS BLOCKED WITH GROUP WEIGHT	EZD30030
C	A NEGATIVE GROUP WEIGHT CONVERTS TO EQUAL WEIGHTS	EZD30040
C		EZD30050
	SUBROUTINE DATA3(X,N,Y,NPTS,WEIGHT,YBAR,YVAR,NCODE,DATAID,ND)	EZD30060
C	MODE - DETERMINES METHOD OF WEIGHTING LEAST-SQUARES FIT	EZD30070
C	+1 (INSTRUMENTAL) WEIGHT(I)=U/SIGMAY(I)**2	EZD30080

C	PERCENT ERROR CONSTANT	EZD30090
C	0 (NO WEIGHTING) WEIGHT(1)= 1	EZD30100
C	-1 (STATISTICAL) WEIGHT =1/Y(I)	EZD30110
	COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW	EZD30120
1	.A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV	EZD30130
	COMMON /PRP/ICOMP(20),CPC(20),CRC(20),CMW(20),CW(20),CTC(20)	EZD30140
1	.CA(20),CB(20),CNAME(20,2)	EZD30150
20	FORMAT(4F10.0,26X,I2,3A4)	EZD30160
1100	FORMAT(8F10.0)	EZD30170
1200	FORMAT(16I5)	EZD30180
1300	FORMAT(3F10.0,I10)	EZD30190
1500	FORMAT(2A4,I2,7F10.0)	EZD30200
1600	FORMAT(6F10.0)	EZD30210
1700	FORMAT(2I5,F10.0,I5)	EZD30220
	DIMENSION X(NPTS,N),Y(NPTS),WEIGHT(NPTS)	EZD30230
	DIMENSION DATAID(NPTS,ND)	EZD30240
C	DATA INPUT	EZD30250
	NPTL=0	EZD30260
	READ 1200,NBLKS	EZD30270
	ICOMP(1)=0	EZD30280
	L=1	EZD30290
	DO 300 JBLK=1,NBLKS	EZD30300
	READ 1500,(CNAME(L,J),J=1,2),IWHOLE,CTC(L),CPC(L),CRC(L),CMW(L),	EZD30310
	ICW(L),CA(L),CB(L)	EZD30320
	L1=L-1	EZD30330
	DO 160 JL=1,L1	EZD30340
	IF(ICOMP(JL).EQ.IWHOLE) GO TO 170	EZD30350
160	CONTINUE	EZD30360
	ICOMP(L)=IWHOLE	EZD30370
	L=L+1	EZD30380
	IF(L.GT.20) GO TO 180	EZD30390
	ICOMP(L)=0	EZD30400
	GO TO 170	EZD30410
180	CONTINUE	EZD30420
	PRINT 1400	EZD30430
1400	FORMAT(1X,20('*'),'MORE THAN 19 COMPOUNDS REQUESTED TO BE READ'//)	EZD30440
	STOP	EZD30450
170	CONTINUE	EZD30460
	READ 1700,IFILE,NPTA,SCALE	EZD30470
	PRINT 1800,(CNAME(L,J),J=1,2),IWHOLE,IFILE,NPTA,SCALE	EZD30480
1800	FORMAT(1X,'COMPOUND ',2A4,' ',I3,' ON UNIT',I2,' ',I5,	EZD30490
1	' DATA POINTS WITH WEIGHT ',G14.6)	EZD30500
	IWT=0	EZD30510
	IF(SCALE.GE.0) GO TO 150	EZD30520
	SCALE=ABS(SCALE)	EZD30530
	IWT=1	EZD30540
150	CONTINUE	EZD30550
	IF(SCALE.EQ.0)SCALE=1.	EZD30560
	SCALE=SQRT(SCALE)	EZD30570
	DO 40L=1,NPTA	EZD30580

```

EZD30590
EZD30600
EZD30610
EZD30620
EZD30630
EZD30640
EZD30650
EZD30660
EZD30670
EZD30680
EZD30690
EZD30700
EZD30710
EZD30720
EZD30730
EZD30740
EZD30750
EZD30760
EZD30770
EZD30780
EZD30790
EZD30800
EZD30810
EZD30820
EZD30830
EZD30840
EZD30850
EZD30860
EZD30870
EZD30880
EZD30890
EZD30900
EZD30910
EZD30920
EZD30930
EZD30940
EZD30950
EZD30960
EZD30970
EZD30980
EZD30990
EZD31000
EZD31010
EZD31020
EZD31030
EZD31040
EZD31050
EZD31060
EZD31070
EZD31080

I=NPIL+L
READ(IFILE,20,END=70)(X(I,J),J=1,3),Y(I),ICONT,(DATAID(I,K),K=1,3)
JL=3
IF(ICONT.EQ.0) GO TO 110
DO 120 JJ=1,ICONT
JS=JL+1
JL=JS+5
IF(JL.GT.N)JL=N
READ(IFILE,1600)(X(I,JJJ),JJJ=JS,JL)
120 CONTINUE
110 CONTINUE
IF(JL.EQ.N) GO TO 130
JL=JL+1
DO 140 JJ=JL,N
X(I,JJJ)=0.
140 CONTINUE
130 CONTINUE
1110 CONTINUE
C
PERCENT WEIGHTING. ASSUMES NCODE=1
WEIGHT(I)=1
IF(Y(I).NE.0) WEIGHT(I)=Y(I)
WEIGHT(I)=WEIGHT(I)/SCALE
IF(IWT.EQ.1)WEIGHT(I)=1/SCALE
40 CONTINUE
NPIL=NPIL+NPTA
300 CONTINUE
NPTS=NPIL
GO TO 80
70 CONTINUE
I=I-1
PRINT 200,I
200 FORMAT(//IX,***** TO FEW DATA. N=,G14.6)
STOP
80 CONTINUE
C
EVALUATE WEIGHTS
C
SUM=0
SUMW=0.
DO 60 I=1,NPTS
IF (NCODE) 1,2,3
1 IF (Y(I).EQ.0) GO TO 2
WEIGHT(I)=1/ABS(Y(I))
GO TO 10
2 WEIGHT(I)=1
GO TO 10
3 WEIGHT(I)=1/WEIGHT(I)**2
10 CONTINUE
SUM=SUM+WEIGHT(I)*Y(I)
SUMW=SUMW+WEIGHT(I)

```



```

210 CONTINUE
    RH02=1.01*RHO1
    P1=PRES(T,RHO1)-P0
    P2=PRES(T,RHO2)-P0
20  IF((ABS(P1-P2).LT.EPSP).OR.(ABS(RHO1-RHO2).LT.ABS(RHO2)*EPSR))
1   GO TO 40
    IF (IT.GT.ITMAX) GO TO 30
    RH03=(RHO1*P2-RHO2*P1)/(P2-P1)
    IF(RHO3.LT.RMIDL) GO TO 50
    IF(RHO3.GT.RTOP) GO TO 190
60  CONTINUE
    RHO1=RHO2
    RHO2=RHO3
    P1=P2
    IT=IT+1
    P2=PRES(T,RHO2)-P0
40  CONTINUE
    RHO1=.99*RHO2
    P1=PRES(T,RHO1)-P0
    IF(RHO2.LT.RMIDL) GO TO 30
    IF(P1.LT.P2) GO TO 130
    GO TO 30
190 CONTINUE
    RH03=RTOP*(50.+IT)/50.
    GO TO 220
50  CONTINUE
    RH03=RTOP*(50.+IT)/50.
220 CONTINUE
    IF(RHO1.LT.RHO2.AND.P1.GT.P2) GO TO 60
    RHO2=RHO1
    RHO1=RHO3
    P2=P1
    IT=IT+1
    P1=PRES(T,RHO1)-P0
    GO TO 20
30  CONTINUE
    ITMAX=40
    RH02=RTOP+DEL
    P2=PRES(T,RHO2)
    CHECK FOR STARTING PCINT
    RHO1=RTOP
    P1=PRES(T,RHO1)
    IF(P1.LT.P0)GO TO 150
70  CONTINUE
    P1=PRES(T,RHO1)
    IF(P1.LT.P0) GO TO 90
    IF(P1.LT.PMIN.AND.CODE.EQ.0.) GO TO 170
    CODE=1.
180  CONTINUE

```

```

EZDL0320
EZDL0330
EZDL0340
EZDL0350
EZDL0360
EZDL0370
EZDL0380
EZDL0390
EZDL0400
EZDL0410
EZDL0420
EZDL0430
EZDL0440
EZDL0450
EZDL0460
EZDL0470
EZDL0480
EZDL0490
EZDL0500
EZDL0510
EZDL0520
EZDL0530
EZDL0540
EZDL0550
EZDL0560
EZDL0570
EZDL0580
EZDL0590
EZDL0600
EZDL0610
EZDL0620
EZDL0630
EZDL0640
EZDL0650
EZDL0660
EZDL0670
EZDL0680
EZDL0690
EZDL0700
EZDL0710
EZDL0720
EZDL0730
EZDL0740
EZDL0750
EZDL0760
EZDL0770
EZDL0780
EZDL0790
EZDL0800
EZDL0810

```

```

      RH02=RH01
      P2=P1
      IF(RH01.LT.RMIDL) GO TO 160
      RH01=RH01-DEL
      GO TO 70
170  CONTINUE
      PMIN=P1
      RHUMIN=RH01
      GO TO 180
160  CONTINUE
      IF(ISTATE(4).LT.5)
1PRINT 200
200  FORMAT(1X,'NO LIQUID ROOT.  MINIMUM USED')
      RH02=RH0MIN
      GO TO 130
150  CONTINUE
      IF(ISTATE(4).LT.5)
1PRINT 300
300  FORMAT(1X,'ROOT TOO LARGE')
      RH02=RH01
      IF(ISTATE(9).EQ.0) GO TO 130
      CALLED FROM DERIVATIVE ROUTINE
      P1=PRES(T,RH02)
      IF(P1.LT.SP) GO TO 240
      RH02=RH02-DEL
      GO TO 130
240  CONTINUE
      RH02=RH02+DEL
      GO TO 130
90  CONTINUE
      SUCCESSIVE BISECTIONS
      RH03=(RH01+RH02)/2
      P3=PRES(T,RH03)
      IF((ABS(P1-P2).LT.EPSP*P0).CR.ABS(RH01-RH02).LT.ABS(RH02)*EPSR)
1  GO TO 130
      IT=IT+1
      IF(IT.GT.ITMAX) GO TO 80
      IF(P3.GT.P0) GO TO 140
      RH01=RH03
      P1=P3
      GO TO 90
140  CONTINUE
      RH02=RH03
      P2=P3
      GO TO 90
80  CONTINUE
      IF(ISTATE(4).LT.5)
1PRINT 100,T,P,RH01,P1,RH02,P2
100  FORMAT(1X,'L DENSITY DIDNCT CONVERGE FOR T=',G11.4,'PRESSURE',
1  G11.4,'RH01=',G11.4,'P1=',G11.4,'RH02=',G11.4,'P2=',G11.4)

```

```

EZDL0820
EZDL0830
EZDL0840
EZDL0850
EZDL0860
EZDL0870
EZDL0880
EZDL0890
EZDL0900
EZDL0910
EZDL0920
EZDL0930
EZDL0940
EZDL0950
EZDL0960
EZDL0970
EZDL0980
EZDL0990
EZDL1000
EZDL1010
EZDL1020
EZDL1030
EZDL1040
EZDL1050
EZDL1060
EZDL1070
EZDL1080
EZDL1090
EZDL1100
EZDL1110
EZDL1120
EZDL1130
EZDL1140
EZDL1150
EZDL1160
EZDL1170
EZDL1180
EZDL1190
EZDL1200
EZDL1210
EZDL1220
EZDL1230
EZDL1240
EZDL1250
EZDL1260
EZDL1270
EZDL1280
EZDL1290
EZDL1300
EZDL1310

```



```

20 CONTINUE
   IF((ABS(P1-P2).LT.EPSP*P0).CR.ABS(RHO1-RHO2).LT.ABS(RHO2)*EPSR)
1    GO TO 40
   IF (IT.GT.ITMAX) GO TO 30
   PROJECTION
   RHO3=(RHO1*P2-RHO2*P1)/(P2-P1)
   IF((RHO3.GT.RMIDV).OR.(RHO3.LT.0))RHO3=(1-IT/50.)*P0/RGAS/T
   RHO1=RHO2
   RHO2=RHO3
   IT=IT+1
   P1=P2
   P2=PRES(T,RHO2)-P0
   GO TO 20
40 CONTINUE
   RHO1=.99*RHO2
   P1=PRES(T,RHO1)-P0
   IF(RHO2.GT.RMIDV) GO TO 30
   IF(P1.LT.P2 ) GO TO 130
30 CONTINUE
   ITMAX=40
   ITMAX=RMIDV/DEL+5
   IT=0
   P1=P1+P0
   P2=P2+P0
   CHECK FOR STARTING PCINT
   RHO1=DEL
70 CONTINUE
   P1=PRES(T,RHO1)
   IF(P1.LT.P0)GO TO 60
   IF(ISTATE(4).LT.5)
1PRINT 300
300 FORMAT(1X,'ROOT TOO SMALL')
   RHO2=RHO1
   GC TO 130
60 CONTINUE
   RHO2=RHO1+DEL
   CODE=0.
   PMAX=P1
   RHOMAX=RHO1
110 CONTINUE
   P2=PRES(T,RHO2)
   IF(P2.GT.P0) GO TO 120
   IF(P2.GT.PMAX.AND.CODE.EQ.0.) GO TO 160
   CODE=1.
170 CONTINUE
   IT=IT+1
   RHO1=RHO2
   P1=P2
   RHO2=RHO2+DEL
   IF(IT.GT.ITMAX) GO TO 180
EZDV0340
EZDV0350
EZDV0360
EZDV0370
EZDV0380
EZDV0390
EZDV0400
EZDV0410
EZDV0420
EZDV0430
EZDV0440
EZDV0450
EZDV0460
EZDV0470
EZDV0480
EZDV0490
EZDV0500
EZDV0510
EZDV0520
EZDV0530
EZDV0540
EZDV0550
EZDV0560
EZDV0570
EZDV0580
EZDV0590
EZDV0600
EZDV0610
EZDV0620
EZDV0630
EZDV0640
EZDV0650
EZDV0660
EZDV0670
EZDV0680
EZDV0690
EZDV0700
EZDV0710
EZDV0720
EZDV0730
EZDV0740
EZDV0750
EZDV0760
EZDV0770
EZDV0780
EZDV0790
EZDV0800
EZDV0810
EZDV0820
EZDV0830

```



```

      IF (RH01.LT.RMIDV) GO TO 110
      IF (ISTATE(4).LT.5)
        1 PRINT 200
        200 FORMAT(1X,'MAXIMUM USED')
        RH02=RHOMAX
        GO TO 130
      180 CONTINUE
      IF (ISTATE(4).LT.5)
        1 PRINT 500
        500 FORMAT(1X,'V ROOT NOT FOUND')
        GO TO 130
      160 CONTINUE
      PMAX=P2
      RHOMAX=RH02
      GO TO 170
      120 CONTINUE
      IT=0
      90 CONTINUE
      C      SUCCESSIVE BISECTIONS
      RH03=(RH01+RH02)/2
      P3=PRES(T,RH03)
      IF ((ABS(P1-P2).LT.EPSP*P0).CR.ABS(RH01-RH02).LT.ABS(RH02)*EPSR)
        1 GO TO 150
      IT=IT+1
      IF (IT.GT.ITMAX) GO TO 80
      IF (P3.GT.P0) GO TO 140
      RH01=RH03
      P1=P3
      GO TO 90
      150 CONTINUE
      RH02=RH03
      GO TO 130
      140 CONTINUE
      RH02=RH03
      P2=P3
      GO TO 90
      80 CONTINUE
      IF (ISTATE(4).LT.5)
        1 PRINT 100,T,P,RH01,P1,RH02,P2
        100 FORMAT (1X,'V DENSITY DIDNOT CONVERGE FOR T=',G11.4,'PRESSURE',
          1 G11.4,'RH01=',G11.4,'P1=',G11.4,'RH02=',G11.4,'P2=',G11.4)
      130 CONTINUE
      DENS=RH02
      RETURN
      END

```

```

EZDV0840
EZDV0850
EZDV0860
EZDV0870
EZDV0880
EZDV0890
EZDV0900
EZDV0910
EZDV0920
EZDV0930
EZDV0940
EZDV0950
EZDV0960
EZDV0970
EZDV0980
EZDV0990
EZDV1000
EZDV1010
EZDV1020
EZDV1030
EZDV1040
EZDV1050
EZDV1060
EZDV1070
EZDV1080
EZDV1090
EZDV1100
EZDV1110
EZDV1120
EZDV1130
EZDV1140
EZDV1150
EZDV1160
EZDV1170
EZDV1180
EZDV1190
EZDV1200
EZDV1210
EZDV1220
EZDV1230
EZDV1240
EZDV1250
EZDV1260
EZDV1270
EZDV1280

```

```

C      FUNCTION ENTH (T,RHO)
C
C      PURPOSE
C      EVALUATES ENTHALPY AS A FUNCTION OF TEMPERATURE AND DENSITY
C      MODIFIED FOR CURVE FITTING
C
C      USAGE
C      RESULT = ENTH(T,RHO)
C
C      DESCRIPTION OF PARAMETERS
C      T      - TEMPERATURE
C      RHO    - DENSITY
C
C      SUBROUTINES NEEDED
C      F12(T,RHO)
C      CALCULATES THE INTEGRAL CF (DZDT)DLN(RHO)
C      PRES(T,RHO)
C      CALCULATES PRESSURE AT T AND RHO
C      FUNCTION ENTH(T,RHO)
C      COMMON /PRM/RGAS,RENRGY,ICRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
C      1      ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
C      TSTAR=ALPHA*T/ICRIT
C      HDEV=-TSTAR*TSTAR*F12(T,RHC)+TSTAR*(PRES(T,RHO)/RGAS/T/RHO-1.)
C      ENTH=HDEV*RENRGY*ICRIT/ALPHA
C      RETURN
C      END
EZDH0010
EZDH0020
EZDH0030
EZDH0040
EZDH0050
EZDH0060
EZDH0070
EZDH0080
EZDH0090
EZDH0100
EZDH0110
EZDH0120
EZDH0130
EZDH0140
EZDH0150
EZDH0160
EZDH0170
EZDH0180
EZDH0190
EZDH0200
EZDH0210
EZDH0220
EZDH0230
EZDH0240
EZDH0250
EZDH0260

```

```

C      FUNCTION ENTRPY(T,RHO)
C
C      PURPOSE
C      CALCULATES THE ENTROPY FOR TEMPERATURE AND DENSITY
C
C      USAGE
C      RESULT = ENTRPY(T,RHO)
C
C      DESCRIPTION OF PARAMETERS
C      T      - TERM
C      T      - TEMPERATURE
C      RHO    - DENSITY
C
C      SUBPROGRAMS NEEDED
C      SUBROUTINES NEEDED
C      F12(T,RHO)
EZDS0010
EZDS0020
EZDS0030
EZDS0040
EZDS0050
EZDS0060
EZDS0070
EZDS0080
EZDS0090
EZDS0100
EZDS0110
EZDS0120
EZDS0130
EZDS0140
EZDS0150
EZDS0160

```

EZDS0170
EZDS0180
EZDS0190
EZDS0200
EZDS0210
EZDS0220
EZDS0230
EZDS0240
EZDS0250
EZDS0260

```

      CALCULATES THE INTEGRAL OF (DZDT)DLN(RHO)
      F11
      CALCULATES THE INTEGRAL OF (Z-1)D LN(RHO)
      FUNCTION ENTRPY(T,RHO)
      COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
      1  ,A(40),B(7),NTERMS,NPARM,NUMB,KTOP,RMIDL,RMIDV
      TSTAR=ALPHA*T/TCRIT
      ENTRPY=RENRGY*(-ALOG(RHO*RGAS*T))-F11(T,RHO)-TSTAR*F12(T,RHO)
      RETURN
      END

```

EZFC0010
EZFC0020
EZFC0030
EZFC0040
EZFC0050
EZFC0060
EZFC0070
EZFC0080
EZFC0090
EZFC0100
EZFC0110
EZFC0120
EZFC0130
EZFC0140
EZFC0150
EZFC0160
EZFC0170
EZFC0180
EZFC0190
EZFC0200
EZFC0210
EZFC0220
EZFC0230
EZFC0240
EZFC0250
EZFC0260
EZFC0270
EZFC0280
EZFC0290
EZFC0300
EZFC0310
EZFC0320

```

      FUNCTION FCHISQ
      PURPOSE
      FCHISQ = SUM((Y-YFIT)**2/SIGMA**2)/NFREE
      EVALUATE REDUCED CHI SQUARE FOR FIT TO DATA
      USAGE
      RESULT = FCHISQ(Y,WEIGHT,NPTS,NFREE,YFIT)
      DESCRIPTION OF PARAMETERS
      Y      - ARRAY OF DATA POINTS
      WEIGHT - ARRAY OF WEIGHTS FOR DATA POINTS
      NPTS   - NUMBER OF DATA POINTS
      NFREE  - NUMBER OF DEGREES OF FREEDOM
      YFIT   - ARRAY OF CALCULATED VALUES OF Y
      SUBROUTINES AND VUNCTION SUBPROGRAMS REQUIRED
      NONE
      FUNCTION FCHISQ (Y,WEIGHT,NPTS,NFREE,YFIT)
      DOUBLE PRECISION CHISQ
      DIMENSION Y(NPTS),WEIGHT(NPTS),YFIT(NPTS)
      11 CHISQ=0
      12 IF (NFREE) 13,13,20
      13 FCHISQ=0
      GO TO 40
      ACCUMULATE CHI SQUARE
      20 DO 30 I=1,NPTS
      30 CHISQ = CHISQ + WEIGHT(I)*(Y(I)-YFIT(I))**2

```

C	DIVIDE BY NUMBER OF DEGREES OF FREEDOM	EZFC0330
C		EZFC0340
	31 FREE =NFREE	EZFC0350
	32 FCHISQ=CHISQ/FREE	EZFC0360
	40, RETURN	EZFC0370
	END	EZFC0380
C	FUNCTION FDERIV	EZFD0010
C		EZFD0020
C	PURPOSE	EZFD0030
C	EVALUATE NUMERICALLY DERIVATIVE OF FUNCTN WITH RESPECT	EZFD0040
C	TO THE ITH VARIABLE	EZFD0050
C		EZFD0060
C	USAGE	EZFD0070
C	RESULT = FDERIV(X,I,NDIM)	EZFD0080
C		EZFD0090
C	DESCRIPTION OF PARAMETERS	EZFD0100
C	X - ARRAY OF INDEPENDENT VARIABLE VALUES	EZFD0110
C	I - NUMBER OF VARIABLE FOR DERIVATIVE	EZFD0120
C	NDIM - NUMBER OF INDEPENDENT VARIABLES	EZFD0130
C		EZFD0140
C	SUBROUTINES NEEDED	EZFD0150
C	FUNCTN(X,NDIM	EZFD0160
C	EVALUATES THE FUNCTION AT POINT X	EZFD0170
C		EZFD0180
	FUNCTION FDERIV (X,I,NDIM)	EZFD0190
	DIMENSION X(NDIM)	EZFD0200
	COMMON /DAT/IPRES,ISTATE(20)	EZFD0210
	ISTATE(9)=1	EZFD0220
	EPMAX=.1	EZFD0230
	EPS=.01	EZFD0240
	N=3	EZFD0250
	SAVE=X(I)	EZFD0260
	IF(ABS(SAVE).LT.EPS) GO TO 10	EZFD0270
	DEL=ABS(EPS*SAVE)	EZFD0280
14	CONTINUE	EZFD0290
	DO 12 IT=1,3	EZFD0300
	X(I)=SAVE+DEL	EZFD0310
	F2=FUNCTN(X,NDIM)	EZFD0320
	X(I)=SAVE-DEL	EZFD0330
	F1=FUNCTN(X,NDIM)	EZFD0340
	DFDX=(F2-F1)/2./DEL	EZFD0350
	IF(ISTATE(5).EQ.1) GO TO 40	EZFD0360

C		EZFD0370
C	TESTS PRECISION OF DERIVATIVE	EZFD0380
C		EZFD0390
	IF (ABS(F1-F2).LT.ABS(F1)*1.E-5) F2=F1	EZFD0400
	IF (ABS(F1-F2)*((10**(6-N)).GT.ABS(F1)) GO TO 40	EZFD0410
20	CONTINUE	EZFD0420
	EPS=EPS*10	EZFD0430
	IF (ABS(SAVE).LT.1.E-6) GO TO 30	EZFD0440
	DEL=ABS(SAVE*EPS)	EZFD0450
	GO TO 12	EZFD0460
30	CONTINUE	EZFD0470
	DEL=EPS	EZFD0480
12	CONTINUE	EZFD0490
	IF (ABS(F1-F2).LT.ABS(F1)*1.E-5) DFDX=0.	EZFD0500
	GO TO 40	EZFD0510
10	DEL=EPS	EZFD0520
	GO TO 14	EZFD0530
40	FDERIV=DFDX	EZFD0540
100	FORMAT(1X,8G14.6)	EZFD0550
	X(I)=SAVE	EZFD0560
	ISTATE(9)=0	EZFD0570
	RETURN	EZFD0580
	END	EZFD0590

C	FUNCTION FLASHP	EZFL0010
C		EZFL0020
C	PURPOSE	EZFL0030
C	EVALUATES THE VAPOR PRESSURE FOR A GIVEN TEMPERATURE	EZFL0040
C	MODIFIED FOR CURVE FITTING	EZFL0050
C		EZFL0060
C	USAGE	EZFL0070
C	RESULT = FLASHP(T)	EZFL0080
C		EZFL0090
C	DESCRIPTION OF PARAMETERS	EZFL0100
C	T - TEMPERATURE	EZFL0110
C		EZFL0120
C	SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED	EZFL0130
C	PRESS - CALCULATES PRESSURE GIVEN T,RHO	EZFL0140
C	RHOL - CALCULATES LIQUID DENSITY	EZFL0150
C	RHOV - CALCULATES VAPOR DENSITY	EZFL0160
C	FUGCOF - CALCULATES THE FUGACITY COEFFICIENT	EZFL0170
C		EZFL0180
C	FUNCTION FLASHP(T,P0)	EZFL0190

```

COMMON /PRM/RGAS,RENGY,ICRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
1  .A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
CGMON /DAT/IPRES,ISTATE(20)
REAL KVALUE
EPS=0.001
ITMAX=20
CURVE FITTING
IF(ISTATE(9).EQ.1) GO TO 210
P=P0
210 CONTINUE
RHOL=DENSL(T,P)
RHOV=DENSV(T,P)
IT=1
40 CONTINUE
KVALUE=FUGCUF(T,RHOL)/FUGCCF(T,RHOV)
P=P*KVALUE
IF(P.LT.1.3*PCRIT) GO TO 30
P=1.3*PCRIT
GO TO 20
30 CONTINUE
IF(ABS(1-KVALUE).LT.EPS) GC TO 25
IT=IT+1
IF(IT.GE.ITMAX) GO TO 20
RHOV=DENSV(T,P)
RHOL=DENSL(T,P)
GO TO 40
20 CONTINUE
IF(ISTATE(4).LE.4) PRINT 200,T,P,KVALUE
200 FORMAT (1X,'VAPOR PRESSURE DID NOT CONVERGE. T=',G14.6,
1  'P=',G14.6,'KVALUE= ',G14.6)
25 FLASHP=P
RETURN
END
EZFL0200
EZFL0210
EZFL0220
EZFL0230
EZFL0240
EZFL0250
EZFL0260
EZFL0270
EZFL0280
EZFL0290
EZFL0300
EZFL0310
EZFL0320
EZFL0330
EZFL0340
EZFL0350
EZFL0360
EZFL0370
EZFL0380
EZFL0390
EZFL0400
EZFL0410
EZFL0420
EZFL0430
EZFL0440
EZFL0450
EZFL0460
EZFL0470
EZFL0480
EZFL0490
EZFL0500
EZFL0510
EZFL0520

```

```

C FUNCTION FUGCOF(T,RHO) EZFG0010
C EZFG0020
C PURPOSE EZFG0030
C EVALUATES THE FUGACITY COEFFICIENT EZFG0040
C EZFG0050
C USAGE EZFG0060
C RESULT = FUGCOF(T,RHO) EZFG0070
C EZFG0080
C DESCRIPTION OF PARAMETERS EZFG0090

```

```

C      T - TEMPERATURE
C      RHO - DENSITY
C
C      SUGROUTINES NEEDED
C      F11
C      CALCULATES THE INTEGRAL CF (Z-1)D LN(RHO)
C      PRES(T,RHO)
C      CALCULATES PRESSURE AT T AND RHO
C      FUNCTION FUGCOF(T,RHO)
C      COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
C      ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
C      FP=ALOG(RHO*RGAS*T)+F11(T,RHO)+(PRES(T,RHO)/RHO/RGAS/T-1. )
C      IF(FP.GT.100)FP=100.
C      FUGCOF=EXP(FP)
C      RETURN
C      END
EZFG0100
EZFG0110
EZFG0120
EZFG0130
EZFG0140
EZFG0150
EZFG0160
EZFG0170
EZFG0180
EZFG0190
EZFG0200
EZFG0210
EZFG0220
EZFG0230
EZFG0240
EZFG0250

```

```

C      FUNCTION FUNCN(X,NDIM)
C      PURPOSE
C      EVALUATES THE FITTED FUNCTION AT THE POINT X
C
C      USAGE
C      RESULT = FUNCN(X,NDIM)
C
C      DESCRIPTION OF PARAMETERS
C      X - ARRAY OF VALUES OF INDEPENDENT VARIABLES
C      NDIM - NUMBER OF INDEPENDENT VARIABLES
C
C      FUNCTION FUNCN(X,NDIM)
C      DIMENSION X(NDIM)
C      COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
C      ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
C      COMMON /PRP/ICUMP(20),CPC(20),CRC(20),CMW(20),CW(20),CTC(20)
C      ,CA(20),CB(20),CNAME(20,2)
C      INTEGER SL
C      DATA SL/-1/
C      N=NDIM-NPARM
C      DO 20 I=1,NPARM
C      A(I)=X(N+I)
C      X1=ABS(X(I))
C      IWHOLE=X1+.005
C      IFRACT=(X1-IWHOLE+.005)*100.
EZFN0010
EZFN0020
EZFN0030
EZFN0040
EZFN0050
EZFN0060
EZFN0070
EZFN0080
EZFN0090
EZFN0100
EZFN0110
EZFN0120
EZFN0130
EZFN0140
EZFN0150
EZFN0160
EZFN0170
EZFN0180
EZFN0190
EZFN0200
EZFN0210
EZFN0220
EZFN0230
EZFN0240
EZFN0250
EZFN0260

```

```

      C      LIOVAP=SIGN(1.,X(1))
      C      IF(IWHOLE.GT.99) GO TO MIXTURE
      C      PURE
      C      DO 50 L=1,20
      C      IF(ICOMP(L).EQ.IWHOLE) GO TO 60
      C      50 CONTINUE
      C      PRINT 200,IWHOLE
      C      200 FORMAT(IX,'COMPONENT',15,' NDT IN DATA SET')
      C      STOP
      C      60 CONTINUE
      C      IF(SL.EQ.L) GO TO 30
      C      TCRIT=CTC(L)
      C      PCRIT=CPCL)
      C      RHOC=CRC(L)
      C      RENRGV=1.9872/CW(L)
      C      W=CW(L)
      C      ALPHA=CALL)
      C      BETA=CB(L)
      C      RTOP=4*RHOC
      C      RMIDL=RHOC
      C      RMIDV=RHOC
      C      100 FORMAT(IX,8G14.6)
      C      SL=L
      C      30 CONTINUE
      C      CALCULATE PROPERTIES
      C      IF(IFRACT.EQ.30.AND.LIQVAP.EQ.-1) GO TO 1
      C      IF(IFRACT.EQ.30.AND.LIQVAP.EQ.1) GO TO 2
      C      IF(IFRACT.EQ.40.AND.LIQVAP.EQ.-1) GO TO 3
      C      IF(IFRACT.EQ.40.AND.LIQVAP.EQ.1) GO TO 4
      C      IF(IFRACT.EQ.75) GO TO 5
      C      IF(IFRACT.EQ.60) GO TO 6
      C      IF(IFRACT.EQ.25) GO TO 7
      C      LIQUID DENSITY
      C      1 FUNCN=DENSL(X(2),X(3))
      C      GO TO 40
      C      VAPOR DENSITY
      C      2 FUNCN=DENSV(X(2),X(3))
      C      GO TO 40
      C      LIQUID ENTHALPY
      C      3 RHOL=DENSL(X(2),X(3))
      C      FUNCN=ENTH(X(2),RHOL)
      C      GO TO 40
      C      VAPOR ENTHALPY

```

```

EZFN0270
EZFN0280
EZFN0290
EZFN0300
EZFN0310
EZFN0320
EZFN0330
EZFN0340
EZFN0350
EZFN0360
EZFN0370
EZFN0380
EZFN0390
EZFN0400
EZFN0410
EZFN0420
EZFN0430
EZFN0440
EZFN0450
EZFN0460
EZFN0470
EZFN0480
EZFN0490
EZFN0500
EZFN0510
EZFN0520
EZFN0530
EZFN0540
EZFN0550
EZFN0560
EZFN0570
EZFN0580
EZFN0590
EZFN0600
EZFN0610
EZFN0620
EZFN0630
EZFN0640
EZFN0650
EZFN0660
EZFN0670
EZFN0680
EZFN0690
EZFN0700
EZFN0710
EZFN0720
EZFN0730
EZFN0740
EZFN0750
EZFN0760

```


C	4	RHOV=DENSU(X(2),X(3))	EZFN0770
		FUNCN=ENTH(X(2),RHOV)	EZFN0780
		GO TO 40	EZFN0790
C			EZFN0800
C		VAFOR PRESSURE	EZFN0810
C	5	FUNCN=FLASHP(X(2),X(3))	EZFN0820
		GO TO 40	EZFN0830
C			EZFN0840
C		PRESSURE	EZFN0850
C			EZFN0860
C	6	FUNCN=PRES(X(2),X(3))	EZFN0870
		GO TO 40	EZFN0880
C			EZFN0890
C		SPCEIFIC VOLUME HEAT CAPACITY	EZFN0900
C			EZFN0910
C			EZFN0920
	7	FUNCN=CV(X(2),X(3))	EZFN0930
		GO TO 40	EZFN0940
	40	RETURN	EZFN0950
		END	EZFN0960

C	SUBROUTINE GJEL(A,ND,MD,DETD,IER)		EZGJ0010
C			EZGJ0020
C	PURPOSE		EZGJ0030
C	SIMULTANEOUS SOLUTION OF LINEAR EQUATIONS BY GAUSS-JORDAN		EZGJ0040
C	USUSGE		EZGJ0050
C	CALL GEJEL(A,ND,MD,DETD,IER)		EZGJ0060
C			EZGJ0070
C	DESCRIPTION OF PARAMETERS		EZGJ0080
C	A IS THE ND BY MD AUGMENTED MATRIX		EZGJ0090
C	THE FIRST ND COLUMNS RETURNS THE INVERSE MATRIX		EZGJ0100
C	THE LAST MD-ND COLUMNS CONTAIN THE SOLUTION VECTORS		EZGJ0110
C	DETD RETURNS THE DETERMINANT		EZGJ0120
C			EZGJ0130
C	SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED		EZGJ0140
C	NONE		EZGJ0150
C			EZGJ0160
	SUBROUTINE GJEL(A,ND,MD,DETD,IER)		EZGJ0170
	DIMENSION A(ND,MD)		EZGJ0180
	DOUBLE PRECISION A,FACT,DABS		EZGJ0190
	INTEGER*2 PIVOTS(100),CPIVCT(100)		EZGJ0200
	DATA EPS/1.E-20/		EZGJ0210
	IER=0		EZGJ0220

```

EZGJ0230
EZGJ0240
EZGJ0250
EZGJ0260
EZGJ0270
EZGJ0280
EZGJ0290
EZGJ0300
EZGJ0310
EZGJ0320
EZGJ0330
EZGJ0340
EZGJ0350
EZGJ0360
EZGJ0370
EZGJ0380
EZGJ0390
EZGJ0400
EZGJ0410
EZGJ0420
EZGJ0430
EZGJ0440
EZGJ0450
EZGJ0460
EZGJ0470
EZGJ0480
EZGJ0490
EZGJ0500
EZGJ0510
EZGJ0520
EZGJ0530
EZGJ0540
EZGJ0550
EZGJ0560
EZGJ0570
EZGJ0580
EZGJ0590
EZGJ0600
EZGJ0610
EZGJ0620
EZGJ0630
EZGJ0640
EZGJ0650
EZGJ0660
EZGJ0670
EZGJ0680
EZGJ0690
EZGJ0700
EZGJ0710
EZGJ0720

      N=ND
      M=MD
      DET=1.
      DO 4 I=1,N
        IF(I.EQ.N) GO TO 30
        FIND LARGEST COLUMN PIVOT
        LPIVOT=I
        IPIVOT=I
        FACT=DABS(A(I,I))
        DO 10 II=1,N
          DO 10 JJ=1,N
            IF(DABS(A(JJ,II)).LE.FACT) GO TO 10
            FACT=DABS(A(JJ,II))
            LPIVOT=JJ
            IPIVOT=II
        10 CONTINUE
      C      TRADE COLUMNS
        CPIVOT(I)=IPIVOT
        DO 60 K=1,N
          FACT=A(K,I)
          A(K,I)=A(K,IPIVOT)
          A(K,IPIVOT)=FACT
        60 CONTINUE
      C      TRADE ROWS
        PIVOTS(I)=LPIVOT
        DO 20 K=1,M
          FACT=A(I,K)
          A(I,K)=A(LPIVOT,K)
          A(LPIVOT,K)=FACT
        20 CONTINUE
        30 CONTINUE
        CPIVOT(N)=N
        PIVOTS(N)=N
        IF(A(I,I))1.2,1
        2 DET=0.
        IER=N+1
        RETURN
        3 DET=0.
        IER=1
        GO TO 8
      C      1 IF(DABS(A(I,I)).LT.EPS) GO TO 3
        FORM DETERMINANTS
        8 DET=A(I,I)*DET
        IF(ABS(DET).GE.1.E-60.OR.DET.EQ.0) GO TO 90
        PRINT 200,DET
        DET=0
        90 CONTINUE
        200 FORMAT(1X,'MATRIX IS ILL CONDITIONED. DETERMINANT IS ',G14.6)
        A(I,I)=1.

```

```

      DO 5 J=1,M
C     NCRMALIZE
      A(I,J)=A(I,J)/FACT
5     CONTINUE
      DO 6 J=2,N
      L=MOD(I+J-2,N)+1
      IF(A(L,I).EQ.0.)GO TO 6 .
      FACT=A(L,I)
      A(L,I)=0.
      DO 7 K=1,M
      LL=MOD(I+K-2,M)+1
      IF(A(I,LL).EQ.0.)GO TO 7
C     REDUCE
      A(L,LL)=A(L,LL)-A(I,LL)*FACT
7     CONTINUE
6     CONTINUE
4     CONTINUE
C     TRANSFER COLUMNS OF INVERSE
      DO 40 IR=1,N
      I=N-IR+1
      IF(PIVOTS(I).EQ.1) GO TO 40
      LPIVOT=PIVOTS(I)
      DO 50 J=1,N
      FACT=A(J,I)
      A(J,I)=A(J,LPIVOT)
      A(J,LPIVOT)=FACT
50    CONTINUE
40    CONTINUE
C     TRANSFER ROWS OF INVERSE
      DO 70 IR=1,N
      I=N-IR+1
      IF(CPIVOT(I).EQ.1) GO TO 70
      JPIVOT=CPIVOT(I)
      DO 80 J=1,M
      FACT=A(I,J)
      A(I,J)=A(JPIVOT,J)
      A(JPIVOT,J)=FACT
80    CONTINUE
70    CONTINUE
      DETD=DET
      RETURN
      END

```

```

EZGJ0730
EZGJ0740
EZGJ0750
EZGJ0760
EZGJ0770
EZGJ0780
EZGJ0790
EZGJ0800
EZGJ0810
EZGJ0820
EZGJ0830
EZGJ0840
EZGJ0850
EZGJ0860
EZGJ0870
EZGJ0880
EZGJ0890
EZGJ0900
EZGJ0910
EZGJ0920
EZGJ0930
EZGJ0940
EZGJ0950
EZGJ0960
EZGJ0970
EZGJ0980
EZGJ0990
EZGJ1000
EZGJ1010
EZGJ1020
EZGJ1030
EZGJ1040
EZGJ1050
EZGJ1060
EZGJ1070
EZGJ1080
EZGJ1090
EZGJ1100
EZGJ1110
EZGJ1120
EZGJ1130
EZGJ1140

```

SUBROUTINE LBLEZ	EZLB0010
DATA I/O/	EZLB0020
IF(I.EQ.0) PRINT 20	EZLB0030
20 FORMAT(1H1,20(/),50X,'*',6(4X,'*')//50X,'*',12X,'EZFIT',12X,'*',	EZLB0040
1//50X,'*',4X,'NONLINEAR REGRESSION',5X,'*',//50X,	EZLB0050
2'*,13X,'BY',14X,'*'/50X,'*',9X,'KEVIN GOIN',10X,'*'/	EZLB0060
3 50X,'*',7X,'OCTOBER 20, 1976',6X,'*'/50X,'*',	EZLB0070
4 6(4X,'*')////)	EZLB0080
I=1	EZLB0090
RETURN	EZLB0100
END	EZLB0110

C SUBROUTINE MESSG(TEXT,NCHR)	EZMS0010
C	EZMS0020
C PURPOSE	EZMS0030
C PRINTS A MESSAGE OF UP TO 80 CHARACTERS	EZMS0040
C	EZMS0050
C USAGE	EZMS0060
C CALL MESSG(TEXT,NCHR)	EZMS0070
C	EZMS0080
C DESCRIPTION OF PARAMETERS	EZMS0090
C TEXT - CHARACTER STRING TO BE PRINTED	EZMS0100
C NCHR - NUMBER OF CHARACTERS TO BE PRINTED	EZMS0110
C	EZMS0120
C SUBROUTINE MESSG(TEXT,NCHR)	EZMS0130
C LOGICAL*1 TEXT	EZMS0140
C DIMENSION TEXT(NCHR)	EZMS0150
C PRINT 2000,TEXT	EZMS0160
2000 FORMAT(1X,80A1)	EZMS0170
C RETURN	EZMS0180
C END	EZMS0190


```

IFRACT=(X1-IWHDLE+.003)*100
IF(IWHDLE.EQ.LW.AND.IFRACT.EQ.LF) GO TO 140
C   PREPARE SUMMARIES AND GROUP HEADING
IF(IPRINT.EQ.1) GO TO 240
IPRINT=1
GO TO 250
C   240 CONTINUE
SUMMARY
IF(JO.NE.0)SUM1=SUM1/J0
IF(J0.NE.0)SUM2=SUM2/J0
PRINT 100
CALL MSGG('AVE. ABS. PERCENT. NUMBER PTS..AVE.ABS.DEVIATION ',48)
PRINT 100
CALL MSGG('CONTRIBUTION TO CHISQUARED',26)
PRINT 100,CHISQ
CHISQ=0
C   250 CONTINUE
HEADING
PRINT 500
PRINT 400,HEADER
IF(IWHDLE.NE.LW) PRINT 1900,IWHDLE
IF(IFRACT.NE.LF.OR.IWHDLE.NE.LW) PRINT 1800,IFRACT
1800 FORMAT(57X,'DATA TYPE','15///')
1900 FORMAT(55X,'COMPOUND CODE','15///')
PRINT 1600
1600 FORMAT(5X,'DATAID',8X,'YEXF',8X,'YCALC',7X,'PERCENT',7X,'DELTA',
1 8X,'WEIGHT',6X,'CONTROL',5X,'X2',11X,'X3',11X,'X4',57X,'X',S...
2 ,//)
SUM1=0
SUM2=0.
J0=0
LF=IFRACT
LW=IWHDLE
C   140 CONTINUE
J0=J0+1
SUM=SUM+ABS(PERC)
SUM1=SUM1+ABS(PERC)
SUM2=SUM2+ABS(DIFF)
CHISQ=CHISQ+WEIGHT(I)*DIFF*DIFF
IF(IFRACT.EQ.60) GO TO 220
IF(JXPRT.EQ.0)
1PRINT 2000,(DATAID(I,K),K=1,ND),V(I),YC,PERC,DIFF,WEIGHT(I),
1 (X(I,K),K=1,N)
2000 FORMAT(1X,3A4,1X,9G13.5,(/53X,6G13.5))
IF(IXPRT.EQ.0) GO TO 20
IF(IFRACT.EQ.IDH) GO TO 220
IF(IFRACT.EQ.IRHC) GO TO 210
IF(IFRACT.EQ.IVP) GO TO 230
EZ0U0510
EZ0U0520
EZ0U0530
EZ0U0540
EZ0U0550
EZ0U0560
EZ0U0576
EZ0U0580
EZ0U0590
EZ0U0600
EZ0U0610
EZ0U0620
EZ0U0630
EZ0U0640
EZ0U0650
EZ0U0660
EZ0U0670
EZ0U0680
EZ0U0690
EZ0U0700
EZ0U0710
EZ0U0720
EZ0U0730
EZ0U0740
EZ0U0750
EZ0U0760
EZ0U0770
EZ0U0780
EZ0U0790
EZ0U0800
EZ0U0810
EZ0U0820
EZ0U0830
EZ0U0840
EZ0U0850
EZ0U0860
EZ0U0870
EZ0U0880
EZ0U0890
EZ0U0900
EZ0U0910
EZ0U0920
EZ0U0930
EZ0U0940
EZ0U0950
EZ0U0960
EZ0U0970
EZ0U0980
EZ0U0990
EZ0U1000

```

```

      C      220  CONTINUE
      MODIFIED FOR DELTA P OUTPUT
      P=Y(1)+RGAS*Z(2)*Z(3)
      IF(Z(1).LE.0) RHO=DENSL(Z(2),P)
      IF(Z(1).GT.0) RHO=DENSV(Z(2),P)
      PECR=(Z(3)-RHO)*100/Z(3)
      RSUM=RSUM+ABS(PECR)
      APECR=ABS(PECR)
      IF(APECR.LT..01) N1=N1+1
      IF(APECR.LT..1.AND.APECR.GE..01)N2=N2+1
      IF(APECR.LT..1..AND.APECR.GE..1) N3=N3+1
      IF(APECR.LT..10..AND.APECR.GE..1.)N4=N4+1
      IF(APECR.LT..100..AND.APECR.GE..10.)N5=N5+1
      IF(APECR.GE..100)N6=N6+1
      IF(JXPRT.EQ.0)
        1PRINT 2100,(DATAID(I,K),K=1,ND),Y(1),YC,PERC,DIFF,WEIGHT(I),
        1 (X(I,K),K=1,N),RHO,PECR
      2100 FORMAT(1X,3A4,1X,8G13.5,F8.5,F7.2)
      GO TO 20
      230  CONTINUE
      RHO=DENSL(Z(2),Z(3))
      RHOV=DENSV(Z(2),Z(3))
      PRINT 2200,RHOV,RHOL
      2200 FORMAT(68X,'SATURATION VAPOR AND LIQUID DENSITIES',2G13.5)
      GO TO 20
      210  CONTINUE
      PRESC=PRESC(Z(2),Y(1))
      PERC2=(Z(3)-PRESC)*100/Z(3)
      1700 FORMAT(69X,'PEXP,PCALC,PERCENT',5X,3G13.5)
      PRINT 1700,Z(3),PRESC,PERC2
      20  CONTINUE
      SUM1=SUM1/J0
      SUM2=SUM2/J0
      PRINT 100
      CALL MESSG('AVE. ABS. PERCENT,NUMBER PTS.,AVE.ABS.DEVIATION ',48)
      PRINT 100,SUM1,J0,SUM2
      PRINT 100
      CALL MESSG('CONTRIBUTION TC CHISQUARED',26)
      PRINT 100,CHISQR
      CHISQR=0
      PRINT 100
      IF (RSUM.EQ.0) GO TO 260
      RSUM=RSUM/NPTS
      CALL MESSG('DENSITY AAPD',12)
      PRINT 100,RSUM
      PRINT 100
      PRINT 2300,N1,N2,N3,N4,N5,N6
      2300 FORMAT(1X,'DENSITY ERROR DISTRIBUTION',/,7X,'<.01',.4X,'.01-.1',5X,EZ0U1500
EZ0U1010
EZ0U1020
EZ0U1030
EZ0U1040
EZ0U1050
EZ0U1060
EZ0U1070
EZ0U1080
EZ0U1090
EZ0U1100
EZ0U1110
EZ0U1120
EZ0U1130
EZ0U1140
EZ0U1150
EZ0U1160
EZ0U1170
EZ0U1180
EZ0U1190
EZ0U1200
EZ0U1210
EZ0U1220
EZ0U1230
EZ0U1240
EZ0U1250
EZ0U1260
EZ0U1270
EZ0U1280
EZ0U1290
EZ0U1300
EZ0U1310
EZ0U1320
EZ0U1330
EZ0U1340
EZ0U1350
EZ0U1360
EZ0U1370
EZ0U1380
EZ0U1390
EZ0U1400
EZ0U1410
EZ0U1420
EZ0U1430
EZ0U1440
EZ0U1450
EZ0U1460
EZ0U1470
EZ0U1480
EZ0U1490
EZ0U1500

```

```

1 . . . 1-1 . . . 4X . '1.-10 . . . 2X . '10.-100 . . . 5X . '>100 . . . /1X,6110//)
260 CONTINUE
SUM=SUM/NPTS
PRINT 300,SUM
PRINT 100
PRINT 100
PRINT 100
IPRINT=0 .
RETURN
END
EZDU01510
EZDU01520
EZDU01530
EZDU01540
EZDU01550
EZDU01560
EZDU01570
EZDU01580
EZDU01590
EZDU01600

```

```

C FUNCTION U(T,RHO)
C
C PURPOSE
C CALCULATES THE INTERNAL ENERGY
C
C USAGE
C RESULT=U(T,RHO)
C DESCRIPTION OF PARAMETERS
C T-ABSOLUTE TEMPERATURE
C RHO-DENSITY
C
C SUBROUTINES NEEDED
C F12(T,RHO)
C CALCULATES THE INTEGRAL OF (DZDT)DLN(RHO)
C
C FUNCTION U(T,RHO)
COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
1 ,A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
TSTAR=ALPHA*T/TCRIT
U=RENRGY*TCRIT*(-TSTAR*ISTAR*F12(T,RHO))/ALPHA
RETURN
END
EZDU0010
EZDU0020
EZDU0030
EZDU0040
EZDU0050
EZDU0060
EZDU0070
EZDU0080
EZDU0090
EZDU0100
EZDU0110
EZDU0120
EZDU0130
EZDU0140
EZDU0150
EZDU0160
EZDU0170
EZDU0180
EZDU0190
EZDU0200
EZDU0210
EZDU0220

```



```

EZPR0010
EZPR0020
EZPR0030
EZPR0040
EZPR0050
EZPR0060
EZPR0070
EZPR0080
EZPR0090
EZPR0100
EZPR0110
EZPR0120
EZPR0130
EZPR0140
EZPR0150
EZPR0160
EZPR0170
EZPR0180
EZPR0190
EZPR0200
EZPR0210
EZPR0220
EZPR0230
EZPR0240
EZPR0250
EZPR0260
EZPR0270
EZPR0280
EZPR0290
EZPR0300
EZPR0310
EZPR0320
EZPR0330
EZPR0340
EZPR0350
EZPR0360
EZPR0370
EZPR0380
EZPR0390
EZPR0400
EZPR0410
EZPR0420
EZPR0430
EZPR0440
EZPR0450
EZPR0460
EZPR0470
EZPR0480
EZPR0490
EZPR0500

FUNCTION PRES
PURPOSE
CALCULATES THE PRESSURE FOR THE TCHEBYCHEF POLYNOMIAL EQUATION
PURE COMPONENT FORM

USAGE
RESULT = PRES(T,RHO)

DESCRIPTION OF PARAMETERS
T-ABSOLUTE TEMPERATURE
RHO - DENSITY

SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED
NONE

FUNCTION PRES(T,RHO)
COMMON /PRM/RGAS,RENRGY,TCRIT,PCRIT,RHOC,W,ALPHA,BETA,XMW
1 A(40),B(7),NTERMS,NPARM,NUMB,RTOP,RMIDL,RMIDV
COMMON /XTN/AXTN(60)
REAL*8 Z,X,X6,X4,C1,C2,C3,C4,C5,C6,C7,C8,C9
Y1(U)=U
Y2(U)=2*U*U-1
Y3(U)={4*U*U-3}*U
Y4(U)={8*U*U-8}*U*U+1
Y5(U)={16*U*U-20}*U*U+5)*U
Y6(U)={32*U*U-48}*U*U+18)*U*U-1
Y7(U)={64*U*U-112}*U*U+56)*U*U-7)*U
Y8(U)={128*U*U-256)*U*U+160)*U*U-32)*U*U+1
TSTAR=ALPHA*T/TCRIT
RHOS=BETA*RHO/RHOC
X=1/TSTAR
Y=RHOS/4.
C1={(((A(6)*X+A(5))*X+A(4))*X+A(3))*X+A(2))*X+A(1))
C2={(((A(12)*X+A(11))*X+A(10))*X+A(9))*X+A(8))*X+A(7))
C3={(((A(18)*X+A(17))*X+A(16))*X+A(15))*X+A(14))*X+A(13))
C4={(((A(24)*X+A(23))*X+A(22))*X+A(21))*X+A(20))*X+A(19))
C5={(((A(28)*X+A(27))*X+A(26))*X+A(25))
C6={(((A(32)*X+A(31))*X+A(30))*X+A(29))
C7={(((A(36)*X+A(35))*X+A(34))*X+A(33))
C8={(((A(40)*X+A(39))*X+A(38))*X+A(37))
X6=X**6
X4=X**4
C1=C1+(AXTN(6)*X+AXTN(5))*X6
C2=C2+(AXTN(8)*X+AXTN(7))*X6
C3=C3+(AXTN(10)*X+AXTN(9))*X6
C4=C4+(AXTN(12)*X+AXTN(11))*X6
C5=C5+(((AXTN(16)*X+AXTN(15))*X+AXTN(14))*X+AXTN(13))*X4

```



```

1      .A(40),B(7),NTERMS,NPARM,NUMB,RTUP,RMIDL,RMIDV
Y10(U)=U
Y11(U)=U*U/2
Y12(U)=(.666667*U*U-1)*U
Y13(U)=(U*U-1.5)*U*U
Y14(U)=(1.6*U*U-2.66667)*U*U+1)*U
Y15(U)=(12.66667*U*U-5.)*U*U+2.5)*U*U
Y16(U)=(14.57143*U*U-9.6)*U*U+6.)*U*U-1.)*U
Y17(U)=(18.*U*U-18.6667)*U*U+14.)*U*U-3.5)*U*U
Y18(U)=(14.2222*U*U-36.5714)*U*U+32.)*U*U-10.6667)*U*U+1)*U
TSTAR=ALPHA*T/TCRIT
RHOS=BETA*RHO/RHOC
X=1/TSTAR
Y=RHOS/4.
DC1=-((((((AXTN(6))*X*7+AXTN(5))*6)*X+A(6)*5)*X+A(5)*4)*X+
1  A(4)*3)*X+A(3)*2)*X+A(2))*X*X
DC2=-((((((AXTN(8))*X*7+AXTN(7))*6)*X+A(12)*5)*X+A(11)*4)*X+
1  A(10)*3)*X+A(9)*2)*X+A(8))*X*X
DC3=-((((((AXTN(10))*X*7+AXTN(9))*6)*X+A(18)*5)*X+A(17)*4)*X+
1  A(16)*3)*X+A(15)*2)*X+A(14))*X*X
DC4=-((((((AXTN(12))*X*7+AXTN(11))*6)*X+A(24)*5)*X+A(23)*4)*X+
1  A(22)*3)*X+A(21)*2)*X+A(20))*X*X
DC5=-((((((AXTN(16))*X*7+AXTN(15))*6)*X+AXTN(14)*5)*X+AXTN(13)*4)*X
1  +A(28)*3)*X+A(27)*2)*X+A(26))*X*X
DC6=-((((((AXTN(20))*X*7+AXTN(19))*6)*X+AXTN(18)*5)*X+AXTN(17)*4)*X
1  +A(32)*3)*X+A(31)*2)*X+A(30))*X*X
DC7=-((((((AXTN(24))*X*7+AXTN(23))*6)*X+AXTN(22)*5)*X+AXTN(21)*4)*X
1  +A(36)*3)*X+A(35)*2)*X+A(34))*X*X
DC8=-((((((AXTN(28))*X*7+AXTN(27))*6)*X+AXTN(26)*5)*X+AXTN(25)*4)
1  *X+A(40)*3)*X+A(39)*2)*X+A(38))*X*X
DC9=-((((((AXTN(32))*X*7+AXTN(31))*6)*X+AXTN(30)*5)*X+AXTN(29)*4)
1  *X+AXTN(4)*3)*X+AXTN(3)*2)*X+AXTN(2))*X*X
F12=DC1*Y10(Y)+DC2*Y11(Y)+DC3*Y12(Y)+DC4*Y13(Y)+DC5*Y14(Y)
1  +DC6*Y15(Y)+DC7*Y16(Y)+DC8*Y17(Y)+DC9*Y18(Y)
RETURN
END

```

```

EZ120190
EZ120200
EZ120210
EZ120220
EZ120230
EZ120240
EZ120250
EZ120260
EZ120270
EZ120280
EZ120290
EZ120300
EZ120310
EZ120320
EZ120330
EZ120340
EZ120350
EZ120360
EZ120370
EZ120380
EZ120390
EZ120400
EZ120410
EZ120420
EZ120430
EZ120440
EZ120450
EZ120460
EZ120470
EZ120480
EZ120490
EZ120500
EZ120510
EZ120520
EZ120530
EZ120540

```

APPENDIX C

BANKED

Bank for Experimental Data

Abstract

BANKED is a flexible data structure based on computer cards that will handle experimental data for a maximum of 999 chemical species, 99 data types and mixtures of 999 components. It features identification of each data point along with the bibliographical source. Because of its basic structure the cards can be arranged from disorder by simple sorting. It also supplies a set of physical properties for the species in BANKED.

Basic Structure

The BANKED Data base consists of three types of cards: The experimental data, the bibliographic information and physical properties information. The experimental data cards contain the independent variables, the dependent variable, control information identifying data type, bibliographic reference and data point reference number. The bibliographic cards have the reference code that is on the data card and the journal reference from which the data was obtained. The

physical properties card contains an acronym the for species, the data bank's species code, and various physical properties for the species, such as critical properties and molecular weight.

Experimental Data Cards

Several items of information are required for a data card. The method here identifies the data point as to the source, which actual point it is, the type of data, the independent variables and the dependent variable. The cards are laid out in six ten column fields, a two digit sequence number, a four character bibliographic reference and a seven digit data point reference number. The sequence number identifies the number of data cards needed for that type of point and also their order.

The first card for a data point has the control variable, two independent variables, usually temperature and pressure, the independent variable, the sequence number, bibliography code and data point identification number. (The format is 4F10.0, 26X, I2, 1X, A4,I7) The sequence number is one less than the number of cards needed for the data point. For explanation of the bibliography code see below. The following cards consist of six additional independent variables, a sequence number, bibliography code and data point identification number. (The format is 6F10.0,6X,12,1X,A4,I7.) The sequence numbers for each card for a specific point decrease so that the last card for the point has a sequence number of

0. Some examples of various data types are given in Figure 1.

The control variable contains information to specify the exact type of data that the point is. It's basic form is

$$X_1 = SHXXX,DD$$

(See Table III for a summary of its meaning.) The control variable is punched on the card so that SHXXX and DD can be read as separate integers (I6,1X,I2). The value of H specifies whether the datum is for a mixture or pure fluid. When it has the value 0, the point is a pure fluid and when it is 1 it is for a mixture. Therefore, for pure fluids the absolute value of X_1 is less than 1000. The sign, S, specifies whether the point is for a gas(+), i.e. $\rho < \rho_c$ or a liquid(-), $\rho > \rho_c$. The term DD is the code for the type of data this point is. Some of these types are given in Table II. There is room for 99 data types. The remaining term, XXX, has different meanings according to whether the point is for a mixture or pure fluid.

For pure fluids XXX is the code for the chemical species. These codes are given in Table I. There is a capability of handling 999 species with this system. For mixtures XXX specifies the number of components. With this and the data point type, the exact number of independent variables is fixed. Following the first card, the first XXX variables are the coded overall composition for mixtures.

TABLE I

Codes for Chemical Species

<u>XXX Specie</u>	<u>Hydrocarbons</u>
026 Ammonia	032 Acetylene
016 Argon	033 Benzene
017 Carbon dioxide	004 Butane
018 Carbon monoxide	030 Cyclohexane
	029 Cyclopentane
	010 Decane
	012 Dodecane
	002 Ethane
	022 Ethylene
	007 Heptane
	006 Hexane
	014 Isobutane
	015 Isopentane
	001 Methane
	009 Nonane
	008 Octane
	005 Pentane
	003 Propane
	023 Propylene
	034 Toluene
	013 Tridecane
	012 Undecane
<u>Freons</u>	
036 R-11 C Cl ₃ F	
037 R-12 C Cl ₂ F ₂	
038 R-13 C Cl F ₃	
039 R-14 C F ₄	
040 R-21 C H Cl ₂ F	
041 R-22 C H Cl F ₂	
042 R-23 C H F ₃	
043 R-113 C Cl ₂ F C Cl F ₂	
044 R-114 C Cl F ₂ C Cl F ₂	
045 R-115 C ₂ Cl F ₅	
046 R-C318 C ₄ F ₈	
047 R-500 C Cl ₂ F ₂ /C H ₃ C H F ₂	
048 R-502 C H Cl F ₂ /C Cl F ₂ C F ₂	
049 R-142b	
050 R-152a	
<u>XXX Specie</u>	
019 Helium	
031 Hydrogen	
028 Hydrogen Chloride	
035 Hydrogen Sulfide	
021 Nitric Oxide	
024 Nitrogen	
020 Nitrous Oxide	
027 Water	

TABLE II

Codes for Data Types

<u>DD</u>	<u>Type</u>	<u>Variable Order</u>
05	T_B , Bubble point temperature	Control, pressure, blank, T_B ; compositions
06	P_B , Bubble point pressure	Control, temperature, blank, P_B ; compositions
10	Adiabatic flash pressure	Control, temperature, V/L ratio, P; compositions
12	Δu , Internal energy departure	Control, temperature, density, ΔU ; (mixture: compositions)
14	ΔS , entropy departure	Control, temperature, density, ΔS ; (mixture: compositions)
15	Adiabatic flash temperature	Control, pressure, V/L ratio, T; compositions
20	C_P , specific heat at constant P	Control, temperature, density, C_P ; (mixture: compositions)
21	C_P	Control, temperature, pressure, C_P ; (mixture: compositions)
25	C_V , specific heat at constant v	Control, temperature, density, C_V ; (mixture: compositions)
26	C_V	Control, temperature, pressure, C_V ; (mixture: compositions)
30	ρ , density	Control, temperature, pressure, ρ ; (mixture: compositions)
35	a, diffusivity	Control, temperature, pressure, a; (mixture: compositions)
36	a, diffusivity	Control, temperature, density, a; (mixture: compositions)
40	ΔH , enthalpy departure	Control, temperature, pressure, ΔH ; (mixture: compositions)

TABLE II (continued)

<u>DD</u>	<u>Type</u>	<u>Variable Order</u>
41	ΔH , enthalpy departure	Control, temperature, density, ΔH ; (mixture: compositions)
45	Flash V/L ratio	Control, temperature, pressure, V/L; compositions, K-values
50	H_J , Joule Thompson coefficient	Control, temperature, pressure, H_J ; (mixture: compositions)
60	P, pressure	Control, temperature, density, P; (mixture: compositions)
65	W, speed of sound	Control, temperature, density, W; (mixture: compositions)
70	K, thermal conductivity	Control, temperature, density, K; (mixture: compositions)
75	$P\sigma$, vapor pressure	Control, temperature, pressure, $P\sigma$
80	B_2 , 2nd Virial coefficient	Control, temperature, blank, B_2
85	B_3 , 3rd Virial coefficient	Control, temperature, blank, B_3
90	ν , viscosity	Control, temperature, density, ν ; (mixture: compositions)
95	T_D , dew point temperature	Control, pressure, blank, T_D ; (mixture: compositions)
96	P_D , dew point pressure	Control, temperature, blank, P_D ; (mixture: compositions)

TABLE III

Format of Control Variable, X_1

$$X_1 = \text{SHXXX.DD}$$

S = + Gas, $\rho < \rho_c$
 - Liquid, $\rho > \rho_c$

H = 0 Pure Fluid
 1 Mixture

Pure Fluid

Mixture

XXX = Code for Chemical Species

XXX = Number of Components

DD = Code for Data Type

DD = Code for Data Type

Figure 1. Example Data Cards: (a) Methane density; (b) Pressure for methane and propane mixture; (c) K-value for light component in mixture of methane, propane, heptane, and decane.

The whole portion of the variable is the species code and the fraction is the mole fraction of that specie. These are punched so that they could be read as separate numbers (F4.0,F6.5). The data type then specifies how many other variables are needed.

Bibliographic Card

The bibliographic cards are used to reference the source of the experimental data. The card consists of a four character code and a seventy-six character reference field. The code consists of a three digit sequence number and the initial of the author. The typical card is:

001M, MICHELS, WIJKER, WIJKER, "ISOTHERMS OF ARGON..."PHYSICA, XV, NO. 7, P62 (1949).

The reference field is in a standard journal reference style.

Physical Properties Card

The physical properties cards are used to supply information on each chemical specie. For each substance there is a set of four cards. On the first card the first field is a twelve character acronym identifying the species. The second field is a three digit code used on the data cards to identify the species. These codes are listed in Table I. The next four fields, which are fifteen columns wide, contain the critical properties and molecular weight. The last five columns in each card are used to sequence the cards. The first three digits are the species code and the last two are

the card number. The following cards consist of five fifteen column data fields and a five digit sequence number. The arrangement of the data on the cards is as follows:

- Card 1 Acronym, species code, critical temperature, critical pressure, critical density molecular weight, species code, 01
- Card 2 Acentric factor, L-J ϵ , L-J σ , boiling point, melting point, specie code, 02
- Card 3 Ideal gas parameter 1,2,3,4,5, species code, 03
- Card 4 Ideal gas parameter 6,7, blank, blank, blank, species code, 04

The ideal gas parameters are for the equation for ideal gas enthalpy

$$H^* = B_1 + B_2T + B_3T^2 + B_4T^3 + B_5T^4 + B_6T^5$$

where the enthalpy is in BTU/lb and temperature, T, in degrees R. For the heat capacity

$$C_p^* = B_2 + 2B_3T - 3B_4T^2 + 4B_5T^3 + 5B_6T^4$$

and for entropy

$$S^* = B_2 \ln T/T_B + 2B_3(T-T_B) + \frac{3}{2} B_4(T^2-T_B^2) + \frac{4}{3} B_5(T^3-T_B^3) + \frac{5}{4} B_6(T^4-T_B^4) + B_7$$

Where T_B is the base temperature for the entropy equations ($1^\circ R$). The data bases are 0 Btu/lb at $0^\circ R$ for enthalpy and 0 Btu/lb at $0^\circ R$ and 1 atm pressure for entropy. The coefficients for

the hydrocarbons were extracted from the work of Passut and Danner¹. The properties are given in psia, Btu/lb, lb mole/ft³, and °R. The primary reference for them is Sherwood and Reid².

The physical properties information also has a short summary version which takes only one card. It has a short eight digit acronym, two digit compound code, and then in F10.0 formats, critical temperature critical pressure, critical density, molecular weight, acentric factor, α a temperature scaling factor and β a density scaling factor.

References

- (1) Passut, C. and Danner, R., "Correlation of Ideal Gas Enthalpy, Heat Capacity and Entropy", IEC, Process Design and Development, Vol. II, pp. 543-546 (1972).
- (2) Sherwood and Reid, Properties of Gases and Liquids, 2nd Ed., McGraw-Hill, New York (1966).

APPENDIX D
TABULATED RESULTS FOR 43 PARAMETER
EQUATION OF STATE

TABLE 1. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF THE WORKING DATA SET. PRESSURES BELOW 10,000 PSIA.

DATA ID	T RANKINE	P PSIA	RHO EXP LB/MCL/FT ³	RHO CALC LB/MCL/FT ³	ERROR PERCENT
001H	153	707.67	2900.760	3.303990	-0.24
001H	161	707.67	4351.137	3.319604	-0.49
001H	169	707.67	5801.520	3.335444	-0.75
001H	177	707.67	7251.895	3.350917	-1.00
001H	145	707.67	1450.330	3.287703	-0.33
001H	162	779.67	4351.137	3.202991	-0.33
001H	170	779.67	5801.520	3.221436	-0.33
001H	178	779.67	7251.895	3.239182	-0.33
001H	146	779.67	1450.330	3.164415	-0.23
001H	154	779.67	2900.760	3.110493	-0.23
001H	179	851.67	7251.895	3.018445	-0.23
001H	147	851.67	1450.330	3.043347	-0.33
001H	155	851.67	2900.760	3.066489	-0.13
001H	163	851.67	4351.137	3.088283	-0.40
001H	171	851.67	5801.520	3.097853	-0.40
001H	104	923.67	4351.137	2.937853	-0.03
001H	172	923.67	5801.520	2.936414	-0.25
001H	180	923.67	7251.895	2.943286	-0.47
001H	148	923.67	1450.330	2.843719	-0.40
001H	156	923.67	2900.760	2.877216	-0.13
001H	165	995.67	4351.137	2.717596	-0.00
001H	173	995.67	5801.520	2.756696	-0.10
001H	181	995.67	7251.895	2.762431	-0.34
001H	149	995.67	1450.330	2.622050	-0.21
001H	157	995.67	2900.760	2.673396	-0.13
001H	174	1067.67	5801.520	2.537271	-0.12
001H	182	1067.67	7251.895	2.538981	-0.21
001H	158	1067.67	2900.760	2.403463	-0.37
001H	166	1067.67	4351.137	2.476576	-0.10
001H	183	1139.67	7251.895	2.335173	-0.02
001H	175	1139.67	5801.520	2.249156	-0.35
001H	167	1139.67	4351.137	2.131257	-0.42
001H	184	1211.67	7251.895	1.953561	-0.42
001H	133	1247.67	8702.273	1.900231	-0.47
001H	159	1211.67	2900.760	1.803535	-0.40
001H	176	1211.67	5801.520	1.803535	-0.14
001H	125	1247.67	6526.703	1.680219	-0.03
001H	34	1319.67	8702.273	1.548993	-0.14
001H	35	1351.67	8702.273	1.170501	-0.05
001H	17	1247.67	5076.324	0.922884	-1.04
001H	36	1463.67	8702.273	0.772599	-0.33
001H	37	1535.67	8702.273	0.744249	-0.55
001H	27	1591.67	6526.703	0.674616	-0.44
001H	38	1607.67	8702.273	0.605165	-0.44
001H	23	1463.67	6526.703	0.52996	-0.05
001H	39	1679.67	8702.273	0.52996	-0.05
001H	40	1751.67	8702.273	0.52996	-0.05
001H	105	1535.67	6526.703	0.52996	-0.25
001H	129	1535.67	8702.273	0.52996	-0.25
001H	108	2003.67	8702.273	0.440071	-0.19
001H	20	1463.67	5076.324	0.428845	-0.09
001H	19	1391.67	8702.273	0.458806	-0.04
001H	31	1679.67	6526.703	0.450565	-0.23
001H	30	1607.67	8702.273	0.471735	-0.05
001H	109	2075.67	8702.273	0.421461	-0.65
001H	107	1859.67	8702.273	0.465405	-0.24
001H	99	1551.67	6526.703	0.495174	-0.29
001H				0.341930	0.30

TABLE 1. CONTINUED. PRESSURES BELOW 10,000 PSIA.

DATA ID	T RANKINE	P PSIA	RHO EXP LB/MCL/FT ³	RHO CALC LB/MCL/FT ³	ERROR PERCENT
001H	10	1319.67	3625.950	0.361120	-0.12
001H	98	1859.67	6526.703	0.361572	0.40
001H	11	1591.67	3625.950	0.311301	0.32
001H	24	1751.67	5076.324	0.309002	0.51
001H	25	1679.67	5076.324	0.322114	0.48
001H	22	1607.67	5076.324	0.346666	0.72
001H	21	1535.67	5076.324	0.382550	0.19
001H	160	1211.67	6526.703	0.347896	-0.46
001H	132	1751.67	6526.703	0.398460	0.43
001H	101	2075.67	6526.703	0.309854	0.16
001H	100	2003.67	6526.703	0.324920	0.21
001H	97	1767.67	6526.703	0.364926	0.15
001H	112	2251.67	8702.273	0.365832	0.15
001H	111	2219.67	8702.273	0.381037	0.25
001H	110	2147.67	8702.273	0.358460	0.16
001H	16	1751.67	3625.950	0.209425	0.30
001H	15	1679.67	3625.950	0.221327	0.47
001H	14	1607.67	3625.950	0.236656	0.45
001H	13	1535.67	3625.950	0.255771	0.39
001H	12	1463.67	3625.950	0.275131	0.53
001H	81	2251.67	5076.324	0.211347	0.29
001H	56	2219.67	5076.324	0.219784	0.11
001H	55	2147.67	5076.324	0.228773	0.11
001H	94	2075.67	5076.324	0.238645	0.14
001H	93	2003.67	5076.324	0.249565	0.19
001H	91	1531.67	5076.324	0.261771	0.29
001H	90	1859.67	5076.324	0.275604	0.41
001H	39	1787.67	5076.324	0.291739	0.49
001H	104	2251.67	6526.703	0.272672	0.26
001H	103	2219.67	6526.703	0.284135	0.16
001H	102	2147.67	6526.703	0.296773	0.17
001H	82	1659.67	3625.950	0.152677	0.34
001H	152	1211.67	1450.380	0.131321	0.45
001H	150	1067.67	1450.380	0.130073	-0.96
001H	32	1931.67	3625.950	0.183734	0.21
001H	84	2003.67	3625.950	0.175783	0.15
001H	85	2075.67	3625.950	0.168523	0.11
001H	86	2147.67	3625.950	0.161514	0.09
001H	87	2291.67	3625.950	0.150205	0.09
001H	87	1463.67	3625.950	0.156003	0.13
001H	4	2219.67	2175.570	0.154144	0.36
001H	5	1535.67	2175.570	0.143622	0.37
001H	151	1139.67	1450.380	0.146722	0.37
001H	3	1607.67	2175.570	0.135265	0.26
001H	3	1751.67	2175.570	0.121769	0.37
001H	7	1679.67	2175.570	0.121769	0.37
001H	74	1859.67	2175.570	0.112789	0.31
001H	73	1787.67	2175.570	0.113044	0.16
001H	76	2003.67	2175.570	0.113369	0.29
001H	75	1931.67	2175.570	0.108246	0.11
001H	80	2251.67	2175.570	0.099825	0.11
001H	79	2219.67	2175.570	0.092706	0.09
001H	78	2147.67	2175.570	0.096125	0.07
001H	77	2075.67	2175.570	0.095833	0.06
001H	5	509.67	452.052	3.465329	-0.43
001H	5	559.67	2716.304	3.465329	-0.26
001H	4	554.67	4607.340	3.465329	-0.00

TABLE 1. CONTINUED. PRESSURES BELOW 10,000 PSIA.

DATA ID	T RANKLINE	P PSIA	RHC EXP LAMCL/FT 3	RHC CALC LAMCL/FT 3	ERROR PERCENT	
0010	7	529.67	1003.522	3.465325	3.464945	-0.13
0010	6	539.67	1464.684	3.469329	3.465220	-0.12
0010	12	734.67	3344.042	3.265255	3.264132	-0.22
0010	13	719.67	1344.375	3.265253	3.269740	-0.14
0010	11	759.67	6793.367	3.063851	3.063740	-0.00
0010	17	834.67	3255.107	3.063851	3.063945	-0.00
0010	16	859.67	6587.645	3.063851	3.063851	-0.00
0010	18	819.67	1291.138	3.063851	3.063740	-0.02
0010	22	559.67	2701.389	2.775464	2.731717	-0.25
0010	21	1009.67	8111.273	2.775464	2.765104	-0.37
0010	23	539.67	576.326	2.523149	2.789671	-0.51
0010	26	1109.67	9176.320	2.523149	2.516731	-0.25
0010	27	1059.67	4755.152	2.523149	2.521635	-0.05
0010	23	1034.67	2375.500	2.220370	2.522669	-0.01
0010	31	1159.67	6746.285	2.220370	2.221820	-0.07
0010	32	1134.67	5059.477	2.220370	2.216275	-0.15
0010	36	1259.67	9696.043	1.982475	1.964162	-0.15
0010	37	1209.67	6948.297	1.982475	1.966502	-0.20
0010	38	1159.67	4277.137	1.982475	1.964454	-0.21
0010	41	1259.67	7432.641	1.734666	1.740597	-0.34
0010	42	11209.67	5306.883	1.734666	1.724694	-0.37
0010	43	1159.67	3303.629	1.734666	1.694545	-0.31
0010	45	1159.67	9759.355	1.500250	1.502543	-0.54
0010	46	1259.67	6297.555	1.500250	1.496277	-0.13
0010	50	1359.67	8342.117	1.261574	1.258076	-0.28
0010	51	1259.67	5631.652	1.261574	1.255915	-0.40
0010	59	1459.67	7780.344	0.792990	0.786680	-0.30
0010	63	1559.67	9602.172	0.504630	0.506510	-0.33
0010	64	1459.67	5686.734	0.504630	0.503582	-0.13
0010	70	1209.67	2372.065	0.252315	0.252358	-0.02
0010	63	1959.67	5006.074	0.252315	0.253751	-0.56
0010	69	1459.67	3322.342	0.252315	0.253462	-0.45
0010	67	2459.67	6564.253	0.252315	0.252884	-0.23
0010	69	2459.67	7612.117	0.252315	0.253411	-0.23
0010	79	1009.67	871.402	0.100926	0.100915	-0.11
0010	73	1059.67	949.238	0.100926	0.101524	-0.39
0010	77	1109.67	1020.631	0.100926	0.101460	-0.53
0010	76	1159.67	1089.934	0.100926	0.101431	-0.55
0010	75	1209.67	1157.043	0.100926	0.101461	-0.53
0010	71	2859.67	3104.061	0.100926	0.101233	-0.50
0010	72	2459.67	2644.306	0.100926	0.101154	-0.21
0010	73	1959.67	2069.074	0.100926	0.101264	-0.34
0010	74	1459.67	1474.609	0.100926	0.101370	-0.44
0010	80	2859.67	1852.205	0.027755	0.027787	-0.12
0010	81	2459.67	730.966	0.027755	0.027776	-0.06
0010	82	1559.67	579.452	0.027755	0.027764	-0.10
0010	83	1459.67	426.617	0.027755	0.027600	-0.17
0010	84	1159.67	332.747	0.027755	0.027870	-0.27
0010	85	559.67	267.416	0.027755	0.027870	-0.44
0010	86	859.67	232.317	0.005551	0.027870	-0.42
0010	87	859.67	170.363	0.005551	0.005552	-0.02
0010	88	2459.67	146.450	0.005551	0.005552	-0.01
0010	89	1559.67	116.564	0.005551	0.005552	-0.02
0010	90	1459.67	36.624	0.005551	0.005553	-0.04
0010	91	1159.67	68.574	0.005551	0.005554	-0.06
0010	92	559.67	56.442	0.005551	0.005554	-0.12
0010	93	559.67	50.300	0.005551	0.005554	-0.15
0010	94	759.67	44.034	0.005551	0.005556	-0.12

TABLE 1. CONTINUED. PRESSURES BELOW 10,000 PSIA.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
001U	95	2859.67	34.069	0.001110	0.001110	-0.00
001U	96	2459.67	29.301	0.001110	0.001110	-0.00
001U	98	1459.67	17.377	0.001110	0.001110	0.00
001U	97	1959.67	23.340	0.001110	0.001110	0.00
001U	99	1159.67	13.796	0.001110	0.001110	0.01
001U	100	959.67	11.404	0.001110	0.001110	0.02
001U	101	859.67	10.206	0.001110	0.001111	0.04
001U	102	759.67	9.003	0.001110	0.001111	0.06
001U	103	659.67	7.790	0.001110	0.001111	0.10
001U	104	2859.67	3.407	0.000111	0.000111	0.02
001U	105	2459.67	2.930	0.000111	0.000111	0.00
001U	106	1959.67	2.335	0.000111	0.000111	0.00
001U	107	1459.67	1.739	0.000111	0.000111	0.02
001U	108	1159.67	1.531	0.000111	0.000111	-0.01
001U	109	959.67	1.143	0.000111	0.000111	0.01
001U	110	859.67	1.024	0.000111	0.000111	0.04
001U	111	759.67	0.905	0.000111	0.000111	0.07
001U	112	659.67	0.785	0.000111	0.000111	-0.00
001U	113	559.67	0.666	0.000111	0.000111	0.09
002K	1	545.67	62.063	3.453338	3.459388	0.17
002K	2	545.67	324.939	3.456499	3.460158	0.11
002K	3	545.67	682.358	3.460219	3.461201	0.03
002K	4	545.67	1120.520	3.464846	3.462478	-0.07
002K	5	545.67	1559.696	3.469402	3.463734	-0.16
002K	6	545.67	1996.843	3.473966	3.464982	-0.26
002K	7	545.67	2435.004	3.478447	3.466228	-0.35
002K	8	545.67	2873.137	3.482901	3.467458	-0.44
002K	9	545.67	3311.282	3.487295	3.468681	-0.53
002K	10	545.67	3749.429	3.491697	3.469891	-0.62
002K	11	545.67	4187.570	3.496019	3.471095	-0.71
002K	12	545.67	4625.730	3.500315	3.472287	-0.80
001U	60	1022.67	1160.667	2.506104	2.502576	-0.14
001U	59	1013.67	1079.793	2.539873	2.538849	-0.04
001U	58	1004.67	1003.300	2.572274	2.573609	0.05
001U	57	995.67	931.017	2.603557	2.606995	0.13
001U	56	986.67	862.788	2.633807	2.639102	0.20
001U	55	977.67	798.456	2.663132	2.670038	0.26
001U	54	968.67	737.836	2.691446	2.699876	0.31
001U	53	959.67	680.814	2.719089	2.728702	0.35
001U	52	950.67	627.207	2.745793	2.756563	0.39
001U	51	941.67	576.399	2.771898	2.733536	0.42
001U	50	932.67	529.734	2.797160	2.809669	0.45
001U	49	923.67	485.585	2.821737	2.835005	0.47
001U	48	914.67	444.323	2.845817	2.859595	0.48
001U	47	905.67	405.806	2.869362	2.883474	0.49
001U	46	896.67	369.906	2.892094	2.906688	0.50
001U	45	887.67	336.510	2.914454	2.929254	0.51
001U	44	878.67	305.489	2.936165	2.951213	0.51
001U	43	869.67	276.729	2.957700	2.972598	0.50
001U	42	860.67	250.118	2.978527	2.993428	0.50
001U	41	851.67	225.540	2.998875	3.013732	0.50
001U	40	842.67	202.896	3.018711	3.033529	0.49
001U	39	833.67	182.059	3.038280	3.052841	0.48
001U	38	824.67	162.943	3.057297	3.071692	0.47
001U	37	815.67	145.434	3.076009	3.090093	0.46
001U	36	806.67	129.441	3.094395	3.108064	0.44
001U	35	797.67	114.873	3.112166	3.125620	0.43
001U	34	788.67	101.636	3.129851	3.142778	0.41

TABLE 1. CONTINUED. PRESSURES BELOW 10,000 PSIA.

DATA ID		T RANKINE	P PSIA	RHO EXP LB/MLL/FT ³	RHO CALC LB/MLL/FT ³	ERROR PERCENT
0010	33	779.67	89.640	3.146898	3.159547	0.40
0010	32	770.67	78.800	3.163837	3.175935	0.38
0010	31	761.67	69.033	3.180082	3.191999	0.37
0010	30	752.67	60.253	3.196201	3.207626	0.36
0010	29	743.67	52.410	3.211890	3.222943	0.34
0010	28	734.67	45.405	3.227130	3.237917	0.33
0010	27	725.67	39.177	3.242215	3.252555	0.32
0010	26	716.67	33.661	3.256828	3.266857	0.31
0010	25	707.67	28.795	3.270960	3.280824	0.30
0010	24	698.67	24.520	3.284900	3.294464	0.29
0010	23	689.67	20.779	3.298333	3.307762	0.29
0010	22	680.67	17.520	3.311243	3.320735	0.29
0010	21	671.67	14.696	3.323621	3.333358	0.29
0010	20	662.67	12.259	3.336036	3.345622	0.29
0010	19	653.67	10.168	3.348004	3.357531	0.28
0010	18	644.67	8.334	3.359555	3.369055	0.29
0010	17	635.67	6.669	3.370454	3.380127	0.29
0010	16	626.67	5.191	3.380969	3.390806	0.29
0010	15	617.67	4.519	3.390884	3.401138	0.30
0010	14	608.67	3.627	3.400526	3.410892	0.30
0010	13	599.67	2.889	3.409888	3.420105	0.30
0010	12	590.67	2.283	3.418630	3.428720	0.30
0010	11	581.67	1.739	3.426734	3.436855	0.29
0010	10	572.67	1.390	3.434099	3.4443820	0.28
0010	9	563.67	1.070	3.441050	3.450083	0.26
0010	8	554.67	0.815	3.447342	3.455265	0.23
0010	7	545.67	0.615	3.452935	3.459206	0.18
0010	6	536.67	0.459	3.457791	3.461527	0.11
0010	5	527.67	0.339	3.461830	3.461791	-0.00
0010	4	518.67	0.247	3.464907	3.459270	-0.16
0010	3	509.67	0.178	3.466985	3.452724	-0.41
0010	2	500.67	0.126	3.467920	3.439583	-0.52
0010	1	491.67	0.089	3.467471	3.412505	-1.59

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.31
FOR 265 DATA POINTS.

TABLE 2. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF THE WORKING DATA SET. PRESSURES ABOVE 10,000 PSIA.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
001H	209	707.67	20305.316	3.474451	3.371170	-2.97
001H	201	707.67	17404.547	3.449228	3.360277	-2.58
001H	193	707.67	13053.406	3.409220	3.342912	-1.94
001H	210	779.67	20305.316	3.378994	3.285140	-2.78
001H	185	707.67	10152.656	3.380639	3.330545	-1.48
001H	194	779.67	13053.406	3.305564	3.247353	-1.76
001H	202	779.67	17404.547	3.350917	3.270712	-2.39
001H	186	779.67	10152.656	3.273430	3.230444	-1.31
001H	203	851.67	17404.547	3.240397	3.170572	-2.15
001H	187	851.67	10152.656	3.150901	3.116120	-1.10
001H	195	851.67	13053.406	3.186561	3.139300	-1.54
001H	204	923.67	17404.547	3.117762	3.059891	-1.88
001H	212	923.67	20305.316	3.155201	3.083850	-2.26
001H	213	995.67	20305.316	3.026880	2.967161	-1.97
001H	188	923.67	10152.656	3.012630	2.935515	-0.90
001H	196	923.67	13053.406	3.057257	3.017557	-1.31
001H	197	995.67	13053.406	2.911029	2.879411	-1.09
001H	205	995.67	17404.547	2.933396	2.935046	-1.62
001H	189	995.67	10152.656	2.835659	2.835368	-0.71
001H	206	1067.67	17404.547	2.835813	2.797414	-1.35
001H	214	1067.67	20305.316	2.887279	2.838863	-1.68
001H	198	1067.67	13053.406	2.746869	2.723166	-0.36
001H	215	1139.67	20305.316	2.736467	2.698881	-1.37
001H	190	1067.67	10152.656	2.674840	2.661508	-0.50
001H	207	1139.67	17404.547	2.673603	2.645626	-1.05
001H	199	1139.67	13053.406	2.560690	2.546257	-0.56
001H	216	1211.67	20305.316	2.565234	2.547704	-0.68
001H	65	1247.67	20305.316	2.480828	2.469224	-0.51
001H	191	1139.67	10152.656	2.464258	2.458313	-0.24
001H	208	1211.67	17404.547	2.491521	2.479607	-0.48
001H	66	1319.67	20305.316	2.310591	2.302430	-0.35
001H	57	1247.67	17404.547	2.396820	2.391379	-0.23
001H	200	1211.67	13053.406	2.348136	2.346023	-0.09
001H	49	1247.67	14503.789	2.293781	2.295535	0.07
001H	58	1319.67	17404.547	2.206232	2.205198	-0.05
001H	192	1211.67	10152.656	2.217518	2.217257	-0.01
001H	41	1247.67	11603.027	2.152181	2.165918	0.55
001H	67	1391.67	20305.316	2.135590	2.129516	-0.28
001H	50	1319.67	14503.789	2.062096	2.078241	0.49
001H	59	1391.67	17404.547	2.005698	2.008413	0.13
001H	68	1463.67	20305.316	1.957222	1.953329	-0.20
001H	60	1463.67	17404.547	1.801661	1.807323	0.31
001H	42	1319.67	11603.027	1.874701	1.894294	1.05
001H	51	1391.67	14503.789	1.830182	1.844132	0.76
001H	69	1535.67	20305.316	1.779475	1.779940	0.03
001H	70	1607.67	20305.316	1.614617	1.616924	0.14
001H	61	1535.67	17404.547	1.607135	1.613228	0.35
001H	52	1463.67	14503.789	1.599246	1.607036	0.55
001H	43	1391.67	11603.027	1.520044	1.594632	0.53
001H	71	1679.67	20305.316	1.472070	1.470792	-0.09
001H	62	1607.67	17404.547	1.434917	1.438913	0.28
001H	53	1535.67	14503.789	1.390615	1.391790	0.08
001H	44	1463.67	11603.027	1.315704	1.314510	-0.09
001H	72	1751.67	20305.316	1.347390	1.344566	-0.21
001H	63	1679.67	17404.547	1.292174	1.291654	-0.04
001H	54	1607.67	14503.789	1.217766	1.216303	-0.12
001H	137	1787.67	20305.316	1.292174	1.288852	-0.26
001H	129	1787.67	17404.547	1.123484	1.119905	-0.32

TABLE 2. CONTINUED. PRESSURES ABOVE 10,000 PSIA.

DATA ID	T RANKINE	P PSIA	RHD EXP LB/MCL/FT ³	RHU CALC LB/MCL/FT ³	ERROR PERCENT
001H	139	1931.67	20305.316	1.109822	-0.15
001H	138	1859.67	20305.316	1.190822	-0.26
001H	64	1751.67	17404.547	1.174465	-0.27
001H	45	1535.67	11603.789	1.108758	-0.83
001H	130	1659.67	17404.547	1.034664	-0.36
001H	55	1679.67	14503.739	1.035472	-0.26
001H	140	2003.67	20305.316	1.038382	-0.03
001H	131	1531.67	17404.547	1.058094	-0.19
001H	46	1607.67	11603.027	0.956645	-0.19
001H	56	1751.67	14503.789	0.951976	-0.74
001H	121	1787.67	14503.789	0.975441	-0.75
001H	141	2075.67	20305.316	0.976956	-0.11
001H	142	2147.67	20305.316	0.925130	-0.21
001H	132	2003.67	17404.547	0.857800	-0.02
001H	133	2075.67	17404.547	0.844460	-0.15
001H	123	1931.67	14503.789	0.800231	-0.13
001H	124	1859.67	14503.789	0.861023	-0.22
001H	47	1679.67	11603.027	0.849008	-0.40
001H	144	2291.67	20305.316	0.834702	-0.06
001H	143	2219.67	20305.316	0.876029	0.51
001H	134	2147.67	17404.547	0.722843	0.34
001H	136	2291.67	14503.789	0.722843	0.82
001H	126	2003.67	14503.789	0.749315	0.01
001H	125	2075.67	14503.789	0.706026	0.16
001H	43	1791.67	11603.027	0.766303	-0.17
001H	113	1767.67	11603.027	0.733762	-0.10
001H	135	2215.67	17404.547	0.753076	0.30
001H	126	2147.67	14503.789	0.683247	0.32
001H	128	2291.67	14503.789	0.606647	0.56
001H	115	1931.67	11603.027	0.606647	0.05
001H	114	1859.67	11603.027	0.678575	0.01
001H	127	2219.67	14503.789	0.638361	0.44
001H	116	2147.67	11603.027	0.534391	0.26
001H	117	2075.67	11603.027	0.562745	0.18
001H	116	2003.67	11603.027	0.556399	0.10
001H	119	2213.67	11603.027	0.509355	0.36
001H	120	2291.67	11603.027	0.4697107	0.46
001H	1	669.67	14694.000	3.469329	-2.17
001H	2	669.67	13368.641	3.469329	-1.99
001H	3	634.67	10222.074	3.469329	-1.30
001H	5	609.67	14063.938	3.262557	-1.62
001H	9	784.67	10370.429	3.262557	-1.35
001H	10	919.67	14503.699	3.061851	-1.35
001H	14	909.67	13417.594	3.049779	-1.35
001H	15	909.67	15720.836	2.745144	-1.09
001H	19	1079.67	13351.844	2.750670	-0.29
001H	20	1169.67	14470.148	2.527149	-0.62
001H	24	1159.67	13593.023	2.508450	-0.62
001H	25	1259.67	13575.109	2.223149	-0.62
001H	29	1259.67	15202.945	2.223149	-0.32
001H	34	1309.67	12459.277	1.969923	0.32
001H	35	1429.67	11806.418	1.734666	0.57
001H	39	1359.67	13253.949	1.500250	0.60
001H	40	1459.67	13776.328	1.261574	0.56
001H	44	1459.67	11073.102	1.261574	0.10
001H	43	1459.67	14775.563	0.752990	0.33
001H	53	1959.67	13176.977	0.504030	0.19

TABLE 2. CONTINUED. PRESSURES ABOVE 10,000 PSIA.

DATA ID	T RANKINE	P PSIA	RHC EXP LBMOL/FT ³	RHC CALC LBMOL/FT ³	ERROR PERCENT	
0010	30	1209.67	10162.066	2.220370	2.225070	0.21

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.68
FOR 117 DATA POINTS.

TABLE 3. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF
HOLSER AND KENNEDY, AM. J. OF SCI., V. 256, 744(1958).

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
001H	1	1247.67	2175.570	0.205706	0.206447	0.36
001H	2	1319.67	2175.570	0.182825	0.183794	0.53
001H	3	1391.67	2175.570	0.166580	0.167426	0.51
001H	4	1463.67	2175.570	0.154142	0.154701	0.36
001H	5	1535.67	2175.570	0.143909	0.144346	0.30
001H	6	1607.67	2175.570	0.135265	0.135654	0.29
001H	7	1679.67	2175.570	0.127789	0.128191	0.31
001H	8	1751.67	2175.570	0.121308	0.121675	0.30
001H	9	1247.67	3625.950	0.457606	0.453154	-0.97
001H	10	1319.67	3625.950	0.361120	0.360677	-0.12
001H	11	1391.67	3625.950	0.311301	0.312293	0.32
001H	12	1463.67	3625.950	0.279131	0.280147	0.36
001H	13	1535.67	3625.950	0.255371	0.256380	0.39
001H	14	1607.67	3625.950	0.236656	0.237684	0.43
001H	15	1679.67	3625.950	0.221327	0.222369	0.47
001H	16	1751.67	3625.950	0.208425	0.209459	0.50
001H	17	1247.67	5076.324	1.124578	1.122955	-0.14
001H	18	1319.67	5076.324	0.640007	0.6330754	-1.45
001H	19	1391.67	5076.324	0.498806	0.498596	-0.04
001H	20	1463.67	5076.324	0.428649	0.429022	0.09
001H	21	1535.67	5076.324	0.382550	0.383275	0.19
001H	22	1607.67	5076.324	0.348662	0.349790	0.32
001H	23	1679.67	5076.324	0.322114	0.323675	0.48
001H	24	1751.67	5076.324	0.300902	0.302433	0.51
001H	25	1247.67	6526.703	1.660219	1.662582	0.14
001H	26	1319.67	6526.703	1.058022	1.044664	-1.26
001H	27	1391.67	6526.703	0.744249	0.740161	-0.55
001H	28	1463.67	6526.703	0.608136	0.605166	-0.49
001H	29	1535.67	6526.703	0.527483	0.526007	-0.28
001H	30	1607.67	6526.703	0.471735	0.471939	0.05
001H	31	1679.67	6526.703	0.430565	0.431788	0.28
001H	32	1751.67	6526.703	0.398460	0.400168	0.43
001H	33	1247.67	8702.273	1.955015	1.963391	0.43
001H	34	1319.67	8702.273	1.548993	1.564987	1.03
001H	35	1391.67	8702.273	1.170501	1.166373	-0.35
001H	36	1463.67	8702.273	0.922884	0.913092	-1.06
001H	37	1535.67	8702.273	0.772599	0.766183	-0.83
001H	38	1607.67	8702.273	0.674616	0.671590	-0.45
001H	39	1679.67	8702.273	0.605165	0.604639	-0.09
001H	40	1751.67	8702.273	0.552965	0.553996	0.19
001H	41	1247.67	11603.027	2.158131	2.165918	0.36
001H	42	1319.67	11603.027	1.874701	1.894294	1.05
001H	43	1391.67	11603.027	1.580044	1.594682	0.93
001H	44	1463.67	11603.027	1.315704	1.314610	-0.09
001H	45	1535.67	11603.027	1.108758	1.101233	-0.68
001H	46	1607.67	11603.027	0.958066	0.951978	-0.64
001H	47	1679.67	11603.027	0.849008	0.845622	-0.40
001H	48	1751.67	11603.027	0.767640	0.766363	-0.17
001H	49	1247.67	14503.789	2.293781	2.295333	0.07
001H	50	1319.67	14503.789	2.068096	2.072241	0.49
001H	51	1391.67	14503.789	1.830182	1.844132	0.76
001H	52	1463.67	14503.789	1.598246	1.607036	0.55
001H	53	1535.67	14503.789	1.390615	1.391790	0.08
001H	54	1607.67	14503.789	1.217766	1.216303	-0.12
001H	55	1679.67	14503.789	1.083472	1.080622	-0.26
001H	56	1751.67	14503.789	0.979441	0.976052	-0.35
001H	57	1247.67	17404.547	2.396820	2.391379	-0.23
001H	58	1319.67	17404.547	2.206232	2.205198	-0.05
001H	59	1391.67	17404.547	2.005898	2.008413	0.13

TABLE 3. CONTINUED. HOLSER AND KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT
001H	60	1463.67	17404.547	1.801661	1.807323	0.31
001H	61	1535.67	17404.547	1.607135	1.613228	0.38
001H	62	1607.67	17404.547	1.434517	1.438913	0.29
001H	63	1679.67	17404.547	1.292174	1.291684	-0.04
001H	64	1751.67	17404.547	1.174465	1.171308	-0.27
001H	65	1247.67	20305.316	2.480828	2.468224	-0.51
001H	66	1319.67	20305.316	2.310591	2.302430	-0.35
001H	67	1391.67	20305.316	2.135590	2.129516	-0.28
001H	68	1463.67	20305.316	1.957222	1.953329	-0.20
001H	69	1535.67	20305.316	1.779475	1.779940	0.03
001H	70	1607.67	20305.316	1.614617	1.616924	0.14
001H	71	1679.67	20305.316	1.472070	1.470792	-0.09
001H	72	1751.67	20305.316	1.347395	1.344566	-0.21
001H	73	1787.67	2175.570	0.118369	0.118707	0.29
001H	74	1859.67	2175.570	0.113044	0.113261	0.19
001H	75	1931.67	2175.570	0.108246	0.108307	0.11
001H	76	2003.67	2175.570	0.103838	0.103936	0.09
001H	77	2075.67	2175.570	0.099833	0.099896	0.06
001H	78	2147.67	2175.570	0.096125	0.096193	0.07
001H	79	2219.67	2175.570	0.092708	0.092781	0.08
001H	80	2291.67	2175.570	0.089525	0.089624	0.11
001H	81	1787.67	3625.950	0.202819	0.203707	0.44
001H	82	1859.67	3625.950	0.192678	0.193330	0.34
001H	83	1931.67	3625.950	0.183794	0.184188	0.21
001H	84	2003.67	3625.950	0.175783	0.176042	0.15
001H	85	2075.67	3625.950	0.168523	0.168713	0.11
001H	86	2147.67	3625.950	0.161914	0.162068	0.09
001H	87	2219.67	3625.950	0.155804	0.156003	0.13
001H	88	2291.67	3625.950	0.150203	0.150436	0.15
001H	89	1787.67	5076.324	0.291739	0.293167	0.49
001H	90	1859.67	5076.324	0.275604	0.276731	0.41
001H	91	1931.67	5076.324	0.261771	0.262522	0.29
001H	92	2003.67	5076.324	0.249565	0.250050	0.19
001H	93	2075.67	5076.324	0.238643	0.238968	0.14
001H	94	2147.67	5076.324	0.228773	0.229025	0.11
001H	95	2219.67	5076.324	0.219784	0.220028	0.11
001H	96	2291.67	5076.324	0.211347	0.211631	0.23
001H	97	1787.67	6526.703	0.384928	0.385647	0.45
001H	98	1859.67	6526.703	0.361572	0.363031	0.40
001H	99	1931.67	6526.703	0.341930	0.342964	0.30
001H	100	2003.67	6526.703	0.324920	0.325595	0.21
001H	101	2075.67	6526.703	0.309854	0.310337	0.16
001H	102	2147.67	6526.703	0.296377	0.296773	0.13
001H	103	2219.67	6526.703	0.284139	0.284599	0.16
001H	104	2291.67	6526.703	0.272872	0.273580	0.26
001H	105	1787.67	8702.273	0.531525	0.532857	0.25
001H	106	1859.67	8702.273	0.495174	0.496633	0.29
001H	107	1931.67	8702.273	0.465405	0.466510	0.24
001H	108	2003.67	8702.273	0.440071	0.440889	0.19
001H	109	2075.67	8702.273	0.421461	0.418705	-0.65
001H	110	2147.67	8702.273	0.398460	0.399221	0.19
001H	111	2219.67	8702.273	0.381037	0.381909	0.23
001H	112	2291.67	8702.273	0.365882	0.366375	0.13
001H	113	1787.67	11603.027	0.734477	0.733762	-0.10
001H	114	1859.67	11603.027	0.678575	0.678675	0.01
001H	115	1931.67	11603.027	0.633345	0.633665	0.05
001H	116	2003.67	11603.027	0.595399	0.595968	0.10
001H	117	2075.67	11603.027	0.562745	0.563763	0.18
001H	118	2147.67	11603.027	0.534391	0.535804	0.26

TABLE 3. CONTINUED. HOLSER AND KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
001H	119	2219.67	11603.027	0.505355	0.511207	0.36
001H	120	2291.67	11603.027	0.487107	0.489328	0.46
001H	121	1787.67	14503.789	0.935581	0.932627	-0.32
001H	122	1859.67	14503.789	0.861023	0.859129	-0.22
001H	123	1931.67	14503.789	0.800231	0.799226	-0.13
001H	124	2003.67	14503.789	0.749233	0.749313	0.01
001H	125	2075.67	14503.789	0.705779	0.706928	0.16
001H	126	2147.67	14503.789	0.668247	0.670352	0.32
001H	127	2219.67	14503.789	0.635551	0.632361	0.44
001H	128	2291.67	14503.789	0.606647	0.610056	0.56
001H	129	1787.67	17404.547	1.123424	1.119905	-0.32
001H	130	1859.67	17404.547	1.034664	1.031532	-0.30
001H	131	1931.67	17404.547	0.960454	0.958645	-0.19
001H	132	2003.67	17404.547	0.897800	0.897605	-0.02
001H	133	2075.67	17404.547	0.844460	0.845700	0.15
001H	134	2147.67	17404.547	0.798205	0.800938	0.34
001H	135	2219.67	17404.547	0.758076	0.761351	0.50
001H	136	2291.67	17404.547	0.722843	0.727342	0.62
001H	137	1787.67	20305.316	1.292174	1.288352	-0.26
001H	138	1859.67	20305.316	1.193371	1.190822	-0.26
001H	139	1931.67	20305.316	1.105822	1.108203	-0.15
001H	140	2003.67	20305.316	1.038382	1.038094	-0.03
001H	141	2075.67	20305.316	0.976958	0.978018	0.11
001H	142	2147.67	20305.316	0.923130	0.925987	0.31
001H	143	2219.67	20305.316	0.876029	0.880455	0.51
001H	144	2291.67	20305.316	0.834705	0.840221	0.66
001H	145	707.67	1450.380	3.287703	3.288570	0.03
001H	146	779.67	1450.380	3.164415	3.170595	0.20
001H	147	851.67	1450.380	3.018449	3.029176	0.36
001H	148	923.67	1450.380	2.843719	2.855227	0.40
001H	149	995.67	1450.380	2.622060	2.627680	0.21
001H	150	1067.67	1450.380	0.180073	0.178315	-0.98
001H	151	1139.67	1450.380	0.148722	0.149271	0.37
001H	152	1211.67	1450.380	0.131321	0.131917	0.45
001H	153	707.67	2900.760	3.303990	3.296171	-0.24
001H	154	779.67	2900.760	3.184170	3.181765	-0.08
001H	155	851.67	2900.760	3.043247	3.046144	0.09
001H	156	923.67	2900.760	2.877216	2.882515	0.18
001H	157	995.67	2900.760	2.673396	2.676924	0.13
001H	158	1067.67	2900.760	2.403463	2.394662	-0.37
001H	159	1139.67	2900.760	1.900381	1.850967	-2.60
001H	160	1211.67	2900.760	0.347898	0.346298	-0.46
001H	161	707.67	4351.137	3.319804	3.303509	-0.49
001H	162	779.67	4351.137	3.202991	3.192388	-0.33
001H	163	851.67	4351.137	3.066489	3.061918	-0.15
001H	164	923.67	4351.137	2.907853	2.906694	-0.03
001H	165	995.67	4351.137	2.717596	2.717540	-0.00
001H	166	1067.67	4351.137	2.476576	2.474079	-0.10
001H	167	1139.67	4351.137	2.131257	2.119596	-0.55
001H	168	1211.67	4351.137	1.232479	1.265021	2.64
001H	169	707.67	5801.520	3.335448	3.310596	-0.75
001H	170	779.67	5801.520	3.221436	3.202519	-0.59
001H	171	851.67	5801.520	3.088833	3.076671	-0.40
001H	172	923.67	5801.520	2.936414	2.928997	-0.25
001H	173	995.67	5801.520	2.756696	2.752368	-0.16
001H	174	1067.67	5801.520	2.537271	2.534334	-0.12
001H	175	1139.67	5801.520	2.249156	2.248029	-0.05
001H	176	1211.67	5801.520	1.803535	1.811907	0.46
001H	177	707.67	7251.895	3.350917	3.317452	-1.00

TABLE 3. CONTINUED. HOLSER AND KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
001H	178	779.67	7251.895	3.239188	3.212213	-0.83
001H	179	851.67	7251.895	3.110493	3.090551	-0.64
001H	180	923.67	7251.895	2.963260	2.949272	-0.47
001H	181	995.67	7251.895	2.792431	2.783003	-0.34
001H	182	1067.67	7251.895	2.588981	2.583420	-0.21
001H	183	1139.67	7251.895	2.335173	2.335678	0.02
001H	184	1211.67	7251.895	1.998961	2.007324	0.42
001H	185	707.67	10152.656	3.380639	3.330545	-1.48
001H	186	779.67	10152.656	3.273430	3.230444	-1.31
001H	187	851.67	10152.656	3.150901	3.116120	-1.10
001H	188	923.67	10152.656	3.012680	2.985515	-0.90
001H	189	995.67	10152.656	2.855659	2.835368	-0.71
001H	190	1067.67	10152.656	2.674840	2.661508	-0.50
001H	191	1139.67	10152.656	2.464258	2.458313	-0.24
001H	192	1211.67	10152.656	2.217518	2.217257	-0.01
001H	193	707.67	13053.406	3.409220	3.342912	-1.94
001H	194	779.67	13053.406	3.305564	3.247363	-1.76
001H	195	851.67	13053.406	3.188561	3.139300	-1.54
001H	196	923.67	13053.406	3.057297	3.017357	-1.31
001H	197	995.67	13053.406	2.911029	2.879411	-1.09
001H	198	1067.67	13053.406	2.746869	2.723166	-0.86
001H	199	1139.67	13053.406	2.560690	2.546257	-0.56
001H	200	1211.67	13053.406	2.348136	2.346023	-0.09
001H	201	707.67	17404.547	3.449228	3.360277	-2.58
001H	202	779.67	17404.547	3.350917	3.270712	-2.39
001H	203	851.67	17404.547	3.240397	3.170572	-2.15
001H	204	923.67	17404.547	3.117762	3.059091	-1.88
001H	205	995.67	17404.547	2.983396	2.935046	-1.62
001H	206	1067.67	17404.547	2.835813	2.797414	-1.35
001H	207	1139.67	17404.547	2.673603	2.645020	-1.05
001H	208	1211.67	17404.547	2.491521	2.479607	-0.48
001H	209	707.67	20305.316	3.474451	3.371170	-2.97
001H	210	779.67	20305.316	3.378994	3.285140	-2.79
001H	211	851.67	20305.316	3.272502	3.189548	-2.53
001H	212	923.67	20305.316	3.155201	3.083850	-2.26
001H	213	995.67	20305.316	3.026890	2.967161	-1.97
001H	214	1067.67	20305.316	2.887279	2.838863	-1.68
001H	215	1139.67	20305.316	2.736467	2.698881	-1.37
001H	216	1211.67	20305.316	2.565234	2.547704	-0.68

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.50
FOR 216 DATA POINTS.

TABLE 4. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF KEENAN, KEYES, ET AL., "STEAM TABLES" JOHN WILEY, 1969

DATA ID	T RANKINE	P PSIA	RHO EXP LB/MOL/FT3	RHO CALC LB/MOL/FT3	PERCENT ERROR	
0010	1	669.67	14094.000	3.465325	3.593279	-2.17
0010	2	659.67	13368.641	3.469329	3.400455	-1.99
0010	3	634.67	10222.074	3.465325	3.417151	-1.50
0010	4	584.67	4607.340	3.469329	3.448634	-0.60
0010	5	539.67	2713.304	3.465329	3.460434	-0.12
0010	6	529.67	1464.034	3.469329	3.465225	-0.12
0010	7	509.67	452.052	3.469329	3.464945	-0.13
0010	8	409.67	14063.933	3.265253	3.454256	-0.43
0010	9	784.67	10370.430	3.265253	3.224321	-1.25
0010	10	759.67	6793.807	3.265253	3.240375	-0.76
0010	11	734.67	3344.042	3.265253	3.258135	-0.22
0010	12	719.67	1344.375	3.265253	3.269740	0.14
0010	13	519.67	14305.695	3.083385	3.041607	-1.36
0010	14	509.67	13417.554	3.083385	3.049779	-1.23
0010	15	459.67	6587.645	3.083385	3.039357	-1.64
0010	16	434.67	3255.107	3.083385	3.035945	-1.83
0010	17	419.67	1291.132	3.083385	3.053740	-1.09
0010	18	1079.67	15720.336	2.775464	2.745145	-1.09
0010	19	1059.67	13551.944	2.775464	2.750630	-0.97
0010	20	1009.67	8111.273	2.775464	2.769104	-0.27
0010	21	959.67	2701.839	2.775464	2.781717	0.37
0010	22	939.67	576.326	2.775464	2.795671	0.75
0010	23	1160.67	14470.143	2.523149	2.506520	-0.66
0010	24	1159.67	13593.023	2.523149	2.503456	-0.78
0010	25	1109.67	9176.320	2.523149	2.516731	-0.25
0010	26	1034.67	4755.152	2.523149	2.521885	-0.05
0010	27	1034.67	2575.500	2.523149	2.522938	-0.01
0010	28	1289.67	13575.109	2.220370	2.221901	0.06
0010	29	1209.67	10162.066	2.220370	2.225070	0.21
0010	30	1159.67	6746.285	2.220370	2.221626	0.07
0010	31	1134.67	5059.477	2.220370	2.216275	-0.13
0010	32	1159.67	15202.945	1.982475	1.989925	0.38
0010	33	1309.67	12459.277	1.982475	1.994204	0.59
0010	34	1209.67	6956.043	1.982475	1.994162	0.59
0010	35	1159.67	4277.137	1.982475	1.964502	-0.20
0010	36	1159.67	4277.137	1.982475	1.964454	-0.21
0010	37	1429.67	14864.257	1.734666	1.744694	0.58
0010	38	1359.67	11306.413	1.734666	1.743607	0.57
0010	39	1209.67	5303.833	1.734666	1.724094	-0.34
0010	40	1159.67	3303.629	1.734666	1.694545	-2.21
0010	41	1159.67	13253.345	1.500250	1.503503	0.22
0010	42	1209.67	5759.395	1.500250	1.500346	0.06
0010	43	1259.67	6297.852	1.500250	1.495277	-0.34
0010	44	1209.67	4637.852	1.500250	1.494307	-0.39
0010	45	1559.67	13776.328	1.261574	1.262823	0.10
0010	46	1459.67	11073.102	1.261574	1.262007	0.03
0010	47	1359.67	8342.117	1.261574	1.258076	-0.26
0010	48	1259.67	5631.852	1.261574	1.255915	-0.45
0010	49	1209.67	4320.469	1.261574	1.236536	-1.96
0010	50	1209.67	4188.379	1.110185	1.147450	3.36
0010	51	1559.67	14775.563	0.792990	0.796630	0.46
0010	52	1459.67	7780.344	0.792990	0.796630	0.46
0010	53	1259.67	4720.324	0.792990	0.781001	-1.51
0010	54	1209.67	3919.446	0.792990	0.783591	-1.19
0010	55	1559.67	13170.977	0.504639	0.505575	0.19
0010	56	1459.67	9602.172	0.504639	0.506310	0.33

TABLE 4. CONTINUED. KEENAN, KEYES, ET AL.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT	
0010	64	1459.67	5688.734	0.504630	0.503982	-0.13
0010	65	1209.67	3434.606	0.504630	0.495319	-1.35
0010	66	2859.67	7812.117	0.252315	0.253411	0.43
0010	67	2459.67	6564.293	0.252315	0.252884	0.23
0010	68	1959.67	5005.074	0.252315	0.253731	0.38
0010	69	1459.67	3322.942	0.252315	0.253462	0.45
0010	70	1209.67	2372.065	0.252315	0.252392	0.03
0010	71	2859.67	3104.061	0.100926	0.101233	0.30
0010	72	2459.67	2644.306	0.100926	0.101134	0.21
0010	73	1959.67	2069.674	0.100926	0.101264	0.34
0010	74	1459.67	1474.609	0.100926	0.101370	0.44
0010	75	1209.67	1157.043	0.100926	0.101461	0.53
0010	76	1159.67	1089.934	0.100926	0.101481	0.55
0010	77	1109.67	1020.631	0.100926	0.101460	0.53
0010	78	1059.67	943.238	0.100926	0.101324	0.39
0010	79	1009.67	871.402	0.100926	0.100915	-0.01
0010	80	2859.67	952.205	0.027755	0.027797	0.12
0010	81	2459.67	730.966	0.027755	0.027776	0.08
0010	82	1959.67	579.492	0.027755	0.027784	0.10
0010	83	1459.67	426.617	0.027755	0.027803	0.17
0010	84	1159.67	332.747	0.027755	0.027830	0.27
0010	85	959.67	267.416	0.027755	0.027876	0.44
0010	86	859.67	232.317	0.027755	0.027870	0.42
0010	87	2859.67	170.363	0.005551	0.005562	0.02
0010	88	2459.67	146.450	0.005551	0.005552	0.01
0010	89	1959.67	116.564	0.005551	0.005552	0.02
0010	90	1459.67	86.624	0.005551	0.005553	0.04
0010	91	1159.67	68.574	0.005551	0.005554	0.06
0010	92	959.67	56.442	0.005551	0.005558	0.12
0010	93	859.67	50.300	0.005551	0.005561	0.18
0010	94	759.67	44.034	0.005551	0.005566	0.27
0010	95	2859.67	34.069	0.001110	0.001110	-0.00
0010	96	2459.67	29.301	0.001110	0.001110	-0.00
0010	97	1959.67	25.340	0.001110	0.001110	0.00
0010	98	1459.67	17.377	0.001110	0.001110	0.00
0010	99	1159.67	13.796	0.001110	0.001110	0.01
0010	100	959.67	11.404	0.001110	0.001110	0.02
0010	101	859.67	10.206	0.001110	0.001111	0.04
0010	102	759.67	9.003	0.001110	0.001111	0.06
0010	103	659.67	7.790	0.001110	0.001111	0.10
0010	104	2859.67	3.407	0.000111	0.000111	0.02
0010	105	2459.67	2.930	0.000111	0.000111	0.00
0010	106	1959.67	2.335	0.000111	0.000111	0.03
0010	107	1459.67	1.739	0.000111	0.000111	0.02
0010	108	1159.67	1.381	0.000111	0.000111	-0.01
0010	109	959.67	1.143	0.000111	0.000111	0.01
0010	110	859.67	1.024	0.000111	0.000111	0.04
0010	111	759.67	0.905	0.000111	0.000111	0.07
0010	112	659.67	0.785	0.000111	0.000111	-0.00
0010	113	559.67	0.666	0.000111	0.000111	0.09

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.45
FOR 103 DATA POINTS.

TABLE 5. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF KENNEDY, AM. J. OF SCI., V. 255, 724(1957).

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
001K	1	851.67	145.038	0.016852	0.016895	0.25
001K	2	869.67	145.038	0.016406	0.016451	0.27
001K	3	887.67	145.038	0.015990	0.016036	0.29
001K	4	887.67	290.076	0.033919	0.034063	0.43
001K	5	905.67	145.038	0.015601	0.015648	0.30
001K	6	905.67	290.076	0.032899	0.033040	0.43
001K	7	923.67	145.038	0.015573	0.015283	-1.86
001K	8	923.67	290.076	0.031974	0.032103	0.41
001K	9	923.67	435.114	0.050868	0.050957	0.17
001K	10	941.67	145.038	0.014891	0.014939	0.32
001K	11	941.67	290.076	0.031122	0.031240	0.38
001K	12	941.67	435.114	0.049139	0.049293	0.31
001K	13	959.67	145.038	0.014517	0.014613	0.66
001K	14	959.67	290.076	0.030330	0.030440	0.36
001K	15	959.67	435.114	0.047607	0.047789	0.38
001K	16	959.67	580.152	0.066954	0.067117	0.24
001K	17	977.67	145.038	0.014220	0.014304	0.59
001K	18	977.67	290.076	0.029592	0.029695	0.35
001K	19	977.67	435.114	0.046224	0.046418	0.42
001K	20	977.67	580.152	0.064597	0.064825	0.35
001K	21	977.67	725.190	0.085424	0.085446	0.03
001K	22	995.67	145.038	0.013901	0.014010	0.79
001K	23	995.67	290.076	0.028904	0.028997	0.32
001K	24	995.67	435.114	0.044960	0.045159	0.44
001K	25	995.67	580.152	0.062490	0.062769	0.45
001K	26	995.67	725.190	0.082049	0.082222	0.21
001K	27	995.67	870.228	0.104527	0.104128	-0.38
001K	28	1013.67	145.038	0.013714	0.013730	0.12
001K	29	1013.67	290.076	0.028256	0.028341	0.30
001K	30	1013.67	435.114	0.043801	0.043995	0.44
001K	31	1013.67	580.152	0.060612	0.060906	0.49
001K	32	1013.67	725.190	0.079092	0.079375	0.36
001K	33	1013.67	870.228	0.099833	0.099837	0.00
001K	34	1013.67	1015.266	0.123688	0.122969	-0.58
001K	35	1031.67	145.038	0.013448	0.013462	0.11
001K	36	1031.67	290.076	0.027646	0.027723	0.28
001K	37	1031.67	435.114	0.042738	0.042913	0.41
001K	38	1031.67	580.152	0.058923	0.059205	0.48
001K	39	1031.67	725.190	0.076493	0.076829	0.44
001K	40	1031.67	870.228	0.095886	0.096106	0.23
001K	41	1031.67	1015.266	0.117636	0.117505	-0.15
001K	42	1031.67	1160.304	0.143018	0.141761	-0.88
001K	43	1049.67	145.038	0.013192	0.013207	0.11
001K	44	1049.67	290.076	0.027068	0.027138	0.26
001K	45	1049.67	435.114	0.041745	0.041902	0.38
001K	46	1049.67	580.152	0.057382	0.057639	0.45
001K	47	1049.67	725.190	0.074170	0.074527	0.48
001K	48	1049.67	870.228	0.092485	0.092809	0.35
001K	49	1049.67	1015.266	0.112750	0.112821	0.06
001K	50	1049.67	1160.304	0.135529	0.135055	-0.35
001K	51	1049.67	1305.342	0.161914	0.160282	-1.01
001K	52	1067.67	145.038	0.012951	0.012962	0.09
001K	53	1067.67	290.076	0.026519	0.026534	0.24
001K	54	1067.67	435.114	0.040812	0.040955	0.35
001K	55	1067.67	580.152	0.055957	0.056189	0.41
001K	56	1067.67	725.190	0.072074	0.072428	0.49
001K	57	1067.67	870.228	0.089502	0.089858	0.40
001K	58	1067.67	1015.266	0.108483	0.108727	0.23
001K	59	1067.67	1160.304	0.129410	0.129379	-0.02

TABLE 5. CONTINUED. KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT
001K	60	1067.67	1305.342	0.152986	0.152315	-0.44
001K	61	1067.67	1450.380	0.180073	0.178315	-0.98
001K	62	1103.67	145.038	0.012493	0.012502	0.07
001K	63	1103.67	290.076	0.025498	0.025555	0.22
001K	64	1103.67	435.114	0.039091	0.039222	0.33
001K	65	1103.67	580.152	0.053382	0.053579	0.37
001K	66	1103.67	725.190	0.068393	0.068718	0.48
001K	67	1103.67	870.228	0.084364	0.084755	0.46
001K	68	1103.67	1015.266	0.101409	0.101833	0.42
001K	69	1103.67	1160.304	0.119717	0.120136	0.35
001K	70	1103.67	1305.342	0.139565	0.139908	0.25
001K	71	1103.67	1450.380	0.161337	0.161482	0.06
001K	72	1139.67	145.038	0.012076	0.012077	0.01
001K	73	1139.67	290.076	0.024566	0.024618	0.21
001K	74	1139.67	435.114	0.037551	0.037668	0.31
001K	75	1139.67	580.152	0.051093	0.051280	0.37
001K	76	1139.67	725.190	0.065216	0.065516	0.46
001K	77	1139.67	870.228	0.080078	0.080451	0.46
001K	78	1139.67	1015.266	0.095674	0.096171	0.52
001K	79	1139.67	1160.304	0.112203	0.112786	0.52
001K	80	1139.67	1305.342	0.129895	0.130430	0.41
001K	81	1139.67	1450.380	0.148722	0.149271	0.37
001K	82	1175.67	145.038	0.011677	0.011633	0.05
001K	83	1175.67	290.076	0.023722	0.023759	0.16
001K	84	1175.67	435.114	0.036180	0.036262	0.23
001K	85	1175.67	580.152	0.049048	0.049230	0.37
001K	86	1175.67	725.190	0.062445	0.062704	0.41
001K	87	1175.67	870.228	0.076375	0.076734	0.47
001K	88	1175.67	1015.266	0.090909	0.091378	0.51
001K	89	1175.67	1160.304	0.106094	0.106702	0.57
001K	90	1175.67	1305.342	0.122120	0.122786	0.55
001K	91	1175.67	1450.380	0.139062	0.139726	0.48
001K	92	1211.67	145.038	0.011312	0.011315	0.03
001K	93	1211.67	290.076	0.022938	0.022967	0.13
001K	94	1211.67	435.114	0.034898	0.034980	0.23
001K	95	1211.67	580.152	0.047218	0.047380	0.34
001K	96	1211.67	725.190	0.059972	0.060199	0.38
001K	97	1211.67	870.228	0.073122	0.073468	0.47
001K	98	1211.67	1015.266	0.086792	0.087228	0.50
001K	99	1211.67	1160.304	0.101025	0.101522	0.49
001K	100	1211.67	1305.342	0.115800	0.116399	0.52
001K	101	1211.67	1450.380	0.131321	0.131917	0.45
001K	102	1247.67	145.038	0.010968	0.010972	0.03
001K	103	1247.67	290.076	0.022204	0.022233	0.13
001K	104	1247.67	435.114	0.033727	0.033802	0.22
001K	105	1247.67	580.152	0.045562	0.045698	0.30
001K	106	1247.67	725.190	0.057755	0.057943	0.32
001K	107	1247.67	870.228	0.070235	0.070560	0.46
001K	108	1247.67	1015.266	0.083210	0.083576	0.44
001K	109	1247.67	1160.304	0.096607	0.097020	0.43
001K	110	1247.67	1305.342	0.110452	0.110924	0.43
001K	111	1247.67	1450.380	0.124800	0.125326	0.42
001K	112	1283.67	145.038	0.010645	0.010650	0.04
001K	113	1283.67	290.076	0.021515	0.021550	0.16
001K	114	1283.67	435.114	0.032620	0.032714	0.29
001K	115	1283.67	580.152	0.044041	0.044157	0.26
001K	116	1283.67	725.190	0.055759	0.055894	0.24
001K	117	1283.67	870.228	0.067685	0.067941	0.38
001K	118	1283.67	1015.266	0.080041	0.080318	0.35

TABLE 5. CONTINUED. KENNEDY.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT	
001K	119	1283.67	1160.304	0.092683	0.093044	0.39
001K	120	1283.67	1305.342	0.105706	0.106142	0.41
001K	121	1283.67	1450.380	0.119141	0.119635	0.41
001K	122	1319.67	145.038	0.010340	0.010347	0.06
001K	123	1319.67	290.076	0.020880	0.020912	0.15
001K	124	1319.67	435.114	0.031624	0.031705	0.26
001K	125	1319.67	580.152	0.042643	0.042737	0.22
001K	126	1319.67	725.190	0.053913	0.054018	0.20
001K	127	1319.67	870.228	0.065401	0.065562	0.25
001K	128	1319.67	1015.266	0.077140	0.077381	0.31
001K	129	1319.67	1160.304	0.089157	0.089490	0.37
001K	130	1319.67	1305.342	0.101465	0.101903	0.43
001K	131	1319.67	1450.380	0.114161	0.114637	0.42
001K	132	1355.67	145.038	0.010056	0.010062	0.06
001K	133	1355.67	290.076	0.020294	0.020314	0.10
001K	134	1355.67	435.114	0.030697	0.030765	0.22
001K	135	1355.67	580.152	0.041342	0.041421	0.19
001K	136	1355.67	725.190	0.052200	0.052291	0.17
001K	137	1355.67	870.228	0.063277	0.063384	0.17
001K	138	1355.67	1015.266	0.074505	0.074710	0.28
001K	139	1355.67	1160.304	0.085995	0.086279	0.33
001K	140	1355.67	1305.342	0.097668	0.098101	0.44
001K	141	1355.67	1450.380	0.109718	0.110188	0.43
001K	142	1391.67	145.038	0.009789	0.009793	0.04
001K	143	1391.67	290.076	0.019739	0.019753	0.07
001K	144	1391.67	435.114	0.029860	0.029885	0.09
001K	145	1391.67	580.152	0.040132	0.040196	0.16
001K	146	1391.67	725.190	0.050608	0.050692	0.16
001K	147	1391.67	870.228	0.061243	0.061379	0.22
001K	148	1391.67	1015.266	0.072104	0.072264	0.22
001K	149	1391.67	1160.304	0.083090	0.083355	0.32
001K	150	1391.67	1305.342	0.094270	0.094659	0.41
001K	151	1391.67	1450.380	0.105770	0.106183	0.39
001K	152	1427.67	145.038	0.009536	0.009539	0.03
001K	153	1427.67	290.076	0.019214	0.019224	0.05
001K	154	1427.67	435.114	0.029023	0.029060	0.13
001K	155	1427.67	580.152	0.039004	0.039053	0.13
001K	156	1427.67	725.190	0.049135	0.049205	0.13
001K	157	1427.67	870.228	0.059397	0.059522	0.21
001K	158	1427.67	1015.266	0.069895	0.070010	0.16
001K	159	1427.67	1160.304	0.080450	0.080673	0.28
001K	160	1427.67	1305.342	0.091220	0.091517	0.33
001K	161	1427.67	1450.380	0.102246	0.102547	0.29
001K	162	1463.67	145.038	0.009296	0.009297	0.02
001K	163	1463.67	290.076	0.018727	0.018725	-0.01
001K	164	1463.67	435.114	0.028259	0.028284	0.09
001K	165	1463.67	580.152	0.037941	0.037981	0.10
001K	166	1463.67	725.190	0.047758	0.047817	0.12
001K	167	1463.67	870.228	0.057688	0.057796	0.19
001K	168	1463.67	1015.266	0.067778	0.067922	0.21
001K	169	1463.67	1160.304	0.078025	0.078199	0.22
001K	170	1463.67	1305.342	0.088429	0.088630	0.23
001K	171	1463.67	1450.380	0.099006	0.099221	0.22
001K	172	1499.67	145.038	0.009067	0.009069	0.02
001K	173	1499.67	290.076	0.018244	0.018252	0.04
001K	174	1499.67	435.114	0.027536	0.027553	0.06
001K	175	1499.67	580.152	0.036939	0.036973	0.09
001K	176	1499.67	725.190	0.046472	0.046516	0.09
001K	177	1499.67	870.228	0.056111	0.056183	0.13

TABLE 5. CONTINUED. KENNEDY.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT	
001K	178	1499.67	1015.266	0.065285	0.065979	0.14
001K	179	1499.67	1160.304	0.075791	0.075905	0.15
001K	180	1499.67	1305.342	0.085246	0.085964	0.14
001K	181	1499.67	1450.380	0.095992	0.096159	0.17
001K	182	1535.67	145.038	0.008852	0.008851	-0.01
001K	183	1535.67	290.076	0.017804	0.017804	0.00
001K	184	1535.67	435.114	0.026854	0.026861	0.03
001K	185	1535.67	580.152	0.036000	0.036023	0.07
001K	186	1535.67	725.190	0.045259	0.045293	0.08
001K	187	1535.67	870.228	0.054626	0.054673	0.09
001K	188	1535.67	1015.266	0.064095	0.064164	0.11
001K	189	1535.67	1160.304	0.073666	0.073768	0.14
001K	190	1535.67	1305.342	0.083410	0.083438	0.09
001K	191	1535.67	1450.380	0.093156	0.093325	0.18
001K	192	1571.67	145.038	0.008645	0.008644	-0.01
001K	193	1571.67	290.076	0.017376	0.017379	0.02
001K	194	1571.67	435.114	0.026213	0.026206	-0.03
001K	195	1571.67	580.152	0.035114	0.035126	0.03
001K	196	1571.67	725.190	0.044113	0.044141	0.06
001K	197	1571.67	870.228	0.053234	0.053253	0.03
001K	198	1571.67	1015.266	0.062411	0.062462	0.08
001K	199	1571.67	1160.304	0.071687	0.071770	0.12
001K	200	1571.67	1305.342	0.081108	0.081179	0.09
001K	201	1571.67	1450.380	0.090530	0.090690	0.18
001K	202	1607.67	145.038	0.008451	0.008447	-0.05
001K	203	1607.67	290.076	0.016584	0.016974	-0.06
001K	204	1607.67	435.114	0.025599	0.025534	-0.06
001K	205	1607.67	580.152	0.034274	0.034276	0.01
001K	206	1607.67	725.190	0.043030	0.043053	0.05
001K	207	1607.67	870.228	0.051896	0.051914	0.04
001K	208	1607.67	1015.266	0.060814	0.060862	0.08
001K	209	1607.67	1160.304	0.069811	0.069896	0.12
001K	210	1607.67	1305.342	0.078530	0.079018	0.11
001K	211	1607.67	1450.380	0.088070	0.088230	0.18
001K	212	1643.67	145.038	0.008263	0.008258	-0.06
001K	213	1643.67	290.076	0.016594	0.016589	-0.03
001K	214	1643.67	435.114	0.025005	0.024993	-0.05
001K	215	1643.67	580.152	0.033477	0.033471	-0.02
001K	216	1643.67	725.190	0.041998	0.042023	0.06
001K	217	1643.67	870.228	0.050631	0.050650	0.04
001K	218	1643.67	1015.266	0.059306	0.059353	0.08
001K	219	1643.67	1160.304	0.068044	0.068133	0.13
001K	220	1643.67	1305.342	0.076500	0.076990	0.12
001K	221	1643.67	1450.380	0.085762	0.085924	0.19
001K	222	1679.67	145.038	0.008086	0.008079	-0.10
001K	223	1679.67	290.076	0.016237	0.016222	-0.09
001K	224	1679.67	435.114	0.024441	0.024430	-0.04
001K	225	1679.67	580.152	0.032713	0.032705	-0.02
001K	226	1679.67	725.190	0.041024	0.041045	0.05
001K	227	1679.67	870.228	0.049433	0.049452	0.04
001K	228	1679.67	1015.266	0.057820	0.057927	0.08
001K	229	1679.67	1160.304	0.066377	0.066469	0.14
001K	230	1679.67	1305.342	0.074810	0.075079	0.36
001K	231	1679.67	1450.380	0.083611	0.083758	0.17
001K	232	1715.67	145.038	0.007913	0.007906	-0.08
001K	233	1715.67	290.076	0.015880	0.015871	-0.06
001K	234	1715.67	435.114	0.023902	0.023894	-0.03
001K	235	1715.67	580.152	0.031986	0.031975	-0.03
001K	236	1715.67	725.190	0.040095	0.040116	0.05

TABLE 5. CONTINUED. KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
001K	237	1715.67	870.228	0.048297	0.048316	0.04
001K	238	1715.67	1015.266	0.056531	0.056576	0.08
001K	239	1715.67	1160.304	0.064814	0.064895	0.13
001K	240	1715.67	1305.342	0.073169	0.073275	0.15
001K	241	1715.67	1450.380	0.081547	0.081715	0.21
001K	242	1751.67	145.038	0.007748	0.007742	-0.09
001K	243	1751.67	290.076	0.015545	0.015535	-0.07
001K	244	1751.67	435.114	0.023386	0.023382	-0.02
001K	245	1751.67	580.152	0.031293	0.031280	-0.04
001K	246	1751.67	725.190	0.039215	0.039232	0.04
001K	247	1751.67	870.228	0.047231	0.047236	0.01
001K	248	1751.67	1015.266	0.055252	0.055293	0.07
001K	249	1751.67	1160.304	0.063334	0.063404	0.11
001K	250	1751.67	1305.342	0.071450	0.071568	0.16
001K	251	1751.67	1450.380	0.079637	0.079785	0.19
001K	252	1787.67	145.038	0.007591	0.007584	-0.09
001K	253	1787.67	290.076	0.015225	0.015214	-0.07
001K	254	1787.67	435.114	0.022892	0.022892	-0.00
001K	255	1787.67	580.152	0.030630	0.030616	-0.04
001K	256	1787.67	725.190	0.038373	0.038388	0.04
001K	257	1787.67	870.228	0.046206	0.046207	0.00
001K	258	1787.67	1015.266	0.054047	0.054074	0.05
001K	259	1787.67	1160.304	0.061932	0.061938	0.09
001K	260	1787.67	1305.342	0.069853	0.069949	0.14
001K	261	1787.67	1450.380	0.077832	0.077957	0.16
001K	262	1823.67	145.038	0.007439	0.007432	-0.10
001K	263	1823.67	290.076	0.014917	0.014906	-0.07
001K	264	1823.67	435.114	0.022448	0.022423	-0.11
001K	265	1823.67	580.152	0.029994	0.029982	-0.04
001K	266	1823.67	725.190	0.037567	0.037563	0.04
001K	267	1823.67	870.228	0.045229	0.045227	-0.01
001K	268	1823.67	1015.266	0.052893	0.052912	0.04
001K	269	1823.67	1160.304	0.060580	0.060640	0.10
001K	270	1823.67	1305.342	0.068325	0.068410	0.12
001K	271	1823.67	1450.380	0.076124	0.076222	0.13
001K	272	1859.67	145.038	0.007292	0.007287	-0.08
001K	273	1859.67	290.076	0.014621	0.014611	-0.07
001K	274	1859.67	435.114	0.021964	0.021974	0.04
001K	275	1859.67	580.152	0.029384	0.029375	-0.03
001K	276	1859.67	725.190	0.036794	0.036813	0.05
001K	277	1859.67	870.228	0.044294	0.044290	-0.01
001K	278	1859.67	1015.266	0.051787	0.051804	0.03
001K	279	1859.67	1160.304	0.059306	0.059356	0.08
001K	280	1859.67	1305.342	0.066876	0.066945	0.10
001K	281	1859.67	1450.380	0.074489	0.074572	0.11
001K	282	1895.67	145.038	0.007154	0.007147	-0.10
001K	283	1895.67	290.076	0.014337	0.014328	-0.07
001K	284	1895.67	435.114	0.021555	0.021543	-0.06
001K	285	1895.67	580.152	0.028803	0.028793	-0.04
001K	286	1895.67	725.190	0.036059	0.036076	0.05
001K	287	1895.67	870.228	0.043396	0.043394	-0.01
001K	288	1895.67	1015.266	0.050734	0.050745	0.02
001K	289	1895.67	1160.304	0.058094	0.058130	0.06
001K	290	1895.67	1305.342	0.065487	0.065548	0.09
001K	291	1895.67	1450.380	0.072923	0.073000	0.11
001K	292	1931.67	145.038	0.007019	0.007012	-0.10
001K	293	1931.67	290.076	0.014064	0.014055	-0.06
001K	294	1931.67	435.114	0.021135	0.021129	-0.02
001K	295	1931.67	580.152	0.028245	0.028234	-0.04

TABLE 5. CONTINUED. KENNEDY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
001K	296	1931.67	725.190	0.035354	0.035370	0.05
001K	297	1931.67	870.228	0.042534	0.042536	0.00
001K	298	1931.67	1015.266	0.049716	0.049732	0.03
001K	299	1931.67	1160.304	0.056930	0.056958	0.05
001K	300	1931.67	1305.342	0.064155	0.064214	0.09
001K	301	1931.67	1450.380	0.071436	0.071500	0.09
001K	302	1967.67	145.038	0.006888	0.006883	-0.08
001K	303	1967.67	290.076	0.013801	0.013793	-0.06
001K	304	1967.67	435.114	0.020743	0.020732	-0.05
001K	305	1967.67	580.152	0.027708	0.027698	-0.04
001K	306	1967.67	725.190	0.034675	0.034692	0.05
001K	307	1967.67	870.228	0.041705	0.041713	0.02
001K	308	1967.67	1015.266	0.048738	0.048761	0.05
001K	309	1967.67	1160.304	0.055813	0.055836	0.04
001K	310	1967.67	1305.342	0.062887	0.062938	0.08
001K	311	1967.67	1450.380	0.070008	0.070067	0.09
001K	312	2003.67	145.038	0.006763	0.006758	-0.08
001K	313	2003.67	290.076	0.013553	0.013541	-0.09
001K	314	2003.67	435.114	0.020365	0.020350	-0.08
001K	315	2003.67	580.152	0.027191	0.027133	-0.03
001K	316	2003.67	725.190	0.034022	0.034041	0.06
001K	317	2003.67	870.228	0.040913	0.040924	0.03
001K	318	2003.67	1015.266	0.047804	0.047831	0.06
001K	319	2003.67	1160.304	0.054747	0.054762	0.03
001K	320	2003.67	1305.342	0.061668	0.061717	0.08
001K	321	2003.67	1450.380	0.068650	0.068695	0.07
001K	322	2039.67	145.038	0.006641	0.006638	-0.06
001K	323	2039.67	290.076	0.013308	0.013298	-0.08
001K	324	2039.67	435.114	0.019990	0.019981	-0.04
001K	325	2039.67	580.152	0.026693	0.026687	-0.02
001K	326	2039.67	725.190	0.033396	0.033415	0.06
001K	327	2039.67	870.228	0.040150	0.040165	0.04
001K	328	2039.67	1015.266	0.046912	0.046937	0.05
001K	329	2039.67	1160.304	0.053704	0.053731	0.05
001K	330	2039.67	1305.342	0.060495	0.060546	0.08
001K	331	2039.67	1450.380	0.067344	0.067382	0.06
001K	332	2075.67	145.038	0.006526	0.006522	-0.07
001K	333	2075.67	290.076	0.013073	0.013064	-0.07
001K	334	2075.67	435.114	0.019639	0.019627	-0.06
001K	335	2075.67	580.152	0.026213	0.026210	-0.01
001K	336	2075.67	725.190	0.032796	0.032813	0.05
001K	337	2075.67	870.228	0.039420	0.039436	0.04
001K	338	2075.67	1015.266	0.046052	0.046078	0.06
001K	339	2075.67	1160.304	0.052716	0.052740	0.05
001K	340	2075.67	1305.342	0.059377	0.059422	0.08
001K	341	2075.67	1450.380	0.066099	0.066122	0.03
001K	342	2111.67	145.038	0.014415	0.014410	-55.53
001K	343	2111.67	290.076	0.012845	0.012838	-0.06
001K	344	2111.67	435.114	0.019289	0.019285	-0.02
001K	345	2111.67	580.152	0.025751	0.025750	-0.01
001K	346	2111.67	725.190	0.032217	0.032233	0.05
001K	347	2111.67	870.228	0.038716	0.038734	0.05
001K	348	2111.67	1015.266	0.045224	0.045252	0.06
001K	349	2111.67	1160.304	0.051764	0.051798	0.05
001K	350	2111.67	1305.342	0.058299	0.058341	0.07
001K	351	2111.67	1450.380	0.064862	0.064911	0.08
001K	352	2147.67	145.038	0.006305	0.006301	-0.05
001K	353	2147.67	290.076	0.012621	0.012620	-0.01
001K	354	2147.67	435.114	0.018859	0.018955	0.51

TABLE 5. CONTINUED. KENNEDY.

DATA ID	T RANKINE	P PSIA	RHC EXP LBMOL/FT3	RHC CALC LBMOL/FT3	ERROR PERCENT
001K 355	2147.67	580.152	0.025304	0.025306	0.01
001K 356	2147.67	725.190	0.031659	0.031674	0.05
001K 357	2147.67	870.228	0.038037	0.038058	0.05
001K 358	2147.67	1015.266	0.044424	0.044437	0.07
001K 359	2147.67	1160.304	0.050846	0.050872	0.05
001K 360	2147.67	1305.342	0.057259	0.057303	0.08
001K 361	2147.67	1450.380	0.063683	0.063748	0.10
001K 362	2183.67	145.038	0.006201	0.006197	-0.07
001K 363	2183.67	290.076	0.012413	0.012409	-0.03
001K 364	2183.67	435.114	0.018646	0.018636	-0.05
001K 365	2183.67	580.152	0.024876	0.024878	0.01
001K 366	2183.67	725.190	0.031119	0.031135	0.05
001K 367	2183.67	870.228	0.037381	0.037406	0.07
001K 368	2183.67	1015.266	0.043658	0.043691	0.08
001K 369	2183.67	1160.304	0.049952	0.049990	0.07
001K 370	2183.67	1305.342	0.056256	0.056303	0.08
001K 371	2183.67	1450.380	0.062569	0.062629	0.10
001K 372	2219.67	145.038	0.006101	0.006096	-0.08
001K 373	2219.67	290.076	0.012208	0.012205	-0.02
001K 374	2219.67	435.114	0.018331	0.018328	-0.01
001K 375	2219.67	580.152	0.024460	0.024465	0.02
001K 376	2219.67	725.190	0.030597	0.030614	0.06
001K 377	2219.67	870.228	0.036747	0.036777	0.08
001K 378	2219.67	1015.266	0.042923	0.042952	0.07
001K 379	2219.67	1160.304	0.049097	0.049135	0.09
001K 380	2219.67	1305.342	0.055288	0.055339	0.09
001K 381	2219.67	1450.380	0.061493	0.061551	0.09
001K 382	2255.67	145.038	0.005999	0.005998	-0.02
001K 383	2255.67	290.076	0.012009	0.012008	-0.01
001K 384	2255.67	435.114	0.018035	0.018031	-0.03
001K 385	2255.67	580.152	0.024058	0.024065	0.03
001K 386	2255.67	725.190	0.030093	0.030112	0.06
001K 387	2255.67	870.228	0.036138	0.036169	0.09
001K 388	2255.67	1015.266	0.042213	0.042238	0.06
001K 389	2255.67	1160.304	0.048263	0.048319	0.11
001K 390	2255.67	1305.342	0.054352	0.054410	0.11
001K 391	2255.67	1450.380	0.060422	0.060512	0.15
001K 392	2291.67	145.038	0.005905	0.005903	-0.04
001K 393	2291.67	290.076	0.011817	0.011818	0.01
001K 394	2291.67	435.114	0.017740	0.017743	0.02
001K 395	2291.67	580.152	0.023669	0.023679	0.04
001K 396	2291.67	725.190	0.029605	0.029625	0.07
001K 397	2291.67	870.228	0.035553	0.035582	0.08
001K 398	2291.67	1015.266	0.041505	0.041549	0.11
001K 399	2291.67	1160.304	0.047458	0.047526	0.15
001K 400	2291.67	1305.342	0.053447	0.053513	0.12
001K 401	2291.67	1450.380	0.059407	0.059509	0.17

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.31
FOR 401 DATA POINTS.

TABLE 6. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF
KEYES AND SMITH. PROC. AM. ACAD. ARTS AND SCI., 258(1934).

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT	
002K	1	545.67	62.063	3.453388	3.459388	0.17
002K	2	545.67	324.939	3.456499	3.460155	0.11
002K	3	545.67	682.358	3.460219	3.461201	0.03
002K	4	545.67	1120.520	3.464846	3.462475	-0.07
002K	5	545.67	1558.696	3.469402	3.463734	-0.16
002K	6	545.67	1996.843	3.473966	3.464982	-0.26
002K	7	545.67	2435.004	3.478447	3.466228	-0.35
002K	8	545.67	2873.137	3.482901	3.467458	-0.44
002K	9	545.67	3311.282	3.487295	3.468691	-0.53
002K	10	545.67	3749.429	3.491697	3.469891	-0.62
002K	11	545.67	4187.570	3.496019	3.471095	-0.71
002K	12	545.67	4625.730	3.500315	3.472287	-0.80
002K	13	581.67	61.960	3.427279	3.436846	0.28
002K	14	581.67	324.851	3.430139	3.437660	0.22
002K	15	581.67	682.270	3.433918	3.438769	0.14
002K	16	581.67	1120.432	3.438342	3.440117	0.05
002K	17	581.67	1558.608	3.442808	3.441455	-0.04
002K	18	581.67	1996.755	3.447194	3.442782	-0.13
002K	19	581.67	2434.931	3.451578	3.444101	-0.22
002K	20	581.67	2873.063	3.455995	3.445407	-0.31
002K	21	581.67	3311.209	3.460361	3.446708	-0.39
002K	22	581.67	3749.385	3.464875	3.447995	-0.48
002K	23	581.67	4187.527	3.468801	3.449274	-0.56
002K	24	581.67	4625.703	3.473043	3.450546	-0.65
002K	25	581.67	5063.852	3.477221	3.451812	-0.73
002K	26	626.67	62.475	3.381586	3.391099	0.28
002K	27	626.67	325.351	3.384429	3.392068	0.23
002K	28	626.67	682.755	3.388290	3.393381	0.15
002K	29	626.67	1120.916	3.392756	3.394975	0.07
002K	30	626.67	1559.078	3.397232	3.396560	-0.02
002K	31	626.67	1997.240	3.401732	3.398130	-0.11
002K	32	626.67	2435.372	3.406172	3.399686	-0.19
002K	33	626.67	3311.665	3.410992	3.402766	-0.36
002K	34	626.67	4187.973	3.423674	3.405792	-0.52
002K	35	626.67	5064.266	3.432198	3.408772	-0.68
002K	36	671.67	62.666	3.324335	3.333576	0.28
002K	37	671.67	325.571	3.327233	3.334782	0.23
002K	38	671.67	683.020	3.331563	3.336407	0.15
002K	39	671.67	1121.181	3.335999	3.338377	0.07
002K	40	671.67	1559.343	3.340964	3.340330	-0.02
002K	41	671.67	1997.489	3.346606	3.342269	-0.10
002K	42	671.67	2435.651	3.350359	3.344181	-0.18
002K	43	671.67	3311.958	3.355548	3.347961	-0.34
002K	44	671.67	4188.277	3.362626	3.351668	-0.50
002K	45	671.67	5064.590	3.377533	3.355310	-0.66
002K	46	761.67	102.522	3.180632	3.192213	0.36
002K	47	761.67	326.747	3.184052	3.193889	0.31
002K	48	761.67	684.136	3.188914	3.198525	0.24
002K	49	761.67	1122.269	3.194790	3.199718	0.15
002K	50	761.67	1560.401	3.200495	3.202861	0.07
002K	51	761.67	1998.518	3.205837	3.205957	0.00
002K	52	761.67	2436.665	3.211693	3.209009	-0.08
002K	53	761.67	3312.928	3.222671	3.214987	-0.24
002K	54	761.67	4189.203	3.233426	3.220801	-0.39
002K	55	761.67	5065.480	3.243937	3.226466	-0.54
002K	56	851.67	240.332	2.999573	3.013924	0.48
002K	57	851.67	685.341	3.007576	3.019639	0.40
002K	58	851.67	1123.459	3.016302	3.025162	0.33
002K	59	851.67	1561.606	3.022778	3.030521	0.26

TABLE 6. CONTINUED. KEYES, AND SMITH.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
002K	60	851.67	1999.738	3.030257	3.035761	0.18
002K	61	851.67	2437.885	3.037683	3.040872	0.10
002K	62	851.67	3314.148	3.051950	3.050755	-0.04
002K	63	851.67	4190.426	3.065674	3.060224	-0.18
002K	64	851.67	5066.703	3.079068	3.069313	-0.32
002K	65	941.67	573.409	2.771319	2.733577	0.44
002K	66	941.67	683.255	2.774200	2.786226	0.43
002K	67	941.67	1121.357	2.786129	2.796953	0.39
002K	68	941.67	1559.475	2.797588	2.807178	0.34
002K	69	941.67	1997.578	2.808804	2.816948	0.29
002K	70	941.67	2435.695	2.819651	2.826315	0.24
002K	71	941.67	3311.915	2.840302	2.843962	0.13
002K	72	941.67	4188.176	2.859241	2.860369	0.02
002K	73	941.67	5064.426	2.878553	2.875717	-0.10
002K	74	1031.67	1269.469	2.471950	2.466121	-0.24
002K	75	1031.67	1561.959	2.487291	2.483579	-0.15
002K	76	1031.67	1999.973	2.508924	2.507333	-0.06
002K	77	1031.67	2438.017	2.529092	2.528791	-0.01
002K	78	1031.67	3314.148	2.565641	2.566504	0.03
002K	79	1031.67	4190.133	2.598472	2.599050	0.02
002K	80	1031.67	5066.438	2.628258	2.627612	-0.02
002K	81	1067.67	1656.383	2.315985	2.294660	-0.92
002K	82	1067.67	1997.769	2.342318	2.326921	-0.66
002K	83	1067.67	2435.724	2.372389	2.362311	-0.42
002K	84	1067.67	2873.710	2.399491	2.392896	-0.27
002K	85	1067.67	3311.708	2.424069	2.419930	-0.17
002K	86	1067.67	4187.750	2.468260	2.466315	-0.08
002K	87	1067.67	5063.852	2.506495	2.505430	-0.04
002K	88	1085.67	1911.015	2.227225	2.196980	-1.36
002K	89	1085.67	1998.577	2.236829	2.208494	-1.27
002K	90	1085.67	2436.459	2.276958	2.258304	-0.32
002K	91	1085.67	2874.371	2.311399	2.298965	-0.54
002K	92	1085.67	3312.312	2.341743	2.333556	-0.35
002K	93	1085.67	4188.242	2.394217	2.390674	-0.15
002K	94	1085.67	5064.266	2.438992	2.437205	-0.07
002K	95	1103.67	2145.086	2.120034	2.078967	-1.94
002K	96	1103.67	2437.209	2.160769	2.128958	-1.47
002K	97	1103.67	2875.003	2.208229	2.187422	-0.94
002K	98	1103.67	3312.855	2.247839	2.233996	-0.62
002K	99	1103.67	3750.752	2.282242	2.272959	-0.41
002K	100	1103.67	4188.676	2.312774	2.306618	-0.27
002K	101	1103.67	4626.645	2.340434	2.336328	-0.18
002K	102	1103.67	5064.590	2.365730	2.362986	-0.12
002K	103	1121.67	2476.899	2.010234	1.958883	-2.55
002K	104	1121.67	2875.870	2.079570	2.046383	-1.60
002K	105	1121.67	3313.604	2.136215	2.114874	-1.01
002K	106	1121.67	3751.413	2.181993	2.167727	-0.65
002K	107	1121.67	4189.250	2.220882	2.211414	-0.43
002K	108	1121.67	4627.156	2.254975	2.248730	-0.28
002K	109	1121.67	5065.086	2.285534	2.281390	-0.18
002K	110	1139.67	2785.560	1.862714	1.897367	-2.97
002K	111	1139.67	2873.004	1.891999	1.841216	-2.68
002K	112	1139.67	2877.516	1.893556	1.842834	-2.68
002K	113	1139.67	3314.927	1.993811	1.961702	-1.61
002K	114	1139.67	3752.604	2.061652	2.040707	-1.02
002K	115	1139.67	4190.359	2.114240	2.100667	-0.64
002K	116	1139.67	4628.219	2.158072	2.149323	-0.41
002K	117	1139.67	5066.102	2.195999	2.190441	-0.25
002K	118	1157.67	3137.600	1.671416	1.640926	-1.82

TABLE 6. CONTINUED. KEYES, AND SMITH.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
002K	119	1157.67	3312.105	1.772704	1.733478	-2.21
002K	120	1157.67	3486.935	1.835553	1.800038	-1.93
002K	121	1157.67	3661.810	1.883040	1.852429	-1.63
002K	122	1157.67	3836.816	1.921942	1.895844	-1.36
002K	123	1164.87	3226.852	1.457501	1.519708	4.27
002K	124	1164.87	3313.354	1.606056	1.591427	-0.91
002K	125	1164.87	3487.744	1.723244	1.690964	-1.87
002K	126	1164.87	3662.486	1.792998	1.761762	-1.74
002K	127	1164.87	3837.372	1.844886	1.817172	-1.50
002K	128	1164.87	4012.321	1.886962	1.862843	-1.28
002K	129	1164.87	4099.816	1.908360	1.893024	-1.33

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.58
 FOR 129 DATA POINTS.

TABLE 7. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF
KEYES, SMITH AND GERRY, PRCC. AM. ACAD. ARTS SCI., V 70, 319 (1936).

DATA ID	T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT	
004K	1	842.67	202.621	0.024773	0.024655	-0.48
004K	2	844.47	204.252	0.024773	0.024797	0.10
004K	3	846.27	205.119	0.024773	0.024836	0.26
004K	4	848.07	205.795	0.024773	0.024850	0.31
004K	5	849.87	206.339	0.024773	0.024845	0.29
004K	6	851.67	206.838	0.024773	0.024835	0.25
004K	7	851.67	194.288	0.023121	0.023181	0.26
004K	8	869.67	212.790	0.024773	0.024868	0.38
004K	9	869.67	199.740	0.023121	0.023204	0.36
004K	10	874.17	228.228	0.034682	0.034644	-0.11
004K	11	887.67	301.484	0.035571	0.035537	0.04
004K	12	887.67	295.194	0.034682	0.034745	0.18
004K	13	887.67	218.551	0.024773	0.024883	0.44
004K	14	887.67	205.046	0.023121	0.023216	0.41
004K	15	901.17	385.607	0.046243	0.046142	-0.22
004K	16	905.67	389.192	0.046243	0.046243	0.00
004K	17	905.67	389.501	0.046243	0.046286	0.09
004K	18	905.67	310.185	0.035571	0.035621	0.14
004K	19	905.67	303.638	0.034682	0.034782	0.29
004K	20	905.67	224.151	0.024773	0.024835	0.45
004K	21	905.67	210.189	0.023121	0.023214	0.40
004K	22	923.67	401.259	0.046243	0.046338	0.21
004K	23	923.67	401.346	0.046243	0.046350	0.23
004K	24	923.67	318.738	0.035571	0.035648	0.22
004K	25	923.67	311.815	0.034682	0.034784	0.30
004K	26	923.67	229.662	0.024773	0.024884	0.45
004K	27	923.67	215.259	0.023121	0.023209	0.38
004K	28	941.67	578.865	0.069364	0.069510	0.21
004K	29	941.67	573.927	0.069364	0.068762	-0.86
004K	30	941.67	514.127	0.060316	0.060067	-0.41
004K	31	941.67	412.707	0.046243	0.046369	0.27
004K	32	941.67	412.957	0.046243	0.046401	0.34
004K	33	941.67	327.114	0.035571	0.035665	0.26
004K	34	941.67	319.928	0.034682	0.034797	0.33
004K	35	941.67	235.350	0.024773	0.024908	0.55
004K	36	941.67	220.241	0.023121	0.023200	0.34
004K	37	959.67	596.560	0.069364	0.069457	0.13
004K	38	959.67	594.752	0.069364	0.069197	-0.24
004K	39	959.67	529.823	0.060316	0.060148	-0.28
004K	40	959.67	424.052	0.046243	0.046403	0.35
004K	41	959.67	424.273	0.046243	0.046431	0.41
004K	42	959.67	335.315	0.035571	0.035671	0.28
004K	43	959.67	327.688	0.034682	0.034778	0.28
004K	44	959.67	240.523	0.024773	0.024879	0.43
004K	45	959.67	225.195	0.023121	0.023193	0.31
004K	46	966.87	722.538	0.087802	0.087189	-0.70
004K	47	966.87	717.586	0.086705	0.086408	-0.34
004K	48	966.87	715.557	0.086705	0.086089	-0.71
004K	49	968.67	720.069	0.086705	0.086432	-0.31
004K	50	977.67	739.557	0.087802	0.087641	-0.18
004K	51	977.67	732.709	0.086705	0.086592	-0.13
004K	52	977.67	732.694	0.086705	0.086589	-0.13
004K	53	977.67	731.195	0.086705	0.086361	-0.40
004K	54	977.67	545.092	0.060316	0.060196	-0.20
004K	55	977.67	434.899	0.046243	0.046392	0.32
004K	56	977.67	435.281	0.046243	0.046438	0.42
004K	57	977.67	343.384	0.035571	0.035671	0.28
004K	58	977.67	335.447	0.034682	0.034769	0.25
004K	59	977.67	246.092	0.024773	0.024899	0.51

TABLE 7. CONTINUED. KEYES, SMITH AND GERRY.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
004K	60	977.67	230.118	0.023121	0.28
004K	61	995.67	764.335	0.087802	0.07
004K	62	995.67	757.355	0.086705	0.16
004K	63	995.67	757.032	0.086705	0.10
004K	64	995.67	755.650	0.086705	-0.13
004K	65	995.67	633.242	0.069364	0.41
004K	66	995.67	631.773	0.069364	0.13
004K	67	995.67	559.995	0.060316	-0.16
004K	68	995.67	445.965	0.046243	0.39
004K	69	995.67	446.112	0.046243	0.43
004K	70	995.67	351.320	0.035571	0.26
004K	71	995.67	343.251	0.034682	0.20
004K	72	995.67	251.120	0.024773	0.37
004K	73	995.67	234.997	0.023121	0.25
004K	74	997.47	936.603	0.115607	-0.81
004K	75	997.47	935.021	0.115607	-1.05
004K	76	1013.67	968.308	0.115607	-0.34
004K	77	1013.67	967.338	0.115607	-0.55
004K	78	1013.67	788.247	0.087802	0.22
004K	79	1013.67	780.722	0.086705	0.28
004K	80	1013.67	574.647	0.060316	-0.13
004K	81	1013.67	456.399	0.046243	0.32
004K	82	1013.67	456.781	0.046243	0.42
004K	83	1013.67	359.138	0.035571	0.23
004K	84	1013.67	350.703	0.034682	0.19
004K	85	1013.67	256.425	0.024773	0.37
004K	86	1013.67	239.832	0.023121	0.21
004K	87	1031.67	1002.595	0.115607	-0.06
004K	88	1031.67	1001.493	0.115607	-0.21
004K	89	1031.67	811.673	0.087802	0.34
004K	90	1031.67	803.384	0.086705	0.33
004K	91	1031.67	804.016	0.086705	0.43
004K	92	1031.67	802.620	0.086705	0.21
004K	93	1031.67	668.441	0.069364	0.57
004K	94	1031.67	666.720	0.069364	0.26
004K	95	1031.67	589.006	0.060316	-0.13
004K	96	1031.67	466.864	0.046243	0.29
004K	97	1031.67	467.261	0.046243	0.39
004K	98	1031.67	366.884	0.035571	0.20
004K	99	1031.67	358.271	0.034682	0.17
004K	100	1031.67	261.627	0.024773	0.34
004K	101	1031.67	244.638	0.023121	0.18
004K	102	1049.67	1360.631	0.173410	-1.43
004K	103	1049.67	833.952	0.087802	0.33
004K	104	1049.67	825.826	0.086705	0.39
004K	105	1040.67	1331.561	0.173410	-1.83
004K	106	1040.67	1330.018	0.173410	-2.01
004K	107	1041.57	1333.927	0.173410	-1.35
004K	108	1042.47	1339.483	0.173410	-1.50
004K	109	1049.67	825.488	0.086705	0.34
004K	110	1049.67	603.071	0.060316	-0.15
004K	111	1049.67	477.283	0.046243	0.28
004K	112	1049.67	477.577	0.046243	0.34
004K	113	1049.67	374.540	0.035571	0.16
004K	114	1049.67	365.663	0.034682	0.11
004K	115	1049.67	266.682	0.024773	0.26
004K	116	1049.67	249.414	0.023121	0.14
004K	117	1055.07	1488.564	0.198183	-1.91
004K	118	1067.67	1532.639	0.198183	-1.66

TABLE 7. CONTINUED. KEYES, SMITH AND GERRY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
004K	119	1067.67	1415.287	0.173410	0.171684	-1.00
004K	120	1067.67	1417.463	0.173410	0.172089	-0.76
004K	121	1067.67	1415.890	0.173410	0.171796	-0.93
004K	122	1067.67	1067.127	0.115607	0.115885	0.24
004K	123	1067.67	1066.495	0.115607	0.115797	0.16
004K	124	1067.67	856.233	0.087802	0.088118	0.36
004K	125	1067.67	847.077	0.086705	0.086987	0.33
004K	126	1067.67	847.136	0.086705	0.086994	0.33
004K	127	1067.67	848.150	0.086705	0.087119	0.48
004K	128	1067.67	847.151	0.086705	0.086996	0.34
004K	129	1067.67	701.773	0.069364	0.069731	0.53
004K	130	1067.67	700.847	0.069364	0.069625	0.38
004K	131	1067.67	616.959	0.060316	0.060208	-0.18
004K	132	1067.67	487.247	0.046243	0.046325	0.18
004K	133	1067.67	487.747	0.046243	0.046377	0.29
004K	134	1067.67	382.124	0.035571	0.035611	0.11
004K	135	1067.67	373.159	0.034682	0.034718	0.10
004K	136	1067.67	271.914	0.024773	0.024639	0.27
004K	137	1067.67	254.206	0.023121	0.023149	0.12
004K	138	1071.27	1674.887	0.231213	0.224437	-2.93
004K	139	1085.67	1740.256	0.231213	0.226501	-2.04
004K	140	1085.67	1597.362	0.198183	0.196045	-1.08
004K	141	1085.67	1469.782	0.173410	0.172473	-0.54
004K	142	1085.67	877.646	0.087802	0.088074	0.31
004K	143	1085.67	868.593	0.086705	0.086995	0.33
004K	144	1085.67	868.505	0.086705	0.086985	0.32
004K	145	1085.67	630.700	0.060316	0.060191	-0.21
004K	146	1085.67	497.579	0.046243	0.046327	0.18
004K	147	1085.67	497.770	0.046243	0.046346	0.22
004K	148	1085.67	389.663	0.035571	0.035596	0.07
004K	149	1085.67	380.522	0.034682	0.034706	0.07
004K	150	1085.67	276.867	0.024773	0.024816	0.17
004K	151	1085.67	258.952	0.023121	0.023142	0.09
004K	152	1090.17	1919.260	0.277456	0.267745	-3.50
004K	153	1103.67	1993.683	0.277456	0.270211	-2.61
004K	154	1103.67	1818.325	0.231213	0.228193	-1.31
004K	155	1103.67	1660.528	0.198183	0.196955	-0.62
004K	156	1103.67	1523.351	0.173410	0.173160	-0.14
004K	157	1103.67	1522.954	0.173410	0.173094	-0.18
004K	158	1103.67	1522.396	0.173410	0.173003	-0.23
004K	159	1103.67	1129.293	0.115607	0.116109	0.43
004K	160	1103.67	1129.161	0.115607	0.116092	0.42
004K	161	1103.67	891.283	0.086705	0.087166	0.53
004K	162	1103.67	890.402	0.086705	0.087065	0.41
004K	163	1103.67	734.604	0.069364	0.069731	0.53
004K	164	1103.67	733.561	0.069364	0.069618	0.37
004K	165	1111.77	2231.414	0.346820	0.330975	-4.57
004K	166	1121.67	2301.574	0.346820	0.333922	-3.72
004K	167	1121.67	2090.062	0.277456	0.272620	-1.74
004K	168	1121.67	1893.467	0.231213	0.229307	-0.82
004K	169	1121.67	1721.753	0.198183	0.197589	-0.30
004K	170	1121.67	1574.040	0.173410	0.173448	0.02
004K	171	1135.17	2621.885	0.462427	0.432372	-6.50
004K	172	1139.67	2665.784	0.462427	0.435385	-5.85
004K	173	1139.67	2426.936	0.346820	0.338125	-2.51
004K	174	1139.67	2183.400	0.277456	0.274285	-1.14
004K	175	1139.67	1967.229	0.231213	0.230233	-0.42
004K	176	1139.67	1781.729	0.198183	0.198098	-0.04
004K	177	1139.67	1624.022	0.173410	0.173712	0.17

TABLE 7. CONTINUED. KEYES, SMITH AND GERRY.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
004K 178	1139.67	1623.316	0.173410	0.173608	0.11
004K 179	1139.67	1624.330	0.173410	0.173757	0.20
004K 180	1139.67	1188.946	0.115607	0.116184	0.50
004K 181	1139.67	1188.079	0.115607	0.116081	0.41
004K 182	1139.67	933.184	0.086705	0.087172	0.54
004K 183	1139.67	932.169	0.086705	0.087062	0.41
004K 184	1139.67	766.981	0.069364	0.069744	0.55
004K 185	1139.67	765.761	0.069364	0.069620	0.37
004K 186	1147.77	2852.855	0.554912	0.514321	-7.31
004K 187	1157.67	3233.597	1.734098	1.696316	-2.18
004K 188	1157.67	2967.973	0.554912	0.523398	-5.68
004K 189	1157.67	2839.745	0.462427	0.444818	-3.81
004K 190	1157.67	2548.138	0.346820	0.340630	-1.73
004K 191	1157.67	2274.150	0.277456	0.275456	-0.72
004K 192	1160.37	3097.786	0.693640	0.661057	-4.70
004K 195	1175.67	3936.868	1.734098	1.709710	-1.41
004K 197	1175.67	3393.877	0.867050	0.860794	-0.72
004K 198	1175.67	3318.749	0.693640	0.674065	-2.82
004K 199	1175.67	3176.398	0.554912	0.534878	-3.61
004K 200	1175.67	3008.123	0.462427	0.450131	-2.66
004K 201	1175.67	2665.725	0.346820	0.342579	-1.22
004K 202	1175.67	2359.023	0.277456	0.275593	-0.67
004K 203	1175.67	2108.257	0.231213	0.231227	0.01
004K 204	1175.67	1905.827	0.198183	0.199937	0.39
004K 205	1175.67	1720.842	0.173410	0.174016	0.35
004K 206	1175.67	1720.210	0.173410	0.173931	0.30
004K 207	1175.67	1721.033	0.173410	0.174042	0.36
004K 208	1175.67	1246.924	0.115607	0.116211	0.52
004K 209	1175.67	1246.322	0.115607	0.116144	0.46
004K 210	1175.67	974.069	0.086705	0.087152	0.52
004K 211	1175.67	973.276	0.086705	0.087071	0.42
004K 212	1175.67	798.137	0.069364	0.069687	0.47
004K 213	1175.67	797.388	0.069364	0.069615	0.36
004K 214	1193.67	4663.168	1.734098	1.720631	-0.78
004K 215	1193.67	3856.421	1.156065	1.251822	8.28
004K 216	1193.67	3714.511	0.867050	0.917760	5.85
004K 218	1211.67	4275.895	1.156065	1.190921	3.02
004K 217	1211.67	5403.227	1.734098	1.723244	-0.34
004K 219	1211.67	4032.233	0.867050	0.874290	0.84
004K 220	1211.67	3831.599	0.693640	0.631606	-1.73
004K 221	1211.67	3578.862	0.554912	0.543959	-1.97
004K 222	1211.67	3333.474	0.462427	0.455644	-1.47
004K 223	1211.67	2893.872	0.346820	0.344849	-0.57
004K 224	1211.67	2534.191	0.277456	0.277365	-0.03
004K 225	1211.67	2243.714	0.231213	0.231765	0.24
004K 226	1211.67	2008.511	0.198183	0.198993	0.41
004K 227	1211.67	1814.076	0.173410	0.174121	0.41
004K 228	1211.67	1813.548	0.173410	0.174056	0.37
004K 229	1211.67	1815.532	0.173410	0.174301	0.51
004K 230	1211.67	1303.256	0.115607	0.116180	0.50
004K 231	1211.67	1303.197	0.115607	0.116174	0.49
004K 232	1211.67	1014.278	0.086705	0.087133	0.49
004K 233	1211.67	1013.514	0.086705	0.087059	0.41
004K 234	1211.67	829.264	0.069364	0.069673	0.45
004K 235	1211.67	828.647	0.069364	0.069616	0.36
004K 236	1229.67	4699.945	1.156065	1.165588	0.82
004K 237	1229.67	4343.340	0.867050	0.858418	-1.00
004K 238	1247.67	5128.516	1.156065	1.154785	-0.11
004K 239	1247.67	4661.988	0.867050	0.857011	-1.16

TABLE 7. CONTINUED. KEYES, SMITH AND GERRY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
004K	240	1247.67	4329.035	0.693640	0.682468	-1.61
004K	241	1247.67	3964.323	0.554912	0.546486	-1.52
004K	242	1247.67	3645.452	0.462427	0.457928	-0.97
004K	243	1247.67	3112.351	0.346820	0.345822	-0.27
004K	244	1247.67	2698.425	0.277456	0.277735	0.12
004K	245	1247.67	2373.500	0.231213	0.231896	0.30
004K	246	1247.67	2115.267	0.198183	0.199019	0.42
004K	247	1247.67	1905.019	0.173410	0.174182	0.45
004K	248	1247.67	1905.078	0.173410	0.174189	0.45
004K	249	1247.67	1905.137	0.173410	0.174196	0.45
004K	250	1247.67	1358.529	0.115607	0.116145	0.47
004K	251	1247.67	1358.500	0.115607	0.116143	0.46
004K	252	1247.67	1053.475	0.086705	0.087075	0.43
004K	253	1247.67	1053.122	0.086705	0.087042	0.39
004K	254	1247.67	859.789	0.069364	0.069639	0.40
004K	255	1247.67	859.230	0.069364	0.069590	0.33
004K	256	1265.07	4975.309	0.867050	0.854950	-1.40
004K	257	1283.67	5286.477	0.867050	0.853789	-1.53
004K	258	1283.67	4818.031	0.693640	0.683881	-1.41
004K	259	1283.67	4343.383	0.554912	0.548845	-1.09
004K	260	1283.67	3949.171	0.462427	0.459434	-0.65
004K	261	1283.67	3324.040	0.346820	0.346471	-0.10
004K	262	1283.67	2857.940	0.277456	0.278019	0.20
004K	263	1283.67	2499.786	0.231213	0.231936	0.31
004K	264	1283.67	2218.554	0.198183	0.198903	0.36
004K	265	1283.67	1993.933	0.173410	0.174209	0.46
004K	266	1283.67	1993.669	0.173410	0.174181	0.44
004K	267	1283.67	1992.757	0.173410	0.174083	0.39
004K	268	1283.67	1413.098	0.115607	0.116123	0.45
004K	269	1283.67	1413.230	0.115607	0.116140	0.46
004K	270	1283.67	1092.244	0.086705	0.087027	0.37
004K	271	1283.67	1092.111	0.086705	0.087016	0.36
004K	272	1283.67	889.946	0.069364	0.069604	0.35
004K	273	1283.67	889.814	0.069364	0.069593	0.33
004K	274	1319.67	5293.277	0.693640	0.683823	-1.42
004K	275	1319.67	4709.402	0.554912	0.549520	-0.97
004K	276	1319.67	4242.875	0.462427	0.460020	-0.52
004K	277	1319.67	3529.673	0.346820	0.346768	-0.01
004K	278	1319.67	3012.606	0.277456	0.278041	0.21
004K	279	1319.67	2622.928	0.231213	0.231904	0.30
004K	280	1319.67	2320.371	0.198183	0.198855	0.34
004K	281	1319.67	2080.833	0.173410	0.174186	0.45
004K	282	1319.67	2080.730	0.173410	0.174175	0.44
004K	283	1319.67	2079.320	0.173410	0.174034	0.36
004K	284	1319.67	1466.549	0.115607	0.116077	0.41
004K	285	1319.67	1467.240	0.115607	0.116139	0.46
004K	286	1319.67	1130.851	0.086705	0.087007	0.35

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.73
FOR 283 DATA POINTS.

TABLE 8. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF
KELL AND WALLEY, PHIL. TRANS. ROY. SOC. (LONDON), 258A, 565 (1965).

DATA ID		T RANKINE	P PSIA	RHO EXP LBMOL/FT3	RHO CALC LBMOL/FT3	ERROR PERCENT
003K	1	491.67	76.870	3.468608	3.412975	-1.60
003K	2	509.67	76.870	3.467884	3.452994	-0.43
003K	3	527.66	76.870	3.462670	3.462022	-0.02
003K	4	536.67	76.870	3.458656	3.461755	0.09
003K	5	536.67	76.870	3.458652	3.461755	0.09
003K	6	536.68	76.870	3.458636	3.461749	0.09
003K	7	545.87	76.870	3.453673	3.459359	0.16
003K	8	491.67	182.748	3.469892	3.413616	-1.62
003K	9	509.67	182.748	3.469083	3.453363	-0.45
003K	10	527.66	182.748	3.463821	3.462349	-0.04
003K	11	536.67	182.748	3.459768	3.462069	0.07
003K	12	536.67	182.748	3.459771	3.462069	0.07
003K	13	536.68	182.748	3.459771	3.462068	0.07
003K	14	545.87	182.748	3.454795	3.459670	0.14
003K	15	491.67	290.076	3.471190	3.414249	-1.64
003K	16	509.67	290.076	3.470319	3.453738	-0.48
003K	17	527.66	290.076	3.464999	3.462667	-0.07
003K	18	536.67	290.076	3.460946	3.462386	0.04
003K	19	536.67	290.076	3.460937	3.462386	0.04
003K	20	536.63	290.076	3.460931	3.462388	0.04
003K	21	545.87	290.076	3.455928	3.459987	0.12
003K	22	491.67	397.404	3.472497	3.414893	-1.66
003K	23	509.67	397.404	3.471531	3.454112	-0.50
003K	24	527.66	397.404	3.466159	3.462992	-0.09
003K	25	536.67	397.404	3.462070	3.462705	0.02
003K	26	536.67	397.404	3.462073	3.462705	0.02
003K	27	536.68	397.404	3.462070	3.462702	0.02
003K	28	545.87	397.404	3.457058	3.460300	0.09
003K	29	491.67	610.755	3.475061	3.416141	-1.70
003K	30	509.67	610.755	3.473945	3.454844	-0.55
003K	31	527.66	610.755	3.468486	3.463638	-0.14
003K	32	536.67	610.755	3.464366	3.463332	-0.03
003K	33	536.67	610.755	3.464373	3.463332	-0.03
003K	34	536.68	610.755	3.464366	3.463331	-0.03
003K	35	545.87	610.755	3.459324	3.460921	0.05
003K	36	491.67	823.961	3.477651	3.417375	-1.73
003K	37	509.67	823.961	3.476371	3.455582	-0.60
003K	38	527.66	823.961	3.470801	3.464283	-0.19
003K	39	536.67	823.961	3.466655	3.463955	-0.08
003K	40	536.67	823.961	3.466655	3.463955	-0.08
003K	41	536.68	823.961	3.466648	3.463956	-0.08
003K	42	545.87	823.961	3.461599	3.461541	-0.00
003K	43	491.67	1037.167	3.480205	3.418562	-1.77
003K	44	509.67	1037.167	3.478766	3.456313	-0.65
003K	45	527.66	1037.167	3.473088	3.464917	-0.24
003K	46	536.67	1037.167	3.468888	3.464581	-0.12
003K	47	536.67	1037.167	3.468885	3.464581	-0.12
003K	48	536.68	1037.167	3.468892	3.464575	-0.12
003K	49	545.87	1037.167	3.463808	3.462161	-0.05
003K	50	491.67	1465.029	3.485318	3.420958	-1.85
003K	51	509.67	1465.029	3.483571	3.457757	-0.74
003K	52	527.66	1465.029	3.477706	3.466137	-0.33
003K	53	536.67	1465.029	3.473442	3.465821	-0.22
003K	54	536.67	1465.029	3.473454	3.465821	-0.22
003K	55	536.68	1465.029	3.473440	3.465819	-0.22
003K	56	545.87	1465.029	3.468333	3.463396	-0.14
003K	57	491.67	1893.036	3.490408	3.423278	-1.92
003K	58	509.67	1893.036	3.488351	3.459200	-0.84
003K	59	527.66	1893.036	3.482285	3.467446	-0.43

TABLE 8. CONTINUED. KELL AND WHALLEY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT
003K	60	536.67	1893.036	3.477940	3.467053	-0.31
003K	61	536.67	1893.036	3.477971	3.467053	-0.31
003K	62	536.68	1893.036	3.477950	3.467052	-0.31
003K	63	545.87	1893.036	3.472779	3.464615	-0.24
003K	64	491.67	3049.859	3.504003	3.425213	-2.13
003K	65	509.67	3049.859	3.501190	3.462991	-1.09
003K	66	527.66	3049.859	3.494579	3.470799	-0.68
003K	67	536.67	3049.859	3.490060	3.470334	-0.57
003K	68	536.67	3049.859	3.490074	3.470334	-0.57
003K	69	536.68	3049.859	3.490064	3.470333	-0.57
003K	70	545.87	3049.859	3.484719	3.467873	-0.48
003K	71	491.67	4742.016	3.523414	3.437267	-2.44
003K	72	509.67	4742.016	3.519470	3.468352	-1.45
003K	73	527.66	4742.016	3.512146	3.475573	-1.04
003K	74	536.67	4742.016	3.507337	3.475011	-0.92
003K	75	536.67	4742.016	3.507340	3.475011	-0.92
003K	76	536.68	4742.016	3.507347	3.475007	-0.92
003K	77	545.87	4742.016	3.501812	3.472534	-0.84
003K	78	491.67	6432.285	3.542324	3.444671	-2.76
003K	79	509.67	6432.285	3.537311	3.473496	-1.80
003K	80	527.66	6432.285	3.529247	3.480198	-1.39
003K	81	536.67	6432.285	3.524232	3.479556	-1.27
003K	82	536.67	6432.285	3.524244	3.479556	-1.27
003K	83	536.68	6432.285	3.524234	3.479556	-1.27
003K	84	545.87	6432.285	3.518484	3.477055	-1.18
003K	85	491.67	8123.723	3.560727	3.451563	-3.07
003K	86	509.67	8123.723	3.554790	3.478456	-2.15
003K	87	527.66	8123.723	3.546070	3.484693	-1.73
003K	88	536.67	8123.723	3.540810	3.483974	-1.61
003K	89	536.67	8123.723	3.540817	3.483974	-1.61
003K	90	536.68	8123.723	3.540795	3.483972	-1.60
003K	91	545.87	8123.723	3.534863	3.481461	-1.51
003K	92	491.67	9814.859	3.578628	3.458043	-3.37
003K	93	509.67	9814.859	3.571813	3.483235	-2.48
003K	94	527.66	9814.859	3.562447	3.489055	-2.06
003K	95	536.67	9814.859	3.556948	3.488276	-1.93
003K	96	536.67	9814.859	3.556944	3.488276	-1.93
003K	97	536.68	9814.859	3.556952	3.488276	-1.93
003K	98	545.87	9814.859	3.550800	3.485752	-1.83
003K	99	491.67	11505.707	3.596067	3.464143	-3.67
003K	100	509.67	11505.707	3.588377	3.467864	-2.80
003K	101	527.66	11505.707	3.578424	3.493301	-2.33
003K	102	536.67	11505.707	3.572700	3.492471	-2.25
003K	103	536.67	11505.707	3.572700	3.492471	-2.25
003K	104	536.68	11505.707	3.572718	3.492466	-2.25
003K	105	545.87	11505.707	3.566396	3.489945	-2.14
003K	106	491.67	13196.277	3.613068	3.469935	-3.96
003K	107	509.67	13196.277	3.604592	3.492351	-3.11
003K	108	527.66	13196.277	3.594077	3.497444	-2.69
003K	109	536.67	13196.277	3.588142	3.496561	-2.55
003K	110	536.67	13196.277	3.588154	3.496561	-2.55
003K	111	536.68	13196.277	3.588154	3.496557	-2.55
003K	112	545.87	13196.277	3.581673	3.494032	-2.45
003K	113	491.67	14886.547	3.629610	3.475448	-4.25
003K	114	509.67	14886.547	3.620408	3.496693	-3.42
003K	115	527.66	14886.547	3.609371	3.501476	-2.99
003K	116	536.67	14886.547	3.603233	3.500549	-2.85
003K	117	536.67	14886.547	3.603244	3.500549	-2.85
003K	118	536.68	14886.547	3.603241	3.500549	-2.85

TABLE 8. CONTINUED. KELL AND WHALLEY.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
003K	119	545.87	14886.547	3.498026	-2.74
003K	120	563.67	76.870	3.450313	0.25
003K	121	581.68	76.870	3.436379	0.28
003K	122	599.67	76.870	3.420348	0.29
003K	123	617.67	76.870	3.401388	0.28
003K	124	635.67	76.870	3.380447	0.28
003K	125	653.68	76.870	3.357793	0.28
003K	126	671.68	76.870	3.333630	0.28
003K	127	563.67	290.076	3.450948	0.20
003K	128	581.68	290.076	3.437542	0.23
003K	129	599.67	290.076	3.421054	0.24
003K	130	617.67	290.076	3.402145	0.24
003K	131	635.67	290.076	3.381266	0.24
003K	132	653.68	290.076	3.358689	0.23
003K	133	671.68	290.076	3.334605	0.23
003K	134	563.67	610.755	3.451900	0.13
003K	135	581.68	610.755	3.438538	0.16
003K	136	599.67	610.755	3.422112	0.18
003K	137	617.67	610.755	3.403278	0.17
003K	138	635.67	610.755	3.382494	0.17
003K	139	653.68	610.755	3.360023	0.17
003K	140	671.68	610.755	3.336061	0.17
003K	141	563.67	1037.167	3.451874	0.04
003K	142	581.68	1037.167	3.439849	0.08
003K	143	599.67	1037.167	3.423507	0.09
003K	144	617.67	1037.167	3.404778	0.09
003K	145	635.67	1037.167	3.384113	0.09
003K	146	653.68	1037.167	3.361784	0.08
003K	147	671.68	1037.167	3.337989	0.09
003K	148	563.67	1465.029	3.454414	-0.05
003K	149	581.68	1465.029	3.441160	-0.01
003K	150	599.67	1465.029	3.424920	-0.00
003K	151	617.67	1465.029	3.406209	0.00
003K	152	635.67	1465.029	3.385745	-0.00
003K	153	653.68	1465.029	3.363559	-0.00
003K	154	671.68	1465.029	3.339823	0.00
003K	155	563.67	1893.036	3.455658	-0.15
003K	156	581.68	1893.036	3.442460	-0.10
003K	157	599.67	1893.036	3.426273	-0.09
003K	158	617.67	1893.036	3.407746	-0.08
003K	159	635.67	1893.036	3.387326	-0.09
003K	160	653.68	1893.036	3.365274	-0.08
003K	161	671.68	1893.036	3.341796	-0.08
003K	162	563.67	3049.859	3.458975	-0.39
003K	163	581.68	3049.859	3.445924	-0.34
003K	164	599.67	3049.859	3.429948	-0.32
003K	165	617.67	3049.859	3.411634	-0.31
003K	166	635.67	3049.859	3.391580	-0.31
003K	167	653.68	3049.859	3.369392	-0.31
003K	168	671.68	3049.859	3.346828	-0.30
003K	169	563.67	4742.016	3.463716	-0.73
003K	170	581.68	4742.016	3.450674	-0.68
003K	171	599.67	4742.016	3.435196	-0.65
003K	172	617.67	4742.016	3.417306	-0.64
003K	173	635.67	4742.016	3.397642	-0.63
003K	174	653.68	4742.016	3.376461	-0.62
003K	175	671.68	4742.016	3.353969	-0.61
003K	176	563.67	6432.285	3.468327	-1.07
003K	177	581.68	6432.285	3.455685	-1.00

TABLE 8. CONTINUED. KELL AND WHALLEY.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT
003K	178	599.67	6432.285	3.473965	3.440295	-0.97
003K	179	617.67	6432.285	3.455537	3.422759	-0.95
003K	180	635.67	6432.285	3.435707	3.403514	-0.94
003K	181	653.68	6432.285	3.414376	3.382813	-0.92
003K	182	671.68	6432.285	3.391726	3.360860	-0.91
003K	183	683.67	8123.723	3.521808	3.472820	-1.39
003K	184	681.68	8123.723	3.506670	3.460381	-1.32
003K	185	599.67	8123.723	3.489941	3.445265	-1.28
003K	186	617.67	8123.723	3.471576	3.428070	-1.25
003K	187	635.67	8123.723	3.451909	3.409225	-1.24
003K	188	653.68	8123.723	3.430817	3.388975	-1.22
003K	189	671.68	8123.723	3.408472	3.367531	-1.20
003K	190	683.67	9814.859	3.537480	3.477204	-1.70
003K	191	681.68	9814.859	3.522229	3.464958	-1.63
003K	192	599.67	9814.859	3.505465	3.450106	-1.58
003K	193	617.67	9814.859	3.487168	3.433242	-1.55
003K	194	635.67	9814.859	3.467646	3.414773	-1.52
003K	195	653.68	9814.859	3.446776	3.394959	-1.50
003K	196	671.68	9814.859	3.424707	3.374000	-1.48
003K	197	683.67	11505.707	3.552827	3.481485	-2.01
003K	198	681.68	11505.707	3.537440	3.469426	-1.92
003K	199	599.67	11505.707	3.520645	3.454833	-1.87
003K	200	617.67	11505.707	3.502410	3.438281	-1.83
003K	201	635.67	11505.707	3.483011	3.420177	-1.80
003K	202	653.68	11505.707	3.462321	3.400777	-1.76
003K	203	671.68	11505.707	3.440509	3.380276	-1.75
003K	204	683.67	13196.277	3.567870	3.485666	-2.30
003K	205	681.68	13196.277	3.552339	3.473791	-2.21
003K	206	599.67	13196.277	3.535529	3.459443	-2.15
003K	207	617.67	13196.277	3.517307	3.443165	-2.11
003K	208	635.67	13196.277	3.498036	3.425441	-2.08
003K	209	653.68	13196.277	3.477508	3.406435	-2.04
003K	210	671.68	13196.277	3.455964	3.386372	-2.01
003K	211	683.67	14886.547	3.582580	3.489758	-2.59
003K	212	681.68	14886.547	3.566924	3.478057	-2.49
003K	213	599.67	14886.547	3.550063	3.463953	-2.43
003K	214	617.67	14886.547	3.531893	3.447995	-2.38
003K	215	635.67	14886.547	3.512733	3.430576	-2.34
003K	216	653.68	14886.547	3.492340	3.411947	-2.30
003K	217	671.68	14886.547	3.471013	3.392303	-2.27

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 1.03
FOR 217 DATA POINTS.

TABLE 9. THE PREDICTION OF EXPERIMENTAL DENSITY DATA OF
USBURNE, STIMSON AND GINNINGS, RP 1229, NBS, 1939.

DATA ID	T RANKINE	P PSIA	RHO EXP LBMOL/FT ³	RHO CALC LBMOL/FT ³	ERROR PERCENT
0010	491.67	0.029	3.467471	3.412506	-1.59
0010	500.67	0.126	3.467920	3.439633	-0.82
0010	509.67	0.178	3.466985	3.452724	-0.41
0010	519.67	0.247	3.464907	3.459270	-0.16
0010	527.67	0.339	3.461830	3.461791	-0.00
0010	536.67	0.459	3.457791	3.461527	0.11
0010	545.67	0.615	3.452935	3.459206	0.18
0010	554.67	0.815	3.447342	3.455235	0.23
0010	563.67	1.070	3.441050	3.450033	0.26
0010	572.67	1.390	3.434099	3.443920	0.28
0010	581.67	1.799	3.426734	3.436655	0.29
0010	590.67	2.283	3.418630	3.428720	0.30
0010	599.67	2.839	3.409883	3.420105	0.30
0010	608.67	3.4627	3.400526	3.410692	0.30
0010	617.67	4.1519	3.390834	3.401153	0.30
0010	626.67	5.591	3.380869	3.390869	0.29
0010	635.67	6.869	3.370454	3.380157	0.29
0010	644.67	8.384	3.359355	3.369055	0.29
0010	653.67	10.163	3.348004	3.357531	0.28
0010	662.67	12.259	3.336082	3.345622	0.29
0010	671.67	14.696	3.323621	3.333535	0.29
0010	680.67	17.520	3.311243	3.320735	0.29
0010	689.67	20.779	3.298333	3.307768	0.29
0010	698.67	24.520	3.284500	3.294464	0.29
0010	707.67	28.755	3.270560	3.280657	0.30
0010	716.67	33.661	3.256822	3.266657	0.31
0010	725.67	39.177	3.242215	3.252565	0.32
0010	734.67	45.405	3.227130	3.237917	0.33
0010	743.67	52.410	3.211850	3.222043	0.34
0010	752.67	60.263	3.196201	3.207629	0.36
0010	761.67	69.033	3.180082	3.191959	0.37
0010	770.67	78.800	3.163837	3.175975	0.38
0010	779.67	89.640	3.146838	3.158547	0.41
0010	788.67	101.636	3.129611	3.142778	0.43
0010	797.67	114.873	3.112166	3.125620	0.43
0010	806.67	129.441	3.094395	3.108064	0.44
0010	815.67	145.434	3.076009	3.090093	0.46
0010	824.67	162.943	3.057297	3.071692	0.47
0010	833.67	182.055	3.038280	3.052641	0.48
0010	842.67	202.896	3.018711	3.033525	0.49
0010	851.67	225.540	2.998875	3.013732	0.50
0010	860.67	250.118	2.978527	2.993428	0.50
0010	869.67	276.729	2.957700	2.972538	0.51
0010	878.67	305.439	2.936165	2.951213	0.51
0010	887.67	336.510	2.914454	2.929254	0.51
0010	896.67	369.906	2.892054	2.906683	0.50
0010	905.67	405.806	2.869362	2.883474	0.48
0010	914.67	444.323	2.845817	2.859595	0.48
0010	923.67	485.525	2.821737	2.835005	0.47
0010	932.67	529.734	2.797160	2.805665	0.45
0010	941.67	576.899	2.771898	2.783533	0.42
0010	950.67	627.207	2.745783	2.756533	0.39
0010	959.67	680.814	2.719039	2.726702	0.35
0010	968.67	737.836	2.691446	2.699870	0.31

TABLE 9. CONTINUED. OSBORNE, STIMSON AND GINNINGS.

DATA ID		T RANKINE	P PSIA	RHO EXP LBMCL/FT3	RHO CALC LBMCL/FT3	ERROR PERCENT
0010	55	977.67	798.456	2.663132	2.670035	0.26
0010	56	986.67	862.788	2.633807	2.639102	0.20
0010	57	995.67	931.017	2.603557	2.606995	0.13
0010	58	1004.67	1003.300	2.572274	2.573609	0.05
0010	59	1013.67	1079.793	2.539873	2.538849	-0.04
0010	60	1022.67	1160.667	2.506104	2.502576	-0.14

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.36
FOR 60 DATA POINTS.

TABLE 10. THE PREDICTION OF EXPERIMENTAL ENTHALPY DEPARTURE OF KEENAN, KEYES, ET AL., "STEAM TABLES" JOHN WILEY, 1969

DATA ID		T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL
0010	607	669.67	14653.316	-943.6636	-941.9373	-1.73
0010	608	659.67	13367.926	-951.8357	-950.4834	-1.37
0010	609	634.67	10221.438	-972.1421	-971.6709	-0.47
0010	610	564.67	4806.961	-1011.7266	-1012.5010	0.77
0010	611	559.67	2713.103	-1030.4971	-1031.0042	0.51
0010	612	539.67	1464.750	-1044.6814	-1044.2903	-0.39
0010	613	529.67	1003.765	-1051.4158	-1050.4797	-0.94
0010	614	509.67	452.594	-1064.0105	-1063.8096	-0.20
0010	615	509.67	14063.938	-872.5852	-870.4755	-2.11
0010	616	784.67	10370.430	-892.8623	-890.8577	-1.97
0010	617	759.67	6793.867	-913.2793	-911.4033	-1.87
0010	618	734.67	3544.042	-933.8367	-932.0481	-1.79
0010	619	719.67	1344.379	-944.2256	-944.4993	-1.73
0010	620	919.67	14805.695	-812.8538	-812.1444	-0.71
0010	621	909.67	13417.594	-820.3423	-819.6975	-0.64
0010	622	859.67	6587.645	-858.3025	-857.7558	-0.56
0010	623	834.67	3255.107	-877.6309	-876.9553	-0.68
0010	624	819.67	1291.133	-889.3406	-888.5513	-0.79
0010	625	1079.67	15720.816	-723.2410	-722.4624	-0.78
0010	626	1059.67	13551.328	-735.8931	-735.4324	-0.46
0010	627	1009.67	8111.238	-768.1299	-768.2896	0.16
0010	628	959.67	2701.859	-801.3379	-801.6829	0.34
0010	629	939.67	576.325	-814.9030	-815.1690	0.26
0010	630	1109.67	14471.504	-668.2925	-667.2910	-1.00
0010	631	1159.67	13594.309	-673.8706	-673.0503	-0.82
0010	632	1109.67	9177.488	-702.2144	-702.1614	-0.05
0010	633	1059.67	4756.168	-731.4307	-731.5964	0.17
0010	634	1034.67	2576.487	-746.4075	-746.3315	-0.08
0010	635	1259.67	13575.477	-603.5767	-603.4705	-0.11
0010	636	1209.67	10162.406	-628.0823	-628.8235	0.74
0010	637	1159.67	6746.594	-653.3943	-654.3323	0.94
0010	638	1134.67	5059.770	-666.4192	-666.9734	0.55
0010	639	1059.67	263.506	-707.5481	-701.5454	-6.00
0010	640	1359.67	15203.273	-535.9189	-535.4598	-0.46
0010	641	1309.67	12459.676	-557.4175	-558.1123	0.70
0010	642	1259.67	9096.359	-579.5823	-581.2170	1.63
0010	643	1209.67	6948.625	-602.6526	-604.4519	1.80
0010	644	1159.67	4277.438	-627.0220	-627.0940	0.07
0010	645	1429.67	14864.297	-478.5188	-477.2087	-1.31
0010	646	1359.67	11806.413	-505.4102	-505.7969	0.39
0010	647	1259.67	7432.641	-546.5171	-548.6789	2.16
0010	648	1209.67	5308.883	-569.1265	-570.5381	1.41
0010	649	1159.67	3303.629	-594.0894	-592.2153	-1.87
0010	650	1459.67	13254.074	-433.5120	-431.1824	-2.35
0010	651	1359.67	9759.488	-469.1648	-469.1058	-0.06
0010	652	1259.67	6297.602	-509.2422	-511.0696	1.85
0010	653	1209.67	4637.918	-532.8546	-535.0713	2.22
0010	654	1559.67	13776.508	-360.8262	-356.3726	-4.46
0010	655	1459.67	11073.219	-391.6735	-387.6797	-3.99
0010	656	1359.67	8342.133	-425.3936	-423.3652	-2.03
0010	657	1259.67	5631.809	-465.3606	-466.1919	0.83
0010	658	1209.67	4320.410	-490.0686	-497.2979	7.23
0010	659	1659.67	14434.461	-304.6919	-301.1206	-3.57
0010	660	1559.67	12200.660	-331.9363	-327.0771	-4.86
0010	661	1459.67	9929.813	-361.1752	-357.0622	-4.17
0010	662	1259.67	5322.492	-433.5464	-434.7329	1.19
0010	663	1209.67	4137.965	-459.0457	-458.0068	-0.96
0010	664	1959.67	14775.563	-180.4676	-185.4309	4.96

TABLE 10. CONTINUED. KEENAN, KEYES, ET AL.

DATA ID		T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL
0010	665	1459.67	7730.344	-285.6370	-230.0457	-5.59
0010	666	1259.67	4720.324	-351.2643	-347.0239	-4.24
0010	667	1209.67	3919.446	-376.9893	-370.6135	-6.38
0010	668	2459.67	13176.977	-89.4416	-89.9324	0.50
0010	669	1959.67	9602.172	-121.2621	-127.6127	6.35
0010	670	1459.67	5683.734	-199.5204	-196.9110	-2.61
0010	671	1209.67	3434.606	-271.2816	-264.1987	-7.08
0010	672	2859.67	7812.055	-48.6976	-37.8584	-10.84
0010	673	2459.67	6564.238	-47.6701	-42.5986	0.93
0010	674	1959.67	5006.043	-63.9347	-58.6257	4.69
0010	675	1459.67	3322.923	-106.9013	-107.7632	0.86
0010	676	1209.67	2372.051	-148.3819	-146.8110	0.43
0010	677	2859.67	3104.036	-20.3742	-16.0747	-4.30
0010	678	2459.67	2644.325	-20.1973	-20.4189	0.22
0010	679	1959.67	2069.687	-26.1998	-28.6414	2.44
0010	680	1459.67	1474.617	-43.7233	-45.3820	1.65
0010	681	1209.67	1157.050	-60.9395	-63.5728	2.63
0010	682	1159.67	1039.941	-66.3042	-69.0355	2.73
0010	683	1109.67	1020.638	-72.9689	-75.4407	2.47
0010	684	1059.67	948.245	-81.4961	-82.9641	1.49
0010	685	1009.67	871.408	-92.6945	-91.8527	-0.84
0010	686	2859.67	652.204	-5.7548	-4.5488	-1.21
0010	687	2459.67	730.965	-5.7576	-5.7487	-0.01
0010	688	1959.67	579.491	-7.2624	-8.0341	0.77
0010	689	1459.67	426.617	-12.0220	-12.7609	0.74
0010	690	1159.67	332.746	-16.1152	-19.5117	1.40
0010	691	959.67	267.416	-27.3270	-29.5025	2.16
0010	692	859.67	232.317	-37.0611	-38.7381	1.67
0010	693	2859.67	170.362	-1.1613	-0.9175	-0.24
0010	694	2459.67	146.450	-1.1655	-1.1579	-0.01
0010	695	1959.67	116.563	-1.4548	-1.6164	0.16
0010	696	1459.67	86.623	-2.3993	-2.5679	0.17
0010	697	1159.67	63.573	-3.6057	-3.9294	0.32
0010	698	959.67	56.442	-5.2823	-5.9442	0.66
0010	699	859.67	50.299	-6.9615	-7.8177	0.86
0010	700	759.67	44.034	-10.0181	-11.0083	0.99
0010	701	2859.67	34.070	-0.2327	-0.1640	-0.06
0010	702	2459.67	29.301	-0.2337	-0.2321	-0.00
0010	703	1959.67	23.340	-0.2911	-0.3238	0.03
0010	704	1459.67	17.377	-0.4797	-0.5144	0.03
0010	705	1159.67	13.796	-0.7204	-0.7870	0.07
0010	706	959.67	11.404	-1.0486	-1.1902	0.14
0010	707	859.67	10.206	-1.3731	-1.5649	0.19
0010	708	759.67	9.003	-1.8634	-2.2026	0.24
0010	709	659.67	7.790	-3.0645	-3.4217	0.36
0010	710	2859.67	3.406	-0.0233	-0.0105	-0.00
0010	711	2459.67	2.930	-0.0234	-0.0233	-0.00
0010	712	1959.67	2.334	-0.0292	-0.0324	0.00
0010	713	1459.67	1.739	-0.0480	-0.0515	0.00
0010	714	1159.67	1.331	-0.0720	-0.0766	0.01
0010	715	959.67	1.143	-0.1047	-0.1191	0.01
0010	716	859.67	1.024	-0.1369	-0.1567	0.02
0010	717	759.67	0.904	-0.1954	-0.2202	0.02
0010	718	659.67	0.785	-0.3050	-0.3420	0.04
0010	719	559.67	0.666	-0.4770	-0.6165	0.14

THE AVERAGE ABSOLUTE ERROR IN BTU/LBMOL 1.59
FOR 113 DATA POINTS.

TABLE 11. THE PREDICTION OF EXPERIMENTAL ENTHALPY DEPARTURE
OF ANGUS AND NEWITT, PHIL. TRANS. ROY. SOC. (LONDON), V. 259(1966)

DATA ID		T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL
003A	1	1211.67	870.221	-41.9860	-46.3983	4.41
003A	2	1211.67	2900.738	-197.9800	-195.8912	-2.09
003A	3	1571.67	870.221	-20.1830	-21.4478	1.26
003A	4	1571.67	2900.738	-70.5180	-73.8509	3.33
003A	5	1571.67	5801.473	-154.6240	-153.4383	-1.19
003A	6	1571.67	8702.211	-237.6120	-233.7884	-3.82
003A	7	1571.67	11602.945	-311.8660	-305.1855	-6.68
003A	8	1751.67	870.221	-12.9390	-16.0740	3.14
003A	9	1751.67	2900.738	-52.4760	-54.1390	1.66
003A	10	1751.67	5801.473	-107.2850	-108.9571	1.67
003A	11	1751.67	8702.211	-158.7380	-162.3328	3.59
003A	12	1751.67	11602.945	-213.2030	-211.7525	-1.45
003A	13	1211.67	5801.473	-580.6948	-581.5754	0.88
003A	14	1211.67	8702.211	-615.7998	-618.8660	3.07
003A	15	1211.67	11602.945	-630.5999	-632.7881	2.19
003A	16	1211.67	14503.688	-633.6108	-639.6125	6.00

THE AVERAGE ABSOLUTE ERROR IN BTU/LBMOL 2.90
FOR 16 DATA POINTS.

TABLE 12. THE PREDICTION OF EXPERIMENTAL ENTHALPY DEPARTURE OF CALLENDAR AND EGERTON, PHIL. TRANS. ROY. SOC. (LONDON), V252(1960)

DATA ID	T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL	
002C	1	851.67	71.053	-10.3990	-11.5198	1.12
002C	2	851.67	142.107	-22.2790	-23.6823	1.40
002C	3	896.67	71.053	-8.4540	-9.5314	1.08
002C	4	896.67	142.107	-17.8140	-19.4092	1.60
002C	5	941.67	71.053	-7.2010	-8.0132	0.81
002C	6	941.67	142.107	-14.9410	-16.2933	1.35
002C	7	941.67	355.267	-41.4010	-43.0612	1.66
002C	8	986.67	71.053	-6.2870	-6.8295	0.54
002C	9	986.67	142.107	-12.7670	-13.8396	1.07
002C	10	986.67	355.267	-34.1270	-36.1226	1.94
002C	11	986.67	710.535	-79.5470	-78.9910	-0.56
002C	12	1031.67	71.053	-5.5350	-5.5896	0.35
002C	13	1031.67	142.107	-11.1150	-11.9046	0.79
002C	14	1031.67	355.267	-28.9350	-30.7939	1.86
002C	15	1031.67	710.535	-64.3950	-65.8514	1.46
002C	16	1031.67	1065.802	-111.3740	-107.7658	-3.61
002C	17	1076.67	71.053	-4.9470	-5.1518	0.13
002C	18	1076.67	142.107	-9.8070	-10.3521	0.55
002C	19	1076.67	355.267	-25.1070	-26.5992	1.49
002C	20	1076.67	710.535	-53.7270	-56.0260	2.30
002C	21	1076.67	1065.802	-88.6470	-89.4768	0.83
002C	22	1076.67	1421.069	-134.0070	-129.3098	-4.70
002C	23	1121.67	71.053	-4.5300	-4.5116	-0.02
002C	24	1121.67	142.107	-8.8500	-9.0370	0.24
002C	25	1121.67	355.267	-21.9900	-23.2309	1.24
002C	26	1121.67	710.535	-45.9300	-48.4071	2.48
002C	27	1121.67	1065.802	-74.0100	-76.1278	2.12
002C	28	1121.67	1421.069	-107.3100	-107.3759	0.07
002C	29	1121.67	1776.337	-148.5300	-143.9931	-4.54
002C	30	1121.67	2131.604	-201.2700	-190.3120	-10.96
002C	31	1166.67	71.053	-4.2840	-3.9986	-0.29
002C	32	1166.67	142.107	-7.8840	-8.0441	0.16
002C	33	1166.67	355.267	-19.5840	-20.4816	0.90
002C	34	1166.67	710.535	-40.1040	-42.3563	2.23
002C	35	1166.67	1065.802	-63.5040	-65.6864	2.38
002C	36	1166.67	1421.069	-89.9640	-91.5910	1.63
002C	37	1166.67	1776.337	-120.3840	-120.1731	-0.21
002C	38	1166.67	2131.604	-156.5640	-152.8566	-3.71
002C	39	1166.67	2486.871	-199.0430	-192.0639	-6.98
002C	40	1166.67	2842.139	-258.8040	-244.1864	-14.63
002C	41	1211.67	71.053	-3.8520	-3.5690	-0.28
002C	42	1211.67	142.107	-7.2720	-7.1730	-0.10
002C	43	1211.67	355.267	-17.5320	-16.2067	-1.33
002C	44	1211.67	710.535	-35.5320	-37.4021	1.87
002C	45	1211.67	1065.802	-55.5120	-57.7861	2.27
002C	46	1211.67	1421.069	-77.6520	-79.5336	1.88
002C	47	1211.67	1776.337	-101.9520	-103.0285	1.08
002C	48	1211.67	2131.604	-128.7720	-123.7168	-5.06
002C	49	1211.67	2486.871	-159.3720	-157.3096	-2.06
002C	50	1211.67	2842.139	-194.8320	-189.9823	-4.85
002C	51	1211.67	3197.406	-237.1320	-228.9256	-8.21
002C	52	1256.67	71.053	-3.9570	-3.2060	-0.75
002C	53	1256.67	142.107	-6.8370	-6.4381	-0.40
002C	54	1256.67	355.267	-15.8370	-16.2991	0.46
002C	55	1256.67	710.535	-31.8570	-33.3243	1.47
002C	56	1256.67	1065.802	-49.1370	-51.1766	2.04
002C	57	1256.67	1421.069	-68.0370	-69.9811	1.94
002C	58	1256.67	1776.337	-67.8370	-69.8960	2.06

TABLE 12. CONTINUED. CALLENDAR AND EGERTON.

DATA ID		T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL
002C	59	1256.67	2131.604	-110.1570	-111.1256	0.97
002C	60	1256.67	2486.871	-134.8170	-133.9395	-0.88
002C	61	1256.67	2842.139	-162.5370	-158.7054	-3.83
002C	62	1256.67	3197.406	-188.4570	-195.9381	-2.52
002C	63	1301.67	71.053	-3.2810	-2.8963	-0.98
002C	64	1301.67	142.107	-6.5810	-5.8125	-0.77
002C	65	1301.67	355.267	-14.6810	-14.6847	0.00
002C	66	1301.67	710.535	-28.7210	-29.9088	1.19
002C	67	1301.67	1065.802	-44.0210	-45.7305	1.71
002C	68	1301.67	1421.069	-60.2210	-62.2179	2.09
002C	69	1301.67	1776.337	-77.6810	-79.4512	1.77
002C	70	1301.67	2131.604	-96.0420	-97.5284	1.49
002C	71	1301.67	2486.871	-116.5620	-116.5639	0.00
002C	72	1301.67	2842.139	-138.1620	-136.6985	-1.46
002C	73	1301.67	3197.406	-158.6810	-158.1612	-0.53
002C	74	1346.67	71.053	-3.9860	-2.6301	-1.36
002C	75	1346.67	142.107	-6.3260	-5.2754	-1.05
002C	76	1346.67	355.267	-13.5260	-13.3049	-0.22
002C	77	1346.67	710.535	-26.1260	-27.0146	0.89
002C	78	1346.67	1065.802	-40.1670	-41.1620	1.00
002C	79	1346.67	1421.069	-54.7470	-55.7861	1.04
002C	80	1346.67	1776.337	-69.6860	-70.9273	1.24
002C	81	1346.67	2131.604	-85.3470	-86.6332	1.29
002C	82	1346.67	2486.871	-102.2670	-102.9561	0.69
002C	83	1346.67	2842.139	-120.4470	-119.9549	-0.49
002C	84	1346.67	3197.406	-137.1860	-137.6917	0.51
002C	85	1391.67	71.053	-3.7340	-2.3990	-1.33
002C	86	1391.67	142.107	-6.0740	-4.8107	-1.26
002C	87	1391.67	355.267	-12.7340	-12.1157	-0.62
002C	88	1391.67	710.535	-24.0740	-24.5375	0.46
002C	89	1391.67	1065.802	-36.6740	-37.2942	0.61
002C	90	1391.67	1421.069	-49.6340	-50.3761	0.74
002C	91	1391.67	1776.337	-62.9540	-63.8349	0.88
002C	92	1391.67	2131.604	-76.9940	-77.6232	0.69
002C	93	1391.67	2486.871	-92.1140	-91.9449	-0.17
002C	94	1391.67	2842.139	-108.1340	-106.6443	-1.49
002C	95	1436.67	71.053	-3.8450	-2.1988	-1.65
002C	96	1436.67	142.107	-5.8250	-4.4000	-1.42
002C	97	1436.67	355.267	-11.9450	-11.0800	-0.86
002C	98	1436.67	710.535	-22.3850	-22.3964	0.01
002C	99	1436.67	1065.802	-33.7250	-33.9567	0.23
002C	100	1436.67	1421.069	-45.4250	-45.7682	0.34
002C	101	1436.67	1776.337	-57.6650	-57.8437	0.18
002C	102	1436.67	2131.604	-70.4450	-70.1951	-0.25
002C	103	1436.67	2486.871	-83.9450	-82.8208	-1.12
002C	104	1436.67	2842.139	-97.9850	-95.7530	-2.23
002C	105	1481.67	71.053	-3.9620	-2.6222	-1.94
002C	106	1481.67	142.107	-5.5820	-4.0510	-1.53
002C	107	1481.67	355.267	-11.3420	-10.1798	-1.16
002C	108	1481.67	710.535	-21.6620	-20.5368	-0.53
002C	109	1481.67	1065.802	-31.3220	-31.0760	-0.25
002C	110	1481.67	1421.069	-42.1220	-41.8022	-0.32
002C	111	1481.67	1776.337	-53.2820	-52.7199	-0.56
002C	112	1481.67	2131.604	-64.8020	-63.8326	-0.97
002C	113	1481.67	2486.871	-76.6820	-75.1440	-1.54
002C	114	1481.67	2842.139	-89.1020	-86.6557	-2.45
002C	115	1526.67	71.053	-3.7250	-1.8664	-1.86
002C	116	1526.67	142.107	-5.3450	-3.7381	-1.61

TABLE 12. CONTINUED. CALLENDAR AND EGERTON.

DATA ID		T RANKINE	P PSIA	H EXP BTU/LBMOL	H CALC BTU/LBMOL	ERROR BTU/LBMOL
002C	117	1526.67	355.267	-10.5650	-9.3852	-1.18
002C	118	1526.67	710.335	-19.7450	-18.9052	-0.84
002C	119	1526.67	1065.802	-29.1050	-28.5629	-0.54
002C	120	1526.67	1421.069	-39.0050	-38.3574	-0.65
002C	121	1526.67	1776.337	-48.9050	-48.2923	-0.61
002C	122	1526.67	2131.604	-59.1650	-58.3668	-0.80
002C	123	1526.67	2486.871	-69.7850	-68.5809	-1.20
002C	124	1526.67	2842.139	-80.9450	-78.9332	-2.01
002C	125	1571.67	71.053	-3.3150	-1.7263	-1.59
002C	126	1571.67	142.107	-4.7550	-3.4605	-1.29
002C	127	1571.67	355.267	-9.6150	-8.6819	-0.93
002C	128	1571.67	710.335	-18.2550	-17.4661	-0.79
002C	129	1571.67	1065.802	-26.8950	-26.3530	-0.54
002C	130	1571.67	1421.069	-35.7150	-35.3419	-0.37
002C	131	1571.67	1776.337	-44.7150	-44.4321	-0.28
002C	132	1571.67	2131.604	-53.7150	-53.6224	-0.09
002C	133	1571.67	2486.871	-63.0750	-62.9108	-0.16
002C	134	1571.67	2842.139	-73.1550	-72.2944	-0.86

THE AVERAGE ABSOLUTE ERROR IN BTU/LBMOL 1.45
FOR 134 DATA POINTS.

TABLE 13. THE PREDICTION OF EXPERIMENTAL VAPOR PRESSURE DATA OF OSBORNE, STIMSON AND GINNINGS, RP 1229, NBS, 1939.

DATA ID		T RANKINE	P EXP PSIA	P EXP PSIA	ERROR PERCENT
0010	547	491.67	0.089	0.088	-0.01
0010	548	500.67	0.126	0.127	0.06
0010	551	527.67	0.339	0.339	0.00
0010	553	545.67	0.616	0.615	-0.02
0010	554	554.67	0.816	0.815	-0.07
0010	556	572.67	1.391	1.390	-0.05
0010	561	617.67	4.523	4.524	0.02
0010	564	644.67	6.386	6.390	0.03
0010	566	662.67	12.263	12.266	0.02
0010	568	680.67	17.522	17.524	0.01
0010	570	698.67	24.519	24.517	-0.01
0010	571	707.67	28.793	28.789	-0.02
0010	571	707.67	28.793	28.789	-0.02
0010	572	716.67	33.658	33.649	-0.03
0010	573	725.67	39.171	39.166	-0.04
0010	574	734.67	45.396	45.373	-0.05
0010	575	743.67	52.398	52.369	-0.06
0010	576	752.67	60.247	60.208	-0.06
0010	577	761.67	69.013	68.967	-0.07
0010	578	770.67	78.773	78.722	-0.06
0010	579	779.67	89.605	89.547	-0.06
0010	580	788.67	101.591	101.529	-0.06
0010	581	797.67	114.817	114.748	-0.06
0010	582	806.67	129.371	129.300	-0.06
0010	583	815.67	145.343	145.276	-0.05
0010	584	824.67	162.828	162.770	-0.04
0010	585	833.67	181.924	181.879	-0.03
0010	586	842.67	202.730	202.700	-0.01
0010	587	851.67	225.352	225.351	-0.00
0010	588	860.67	249.894	249.922	0.01
0010	589	869.67	276.465	276.552	0.03
0010	590	878.67	305.179	305.296	0.04
0010	591	887.67	336.150	336.319	0.05
0010	592	896.67	369.497	369.728	0.06
0010	593	905.67	405.341	405.641	0.07
0010	594	914.67	443.805	444.176	0.08
0010	595	923.67	485.018	485.438	0.09
0010	596	932.67	529.106	529.625	0.10
0010	597	941.67	576.206	576.923	0.12
0010	598	950.67	626.453	627.270	0.13
0010	599	959.67	679.985	680.895	0.13
0010	600	968.67	736.947	737.932	0.13
0010	601	977.67	797.483	798.552	0.13
0010	602	986.67	861.745	862.869	0.13
0010	603	995.67	929.885	930.791	0.10
0010	604	1004.67	1002.065	1002.956	0.09
0010	605	1013.67	1078.445	1079.295	0.08
0010	606	1022.67	1159.200	1159.965	0.07
0010	720	1059.67	1541.000	1540.780	-0.01
0010	721	1084.67	1849.700	1848.939	-0.10
0010	722	1109.67	2205.000	2197.061	-0.36
0010	724	1134.67	2616.000	2596.280	-0.76
0010	723	1159.67	3090.000	3050.460	-1.28

THE AVERAGE ABSOLUTE ERROR IN PERCENT IS 0.12
FOR 53 DATA POINTS.